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ENGINEERS HAND-BOOK

OF TABLES, CHARTS AND DATA ON THE APPLICATION OF CENTRI-FUGAL FANS AND FAN SYSTEM APPARATUS, INCLUDING ENGINES AND MOTORS, AIR WASHERS, HOT BLAST HEATERS AND SYSTEMS OF AIR DISTRIBUTION

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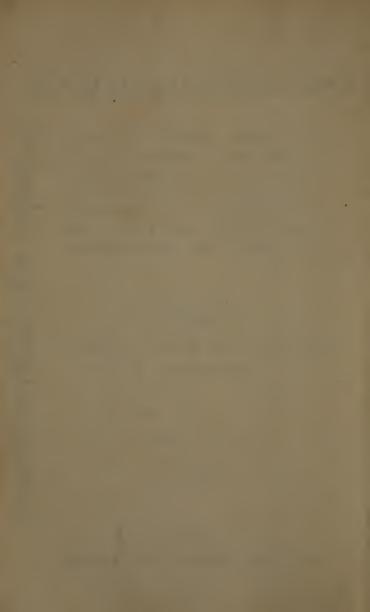
THE BUFFALO FORGE COMPANY BUFFALO, N. Y.

FIRST EDITION

PRICE \$3.00

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PREFACE

THE use of the fan in general engineering practice is rapidly increasing, making it imperative that both the engineer and the architect become familiar with the fundamental principles governing the selection and application of fans for various purposes. Some general information has been published on the subject by the different fan builders, but what has been given out has always been incomplete and frequently misleading, and did not afford sufficient data to be intelligently employed by the engineer. Heretofore no effort has been made to collect and present under one cover the latest and most reliable engineering data concerning fans and their application to various industrial requirements.

This book is intended to be used as a guide in the selection and application of fans, heaters and kindred apparatus, and an effort has been made to so standardize the rules and data given that they may be used with any standard make of equipment. The greater part of the data presented is the result of tests and research made by the engineering staff of the Buffalo Forge Company in the testing laboratories of the company, many of the investigations being made purposely to obtain data for this book. The results of these investigations have in most cases never been heretofore published except in the proceedings of some of the engineering societies, where they were presented by the engineers of this company, and others. The rules and applications as outlined are the same as are used in this company's practice. In preparing this work the theory has been generally omitted, except in such elementary form as was necessary to an understanding of the facts given.

The information herein presented is in complete and reliable form for standard applications, but there are many cases requiring special consideration from the engineer familiar with fan installations.



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PART I

PROPERTIES OF AIR

In this section will be found a discussion of the physical and chemical properties of air and their general relations with respect to "fan engineering." A complete set of psychrometric charts and tables are included.

Air is a mechanical mixture of various gases, ordinarily considered as consisting of oxygen and nitrogen, but also containing a portion of moisture and carbonic acid, and a very small part of other constituents. The proportion of these components will vary under different conditions, but ordinarily pure dry air is composed as follows, in per cent.:

	By Volume	By Weight
Oxygen	 	23.1
Nitrogen	 	76.9

The moisture will vary with the humidity of the air, from 0. to 4 per cent., and the carbonic acid will vary with the purity of the air from perhaps 0.03 to 0.30 per cent., or as usually expressed, from 3 to 30 parts in 10,000.

Weight of Air

The weight of the air varies with its temperature and barometric pressure and also with the amount of moisture it contains. In The weight of one cubic foot of pure dry air expressed in pounds may be determined by the formula

$$W = \frac{2.6982 \text{ p}}{459.2 + \text{t}} \tag{1}$$

where p = absolute pressure in pounds per square inch.

t = temperature of the air in degrees F.

A convenient formula for expressing the weight of dry air at any conditions of temperature and pressure as used by Frank H. Kneeland* is

$$W = \frac{1.3253 \text{ b}}{459.2 + \text{t}}$$

where b = corrected barometer reading in inches of mercury

t = temperature, deg. F.

 $1.3253 \Rightarrow$ weight in lbs. of 459.2 cu. ft. of air at 0° F. and 1" barometric pressure.

^{* &}quot;Some Experiences with the Pitot Tube on High and Low Velocities" Am. Soc. Mech. Engrs., Dec., 1911.

A formula expressing the weight of humid air is given in the Smithsonian Meteorological Tables as

$$W = \frac{0.080723}{1 + 0.0020389 (t - 32)} \times \frac{b - 0.378 e}{29.921}$$
(3)

where t = temperature, deg. Fahr.

b = height of barometer in inches of mercury

e = pressure due to vapor in the air in inches of mercury. According to the latest data the above values should be slightly changed, and we will then have the following formulae as convenient forms for calculating the weight per cubic foot of either dry or moist air.

For dry air
$$W = \frac{0.0028862 \text{ b}}{1 + 0.0021758 \text{ t}}$$
(4)

For moist air
$$W = \frac{0.0028862 \text{ b} - 0.001088 \text{ e}}{1 + 0.0021758 \text{ t}}$$
 (5)

This last gives the weight of a cubic foot of the mixture of air and vapor, either for saturated or partly saturated air.

The weight of the dry air contained in one cubic foot of saturated air may be determined from the formula

$$W = \frac{0.0028862 \text{ b} - 0.002886 \text{ e}}{1 + 0.0021758 \text{ t}}$$
(6)

The weight of vapor or density in pounds per cubic foot of saturated vapor at temperature t is given by the following:

$$D_{s} = \frac{S\left(144 \times 0.4908 \text{ e}\right)}{53.35\left(459.2 + t\right)} \tag{7}$$

where S is the specific weight of water vapor and may be found as

$$S = 0.6221 + 0.001815\sqrt{e} + 0.0000051\sqrt{e^3}$$
(8)

The relationship between the temperature and specific weight of vapor is shown by the diagram on page 14 taken from W. H. Carrier's paper on "Rational Psychrometric Formulae."*

An approximate value for the weight of water vapor contained in one pound of dry air saturated with moisture may be determined from

$$G = \frac{0.624 \text{ e}}{b - e} \tag{9}$$

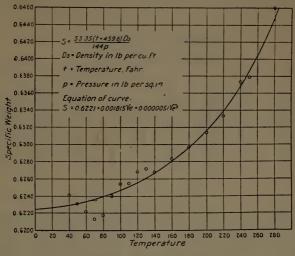
It may be noted from the curve on page 14 that the value of 0.624 for S in the above is only correct at about 70°.

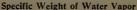
*"Rational Psychrometric Formulae" Am. Soc. Mech. Engrs., Dec., 1911.

PROPERTIES OF DRY AIR

Barometric Pressure 29.921 Inches

Temperature Degrees Fahr.	Weight per Cu. Ft. Pounds	Per Cent. of Volume at 70° F.	B. t. u. Absorbed by One Cu. Ft. Dry Air per Degree F.	Cu. Ft. Dry Air Warmed One Degree per B. t. u.	Temperature Degrees Fahr.	Weight per Cu. Ft. Pounds	Per Cent. of Volume at 70° F.	B. t. u. Absorbed by One Cu. Ft. Dry Air per Degree F.	Cu. Ft. Dry Air Warmed One Degree per B. t. u.
0 5 10	.08636 .08544 .08453	.8680 .8772 .8867	.02080 .02060 .02039	48.08 48.55 49.05	130 135 140	.06732 .06675 .06620	$\begin{array}{c} 1.1133 \\ 1.1230 \\ 1.1320 \end{array}$.01631 .01618 .01605	$ \begin{array}{r} 61.32 \\ 61.81 \\ 62.31 \end{array} $
15 20 25	.08363 .08276 .08190	.8962 .9057 .9152	.02018 .01998 .01977	49.56 50.05 50.58	145 150 160	$.06565 \\ .06510 \\ .06406$	$\begin{array}{c} 1.1417 \\ 1.1512 \\ 1.1700 \end{array}$.01592 .01578 .01554	$\begin{array}{c} 62.82 \\ 63.37 \\ 64.35 \end{array}$
30 35 40	.08107 .08025 .07945	.9246 .9340 .9434	.01957 .01938 .01919	$51.10 \\ 51.60 \\ 52.11$	170 180 190	$.06304 \\ .06205 \\ .06110$	$\begin{array}{c} 1.1890 \\ 1.2080 \\ 1.2270 \end{array}$	$\begin{array}{c} .01530\\ .01506\\ .01484\end{array}$	$\begin{array}{c} 65.36 \\ 66.40 \\ 67.40 \end{array}$
45 50 55	.07866 .07788 .07713	.9530 .9624 .9718	.01900 .01881 .01863	$52.64 \\ 53.17 \\ 53.68$	200 220 240	.06018 .05840 .05673	$\begin{array}{c} 1.2455 \\ 1.2833 \\ 1.3212 \end{array}$.01462 .01419 .01380	$68.41 \\ 70.48 \\ 72.46$
60 65 70	.07640 .07567 .07495	$\begin{array}{r} .9811\\ .9905\\ 1.0000\end{array}$.01846 .01829 .01812	$54.18 \\ 54.68 \\ 55.19$	260 280 300	.05516 .05367 .05225	$\begin{array}{c} 1.3590 \\ 1.3967 \\ 1.4345 \end{array}$.01343 .01308 .01274	$74.46 \\ 76.46 \\ 78.50$
75 80 85	.07424 .07356 .07289	$\begin{array}{c} 1.0095 \\ 1.0190 \\ 1.0283 \end{array}$.01795 .01779 .01763	$55.72 \\ 56.21 \\ 56.72$	350 400 450	$\begin{array}{r} .04903 \\ .04618 \\ .04364 \end{array}$	$\begin{array}{c} 1.5288 \\ 1.6230 \\ 1.7177 \end{array}$.01197 .01130 .01070	83.55 88.50 93.46
90 95 100	.07222 .07157 .07093	$\begin{array}{c} 1.0380 \\ 1.0472 \\ 1.0570 \end{array}$.01747 .01732 .01716	$57.25 \\ 57.74 \\ 58.28$	500 550 600	$\begin{array}{c} .04138\\ .03932\\ .03746\end{array}$	$\begin{array}{c} 1.8113 \\ 1.9060 \\ 2.0010 \end{array}$.01018 .00967 .00923	98.24 103.42 108.35
105 110 115	.07030 .06968 .06908	$\begin{array}{c} 1.0660 \\ 1.0756 \\ 1.0850 \end{array}$.01702 .01687 .01673	58.76 59.28 59.78	700 800 900	$\begin{array}{c} .03423 \\ .03151 \\ .02920 \end{array}$	$\begin{array}{c} 2.1900 \\ 2.3785 \\ 2.5670 \end{array}$.00847 .00782 .00728	$118.07 \\ 127.88 \\ 137.37$
120 125	.06848 .06790	1.0945 1.1040	.01659 .01645	60.28 60.79	1000 1200	.02720 .02392	2.7560 3.1335	.00680 .00603	$147.07 \\ 165.83$





The table on page 13 gives the properties of dry air for various temperatures, and the table on page 15 the properties of saturated air. These are both based on the standard barometric pressure of 29.921 inches.

The table on page 17 giving the weights of saturated and partly saturated air for various barometric and hygrometric conditions will be found especially convenient in making calculations based on other than standard conditions. The weight in pounds per cubic foot of saturated air is given for even barometric pressures and temperatures. The decrement per degree rise in temperature and the increment per 0.1" increase in barometer are also given, thus readily giving the weight of saturated air at any other temperature and pressure. The last column in the table gives the approximate average increment per degree wet-bulb depression which is to be added to the weight of saturated air to obtain the corresponding weight of partly saturated air.

Example. As an example of the use of the table on page 17 we will assume a case where it is desired to find the weight in pounds per cubic foot of air at a temperature of 83° dry- and 68°

1

PROPERTIES OF SATURATED AIR

Weights of Air, Vapor of Water, and Saturated Mixture of Air and Vapor at Different Temperatures, Under Standard Atmospheric Pressure of 29.921 Inches of Mercury

	e	Weight in	a Cubic Foot	of Mixture	d by Sat. F.	at. Air Degree u.
Temperature Degrees Fahr.	Vapor Pressure Inches of Mercury	Weight of the Dry Air Pounds	Weight of the Vapor Pounds	Total Weight of the Mixture Pounds	B. t. u. Absorbed One Cubic Foot S Air per Degree I	Cubic Feet Sat. / Warmed One Deg per B. t. u.
1	2	3	4	5	6	7
0	.0383	.08625	.000069	.08632	.02082	48.04
10	.0631	.08433	.000111	.08444	.02039	49.05
20	.1030	.08247	.000177	.08265	.01998	50.05
30 40 50	$.1640 \\ .2477 \\ .3625$.08063 .07880 .07694	.000276 .000409 .000587	.08091 .07921 .07753	.01955 .01921 .01883	$51.15 \\ 52.06 \\ 53.11$
60	.5220	.07506	.000829	.07589	.01852	54.00
70	.7390	.07310	.001152	.07425	.01811	55.22
80	1.0290	.07095	.001576	.07253	.01788	55.93
90	$\begin{array}{c} 1.4170 \\ 1.9260 \\ 2.5890 \end{array}$.06881	.002132	.07094	.01763	56.72
100		.06637	.002848	.06922	.01737	57.57
110		.06367	.003763	.06743	.01716	58.27
120	3.4380	.06062	.004914	.06553	.01696	$58.96 \\ 59.50 \\ 59.92$
130	4.5200	.05716	.006357	.06352	.01681	
140	5.8800	.05319	.008140	.06133	.01669	
150 160 170	$7.5700 \\ 9.6500 \\ 12.2000$.04864 .04341 .03735	$\begin{array}{c} .010310\\ .012956\\ .016140\end{array}$.05894 .05637 .05349	.01663 .01664 .01671	$\begin{array}{c} 60.14 \\ 60.10 \\ 59.85 \end{array}$
180	$\begin{array}{c} 15.2900 \\ 19.0200 \\ 23.4700 \end{array}$.03035	.019940	.05029	.01682	59.45
190		.02227	.024465	.04674	.01706	58.80
200		.01297	.029780	.04275	.01750	57.15

wet-bulb (or a depression of 15°) when the barometric pressure is 29.40 inches. From the table on page 17 we find that the weight of saturated air at 80° and 29.00 inch barometer is 0.07034 lb. per cu. ft. Also the decrement to be subtracted is 0.00015 lb. per degree of temperature above 80°. That is, the weight at 83° and 29.00 inches would be $0.07034 - (3 \times 0.00015) = 0.06989$ lb. per cu. ft. The increment to be added per 0.1" increase in barometer above 29.00 inches is 0.00025, so that the weight of the saturated mixture at 83° and 29.40 inches will be $0.06989 + (4 \times 0.00025) = 0.07089$ lb. per cu. ft. From the last column in the table we find the increase in weight for each degree wet-bulb depression for a temperature of 83° to be 0.000034 + 0.3 (0.000039 - 0.000034) = 0.0000355.

Then the weight of moist air at 83° , 15° wet-bulb depression, and 29.40 inch barometer will be

0.07034 - 0.00045 + 0.001 + 0.00053 = 0.07142 lb. per cu. ft.

Specific Heat of Air

The specific heat of air is the ratio of the heat required to raise the temperature of a given weight of air through one degree as compared to the heat required to raise the temperature of the same weight of water from 62 to 63 degrees Fahr., i. e., it is the B. t. u. required to raise one pound of air one degree Fahr.

The specific heat of air may be expressed as either of two factors, specific heat at constant pressure or at constant volume. It is the specific heat at constant pressure that is ordinarily referred to. The factors commonly used heretofore have been those determined by Renault—specific heat at constant pressure = 0.2375, and at constant volume = 0.1689. But recent investigation tends to show that the value 0.2375 is too low, and that it should be $C_p = 0.24112 + 0.000009$ t or for ordinary purposes approximately 0.2415.*

For the specific heats of various substances see the table on page 78.

Relation of Velocity to Pressure

The laws governing the flow of air are perhaps less understood than almost any other branch of engineering data. The flow of air under high pressures must necessarily be investigated thermodynamically and the formulae are more or less compli-

^{* &}quot;Rational Psychrometric Formulae" by Willis H. Carrier, Am. Soc. Mech. Engrs., December, 1911, also W. F. G. Swan, Phil. Trans. Royal Soc., Series A, Vol. 210, pp. 199-238.

WEIGHTS OF SATURATED AND PARTLY SATURATED AIR FOR VARIOUS BAROMETRIC AND HYGROMETRIC CONDITIONS—Pounds per Cable Foot

-									
	igis v jsWet	Approx. Av Increase in V per Degree Bulb Depre	.000015 .000016 .000016	.000019 .000021 .000023	.000026 .000029 .000034	.000039 .000044 .000051	.000059 .000068 .000078	.000090 .000103 .000118	.000134 .000153 .000173
		Incr's Wt. per 0.1" Rise in Bar.	.00029 .00028 .00028	.00027 .00027 .00026	.00026 .00025 .00025	.00024 .00024 .00023	.00023 .00023 .00022	.00022 .00021 .00021	.00021 .00021 .00020
	30	Decr's Wt. per Deg. Inc. Dry Bulb	.00019 .00018 .00018	.00017 71000. 71000.	$\begin{array}{c} 00016\\ 00016\\ 00016\\ 00016\end{array}$	71000. 81000. 91000.	.00020 .00022 .00024	.00026 .00029 .00033	$\begin{array}{c} 00036\\ 00038\\ 00038\\ 00041 \end{array}$
		Wt. per Cu. Ft. Saturated Air	.08654 .08468 .08286	.08110 .07942 .07773	.07609 .07440 .07280	.07112 .06939 .06759	.06569 .06367 .06147	.05906 .05644 .05352	.05026 .04662 .04254
		Incr's Wt. per 0.1" Rise in Bar.	.00029 .00028 .00028	.00027 .00027 .00026	.00026 .00025 .00025	.00024 .00024 .00023	.00023 .00023 .00022	.00022 .00021 .00021	.00021 .00021 .00020
ب	29	Decr's Wt. per Deg. Inc. Dry Bulb	.00018 .00018 .00018	01000. 01000. 01000.	00016 00016 00016 00015	.00016 .00017 .00018	.00019 .00020 .00022	$\begin{array}{c} .00024 \\ .00026 \\ .00031 \end{array}$	$\begin{array}{c} 00034\\ 00037\\ 00037\\ 00041 \end{array}$
ches		Wt. per Cu. Ft. Saturated Air	.08365 .08185 .08009	.07839 .07675 .07512	.07353 .07193 .07034	.06870 .06703 .06526	.06339 .06142 .05925	.05689 .05430 .05141	04818 04457 04457 04052
s per or ure—ln		Incr's Wt. per 0.1" Rise in Bar.	.00029 .00028 .00028	.00027 .00027 .00026	.00026 .00025 .00025	.00024 .00024 .00023	.00023 .00023 .00023	.00022 .00021 .00021	.00021 .00021 .00020
-round ic Press	28	Decr's Wt. Der Deg. Inc.	71000. 71000.	.00016 .00016 .00016	.00015 .00015 .00015	.00016 .00016 .00016 .00017	.00018 .00019 .00021	.00023 .00026 .00029	.00032 .00036 .00040
Barometric Pressure—Inches		Wt. per Cu. Ft. Saturated Air	.08077 .07903 .07733	.07569 .07409 .07252	.07098 .06943 .06789	.06629 .06465 .06293	.06111 .05917 .05704	.05471 .05216 .04931	.04611 .04253 .03851
B		Incr's Wt. per 0.1" Rise in Bar.	.00029 .00028 .00028	.00027 .00027 .00026	.00026 .00025 .00025	.00024 .00024 .00023	.00023 .00023 .00023	.00022 .00022 .00021	.00021 .00021 .00020
	27	Decr's Wt. Decr's Wt.	.00016 .00016 .00016	.00016 .00015 .00015	.00015 .00015 .00015	.00016 .00016 .00016	.00018 .00019 .00021	.00023 .00025 .00028	.00031 .00036 .00040
		Wt. per Cu. Ft. Saturated Air	.07788 .07620 .07456	.07297 .07143 .06992	.06843 .06692 .06542	.06388 .06228 .06060	.05882 .05692 .05483	.05253 .05001 .04720	.04404 .04049 .03650
		Incr's Wt. per 0.1" Rise in Bar.	.00029 .00028 .00028	.00027 .00026 .00026	.00026 .00025 .00025	.00024 .00024 .00023	.00023 .00023 .00023	.00022 .00022 .00021	.00021 .00021 .00020
	26	Dry Bulb per Deg. Inc. Decr's Wt.	.00016 .00016 .00016	.00015 .00015 .00015	.00015 .00015 .00015	.00015 .00016 .00016	.00018 .00019 .00021	.00023 .00025 .00025	$\begin{array}{c} 00031 \\ 00035 \\ 00035 \end{array}$
		Wt. per Cu. Ft. Saturated Air	.07500 .07338 .07180	.07027 .06879 .06732	.06588 .06442 .06297	.06146 .05991 .05828	.05653 .05467 .05262	.05036 .04788 .04509	.04197 .03845 .03449
		Dry Bulb Ten	200	30 40 50	60 20 80	90 1100	120 130 140	150 160 170	180 190 200

PROPERTIES OF AIR

cated. For ordinary fan work, however, where air is at low pressure but slight error is introduced if the same formulae are applied to the flow of air as are commonly used for the flow of water. The basic formula for such calculations is

$$V_s = \sqrt{2 \text{ gh}} \tag{10}$$

where $V_s =$ velocity in ft. per second, or

$$V = 60 \sqrt{2 \text{ gh}}$$
(11)

where V = velocity in ft. per min.

g = acceleration due to gravity in feet per second

h = head in ft. causing flow

But we also have

$$\mathbf{h} = \mathbf{h}' \frac{\mathbf{d}}{12\mathbf{W}} \tag{12}$$

where h' = head expressed in in. of water

d = density of water

W = weight of air in lbs. per cu. ft.

Then at 70° F. and 29.92" barometer and with dry air

$$\frac{\mathrm{d}}{12\mathrm{W}} = \frac{62.31}{12 \times 0.07495} = 69.75$$

and we have

$$V = 60\sqrt{2 \text{ gh}' \frac{d}{12W}} = 4005\sqrt{h'}$$
(13)

Thus we see that the velocity at standard conditions stated for a pressure of one inch of water will be 4005 ft. per min., and for one ounce per square inch will be

$$4005\sqrt{1.734} = 5273$$
 ft. per min. (14)

The weight of dry or saturated air at other temperatures may be found from the tables on pages 13 and 15, or for any special condition of temperature, barometer, or humidity from the table on page 17, the use of which has already been explained, (see page 14).

The most convenient formulae for determining the velocity or pressure of air under different conditions of temperature, barometer and humidity, when computing test results are the following:

$$V = 1096.5 \sqrt{\frac{p}{W}}$$
(15)

hence

$$\mathbf{p} = \left(\frac{\mathbf{V}}{1096.5}\right)^2 \mathbf{W} \tag{16}$$

where

V = velocity in ft. per min. p = pressure in in. of water.

W = weight of air in lbs. per cu. ft.

The quantity of air discharged through an orifice or nozzle due to a difference in pressure may be determined from

$$Q = 1096.5 C A \sqrt{\frac{p}{W}}$$

where

C = coefficient of discharge.

A = area of orifice in sq. ft.

p = pressure head in in. of water causing flow of air through orifice.

W = weight of air in lbs. per cu. ft.

For values of coefficients of discharge see "Coefficients of Discharge for Air Measurements" in Part IV, Section II.

In case the pressure is expressed in ounces per square inch these formulae become:

$$V = 1444.5\sqrt{\frac{p}{W}}$$
(17)

$$\mathbf{p} = \left(\frac{\mathbf{V}}{1444.5}\right)^2 \mathbf{W} \tag{18}$$

and

 $Q = 1444.5 \text{ C A } \sqrt{\frac{p}{W}}$

The value to be used for W to be determined for each specific case, as already explained.

Example. As an example of the application of the above we will assume a case of a fan test made under the same atmospheric conditions as those assumed for the example on page 14. That is, the air to be at 83° F. and 15° depression, with the barometer at 29.40 inches. What will be the velocity of this air at a pressure of 1.5 inches of water as measured by a pitot tube? As determined on page 16 the weight of air under the above conditions will be 0.07142 lb. per cu. ft. Then from formula (15) we find the velocity to be

$$V = 1096.5 \sqrt{\frac{1.5}{0.07142}} = 5024$$
 ft. per min.

The above formulae are sufficiently accurate for low pressures such as are ordinarily used in fan work, but for high pressures such as are met in compressed air work, the error becomes excessive and it will be found necessary to use the following thermodynamic formulae. For the flow through an orifice from a higher to a lower pressure, where the absolute initial pressure is less than twice the absolute pressure of the discharge region,

$$V_2 = 6552 \sqrt{T_1 \left[1 - \left(\frac{P_2}{P_1} \right)^{0.29} \right]}$$
(19)

where

 $V_2 =$ velocity in ft. per min. at discharge.

 $P_1 = absolute initial press. in lb. per sq. in.$

 $P_2 = absolute final press. in lb. per sq. in.$

 $T_1 = absolute temp. degrees F. of entering air.$

The discharge through an orifice into a region where the pressure is greater than half the initial pressure, expressed in cubic feet of free air per minute, may then be determined by the formula

$$Q = 631600 \text{CA} \frac{P_1}{\sqrt{T_1}} \sqrt{\left(\frac{P_2}{P_1}\right)^{1.42} - \left(\frac{P_2}{P_1}\right)^{1.71}}$$
(20)

where

 $\mathbf{Q}=\!\mathbf{c}\mathbf{u}.$ ft. free air per min.

C = coefficient of discharge.

A = orifice area in sq. ft.

As already shown for dry air at 70° F. and 29.92 inch barometric pressure, the velocity due to a pressure of one inch of water is 4005 feet per minute and for a pressure of one ounce per square inch is 5273 feet per minute. Since the velocity varies as the square root of the pressure, we have

$$\frac{V}{V_0} = \sqrt{\frac{p}{p_0}} \text{ or } V = V_0 \sqrt{\frac{p}{p_0}}$$
(21)

Taking p_0 as unit pressure, and V_0 the velocity corresponding thereto, assuming dry air at 70° F. and 29.92 inch barometer, the above relation reduces to

$$V = 4005 \gamma p \tag{22}$$

When the pressure is taken in inches

or
$$V = 5273 \gamma$$
 p (23)

when the pressure is expressed in ounces.

The table on page 21 gives the velocity of dry air at standard conditions for various pressures expressed both in inches and ounces. The two tables on pages 22 and 23 give the corresponding velocities of dry air under standard barometric pressure of

 In	i e	, É	6 .	ż	
Inches of Water	Ounces per Sq. In.	Velocity Ft. per Min.	Inches of Water	Ounces per Sq. In.	Velocity Ft. per Min.
jo	Der	Ft.	o T	Der	Ft.
.05 .10 .20	.0289 .0577 .1154	896 1266 1791	4.77 5.00 5.20	$2.750 \\ 2.884 \\ 3.000$	8745 8943 9134
.25 .30 .40	.1443 .1730 .2308	2003 2193 2533	5.50 6.00 6.07	$3.172 \\ 3.460 \\ 3.500$	9392 9810 9864
.43 .50 .60	$\begin{array}{r} .2500 \\ .2884 \\ .3460 \end{array}$	2637 2832 3102	6.50 6.94 7.00	$3.749 \\ 4.000 \\ 4.037$	$10210 \\ 10545 \\ 10595$
.70 .75 .80	.4037 .4326 .4614	$3351 \\ 3468 \\ 3582$	7.50 7.80 8.00	$4.326 \\ 4.500 \\ 4.614$	10968 11187 11328
.87 .90 1.00	.5000 .5190 .5768	3729 3800 4005	8.67 9.00 9.54	$5.000 \\ 5.190 \\ 5.500$	$11792 \\ 12015 \\ 12367$
1.25 1.30 1.50	.7209 .7500 .8650	4478 4566 4905	10.00 10.40 11.00	$5.768 \\ 6.000 \\ 6.344$	$12665 \\ 12915 \\ 13282$
1.73 1.75 2.00	$1.0000 \\ 1.0092 \\ 1.1535$	5273 5298 5664	11.27 12.00 12.14	$\begin{array}{c} 6.500 \\ 6.921 \\ 7.000 \end{array}$	$13445 \\ 13875 \\ 13950$
2.17 2.25 2.50	$\begin{array}{c} 1.2500 \\ 1.2975 \\ 1.4418 \end{array}$	5895 6007 6332	13.00 13.87 14.00	7.497 8.000 8.074	$14440 \\ 14913 \\ 14985$
2.60 2.75 3.00	$1.5000 \\ 1.5860 \\ 1.7300$	6457 6641 6937	15.00 15.61 16.00	8.650 9.000 9.227	$15510 \\ 15820 \\ 16020$
3.03 3.25 3.47	$\begin{array}{c} 1.7500 \\ 1.8740 \\ 2.0000 \end{array}$	6976 7220 7457	17.00 17.34 18.00	$9.805 \\ 10.000 \\ 10.380$	$16513 \\ 16675 \\ 16990$
3.50 3.75 3.90	$2.0185 \\ 2.1630 \\ 2.2500$	7492 - 7756 7910	19.00 19.07 20.00	$10.960 \\ 11.000 \\ 11.535$	17456 17488 17910
4.00 4.25 4.34	$2.3070 \\ 2.4510 \\ 2.5000$	8010 8256 8337	20.81 22.54 24.28	$\begin{array}{c} 12.000 \\ 13.000 \\ 14.000 \end{array}$	18265 19012 19730
4.50 4.75	2.5950 2.7395	8496 8729	26.01 27.74	$15.000 \\ 16.000$	20420 21090

CORRESPONDING PRESSURES AND VELOCITIES OF DRY AIR AT 70° AND 29.92 INCHES BAROMETER

FAI	N E	NGIN	NEERI	N G —	BUF	FALO	FOI	RGE	сомі	PANY
TEMPERATURES		550°	1830 2590 2895	3175 3660 4095	4490 4850 5020	5185 5500 5795	6470 7100 7655	8195 8690 9150	9600 10000 11580	12900 14180
		500°	1704 2411 2696	2952 3409 3812	4175 4510 4668	4821 5114 5390	6027 6602 7131	7624 8085 8523	8938 9336 10780	12037 13203
		300°	1516 2145 2399	2626 3033 3391	3715 4013 4153	4290 4550 4796	5362 5874 6344	6783 7193 7582	7952 8307 9581	10710 11750
SURES ANI	hr.	200°	1413 2000 2235	2447 2827 3160	$3462 \\ 3740 \\ 3870$	3997 4241 4470	4997 5474 5912	6320 6704 7066	7412 7742 8940	9980 10950
CORRESPONDING VELOCITIES FOR DRY AIR AT VARIOUS PRESSURES AND TEMPERATURES 29.02 INCHES BAROMETER	Femperature Degrees Fahr.	150°	1358 1921 2149	2352 2717 3038	3327 3595 3720 •	3843 4076 4296	4804 5262 5683	6076 6443 6792	7124 7440 8592	9593 10523
	Temperatu	00،	1300 1841 2059	2254 2603 2911	3188 3445 3565	$3682 \\ 3906 \\ 4117$	4602 5042 5446	5822 6174 6508	6827 7130 8233	9192 10083
		80°	$1278 \\ 1808 \\ 2022 \\ 2022 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\$	2214 2557 2859	3131 3383 3501	$3616 \\ 3836 \\ 4043$	4520 4952 5348	5718 6064 6392	6704 7003 8086	9027 9903
		70°	1266 1791 2003	$2193 \\ 2533 \\ 2832 \\ $	3102 3351 * 3468	3582 3800 4005	4478 4905 5298	5664 6007 6332	6641 6937 8010	8943 9810
		¢0°	1255 1776 1986	2175 2512 2808	3076 3323 3439	3552 3768 3971	4440 4864 5254	5616 5956 6278	6585 6879 7942	8867 9728
		50°	$1242 \\ 1757 \\ 1965$	$2151 \\ 2485 \\ 2778 \\ $	3043 3287 3402	$3524 \\ 3728 \\ 3929$	4393 4812 5197	5556 5892 6211	6514 6807 7857	8772 9623
CORR	Pressure	Ounces	.0577 .1154 .1443	.1730 .2308 .2884	.3460 .4037 .4326	.4614 .5190 .5768	.7209 .8650 1.0092	$\begin{array}{c} 1.1535\\ 1.2975\\ 1.4418\end{array}$	$\begin{array}{c} 1.5860 \\ 1.7300 \\ 2.3070 \end{array}$	2.8840 3.4600
	Pre	Inches	.25	شغث	.75	8. 0. 1.0 8.	1.25	2.00 2.25 2.50	2.75 3.00 4.00	5.00 6.00

PERATURE	
D TEM	
INA S	
PRESSURES	a
VARIOUS	20.02 INCHES BAROMETE
AT	ES
AIR	INCHI
DRV	0.02
FOR	-
NG VELOCITIES FOR DRY AIR AT VARIOUS PRESSURES AND TEMPERATURE	
CODDESPONDING	

n

-									
	550°	2410 3405 4175	4850 5395 5900	6380 6820 7250	7625 8000 8350	8700 9020 9345	$ \begin{array}{c} 9650 \\ 10220 \\ 10780 \\ 10780 \\ \end{array} $	11300 11800 12280	12750 13200
	500°	2244 3174 3887	4489 5019 5498	5938 6347 6733	7098 7444 7772	8090 8396 8692	8977 9524 10037	10525 10995 11440	11873
	300°	1996 2824 3458	3994 4466 4892	5283 5647 5990	6314 6623 6914	7198 7470 7733	7987 8473 8930	9364 9781 10179	10564 10938
ahr.	200°	1860 2632 3223	$3722 \\ 4162 \\ 4559$	4924 5263 5582	5884 6172 6443	6708 6962 7207	7444 7897 8322	8727 9115 9486	9845 10193
femperature Degrees Fahr.	150°	1788 2530 3098	3578 4000 4382	4733 5059 5366	5656 5933 6194	6448 6692 6928	7155 7591 8000	8462 8762 9118	9464 9798
ſemperature	۰00۱	1714 2424 2969	3428 3833 4199	4535 4848 5142	5420 5685 5935	6179 6412 6638	6856 7274 7665	8038 8396 8737	9068 9388
	80°	1683 2380 2915	3367 3765 4124	4454 4761 5050	5323 5584 5828	6068 6297 6520	6734 7143 7528	7894 8245 8581	8906 9220
	70°	1667 2358 2888	3335 3729 4085	4412 4716 5002	5273 5531 5774	6011 6238 6457	6670 7076 7457	7820 8168 8500	8822 9134
	6 0°	1653 2338 2864	3307 3698 4051	4375 4677 4960	5229 5485 5725	5960 6186 6404	6614 7017 7395	7755 8099 8429	8748 9057
	50°	1635 2313 2833	3272 3658 4007	4329 4626 4907	5172 5426 5664	5896 6120 6335	6543 6942 7315	$7672 \\ 8012 \\ 8338 \\ $	8654 8960
sure	Inches	.1734 .3468 .5202	.6936 .8670 1.0400	$ \begin{array}{c} 1.2140\\ 1.3870\\ 1.5605 \end{array} $	$ \begin{array}{c} 1.7340 \\ 1.9073 \\ 2.0808 \end{array} $	2.2540 2.4275 2.6010	2.7742 3.1210 3.4680	3.8145 4.1615 4.5080	4.8550 5.2020
Pressure	Ounces		40,0	1.000	1.1	1.3	1.6 1.8 2.0	2.2	2.8

PROPERTIES OF AIR

29.92 inches for different pressures and temperatures. One table gives the velocity for even parts of an inch and the other for even parts of an ounce, with the corresponding pressure in the other unit.

Effect of Temperature and Barometric Pressure on Velocity

If considered at the same pressure the effect of changing the temperature of the air will change the corresponding velocity in direct proportion as the square root of the absolute temperatures. That is

$$V = V_0 \sqrt{\frac{460 + t}{460 + t_0}}$$
(24)

The tables on pages 22 and 23 give the corresponding velocities for dry air at various pressures and temperatures, but the velocity for any other temperature may be determined from the above formula.

In connection with fan work we have the same relation that is at constant pressure, the speed, capacity and horsepower of the fan varies as the square root of the ratio of the absolute temperatures. At constant velocity the weight and pressure of the air handled will vary inversely as the ratio of the absolute temperatures.

The velocity of air at constant pressure not only varies with any change in temperature, but also with every change in barometer. The velocity of the air varies inversely as the square root of the ratio of the barometric pressures.

Then we will have

$$V = V_0 \sqrt{\frac{b_0}{b}}$$
(25)

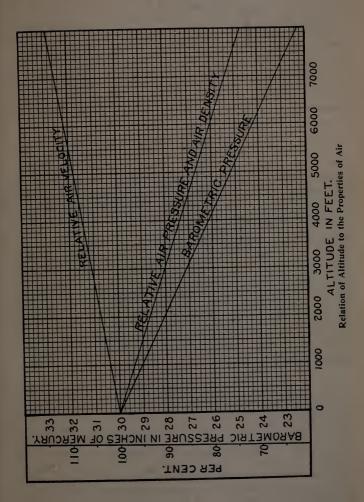
or where we wish to correct for both temperature and barometer

$$V = V_0 \sqrt{\frac{460 + t}{460 + t_0}} \times \sqrt{\frac{b_0}{b}}$$
(26)

In the above formulae V represents the velocity of the air at temperature t degrees Fahr. and barometer b, while V_0 is the corresponding velocity at temperature t_0 and barometer b_0 .

Relation of Altitude to the Properties of Air

The diagram on page 25 shows graphically the effect of different altitudes on the properties of air, and the two lines of relative air velocity and of air pressure and density are especially convenient in fan calculation.



As an illustration of the use of this diagram assume a case where a fan is to handle 150,000 A. P. M. at 0.5 inch static pressure at an altitude of 5000 feet. We must determine what sea level conditions correspond to these conditions at the given altitude and so be able to select a fan of the required capacity. From the chart we find the relative pressure at this altitude is 0.825, so that the sea level pressure corresponding to 0.5 inch at 5000 feet altitude will be $0.5 \div 0.825 = 0.6$ inch. The horsepower required to operate this fan will be 82.5 per cent. of the rated horsepower as given in the fan tables for the corresponding pressure of 0.6 inch static.

Any given amount of air as commonly specified will be increased in volume by this same ratio when we consider an altitude of say 5000 feet. Thus if we ordinarily require a definite quantity of air for a certain purpose this volume should be divided by 0.825 to determine the capacity required if the apparatus is to be installed at an altitude of 5000 feet, and a fan selected to handle this greater volume.

Effect of Temperature on the Volume of Air

Air at constant pressure changes its volume almost exactly in proportion to its absolute temperature (460+temperature deg. Fahr.) The table on page 13 gives the relative volume of a given quantity of air at various temperatures as compared to the volume at 70°. For instance, the volume at 160° will be 1.17 times the volume at 70°. Expressed as a formula for use with other temperatures than those given in the table we will have, where Q is the volume at temperature t and Q₀ the volume at t₀

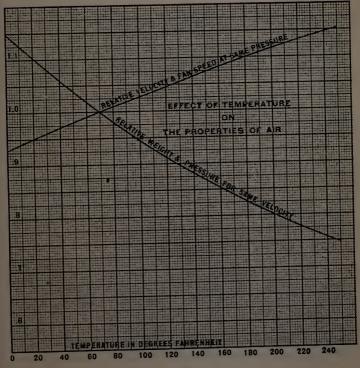
$$Q = Q_0 \left(\frac{460 + t}{460 + t_0}\right)$$
(27)

The effect of temperature on the various properties of air is shown graphically by the diagram on page 27. As air at 70° is commonly used as a standard, these curves give the various relationships relative to air at 70°. Inasmuch as the fan tables given herein are based on air at 70° F., the upper curve of this diagram is especially applicable to fan calculations. Thus we see that if the air to be handled by a fan is at 140°, the velocity and fan speed would have to be increased to 106.5 per cent. of that given in the tables. Or if the velocity remains the same, the pressure and weight of air handled at 140° will be only 88 per cent. of the rated capacity.

Effect of Humidity on Velocity

It may be noted that the tables herein given, consider the various properties of dry air at the standard temperature and barometric pressure. But as a matter of fact, atmospheric air is not dry, so that a correction is necessary in order to reduce the actual observed velocity to the standard condition of dry air. This may be accomplished by means of the following relation, the cubic feet per pound of air being determined from the psychrometric charts on pages 36 and 37.

$$\frac{\text{Actual vel.}}{\text{Vel. Dry Air}} = \sqrt{\frac{\text{Cu. ft. per lb. air as observed}}{\text{Cu. ft. per lb. dry air}}}$$
(28)



HUMIDITY

Humidity is the moisture or water vapor mixed with the air in the atmosphere, and the weight of water vapor a given space will hold is dependent entirely on the temperature. The amount of vapor in any given space is independent of the presence of air, the only effect the air has being due to its temperature.

Absolute Humidity

Absolute humidity is the weight of a given volume of water vapor at a given temperature and percentage of saturation and is usually expressed as grains per cubic foot. The tables on pages 38 to 45 give the weight of water vapor per cubic foot at different temperatures and percentages of saturation.

Relative Humidity

Relative humidity is the ratio of the weight of water vapor in a given space as compared to the weight which the same space is capable of containing when fully saturated at the same temperature. It is the ratio of the absolute humidity for the given condition to the absolute humidity at saturation. The quantity of moisture mixed with the air under different conditions of temperature and saturation is usually determined by means of some form of instrument in which a dry-bulb and a wet-bulb thermometer are used.

Dew-Point

The dew-point is the temperature at which saturation is obtained for a given weight of water vapor, or the point where any reduction in temperature would cause condensation of some of the water vapor. Any given amount of moisture must have some temperature at which saturation will occur and any further lowering of the temperature will cause condensation. This then will be its dew-point.

Dry-Bulb and Wet-Bulb Thermometer

Usually the temperature of the air is determined by means of an ordinary or dry-bulb thermometer. The wet-bulb thermometer has the bulb covered with a piece of clean soft cloth and should be wet or dipped in water before taking a reading. Care should always be taken to keep the cloth free from dirt and to use pure clean water. This thermometer will give a depressed or lower reading than that of the dry-bulb thermometer in proportion to the evaporation from the wet surface of the

HUMIDITY

cloth, and this depression is a measure of the amount of moisture in the air. This depressed reading corresponds to the temperature at which the air would normally saturate without any change in its heat contents. That is, the total heat in the air remains constant at a constant wet-bulb temperature. In order to obtain a true reading it is necessary that the thermometer be placed in a strong current of air.

The Sling Psychrometer

This instrument consists of a wet- and a dry-bulb thermometer mounted on a strip of metal and provided with a handle which permits of the thermometer being rapidly whirled through the air. When being used the instrument should be whirled continuously until no further drop in the wet-bulb reading is noted. The differ-

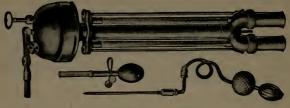


ence between the readings of the two thermometers is the wet-bulb depression, and by referring to the tables on pages 38 to 45 or to the charts on pages 35 to 37 the corresponding psychrometric conditions may be determined. There are other forms of instruments, generally of some stationary type, used for taking humidity readings, but the instrument described is reasonably accurate and is the one used by the United States Weather Bureau.

The Aspiration Psychrometer

The aspiration psychrometer shown herewith is more accurate than the sling psychrometer, as it will be noted from the cut that the bulbs of the two thermometers are enclosed in highly polished tubes so the temperature is not affected by radiation from surrounding objects.

A circulation of air is induced through the tubes by a small suction fan located in the top of the instrument. This fan is



Aspiration Psychrometer

driven at a constant speed by means of the clockwork, which will drive the fan several minutes with one winding, giving a uniform strong current to produce a rapid evaporation from the wet-bulb. The small rubber bulb is used to moisten the wick or muslin covering the wet-bulb.

Relation of Humidity to Heating

To understand more thoroughly the relation of humidity to heating, it is necessary to know that the temperature felt by the body, or the sensible temperature, as it is called, corresponds to the temperature of the wet-bulb thermometer; hence, the drier the air the greater is the difference between the actual and sensible temperatures. Dry air heated much above the normal will still be chilly, slight drafts are very noticeable and colds are easily contracted.

The excessive evaporation from the skin lowers the temperature of the body very rapidly, and as a result higher temperatures are required than would be necessary for comfort if the proper amount of humidity were present. On the other hand, if the percentage of humidity is excessive, evaporation from the body is below normal, with the result that the body heat is not radiated as speedily as is necessary for comfort. In general, the higher the humidity maintained the lower the temperature required for the same degree of personal comfort.

Relation of Dry-Bulb, Wet-Bulb and Dew-Point Temperatures

The relation between the temperature as shown by the drybulb and wet-bulb thermometer, and the relation to the dewpoint should be thoroughly understood by those expecting to become at all familiar with the subject of humidity.

Dew-point, as previously stated, is the temperature at which saturation is obtained for a given amount of water vapor. In other words, the air is at the dew-point when it contains all the moisture it will hold at a given temperature, and when it is impossible to get the air to absorb more water vapor without raising the temperature. When air has been reduced to the dewpoint, both wet- and dry-bulb thermometer register exactly the same; for instance, air at 50° temperature and 100 per cent. saturation will contain 4.076 grains of moisture per cubic foot, under which condition the dry-bulb and wet-bulb thermometer will both register 50°. If this air is heated, both thermometers will rise, but the wet-bulb temperature will rise more slowly and the relative humidity will be rapidly reduced: the dew-point remains constant at 50°, since any given number of grains of moisture per cubic foot has a fixed and definite dew-point or temperature of saturation.

If a cubic foot of air at a temperature of 87° , containing 4.076 grains per cubic foot with the wet-bulb temperature at 65° , is passed through a fine spray of recirculated water, it will absorb moisture; the dry-bulb temperature will immediately begin to fall, but the wet-bulb temperature will remain absolutely constant at 65° until the dry-bulb temperature has dropped to the wet-bulb temperature, namely, 65° . As the absorption takes place the dew-point will be gradually rising from 50° to 65° , when saturation is obtained. At ordinary temperatures the absorption of one grain of moisture per cu. ft. lowers the dry-bulb temperature approximately $8\frac{1}{2}^{\circ}$.

Sensible, Latent and Total Heat

The total heat of air is composed of the sensible heat or heat due to the temperature of the air as indicated by the thermometer, and the latent heat or heat of vaporization of the moisture or vapor in the air. The total heat is a constant quantity for any certain wet-bulb temperature irrespective of any change in the dry-bulb temperature. This fact has been termed by W. H. Carrier* "One of the four fundamental psychrometric principles," and expressed as

"The true wet-bulb temperature of the air depends entirely on the total of the sensible and the latent heat in the air and is independent of their relative proportions. In other words, the wet-bulb temperature of the air is constant, providing the total heat of the air is constant."

^{*&}quot;Rational Psychrometric Formulae" Am. Soc. Mech. Engrs., Dec., 1911.

Thus, if sufficient moisture is introduced into a certain quantity of air, the dry-bulb temperature of the air will be lowered until it is the same as the wet-bulb temperature. This is simply an exchange from sensible heat into latent heat required to vaporize the moisture, keeping the total heat the same. If a further lowering of the temperature takes place, the wet-bulb temperature will lower and the corresponding total heat will be less. If the air should be heated without the addition of more moisture, the dew-point temperature of the air would remain constant but the wet-bulb, as well as the dry-bulb temperature would increase, and the total heat of the air would increase a corresponding amount. The two psychrometric charts on pages 36 and 37 will be found especially convenient for determining the total heat of the air for any wet-bulb temperature.

Psychrometric Charts and Tables

Psychrometric charts giving the properties of air as calculated by W. H. Carrier and published in his paper entitled "Rational Psychrometric Formulae," which was presented before the A. S. M. E. at the 1911 annual meeting, are shown on pages 36 and 37. These two charts are to be used when calculations are being made in terms of pounds of air, while the chart on page 35 should be used for cubic feet of air. For most purposes of calculation it will be found preferable to use the pound as a unit.

The various curves shown on these charts will be found especially valuable in making air calculations. The grains of moisture per pound of dry air are read by passing directly from the dew-point, or intersection of the wet- and dry-bulb temperatures, to the scale on the left edge of the chart. The B. t. u. required to raise one pound of dry air one degree when saturated with moisture, as also the vapor pressure, may be determined by passing vertically from the dew-point to the proper curve, and then to the corresponding scale on the left edge of the chart. The total heat, in B. t. u., above zero degrees contained in one pound of dry air saturated with moisture may be found by passing vertically from the wet-bulb temperature to the total heat curve and then to the left edge of the chart. The volume of air in cubic feet per pound may be found by passing vertically from the dry-bulb temperature to either of the two volume curves and then to the left edge of the chart. One curve gives the volume of dry and the other of saturated air.

Example. As an example of the use of this chart we will assume air at 75° dry-bulb temperature and 60 per cent. relative humidity. From the chart we find that the wet-bulb temperature will be 65.25° , the dew-point 60° , the grains of moisture per pound of dry air 77; the heat required to raise one pound of dry air saturated at 60° through one degree is 0.24664 B. t. u.; and the vapor pressure of air saturated at 60° is 0.523 inches of mercury. Passing vertically from the wet-bulb temperature of 65.25° to the total heat curve and thence to the scale on the left, we find the total heat above zero in one pound of dry air when saturated at 65.25° to be 29.75 B. t. u. This, then, is also the measure of the heat in a pound of air at 75° and 60 per cent. relative humidity, since the wet-bulb temperature is the same.

The cubic feet per pound of air may be found by passing vertically from the dry-bulb temperature to either of the two volume curves, depending on whether the volume of dry or of saturated air is desired. To determine the volume of one pound of partly saturated air as here assumed, we will have from the chart,

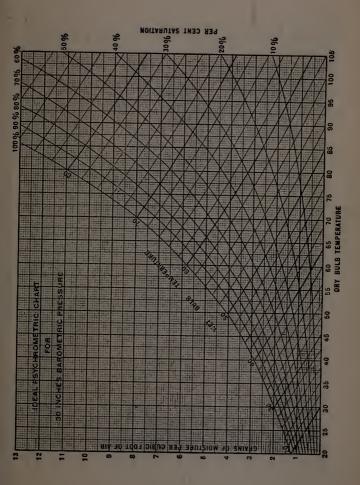
Cu. ft. per lb. at 75° sat. = 13.88 Cu. ft. per lb. at 75° dry = 13.48 .40 = Moisture .60 = Rel. humidity .24 Cu. ft. per lb. at 75° and 60% = 13.72

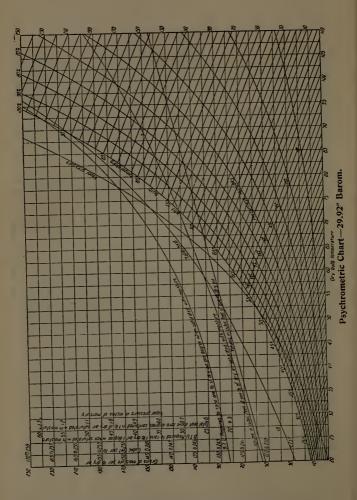
The psychrometric chart on page 35 and tables on pages 38 to 45 are taken from the catalog of the Carrier Air Conditioning Company of America. They show the grains of moisture per cubic foot of saturated air at various temperatures, as well as the relative humidity, the dew-point temperature and the grains of moisture per cubic foot of air for different temperatures as determined by the wet and dry-bulb of the sling psychrometer.

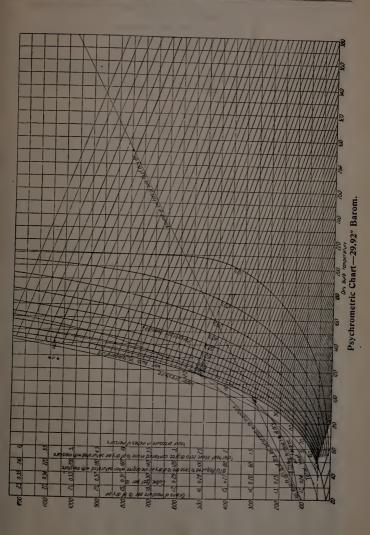
As an example of the use of the chart on page 35 we will assume a case where the dry-bulb temperature is 80° and the wet-bulb thermometer reads 70°, or a 10° depression. From the intersection of the corresponding lines through these two temperatures we find the relative humidity to be 62 per cent. Passing horizontally to the left from this point of intersection to the wet-bulb temperature line (called the saturation curve) we find the dew-point temperature to be 64.5° . If the temperature of the air should be reduced, both the dry and wet-bulb readings will be lowered until they both read 64.5° , when the air will be saturated. The grains of moisture contained in each cubic foot of this air will be found by continuing to the left on the horizontal line through the 64.5° dew-point to the left edge of the chart, where we have a reading of 6.65 grains. If the temperature of the air be further reduced, part of the moisture content will be condensed, the dew-point or saturation temperature will be lowered, and the grains of moisture per cubic foot will be correspondingly less.

In case more accurate readings are desired than can be determined from a chart on as small a scale as the one on page 35, the psychrometric tables may be used.

NOTE.—Large psychrometric charts as shown on pages 36 and 37, with sub-divisions for accurate readings, will be furnished on request by the Carrier Air Conditioning Company of America, 39 Cortlandt St., New York City.







36 38 40 42 44 46 48 50 52 4 56 5 50 61 62 36 64 65 66 67 70	-16	40 42 44 46	36	24 26 28 30 32 34	12 14 16 18 20 22	0 2 4 6 8 10	Dry-Bulb Temp. Grains per	
5.56 5.78 5.94 6.14 6.35 6.56		3.80 4.08 4.37 4.69 5.02 5.37	2.46 2.65 2.85 3.06 3.29 3.54	1.48 1.62 1.77 1.94 2.11 2.28	.86 .94 1.03 1.13 1.24 1.36	.48 .53 .58 .64 .70 .78	Cu. Ft. at Saturation	
5 94 5 94 4 94 5 95 5 95	94		91 91 92 92 93 93	87 87 88 89 89 89	80 81 82 84 85 85	67 70 72 74 76 78	fum.	
57 58 59 60 61 62	56	46 49 50 52 54 56	34 36 38 40 42 44	21 23 25 27 30 32	7 10 12 14 16 19	0.00000	Point .	
5.03 5.24 5.54 5.55 5.77 6.00 6.2 6.4 6.60 6.8 7.1 7.3 7.5	0.00	3.53 3.79 4.11 4.40 4.71 5.05	2.24 2.41 2.62 2.82 3.06 3.29	$1.30 \\ 1.41 \\ 1.56 \\ 1.72 \\ 1.88 \\ 2.05$.69 .76 .85 .95 1.10 1.17	32 37 42 47 47 61	Grs. per Cu. Ft.	Degr
2 89 89 8 89 7 89 8 89 8 89 8 89 8 89 8 90	00	86 87 87 88 88		73 75 76 78 79 81	59 62 65 68 70 71	33 39 44 49 53 56	Hum.	rees
55 56 57 58 59 60 61 62 63 64 64 656 67 67		44 46 48 50 53 55	31 33 35 38 40 42	17 20 22 25 27 29	2 5 10 12 15	-20 -15 -11 -8 -5 -2	Dew- Point	Wet=B
4.95 5.11 5.29 5.44 5.60 5.91		3.27 3.55 3.80 4.13 4.41 4.73	2.02 2.20 2.36 2.61 2.80 3.04	$\begin{array}{c} 1.10 \\ 1.22 \\ 1.37 \\ 1.50 \\ 1.67 \\ 1.85 \end{array}$.51 .58 .65 .72 .56 .96	.16 .21 .26 .32 .37 .44	drs. per Cu. Ft.	ulb D
5 83 9 84 6 84 5 84 1 84		79 80 81 82 82 83		60 63 65 67 69 71	39 44 48 52 55 58	9 17 23 29 34	Per Rel. Hum.	epres
54 55 56 57 58 59		42 44 46 48	29 31 33 35 37 40	$ \begin{array}{r} 13 \\ 16 \\ 19 \\ 21 \\ 24 \\ 26 \\ \end{array} $	-6 -2 +1 -5 8 11	-40 -28 -21 -15 -10	Dew- Point	ssion 3°
4.6 4.7 4.9 5.1 5.2 5.5	1.1	3.00 3.20 3.5 3.5 4.1	1.79 1.98 2.14 2.30 2.51 2.80	.89 1.02 1.15 1.30 1.46 1.62	.33 .41 .50 .59 .68 .79	.05 .10 .15 .20 .26	Grå. per Cu. Ft.	
1779631	0 00	$\begin{array}{cccccccccccccccccccccccccccccccccccc$		54 56 59 62	19 26 31 36 40 44	6 13	C, Rel. Hum.	
52 53 54 55 56 56 56 57		40 42 44 46 49 51	33 35 37	9 12 15 18 21 23	-19 -12 -12 -2 +2 5	-42 -27	Dew- Point	40
4.33 4.48 4.64 4.85 5.01 5.19		$\begin{array}{c} 2.77\\ 3.02\\ 3.28\\ 3.56\\ 3.81\\ 4.14\end{array}$	$1.57 \\ 1.74 \\ 1.94 \\ 2.12 \\ 2.34 \\ 2.54$.70 .83 .96 1.08 1.25 1.41	.16 .25 .32 .41 .49 .60	.04 .11	Ors. Per Cu. Pt.	

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT

HUMIDITY

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE. PER CUBIC FOOT—Barometric Pressure, 30 Inches

	Degrees Wet-Bulb Depression												
q	ate		۱°		1	2°			3°			4°	
Dry-Bulb Temp.	Grains per Cu. Ft. at Saturation	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	Mr Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
77 78 79	9.96 10.28 10.60	96 96 96	76 77 78	9.56 9.87 10.18	91 91 91	74 75 76	9.02 9.35 9.65	87 87 87	73 74 75	8.67 8.94 9.21	83 83 83	71 72 73	8.27 8.53 8.80
80 81 82 83 84	$10.93 \\ 11.28 \\ 11.63 \\ 11.99 \\ 12.36$	96 96 96 96 96	79 80 81 82 83	$\begin{array}{c} 10.50 \\ 10.82 \\ 11.16 \\ 11.51 \\ 11.86 \end{array}$	91 92 92 92 92 92	77 78 79 80 81	$\begin{array}{r} 9.95 \\ 10.37 \\ 10.70 \\ 11.03 \\ 11.37 \end{array}$	87 88 88 88 88	76 77 78 79 80	$9.51 \\ 9.92 \\ 10.23 \\ 10.55 \\ 10.87$	83 84 84 84 84 84	74 75 77 78 79	9.08 9.47 9.77 10.07 10.38
85 86 87 88 89	$12.74 \\13,13 \\13.53 \\13.94 \\14.36$	96 96 96 96 96	84 85 86 87 88	$\begin{array}{c} 12.22 \\ 12.60 \\ 12.99 \\ 13.38 \\ 13.99 \end{array}$	92 92 92 92 92 92		$11.72 \\ 12.08 \\ 12.44 \\ 12.82 \\ 13.21$	88 88 88 88 88	81 82 83 84 85	$11.21 \\ 11.55 \\ 11.90 \\ 12.26 \\ 12.64$	84 84 85 85 85	80 81 82 83 84	$10.70 \\ 11.03 \\ 11.50 \\ 11.85 \\ 12.21$
90 92 94 96 98	14.79 15.69 16.63 17.63 18.67	96 96 96 96 96	89 91 93 95 97	$\begin{array}{c} 14.20 \\ 15.06 \\ 15.97 \\ 16.92 \\ 17.92 \end{array}$	92 92 93 93 93 93	87 89 92 94 96	$13.61 \\ 14.44 \\ 15.47 \\ 16.39 \\ 17.36$	89 89 89 89 89	86 88 90 92 94	$\begin{array}{c} 13.16 \\ 13.96 \\ 14.81 \\ 15.69 \\ 16.62 \end{array}$	85 85 85 86 86	85 87 89 91 93	$\begin{array}{c} 12.57 \\ 13.34 \\ 14.14 \\ 15.16 \\ 16.06 \end{array}$
100 104 108 112 116 120	$19.77 \\ 22.13 \\ 24.72 \\ 27.88 \\ 30.10 \\ 34.80$	96 97 97 97 97 97 97	99 103 107 111 115 119	$18.98 \\ 21.46 \\ 23.98 \\ 27.02 \\ 29.20 \\ 33.76$	93 93 93 94 94 94 94	98 102 106 110 114 118	$18.38 \\ 20.58 \\ 22.99 \\ 26.19 \\ 28.29 \\ 32.71$	89 90 90 90 91 91	96 100 104 109 113 117	$17.59 \\19.91 \\22.25 \\25.07 \\27.39 \\31.67$	86 87 87 87 87 88 88	95 99 103 107 111 115	$17.00 \\ 19.25 \\ 21.51 \\ 24.24 \\ 27.21 \\ 30.62$
A	D'r e		5°			6°			7 °			8°	
Dry-Bulb Temp.	Grains per Cu. Ft. at Saturation	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
20 22 24 26 28	$1.24 \\ 1.36 \\ 1.48 \\ 1.62 \\ 1.77$	26 31 35 39 43	-7 -2 +2 7 10	.32 .42 .52 .63 .76	12 17 22 27 32	$^{-21}_{-12}$ $^{-6}_{-1}$ +4	.15 .23 .33 .44 .52	4 10 16 21	-36 -20 -11 -4	.05 .15 .26 .37	4 10	-32 -17	.07 .18
30 32 34 36 38	$1.94 \\ 2.11 \\ 2.28 \\ 2.46 \\ 2.65$	46 49 52 55 58	$ \begin{array}{r} 14 \\ 17 \\ 20 \\ 23 \\ 25 \end{array} $	$\begin{array}{r} .89 \\ 1.03 \\ 1.19 \\ 1.35 \\ 1.54 \end{array}$	36 39 43 46 50	8 12 16 19 22	.70 .82 .98 1.13 1.32	26 30 34 38 42	$+2 \\ 7 \\ 11 \\ 15 \\ 18 \\ 18 \\ 18 \\ 18 \\ 10 \\ 10 \\ 10 \\ 10$.50 .63 .78 .93 1.11	16 20 25 29 33	-7 -1 5 10 14	.31 .42 .57 .71 .87
40 42 44 46 48 50	2.85 3.06 3.29 3.54 3.80 4.08	60 62 63 65 66 67	28 30 32 35 37 40	$1.71 \\ 1.90 \\ 2.08 \\ 2.30 \\ 2.51 \\ 2.73$	52 55 56 58 60 61	25 27 30 32 35 37	$1.48 \\ 1.69 \\ 1.85 \\ 2.05 \\ 2.28 \\ 2.49$	45 47 49 52 54 55	21 24 27 29 32 34	$1.28 \\ 1.44 \\ 1.61 \\ 1.84 \\ 2.05 \\ 2.24$	37 40 43 45 47 49	18 21 24 27 29 32	$1.06 \\ 1.23 \\ 1.42 \\ 1.59 \\ 1.79 \\ 1.98$

FAN ENGINEERING-BUFFALO FORGE COMPANY

	Barometric Pressure—30 Inches Degrees Wet-Bulb Depression											
				Degre	ees W	et-Bulb	Depr	ression 7°			8°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
52 54 56 58 59	69 70 71 72 72	42 44 47 49 50	3.02 3.28 3.61 3.87 4.00	$ \begin{array}{r} 63 \\ 64 \\ 65 \\ 66 \\ 67 \end{array} $	40 42 44 47 48	$2.75 \\ 3.00 \\ 3.26 \\ 3.55 \\ 3.72$	$57 \\ 59 \\ 60 \\ 61 \\ 62$	$37 \\ 40 \\ 42 \\ 45 \\ 46$	$\begin{array}{c} 2.49 \\ 2.77 \\ 3.01 \\ 3.28 \\ 3.44 \end{array}$	51 53 55 56 57	34 37 40 42 44	$2.23 \\ 2.48 \\ 2.76 \\ 3.01 \\ 3.17$
60 61 62 63 64	73 73 74 74 74 74	$51 \\ 52 \\ 53 \\ 55 \\ 56 \\ 56 \\ $	$\begin{array}{r} 4.19 \\ 4.34 \\ 4.54 \\ 4.71 \\ 4.86 \end{array}$	68 68 69 69 70	49 50 52 53 54	$\begin{array}{c} 3.91 \\ 4.04 \\ 4.24 \\ 4.38 \\ 4.59 \end{array}$		$47 \\ 48 \\ 50 \\ 51 \\ 52$	3.62 3.74 3.93 4.07 4.27	58 58 59 60 60	45 46 47 49 50	3.33 3.45 3.62 3.81 3.94
65 66 67 68 69	75 75 75 76 76	57 58 59 60 61	$5.09 \\ 5.26 \\ 5.43 \\ 5.69 \\ 5.87$	$70 \\ 71 \\ 71 \\ 71 \\ 71 \\ 72$	55 56 57 58 59	$\begin{array}{r} 4.75 \\ 4.98 \\ 5.14 \\ 5.31 \\ 5.56 \end{array}$	66 66 67 67	53 54 55 57 58	$\begin{array}{r} 4.48 \\ 4.63 \\ 4.78 \\ 5.01 \\ 5.18 \end{array}$	61 61 62 62 63	51 52 53 55 56	4.14 4.28 4.49 4.64 4.87
70 71 72 73 74	77 77 77 78 78	$ \begin{array}{c} 62 \\ 63 \\ 64 \\ 66 \\ 67 \end{array} $	$\begin{array}{c} 6.15 \\ 6.35 \\ 6.55 \\ 6.85 \\ 7.07 \end{array}$	72 72 73 73 73 74	$ \begin{array}{r} 61 \\ 62 \\ 63 \\ 64 \\ 65 \end{array} $	5.75 5.93 6.21 6.41 6.71	68 69 69 69	59 60 61 62 63	5.43 5.60 5.87 6.06 6.26	$ \begin{array}{r} 64 \\ 65 \\ 65 \\ 65 \\ 65 \\ 65 \\ \end{array} $	57 58 59 60 62	5.11 5.27 5.53 5.71 5.89
75 76 77 78 79	78 78 79 79 79	68 69 70 71 72	7.30 7.53 7.87 8.12 8.38	74 74 74 75 75	66 67 68 69 70	$\begin{array}{c} 6.92 \\ 7.14 \\ 7.37 \\ 7.71 \\ 7.95 \end{array}$	70 70 71 71 71 71	$\begin{array}{c} 64 \\ 66 \\ 67 \\ 68 \\ 69 \end{array}$	6.59 6.76 7.07 7.30 7.53	66 66 67 67 68		6.18 6.37 6.67 6.89 7.21
80 81 82 83 84	79 80 80 80 80	73 74 75 76 77	8.64 9.02 9.30 9.59 9.89	75 76 76 76 76	72 73 74 75 76	8.20 8.57 8.84 9.11 9.39	72 72 72 73 73	70 71 72 73 74	7.87 8.12 8.37 8.75 9.02		68 70 71 72 73	7.44 7.78 8.02 8.27 8.53
85 86 87 88 89	81 81 81 81 81 81	78 79 80 81 82	$\begin{array}{c c} 10.32 \\ 10.63 \\ 10.96 \\ 11.29 \\ 11.63 \end{array}$	77 77 77 77 77 78	77 78 79 80 81	9.81 10.11 10.42 10.73 11.20	73 73 74 74 74	75 76 78 79 80	9.30 9.58 10.01 10.31 10.63		74 75 76 77 78	8.92 9.19 9.47 9.76 10.19
90 92 94 96 98	81 82 82 82 82 83	83 86 88 90 92	$\begin{array}{c} 11.98\\ 12.87\\ 13.64\\ 14.45\\ 15.50\end{array}$	78 78 79 79 79	82 84 86 88 90	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	75 75 76 76	85 87 89	10.94 11.77 12.48 13.40 14.19		79 81 84 86 88	$\begin{array}{c} 10.50 \\ 11.30 \\ 11.98 \\ 12.87 \\ 13.63 \end{array}$
100 104 108 112 110 120	83 83 84 84 84 84 84 84 84 84 84 84 84 84 84	$102 \\ 106$	$ \begin{array}{r} 16.41 \\ 18.36 \\ 20.77 \\ 23.40 \\ 26.31 \\ 29.58 \\ \end{array} $	80 80 81 81	101 195 109	15.81 17.70 20.02 22.57 25.40 28.88	1 78	91 95 100 104 108 112	15.22 17.04 19.28 21.60 24.50 27.84	2 73 4 74 8 75 0 76 0 76 4 77	90 94 98 103 107 111	$\begin{array}{c} 14.43 \\ 16.37 \\ 18.54 \\ 20.90 \\ 23.60 \\ 26.78 \end{array}$

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT

HUMIDITY

						Pressu						
		90			egrees 10 ^s	Wet-Bu		epression 11°	on	1	12°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
40 42 44 46 48 50	29 33 36 39 41 43	13 17 20 23 26 29	$\begin{array}{r} 0.83 \\ 1.01 \\ 1.19 \\ 1.38 \\ 1.56 \\ 1.75 \end{array}$	22 26 30 32 35 38	$7 \\ 12 \\ 16 \\ 20 \\ 23 \\ 26$	$\begin{array}{r} 0.63 \\ 0.80 \\ 0.99 \\ 1.13 \\ 1.33 \\ 1.55 \end{array}$	15 19 23 26 29 32	-1 6 11 15 19 22	$\begin{array}{r} 0.43 \\ 0.58 \\ 0.76 \\ 0.92 \\ 1.11 \\ 1.30 \end{array}$	7 12 16 20 23 27	$ \begin{array}{r} -14 \\ -3 \\ 4 \\ 10 \\ 14 \\ 18 \\ \end{array} $	0.20 0.37 0.53 0.71 0.88 1.10
52 54 56 58 60 62	46 48 50 51 53 54	32 34 37 40 43 45	$2.01 \\ 2.25 \\ 2.51 \\ 2.74 \\ 3.04 \\ 3.32$	40 42 44 46 48 50	29 32 34 37 40 43	$1.75 \\ 1.97 \\ 2.21 \\ 2.47 \\ 2.76 \\ 3.07$	35 37 39 41 43 45	26 29 32 35 38 40	$1.53 \\ 1.73 \\ 1.96 \\ 2.20 \\ 2.47 \\ 2.76$	29 32 34 37 39 41	22 25 29 32 35 38	$1.27 \\ 1.49 \\ 1.71 \\ 1.99 \\ 2.25 \\ 2.52$
64 66 67 68 69 70	56 57 58 58 59 59	48 50 52 53 54 55	3.68 3.99 4.20 4.34 4.56 4.71	51 53 53 54 55 55 55	46 48 49 51 52 53	3.35 3.71 3.84 4.04 4.25 4.39	47 48 49 50 51 51	43 46 47 49 50 51	3.09 3.36 3.55 3.74 3.94 4.07	43 44 45 46 47 48	41 44 45 46 48 49	2.82 3.08 3.19 3.44 3.63 3.83
71 72 73 74 75 76		56 58 59 60 61 62	$\begin{array}{r} 4.94 \\ 5.19 \\ 5.36 \\ 5.53 \\ 5.80 \\ 5.99 \end{array}$	56 57 57 58 58 58 59	54 56 57 58 59 60	4.62 4.86 5.01 5.26 5.43 5.70	52 53 53 54 54 54 55	52 54 55 56 57 59	$\begin{array}{r} 4.29 \\ 4.51 \\ 4.65 \\ 4.90 \\ 5.05 \\ 5.31 \end{array}$	48 49 50 50 51 51	50 52 53 54 55 57	3.96 4.17 4.39 4.53 4.77 4.92
77 78 79 80 81 82	63 63 64 64 65 65	63 64 66 67 68 69	6.28 6.47 6.79 7.00 7.33 7.56	$59 \\ 60 \\ 60 \\ 61 \\ 61 \\ 61 \\ 61$	$ \begin{array}{r} 62 \\ 63 \\ 64 \\ 65 \\ 66 \\ 67 \\ \end{array} $	5.88 6.17 6.36 6.67 6.88 7.09	56 56 57 57 58 58	60 61 62 63 65 66	$5.58 \\ 5.76 \\ 6.04 \\ 6.23 \\ 6.54 \\ 6.74$	52 53 53 54 55 55	58 59 60 62 63 64	5.18 5.45 5.62 5.90 6.20 6.39
83 84 85 86 87 88	66 66 66 67 67	70 71 72 73 75 76	$7.91 \\ 8.16 \\ 8.41 \\ 8.67 \\ 9.06 \\ 9.34$		69 70 71 72 73 74	$7.43 \\ 7.66 \\ 8.02 \\ 8.27 \\ 8.66 \\ 8.92$	59 59 60 60 61 61	67 68 69 70 72 73	$7.07 \\ 7.29 \\ 7.64 \\ 7.88 \\ 8.25 \\ 8.50$	56 56 57 57 57 57 57	65 66 69 70 71	6.71 6.92 7.26 7.48 7.71 7.94
89 90 92 94 96 98	68 68 69 69 70	77 78 80 82 84 87	$9.76 \\ 10.06 \\ 10.67 \\ 11.48 \\ 12.16 \\ 13.07$		75 76 79 81 83 85	$\begin{array}{r} 9.33 \\ 9.61 \\ 10.20 \\ 10.98 \\ 11.63 \\ 12.51 \end{array}$	$ \begin{array}{r} 61 \\ 61 \\ 62 \\ 63 \\ 63 \\ 64 \\ \end{array} $	74 75 77 79 82 84	$\begin{array}{r} 8.76 \\ 9.09 \\ 9.73 \\ 10.48 \\ 11.11 \\ 11.95 \end{array}$	58 58 59 60 61 61	72 73 76 78 80 82	$\begin{array}{r} 8.33 \\ 8.58 \\ 9.26 \\ 9.98 \\ 10.75 \\ 11.39 \end{array}$
100 104 108 112 116 120	70 71 72 73 74 74 74	89 93 97 101 105 110	$\begin{array}{c} 13.84 \\ 15.71 \\ 17.80 \\ 20.34 \\ 22.99 \\ 25.71 \end{array}$	68 69 70 70 71 72	87 92 96 100 104 108	$13.44 \\ 15.27 \\ 17.30 \\ 19.50 \\ 22.05 \\ 25.01$	65 66 67 68 69 69	86 90 95 99 103 107	$12.85 \\ 14.60 \\ 16.56 \\ 18.94 \\ 21.45 \\ 23.95$		85 89 93 98 102 106	12.26 13.94 15.82 18.11 20.55 23.24

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT Barometric Pressure—30 Inches

				Degr	ees W	et=Bulb	Depr	ession				
4	1-	13	>	1	149	·	I	15	· · · · · · · · · · · · · · · · · · ·		16°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	Mo Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
50 52 54 56 58 59	21 24 27 30 32 33	13 18 22 25 29 30	$\begin{array}{r} 0.86 \\ 1.05 \\ 1.27 \\ 1.51 \\ 1.72 \\ 1.83 \end{array}$	16 19 22 25 27 29	8 13 18 22 25 27	$\begin{array}{r} 0.65\\ 0.83\\ 1.03\\ 1.25\\ 1.45\\ 1.61\end{array}$	$ \begin{array}{r} 10 \\ 14 \\ 17 \\ 20 \\ 23 \\ 24 \end{array} $	0 7 12 17 21 23	$\begin{array}{r} 0.41 \\ 0.61 \\ 0.80 \\ 1.00 \\ 1.24 \\ 1.33 \end{array}$	5 9 12 16 18 20	$ \begin{array}{r} -13 \\ -2 \\ 6 \\ 12 \\ 17 \\ 19 \\ \end{array} $	$\begin{array}{c} 0.20 \\ 0.39 \\ 0.56 \\ 0.80 \\ 0.97 \\ 1.11 \end{array}$
60 61 62 63 64	34 35 36 37 38	32 33 35 36 38	$1.95 \\ 2.08 \\ 2.21 \\ 2.34 \\ 2.49$	30 31 32 33 34	29 30 32 34 35	$1.72 \\ 1.84 \\ 1.97 \\ 2.17 \\ 2.23$	26 27 28 29 30	25 27 29 30 32	$1.50 \\ 1.60 \\ 1.72 \\ 1.84 \\ 1.97$	$21 \\ 22 \\ 24 \\ 25 \\ 26$	21 23 25 27 29	$1.21 \\ 1.31 \\ 1.47 \\ 1.59 \\ 1.71$
65 66 67 68 69	39 40 41 42 43	$40 \\ 41 \\ 43 \\ 44 \\ 45$	$2.65 \\ 2.80 \\ 2.97 \\ 3.14 \\ 3.32$	35 36 37 38 39	$37 \\ 38 \\ 40 \\ 42 \\ 43$	$2.37 \\ 2.52 \\ 2.68 \\ 2.84 \\ 3.01$	31 32 33 34 35	34 35 37 39 40	$2.10 \\ 2.24 \\ 2.39 \\ 2.54 \\ 2.70$	27 29 30 31 32	$31 \\ 32 \\ 34 \\ 36 \\ 37$	$1.83 \\ 2.03 \\ 2.17 \\ 2.32 \\ 2.47$
70 71 72 73 74	44 45 45 46 47	47 48 50 51 52	3.51 3.71 3.83 4.04 4.26	${ \begin{array}{c} 40 \\ 41 \\ 42 \\ 42 \\ 43 \end{array} } $	44 46 47 49 50	3.19 3.38 3.57 3.69 3.90	36 37 38 39 39	42 43 45 46 48	2.87 3.05 3.23 3.43 3.54	33 33 34 35 36	39 41 42 44 45	$2.63 \\ 2.72 \\ 2.89 \\ 3.07 \\ 3.26$
75 76 77 78 79	47 48 48 49 50	54 55 56 57 59	$\begin{array}{r} 4.40 \\ 4.64 \\ 4.78 \\ 5.04 \\ 5.30 \end{array}$	$\begin{array}{r} 44 \\ 44 \\ 45 \\ 46 \\ 46 \\ 46 \end{array}$	51 53 54 55 57	$\begin{array}{r} 4.12 \\ 4.25 \\ 4.48 \\ 4.73 \\ 4.88 \end{array}$	40 41 42 43 43	49 51 52 53 55	3.74 3.96 4.18 4.42 4.56	37 38 39 39 39 40	47 48 50 51 53	$3.46 \\ 3.67 \\ 3.89 \\ 4.01 \\ 4.24$
80 81 82 83 84	$50 \\ 51 \\ 51 \\ 52 \\ 52 \\ 52$	$ \begin{array}{r} 60 \\ 61 \\ 62 \\ 64 \\ 65 \end{array} $	$5.47 \\ 5.75 \\ 5.93 \\ 6.23 \\ 6.43$	47 48 48 49 49	58 59 60 62 63	$5.14 \\ 5.41 \\ 5.58 \\ 5.87 \\ 6.06$	$ \begin{array}{r} 44 \\ 45 \\ 45 \\ 46 \\ 46 \\ 46 \end{array} $	56 57 59 60 61	$\begin{array}{r} 4.81 \\ 5.07 \\ 5.23 \\ 5.52 \\ 5.68 \end{array}$	$\begin{array}{c} 41 \\ 42 \\ 42 \\ 43 \\ 43 \\ 43 \end{array}$	54 55 57 58 59	$\begin{array}{r} 4.48 \\ 4.74 \\ 4.88 \\ 5.01 \\ 5.31 \end{array}$
85 86 87 88 89	$53 \\ 53 \\ 54 \\ 54 \\ 55 \\ 55$	66 67 68 69 71	$\begin{array}{c} 6.75 \\ 6.96 \\ 7.17 \\ 7.53 \\ 7.90 \end{array}$	50 50 51 51 52	64 65 67 68 69	$\begin{array}{c} 6.37 \\ 6.56 \\ 6.90 \\ 7.11 \\ 7.47 \end{array}$	47 47 48 48 49	$ \begin{array}{r} 62 \\ 64 \\ 65 \\ 66 \\ 67 \end{array} $	5.99 6.17 6.49 6.69 7.04	44 44 46 46 47	$ \begin{array}{r} 61 \\ 62 \\ 63 \\ 64 \\ 66 \\ \end{array} $	$5.60 \\ 5.78 \\ 6.22 \\ 6.41 \\ 6.75$
90 92 94 96 98	55 56 57 58 58	72 74 76 79 81	$\begin{array}{r} 8.13 \\ 8.79 \\ 9.48 \\ 10.22 \\ 10.83 \end{array}$	$52 \\ 53 \\ 54 \\ 55 \\ 56 $	70 73 75 77 79	7.69 8.32 8.98 9.69 10.46	49 50 51 52 53	69 71 73 76 78	7.25 7.84 8.48 9.17 9.90	47 48 49 50 50	67 69 72 74 76	6.95 7.53 8.15 8.81 9.34
100 104 108 112 116 120	59 60 62 63 64 65	83 88 92 96 101 105	$11.66 \\ 13.28 \\ 15.33 \\ 17.55 \\ 19.95 \\ 22.40$	56 58 59 60 61 62	82 86 91 95 99 104	$11.07 \\ 12.83 \\ 14.59 \\ 16.72 \\ 19.05 \\ 21.46$	54 55 57 58 59 60	80 85 89 94 98 102	$\begin{array}{c} 10.67 \\ 12.17 \\ 14.09 \\ 16.16 \\ 18.45 \\ 20.75 \end{array}$	51 53 54 55 57 58	79 83 88 92 97 101	$10.08 \\ 11.73 \\ 13.35 \\ 15.39 \\ 17.85 \\ 20.07$

HUMIDITY

	Barometric Pressure—30 Inches											
_		17	0	Deg	rees V	Vet-Bult	Dep	ression			20°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	Mum.	Dew- Point	Grs. per Cu. Ft.	Hum.	Dew- Point	Grs. per Cu. Ft.	Mum.	Dew- Point	Grs. per Cu. Ft.
52 54 56 58 59		$-17 \\ -4 \\ 5 \\ 11 \\ 14$	0.18 0.38 0.55 0.75 0.89	3 7 10 11	$-20 \\ -5 \\ 4 \\ 8$	$0.14 \\ 0.35 \\ 0.54 \\ 0.61$	2 6 7	$-25 \\ -6 \\ 0$	0.10 0.32 0.42	13	-30 -20	0.05 0.14
60 61 62 63 64	17 18 20 21 22	17 19 21 23 25	$\begin{array}{c} 0.98 \\ 1.07 \\ 1.23 \\ 1.33 \\ 1.44 \end{array}$	13 14 16 17 18	$11 \\ 14 \\ 16 \\ 19 \\ 21$	$\begin{array}{c} 0.75 \\ 0.83 \\ 0.98 \\ 1.08 \\ 1.18 \end{array}$	9 10 12 14 15	4 8 11 14 17	$\begin{array}{c} 0.52 \\ 0.63 \\ 0.74 \\ 0.86 \\ 0.98 \end{array}$	5 6 8 10 11	8 1 3 7 11	0.29 0.39 0.49 0.60 0.72
65 66 67 68 69	24 25 26 27 28	27 29 31 33 34	$1.63 \\ 1.75 \\ 1.88 \\ 2.00 \\ 2.16$	20 21 22 23 24	24 26 28 29 31	$1.36 \\ 1.47 \\ 1.59 \\ 1.72 \\ 1.85$	$16 \\ 17 \\ 18 \\ 20 \\ 21$	19 22 24 26 28	$1.09 \\ 1.19 \\ 1.35 \\ 1.50 \\ 1.63$	13 14 15 16 17	14 17 19 22 24	0.86 0.98 1.09 1.20 1.36
70 71 72 73 74	29 30 31 32 33	36 38 40 41 43	$2.31 \\ 2.47 \\ 2.64 \\ 2.81 \\ 2.99$	25 27 28 29 29	33 35 37 38 40	$2.00 \\ 2.23 \\ 2.38 \\ 2.55 \\ 2.63$	$22 \\ 23 \\ 24 \\ 25 \\ 26$	30 32 33 35 37	$1.76 \\ 1.85 \\ 2.04 \\ 2.20 \\ 2.36$	19 20 21 22 23	26 28 30 32 34	$1.52 \\ 1.66 \\ 1.79 \\ 1.94 \\ 2.09$
75 76 77 78 79	34 34 35 36 37	44 46 48 49 50	3.18 3.28 3.49 3.70 3.92	30 31 32 33 34	42 43 45 46 48	$2.81 \\ 2.99 \\ 3.19 \\ 3.39 \\ 3.60$	27 28 29 30 31	39 41 42 44 46	2.53 2.70 2.89 3.08 3.29	24 25 26 27 28	36 38 39 41 43	2.25 2.41 2.59 2.78 2.97
80 81 82 83 84	38 39 39 40 40	52 53 55 56 57	$\begin{array}{r} 4.16 \\ 4.40 \\ 4.53 \\ 4.65 \\ 4.94 \end{array}$	35 36 36 37 37	50 51 52 54 55	$3.83 \\ 4.06 \\ 4.19 \\ 4.44 \\ 4.57$	32 33 33 34 35	47 49 50 52 53	3.50 3.72 3.84 4.08 4.33	29 30 30 31 32	44 46 48 49 51	3.17 3.38 3.49 3.72 3.95
85 86 87 88 89	41 42 43 43 43 44	$59 \\ 60 \\ 61 \\ 62 \\ 64$	$5.22 \\ 5.52 \\ 5.82 \\ 5.99 \\ 6.32$	38 39 40 40 41	57 58 59 61 62	$\begin{array}{r} 4.84 \\ 5.12 \\ 5.41 \\ 5.58 \\ 5.89 \end{array}$	36 36 37 37 38	54 56 57 59 60	$\begin{array}{r} 4.59 \\ 4.73 \\ 5.00 \\ 5.16 \\ 5.46 \end{array}$	33 33 34 35 36	52 54 55 57 58	4.20 4.33 4.60 4.88 5.17
90 92 94 96 98	44 45 46 47 48	65 68 70 72 75	6.51 7.06 7.65 8.28 8.96	41 42 43 44 45	63 68 68 71 73	$\begin{array}{c} 6.06 \\ 6.59 \\ 7.15 \\ 7.76 \\ 8.40 \end{array}$	39 40 41 42 43	$ \begin{array}{r} 61 \\ 64 \\ 67 \\ 69 \\ 72 \end{array} $	5.77 6.28 6.82 7.40 8.03	36 37 38 39 40	59 62 65 67 70	5.33 5.81 6.32 6.87 7.47
100 104 108 112 116 120	49 50 52 53 54 55	77 82 86 91 95 100	9.69 11.06 12.85 14.84 16.87 19.05	46 48 49 51 52 53	76 80 85 90 94 98	$\begin{array}{r} 9.09 \\ 10.62 \\ 12.11 \\ 14.28 \\ 16.21 \\ 18.37 \end{array}$	44 46 47 49 50 51	74 79 84 88 93 97	8.70 10.18 11.62 13.70 15.62 17.69	41 43 45 47 48 49	72 77 82 87 91 96	$\begin{array}{r} 8.10\\ 9.51\\ 11.12\\ 13.12\\ 14.98\\ 16.96\end{array}$

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT

FAN ENGINEERING-BUFFALO FORGE COMPANY

			E	Baron	netric l	Pressure	30	Inches	i			
				Degr		et=Bulb	Depr					
₽.	I	21°			220			23°			24°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	Mum.	Dew- Point	Grs. per Cu. Ft.
66 68 70 72 74	10 13 15 18 20	11 17 22 26 30	$\begin{array}{c} 0.70 \\ 0.97 \\ 1.20 \\ 1.53 \\ 1.81 \end{array}$	7 10 12 15 17	2 11 17 22 27	$\begin{array}{c} 0.49 \\ 0.75 \\ 0.96 \\ 1.28 \\ 1.54 \end{array}$	3 6 9 12 14	$-11 \\ 2 \\ 11 \\ 17 \\ 23$	$\begin{array}{c} 0.21 \\ 0.45 \\ 0.72 \\ 1.02 \\ 1.27 \end{array}$	0 3 6 9 11	-11 2 11 18	0.22 0.48 0.77 1.00
75 76 77 78 79	$21 \\ 22 \\ 23 \\ 24 \\ 25$	$32 \\ 34 \\ 36 \\ 38 \\ 40$	$1.96 \\ 2.12 \\ 2.29 \\ 2.47 \\ 2.65$	18 19 20 21 22	29 31 33 35 37	$1.68 \\ 1.84 \\ 1.99 \\ 2.16 \\ 2.33$	15 16 17 18 19	25 27 29 31 34	$ \begin{array}{r} 1.40 \\ 1.55 \\ 1.69 \\ 1.85 \\ 2.01 \\ \end{array} $	$12 \\ 13 \\ 14 \\ 16 \\ 17$	21 23 26 28 30	$ \begin{array}{c} 1.12\\ 1.26\\ 1.39\\ 1.64\\ 1.80 \end{array} $
80 81 82 83 84	26 27 28 29 29	42 43 45 47 48	$2.74 \\ 3.04 \\ 3.26 \\ 3.48 \\ 3.58$	$23 \\ 24 \\ 25 \\ 26 \\ 26 \\ 26$	39 41 42 44 46	2.52 2.71 2.91 3.12 3.31	20 21 22 23 24	36 38 39 41 43	$2.19 \\ 2.37 \\ 2.56 \\ 2.76 \\ 2.97$	18 19 20 21 21	32 34 36 38 40	1.97 2.14 2.33 2.52 2.59
85 86 87 88 89	30 31 32 32 33	50 52 53 55 56	$3.82 \\ 4.07 \\ 4.33 \\ 4.46 \\ 4.74$	27 28 29 30 31	48 49 51 52 54	3.44 3.68 3.92 4.18 4.45	25 26 26 27 28	$45 \\ 47 \\ 48 \\ 50 \\ 51$	3.18 3.41 3.52 3.76 4.02	$22 \\ 23 \\ 24 \\ 25 \\ 26$	$\begin{array}{r} 42 \\ 44 \\ 46 \\ 47 \\ 49 \end{array}$	2.80 3.02 3.25 3.48 3.73
90 92 94 96 98	31 35 36 37 38	57 60 63 66 68	5.03 5.49 5.99 6.52 7.10	31 32 33 35 36	$55 \\ 58 \\ 61 \\ 64 \\ 66$	$\begin{array}{r} 4.59 \\ 5.02 \\ 5.49 \\ 6.17 \\ 6.72 \end{array}$	29 30 31 32 34	$53 \\ 56 \\ 59 \\ 62 \\ 64$	$\begin{array}{r} 4.29 \\ 4.71 \\ 5.16 \\ 5.64 \\ 6.35 \end{array}$	26 28 29 30 32	$51 \\ 54 \\ 57 \\ 60 \\ 63$	3.85 4.39 4.82 5.29 5.98
100 104 108 112 116 120	$39 \\ 41 \\ 43 \\ 44 \\ 46 \\ 47$	71 76 81 85 90 94	$7.71 \\ 9.07 \\ 10.63 \\ 12.26 \\ 14.33 \\ 16.28$	37 39 41 42 44 45	69 74 79 84 88 93	$7.31 \\ 8.63 \\ 10.14 \\ 11.68 \\ 13.69 \\ 15.60$	35 37 39 40 42 43	67 72 77 82 87 92	$\begin{array}{r} 6.92 \\ 8.19 \\ 9.64 \\ 11.10 \\ 13.04 \\ 14.92 \end{array}$	33 35 37 38 40 41	65 71 76 81 86 90	$\begin{array}{c} 6.52 \\ 7.75 \\ 9.15 \\ 10.54 \\ 12.40 \\ 14.24 \end{array}$
9		259	>	1	269			27)		28°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
75 76 77 78 79	9 11 12 13 14	$ \begin{array}{r} 15 \\ 18 \\ 21 \\ 24 \\ 26 \end{array} $	$\begin{array}{r} 0.84 \\ 1.06 \\ 1.20 \\ 1.34 \\ 1.48 \end{array}$	7 8 9 10 11	8 12 16 19 22	0.66 0.77 0.90 1.03 1.17	4 5 6 8 9	$ \begin{array}{r} -2 \\ 4 \\ 9 \\ 13 \\ 16 \end{array} $	$\begin{array}{r} 0.37 \\ 0.48 \\ 0.60 \\ 0.82 \\ 0.95 \end{array}$	$ \begin{array}{c} 1 \\ 3 \\ 4 \\ 5 \\ 6 \end{array} $	$ \begin{array}{r} -23 \\ -10 \\ -2 \\ 5 \\ 10 \end{array} $	0.09 0.29 0.40 0.51 0.64
80 81 82 83	15 16 17 18	28 31 33 35	$ \begin{array}{c} 1.64 \\ 1.80 \\ 1.98 \\ 2.16 \end{array} $	12 13 14 15	24 27 29 31	$1.31 \\ 1.47 \\ 1.63 \\ 1.80$	$ \begin{array}{ c c c } 10 \\ 11 \\ 12 \\ 13 \end{array} $	20 22 25 27	$1.09 \\ 1.24 \\ 1.40 \\ 1.56$	7 9 10 11	13 17 20 23	0.77 1.02 1.16 1.32

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT

Barometric Pressure-30 Inches

HUMIDITY

RELATIVE HUMIDITY, DEW-POINTS AND GRAINS OF MOISTURE PER CUBIC FOOT Barometric_Pressure—30 Inches

				Deg		Vet-Bull	b De	pressio	n			
<u>.</u>		25	,	1	26	0	-	27	>	1	28°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	Mum.	Dew- Point	Grs. per Cu. Ft.
84 85 86 87 88	19 20 21 22 22 22	37 39 41 43 45	$2.35 \\ 2.55 \\ 2.76 \\ 2.98 \\ 3.07$	16 17 18 19 20	$34 \\ 36 \\ 38 \\ 40 \\ 42$	1.98 2.17 2.36 2.57 2.79	$ \begin{array}{r} 14 \\ 15 \\ 16 \\ 17 \\ 18 \\ \end{array} $	30 32 34 36 38	$ \begin{array}{r} 1.73 \\ 1.91 \\ 2.10 \\ 2.30 \\ 2.51 \\ \end{array} $	$12 \\ 13 \\ 14 \\ 15 \\ 15 \\ 15 \\ 15 \\ 15 \\ 15 \\ 15$	26 28 31 33 35	$ \begin{array}{r} 1.48 \\ 1.66 \\ 1.84 \\ 2.03 \\ 2.09 \end{array} $
89 90 92 94 96	23 24 25 27 28	46 48 51 55 58	3.30 3.55 3.92 4.49 4.94	21 22 23 24 26	44 45 49 52 55	$3.02 \\ 3.25 \\ 3.61 \\ 3.99 \\ 4.58$	19 19 21 22 24	41 43 46 50 53	2:73 2.81 3.30 3.66 4.23	16 17 19 20 22	37 39 43 47 51	2.30 2.52 2.98 3.33 3.88
98 100 104 108 112	29 30 33 35 36	61 63 69 74 79	$5.41 \\ 5.93 \\ 7.30 \\ 8.65 \\ 9.98$	27 28 31 33 35	58 61 67 72 78	$5.04 \\ 5.54 \\ 6.86 \\ 8.16 \\ 9.42$	25 26 29 31 33	56 59 65 71 76	$\begin{array}{r} 4.67 \\ 5.14 \\ 6.42 \\ 7.66 \\ 8.86 \end{array}$	23 24 27 29 31	54 57 63 69 74	4.29 4.74 5.98 7.17 8.58
116 120	38 40	84 89	11.78 13.90	36 38	83 87	$\begin{array}{c} 11.16\\ 13.20 \end{array}$	$\frac{34}{36}$	81 86	$\begin{array}{c} 10.56\\ 12.49 \end{array}$	33 34	79 84	$10.25 \\ 11.79$
e .		29			30			31	, 	1	32°	
Dry-Bulb Temp.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.	% Rel. Hum.	Dew- Point	Grs. per Cu. Ft.
78 79 80 81 82	3 4 5 6 7	$-9 \\ -1 \\ 6 \\ 10 \\ 14$	$\begin{array}{r} 0.31 \\ 0.42 \\ 0.55 \\ 0.68 \\ 0.81 \end{array}$	1 3 4 5	-20 -7 0 7	$0.11 \\ 0.33 \\ 0.45 \\ 0.58$	$\frac{1}{2}$	-18 -6	0.11 0.23	0		
83 84 85 86 87	8 9 10 11 12	18 21 24 27 29	$\begin{array}{c} 0.96 \\ 1.11 \\ 1.27 \\ 1.44 \\ 1.62 \end{array}$	6 7 8 9 10	11 15 19 22 25	$\begin{array}{c} 0.72 \\ 0.87 \\ 1.02 \\ 1.18 \\ 1.35 \end{array}$	3 5 6 7 8	$2 \\ 8 \\ 12 \\ 16 \\ 20$	$\begin{array}{c} 0.36 \\ 0.62 \\ 0.77 \\ 0.92 \\ 1.08 \end{array}$	2 3 4 5 6	-15 -4 3 9 13	$\begin{array}{c} 0.24 \\ 0.37 \\ 0.51 \\ 0.66 \\ 0.81 \end{array}$
88 89 90 92 94	13 14 15 17 18	31 34 36 40 44	$ \begin{array}{r} 1.81 \\ 2.01 \\ 2.22 \\ 2.67 \\ 2.99 \\ \end{array} $	$ \begin{array}{c} 11 \\ 12 \\ 13 \\ 15 \\ 16 \end{array} $	27 30 32 37 41	$1.53 \\ 1.72 \\ 1.92 \\ 2.35 \\ 2.66$	9 10 11 13 14	23 26 28 33 38	$1.26 \\ 1.44 \\ 1.63 \\ 2.04 \\ 2.33$	7 8 9 11 12	17 21 24 29 34	0.98 1.15 1.33 1.73 2.00
96 98 100 104 108	20 21 22 25 27	48 52 55 61 67	$3.53 \\ 3.92 \\ 4.35 \\ 5.53 \\ 6.67$	18 19 21 23 25	45 49 52 59 65	3.17 3.55 4.15 5.09 6.18	16 17 19 21 24	42 46 50 57 63	$2.82 \\ 3.17 \\ 3.76 \\ 4.65 \\ 5.93$	14 15 17 20 22	39 43 47 54 61	$2.47 \\ 2.80 \\ 3.36 \\ 4.43 \\ 5.44$
112 116 120	29 31 33	72 78 83	8.03 9.61 11.44	27 29 31	71 76 81	7.49 8.99 10.73	26 28 29	69 74 80	$\begin{array}{c c} 7.22 \\ 8.68 \\ 10.04 \end{array}$	24 26 28	67 73 78	6.68 8.06 9.70

PART II APPLICATION

The principles of Fan Engineering have found application for a great variety of purposes and an ever increasing use in the manufacturing industries. These applications will be briefly treated under their proper heading, such as Heating, Ventilation, Drying, Cooling, Mechanical Draft, Planing Mill and other exhaust systems and various other miscellaneous uses. Some of these applications, such as heating and ventilation, are so common as to be more or less familiar to all engineers, while others are of a more special nature and the requirements as well as the apparatus used are not so generally understood.

SECTION I

HEATING

Although the heating of buildings is accomplished in many ways, the fundamental requirements and the results desired are the same in all systems; that is, to provide sufficient heat to take care of the radiation and infiltration losses, and if required, to warm the air needed for ventilation.

Heat Losses from Buildings

The heating capacity depends on the amount of the heat losses, so evidently the first step in laying out any heating system is to determine the extent of these losses. The main source of loss will be due to radiation, and as accurate data in the form of factors or coefficients for the various building materials used are available, the total heat loss may be determined when the extent of the surface is known.

Each of the various materials used in building construction has a certain capacity for transmitting heat, or we may say exerts a certain resistance to the transmission of heat, and the transmission of heat may be shown to be the reciprocal of the resistance. This transmission is due to two components, radiation and convection from the surface, and conduction through the material. The radiation and convection factor is independent of the thickness, but varies with the height of the wall, with the difference in temperature between the two sides of the material, and with variation in the air movement or velocity over the surface. While for extreme accuracy all of these variables should be considered, for ordinary calculations we may use a coefficient which will meet the average conditions. We will represent this factor by NK; where N varies with the temperature difference according to the accompanying table, and K is a constant for any given material,

NK = Surface transmission for each material.

 $\frac{1}{\text{NK}} = \text{Surface resistance to the transmission of heat by}$ radiation and convection.

The conductivity of any material will vary with the thickness, so that we will have

A = Conductivity of material itself from surface to surface per unit thickness.

 $\frac{1}{A}$ = Resistance of the material per unit of thickness to the transmission of heat.

W = Thickness of the material.

 $\frac{A}{W}$ = Conductivity of the material.

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 $\frac{W}{A}$ = Resistance of the material to conduction.

L = B. t. u. transmitted per sq. ft. per hour per deg. difference. As the total resistance is composed of the two factors $\frac{1}{NK}$ and $\frac{W}{A}$, we have the transmission in B. t. u. per square foot per degree difference in temperature between the two sides of the material,

$$\mathbf{L} = \frac{1}{\frac{1}{NK} + \frac{W}{A}}$$
(29)

and the total transmission per square foot per hour with temperatures t_1 and t_2 on the two sides of the material will be

$$L_{1} = \frac{t_{1} - t_{2}}{\frac{1}{NK} + \frac{W}{A}} = L (t_{1} - t_{2})$$
(30)

In case we are to consider a double wall or a wall made up of more than one material, we will have greater resistance due to the extra surfaces adding their resistances and also to the added resistances to conduction, thus giving a lower rate of heat transmission. This will then give us

$$L = \frac{1}{\left(\frac{1}{N_{1}K_{1}} + \frac{1}{N_{2}K_{2}} + \&c\right) + \left(\frac{W_{1}}{A_{1}} + \frac{W_{2}}{A_{2}} + \&c\right)}$$
(31)

In case the materials considered are very thin, but slight error will be introduced if we neglect the conduction factor and consider only the resistance of the surface.

This theory of heat transmission was first deduced by Peclet and has been used by the majority of investigators for determining factors of heat transmission. The following values for N, K and A are adapted from the original tables of factors for use in these formulae. The values given for A are for a unit thickness of one inch.

Difference Between Inside and Outside Temperature	N	Difference Between Inside and Outside Temperature	N
5	0.580	50	0.956
10	0.670	55	0.974
15	0.740	60	0.987
20	0.790	65	1.000
25	0.825	70	1.012
25 30 35	0.860	75	1.023
35	0.887	80	1.032
40	0.912	85	1.040
45	0.936	90	1.047

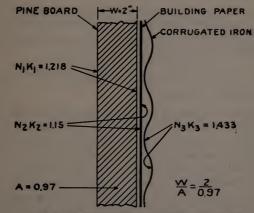
VALUES OF N FOR VARIOUS TEMPERATURE DIFFERENCES

VALUES OF K AND A FOR DIFFERENT MATERIALS

Materials	к	A
Brick	1.275 0.460	5.50 5.50
Brick and 2" Air space Pine Board	1.275 1.275	0.97
Oak Board Double Pine Board, Paper Between	0.475	0.97
Corrugated Iron	$1.500 \\ 1.200 \\ 0.555$	224.00
Pine Board and Corrugated Iron Pine Board and Sheet Iron	$0.575 \\ 0.675$	0.97 0.97
Single Glass Double Glass	$1.095 \\ 0.470$	7.20
Building Paper	1.200	

The values given in the above table apply to the two sides of the material considered, and would be double in case the factor for one side only is desired. That is, the resistance of only one surface would be one-half and the transmission therefore double the values given for the two surfaces. These factors as given apply to wall construction, where there is more or less movement of the air over the surfaces due to the current of air passing up the walls. With a roof or a floor this movement of the air will be greatly lessened and the transmission consequently decreased. The necessary modifications of the factors for other than wall construction are in a great measure a matter of judgment.

The application of the foregoing formula may best be shown by a practical example, in which it is required to determine the coefficient of transmission per square foot per degree difference in temperature for a wall composed of two-inch pine boards covered with building paper and corrugated iron, with a difference of 50° in temperature between the two sides. From the accompanying table we find the value of N to be 0.956.



HEAT TRANSMISSION THROUGH WALLS.

We will have six surface resistances to consider, N K for the two surfaces of the board being 1.218 and for the two surfaces of the corrugated iron 1.433. On account of the fact that the paper and the iron are quite thin the resistance to conduction would be very small and may be omitted for these two materials without serious error.

We will then have the surface resistance $\frac{1}{N_1K_1} = \frac{1}{1.218}$ for the two board surfaces, and assuming the same surface loss for paper as is given for sheet iron, we will have the resistance for the two sides of the paper $\frac{1}{N_2K_2} = \frac{1}{1.15}$

As already stated the resistance of the two surfaces of the iron will be $\frac{1}{N_3K_3} = \frac{1}{1.433}$ The resistance to conduction of the two-inch pine board will be $\frac{W}{A} = \frac{2}{0.97}$ Then we will have the total transmission in B. t. u. per sq. ft. per degree difference in temperature between the two sides of the wall as,

$$L = \frac{1}{\frac{1}{\frac{1}{1.218} + \frac{1}{1.15} + \frac{1}{1.433} + \frac{2}{0.97}}} = 0.224 \text{ B. t. u. per hour.}$$

If we leave out the paper and consider a wall composed of two-inch boards and corrugated iron, the transmission in B. t. u. per sq. ft. of wall per degree difference in temperature between the two sides of the wall would be

$$\mathbf{L} = \frac{1}{\frac{1}{1.218} + \frac{1}{1.433} + \frac{2}{0.97}} = 0.279 \text{ B. t. u. per hour.}$$

The factors on pages 51 and 52 are compiled from the best authorities and will be found to agree with modern engineering practice. Much of our information on this subject dates back to the time of Peclet and other early investigators, but a great deal of work has been done more recently in an effort to obtain authentic data. The principal reason for discrepancies in this part of the work is due to the great difference in building construction. Thus, although as ordinarily considered, the radiation loss is the principal factor to be considered and reliable data is available, nevertheless, due to poor construction, the convection losses may become so great that the apparatus will be unable to furnish the heat required.

For this reason these factors are subject to modifications to care for special cases such as exposure to winds, unequal distribution of heat, infiltration of cold air, etc. The German government standards require these factors to be increased as follows:

Ten per cent. where the exposure is a northerly one and the winds are to be counted on as important factors.

Ten per cent. when the building is heated during the daytime only, and the location of the building is not an exposed one.

Thirty per cent. when the building is heated during the daytime only, and the location of the building is exposed.

Fifty per cent. when the building is heated during the winter months intermittently, with long intervals of non-heating.

It may be noted that some engineers are inclined in a few instances to use slightly higher factors than here given. For instance, N. S. Thompson in his "Mechanical Equipment of Federal Buildings" gives constants for concrete that are 50 per cent. greater than the constants for brick herein quoted instead of 20 per cent. greater as given below, while the constants for brick agree very closely.

HEAT LOSS FROM BUILDINGS

B. t. u. Transmitted per Hour per Square Foot of Surface per Degree Difference in Temperature

Thickness Inches	Plain	Plastered One Side	Air Space and Plastered	Furred and Plastered
$ \begin{array}{r} 4 \\ 8 \frac{1}{2} \\ 13 \\ 17 \frac{1}{2} \\ 22 \\ 26 \frac{1}{2} \end{array} $	0.52 0.37 0.29 0.25 0.22 0.19	$\begin{array}{c} 0.50 \\ 0.36 \\ 0.28 \\ 0.24 \\ 0.21 \\ 0.18 \end{array}$	0.25 0.21 0.19 0.16 0.14	$\begin{array}{c} 0.28\\ 0.23\\ 0.20\\ 0.18\\ 0.16\end{array}$

CONSTANTS FOR BRICK WALLS

For Concrete walls add 20 per cent. to above values.

Outside walls of frame buildings, lath and plaster inside, outside construction as follows:

Clapboards, 7/16" thick		.44
Same with paper lining		.31
Same with 3/4" sheathing		.28
Same with paper and 34" sh	eathing0	.23

Inside ordinary stud partitions.

Lath and plaster, one side	
Sheet iron siding, 1.20.	
Corrugated iron siding 1.50	

Thickness of Board Inches	Pine Board	Double Board Paper Between	Board and Corrugated Iron	Board and Sheet Iron
1/2	0.77	0.32	0.45	0.50
$\frac{1}{1\frac{1}{2}}$	$0.51 \\ 0.43$	0.24 0.19	0.36 0.30	$\begin{array}{c} 0.40 \\ 0.33 \end{array}$
$\frac{1}{2}$	0.35	0.15	0.26	0.28
2 1/2	0.30	0.14	0.23	0.25

FOR VARIOUS WALL CONSTRUCTIONS

DOUBLE 1" BOARDS WITH SAWDUST BETWEEN

Sawdust Inches	B. t. u.
2	0.127
4	0.083
6	0.062
8	0.049

FOR FLOOR SURFACES

Single wooden floor, no plaster beneath joists	.45
Same, lath and plaster beneath joists	
Double wooden floor, no plaster beneath joists	.31
Same, lath and plaster beneath joists0	.18
Concrete—see concrete walls	

Assume temperature of unheated floor space beneath the floor at one-half the difference in temperature between indoors and outdoors.

FLOORS LAID ON THE GROUND

Cement or tile, no wood above0.	31
Cement or tile, wood floors above0.	
Dirt, no floor whatever	
Wood, single, laid near ground0.	10
Assume temperature of earth as plus 30° to 50° F	

FOR ROOFING PURPOSES

Sheet iron		1.20
Slate on 1" boards		
	vel	
Patent tar. gravel and pape		
	concrete, tar and gravel	
2" concrete with cinder fill		0.80
4" " " " "		
6" " " " "		

FOR GLASS SURFACE AND DOORS

Single windows																																				.1.	09	
Double window	'S																				•															.0.	46	
Single skylight			• •			• •		•	•			•	•	• •		•	•	•			•	• •		•	•	•			•		•	•	• •	• •	•	.1.	16	
Double skyligh	t.	•	• •	• •	•	• •	•	•	•	• •	•	•	•	• •	• •	•	•	• •	• •	•	•	• •	•	÷	•	• •	•	•	•	• •	•	•	• •	•	•	.0.	48	
Pine Doors, 1"	11	•	• •	• •	÷	• •	• •	•	•	• •	•	•	•	• •	• •	•	•	•	• •	•	•	• •	•	•	•	• •	•	•	•	• •	•	•	• •	•	•	.0.	41 20	
	2		•	•	• •	•	•	• •	• •	•	•	•	• •	•	•	•	• •	• •	•	•	• •	•	•	• •	• •	•	•	•	• •	•	•	• •	•	•	•	.0.	94 97	

Heat Loss Through Cold Storage Insulation

Extensive experiments have been made by various investigators who were interested in the subject of heat transfer through the various materials commonly used for insulation in cold storage work. Any apparent discrepancy between the figures quoted by different authors for the same material is probably due to the different conditions under which the tests were conducted.

The following table of coefficients has been compiled by F. E. Mathews, principally from data furnished by the Armstrong Cork Co. This table was published in Power, August 8, 1911. These values are for use under the best conditions, and builders are advised to increase them by 25 to 50 per cent., depending on the physical condition of the insulation.

COLD STORAGE INSULATION

Transmission in B. t. u. per Square Feet per Hour per Degree Difference in Temperature for

Insulating Slabs

1" "Nonpareil" cork board (pure cork, no foreign binder)0.271
1" "Rock" cork (water-proofed rock-wool composition board)0.308
1" "Lith" plain (mineral wool flax-fibre composition board)
1" "Lith" water-proofed (same as above, water-proofed)0.350
1" "impregnated cork board" (gran, cork and asphaltic binder)
1" indurated fibre board (indurated wood-pulp board)
Built-up Insulation (wood and air space)

1" American spruce	
7/8" dressed and matched spruce (7/8" sp. paper 7/8" sp.) (sp. paper ⁷ / ₈ "
sp.)	
$(\frac{7}{8}"$ sp. paper $\frac{7}{8}"$ sp.) (1" air space) ($\frac{7}{8}"$ sp. paper $\frac{7}{8}"$ s 6 thicknesses, $\frac{7}{8}"$ sp., 3 papers, 2 air spaces arranged as)
6 thicknesses, 7/8" sp., 3 papers, 2 air spaces arranged as	bove0.144 🛰
8 thicknesses, 7/8" sp., 4 papers, 3 air spaces arranged as	oove

Built-up Insulation (wood, paper and fill)

(%" sp. paper %" sp.) (%" sp. paper %" sp.) 0.198 (%" sp. paper %" sp.) (4" min. wool) (%" sp. paper %" sp.). 0.092 (%" sp. paper %" sp.) (8" mil shavings, damp) (%" sp. paper %" sp.). 0.092 (%" sp. paper %" sp.) (8" mil shavings, damp) (%" sp. paper %" sp.). 0.088 (%" sp. paper %" sp.) (8" mil shavings, dry) (%" sp. paper %" sp.). 0.006 (%" sp. paper %" sp.) (1" mill shavings, dry) (%" sp. paper %" sp.). 0.006 (%" sp. paper %" sp.) (1" Nonpareil cork) (7%" sp. paper %" sp.). 0.018 (%" sp. paper (1" Nonpareil cork) (paper %" sp.). 0.136 (%" sp. paper (2" Nonpareil cork) (paper %" sp.). 0.108 (%" sp. paper (2" Nonpareil cork) (paper %" sp.). 0.108 (%" sp. paper (2" Nonpareil cork) (paper %" sp.). 0.108 (%" sp. paper (2" Nonpareil cork) (paper %" sp.). 0.004	
$(\frac{1}{8}" \text{ sp. paper})$ (2" Nonpareil cork) (paper $\frac{5}{8}" \text{ sp.})$	

Built-up Insulation (wood, paper, air space and fill)

(1%" sp. paper 7%" sp.) (1" air space) (7%" sp.) (6" min. wool) (7%" sp. paper
 (7%" sp. paper 7%" sp.) (1" air space) (7%" sp.) (6" min. wool) (7%" sp. paper 7%" sp.) (7%" sp. paper 7%" sp.) (1" air space) (7%" sp.) (6" gran. cork) (7%" sp. paper 7%" sp.) (7%" sp. paper 7%" sp.) (1" air space) (7%" sp.) (2" Nonpareil cork) (7%" sp. paper 7%" sp.)
$\frac{7}{8}$ sp.) (1 an space) ($\frac{7}{8}$ sp.) (0 gran. cork) ($\frac{7}{8}$ sp.) aper
(7/8" sp. paper 7/8" sp.) (1" air space) (7/8" sp.) (2" Nonpareil cork) (7/8" sp.
paper ¹ / ₈ " sp.) 0.007

(7/8" sp. paper	7/8" sp.) (1" air space) (2" Nonpareil cork) (paper 7/8" sp.)0.088
	$\frac{7}{8}$ " sp.) (1" air space) (3" Nonpareil cork) (paper $\frac{7}{8}$ " sp.). 0.071
$(\frac{7}{8}''$ sp. paper	¹ / ₈ " sp.) (1" air space) (4" Nonpareil cork) (paper ¹ / ₈ " sp.)0.050
$(\frac{7}{8}''$ sp. paper	⁷ / ₈ " sp.) (1" air space) (5" Nonpareil cork) (paper ⁷ / ₈ " sp.)0.038

Brick Wall and Sheet Cork

(13" brick wall) (2" Nonparell corl		0.115
(13" brick wall) (4" Nonpareil core NOTE—Sp. designates American S	uce.	0.061

The data given in the table following is an extract from a report on Heat Transmission of Building Materials, submitted to the American Society of Heating and Ventilating Engineers, 1913, by Prof. L. A. Harding.

These results were obtained in a specially constructed testing plant, using temperature differences that ordinarily occur, either in heating or refrigerating practice. The testing boxes were made up of the various materials stated, having approximately 100 sq. ft. of surface. Heat was introduced inside the boxes by means of electrical resistance coils, the air surrounding the box being artificially cooled. A strong circulation of air was maintained both inside and outside of the box by fans.

TABLE OF UNIT HEAT TRANSMISSION

B. t. u. Transmission per Sq. Ft. per Hour per Degree Difference in Temperature of Air in Contact with the Two Sides

One 4-in. Hollow Tile	
1 in. Concrete (1-3-5 Mix.)	
$\frac{7}{3}$ in. Lumber (T and G)	
One Air Space (from 1 in. to 6 in.)	
1 in. Mineral Wool (Dry)	
1 in. Pitch	
1 in. Shavings (Dry)0.666	
1 in. Granulated Cork	
1 in. Corkboard (all Cork)	
1 in. Hair Felt	
1 in. Indurated Fibre Board0.416	
1 in. Compressed Mineral Wool Board0.33	

Heat Loss from Galvanized Iron Pipes

As already explained (page 47) the resistance of any surface to the transmission of heat is the sum of the various resistances to be met in each case, and the transmission or heat loss is the reciprocal of this total resistance. In the case of a galvanized iron duct the conductivity of the material may be neglected, and we have to consider only the resistance to the transfer of heat from the air to the metal on one side and from the metal to the air on the other side. The air in the pipe would have a direction of flow parallel to the surface so that the heat transfer would be as shown in formula (97), page 404, for longitudinal flow. The conditions on the outside of the pipe or duct would be approximately those of any direct radiation placed in the room.

According to the best authorities the coefficient of transmission K for direct radiation from the outside will vary from 1.6 to 1.8 B. t. u. per sq. ft. per hour per degree difference in temperature between the material and the external air. A factor of K=1.7 B. t. u. is an average value commonly used. Assuming a velocity of 1500 ft. per minute for the air through the pipe, we find from the diagram giving "Rate of Heat Transmission for Longitudinal Flow of Air," on page 406, that for the internal surface of the pipe K=7.5 B. t. u. The total resistance of the duct will then be

$$\frac{1}{K} = \frac{1}{1.7} + \frac{1}{7.5} = 0.723$$

K = 1.38

For average conditions as outlined above we may assume for the heat transfer through galvanized iron ducts per sq. ft. per hour per degree difference in temperature between inside and outside

> r h**our.** e pipe.

K = 1.4 B. t. u.
$H = K (t_a - t_r) = 1.4 (t_a - t_r)$
H = heat lost per square foot per
$t_a = temperature of the air in the$
$t_r = temperature of the room.$

where

Heat Loss Due to Infiltration

The heat loss due to leakage and infiltration is often a difficult quantity to determine, inasmuch as it may depend on so many different factors, such as size, height and construction of the building, distribution of doors, windows and ventilators, and the object for which the building is used. For this reason no fixed rule can be given, and the allowance to be made for this loss is necessarily a result of experience and good judgment. It is customary to allow from two changes per hour to one change in two hours as a measure of this loss, depending, as already stated, on the circumstances of the case considered. For the average application one air change per hour is usually a satisfactory allowance.

Thus if the building is very large the ratio of cubic contents to wall surface would be greater than with a smaller building, hence the air change due to leakage would be less frequent. The existence of large doors frequently opened or of ventilators makes a more rapid air change due to leakage, as does also loosely fitting windows or other faulty construction. Many of the materials used for roofs and siding, such as tile or galvanized iron, are notoriously bad as regards leakage.

The heat required in B. t. u. per hour to warm this air from the outdoor to the room temperature will be

 $H_{i} = \frac{\text{cubic contents } \times \text{ changes per hour } \times \text{ temp. rise}}{55.2}$

Heat Required for Ventilation

The heat required for ventilating is easily computed when the air supplied per hour is actually known. If we consider the specific heat of air at constant pressure to be 0.2415 and the weight of one cu. ft. of air at 70° is 0.0749 lbs., one British thermal unit of heat will raise the temperature of one cu. ft. of air

$$\frac{1}{0.2415 \times 0.0749} = 55.2^{\circ} \text{ F.}$$

From this we may deduce the formula.

$$H' = \frac{60 Q (t_r - t_1)}{55.2}$$
(32)

where

H' = B. t. u. per hour required for ventilation. Q = cu. ft. of air per min. required for ventilation.

 $t_r = room$ temperature.

 $t_1 = entering$, or outdoor, temperature.

Examples illustrating the use of the above formula will be found in Section VIII, Part IV. For a consideration of the heat given off by the occupants of a room or by various sources of heat, such as lights and machinery, see "Special Ventilation Requirements" on pages 61 and 62.

Air Quantity and Final Temperature Required for Heating

In heating a building by means of the fan system, there are three factors to be considered. These are, the heat loss due to transmission and infiltration; the quantity of air required as a heat carrier; the final temperature and the temperature rise of this air in passing through the heater. Ordinarily the heat loss and one of the other factors are given, with the third to be determined. It may be required to use all return or room air, all outdoor air, or a mixture of the two. The relations between the above factors may be expressed by the following equations:

$$Q = \frac{55.2 \text{ H}}{60 (t_2 - t_r)}$$
(33)

and

$$t_2 = \frac{55.2 H}{60 Q} + t_r \tag{34}$$

where H = heat loss in B. t. u. per hour due to transmission and infiltration.

- Q = cu. ft. of air per minute.
- $t_2 = temperature of air leaving heater.$

 $t_r = temperature of room.$

When using all or part outdoor air there will be sufficient heat required at the heater not only to take care of the heat loss, but also to raise the temperature of the air from entering temperature t_1 , to the room temperature, t_r . The total temperature rise will then be $t_2 - t_1$, and

$$H' = \frac{60 Q (t_2 - t_1)}{55.2}$$
(35)

where H' = total heat in B. t. u. per hour required at the heater.

 t_1 = temperature of air entering heater—either outdoor or a mixture of room and outdoor air.

 $t_2 = temperature of air leaving heater.$

The amount of steam required will be

 $\frac{H'}{\text{latent heat of steam}} = \text{lbs. per hour.}$

or approximately lbs. steam per hour = $\frac{H'}{1000}$

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SECTION II VENTILATION

Any room or building used for the habitation or congregation of human beings should be provided with a plentiful supply of fresh air. Strictly speaking, good ventilation is merely a relative term, and the standards as ordinarily accepted are a compromise that will answer the purpose of keeping the air in a building in a fairly fresh condition. The requirements of ventilation are, first, maintaining certain standards of purity of the air within the room or building; second, the removal and prevention of odors; third, the removal of the bodily heat of the occupants together with the heat from such other sources as illumination and power; and fourth, the prevention of excessive rise in humidity which usually accompanies the rise in temperature from bodily heat.

Many of the existing standards of ventilation have been founded on the belief that carbon dioxide was the dangerous element in expired air. The requirements of ventilation as to air purity are more or less arbitrary, and no rational standard has ever been fixed. Later investigations would indicate that carbon dioxide is harmless, and interesting only as indicating how much respiration the air has undergone. In this way it serves as an index of the contamination of the air with organic impurities from the lungs and bodies of the occupants. These organic poisons are little understood, although they undoubtedly constitute the real danger in impure air. The standard of purity which has usually been considered satisfactory is from six to eight parts of carbon dioxide in 10000 parts of air, but it is certain that ten times this amount would not be injurious if provision were made for the removal of organic impurities. In all probability the best index of good ventilation in so far as purity is concerned is freedom from objectionable odors.

It is estimated that the average adult, at rest or doing light work, will breathe approximately 0.25 cu. ft. of air and exhale 0.01 cu. ft. of CO₂ per minute (0.6 cu. ft. per hour), and that only about five per cent. or less of the oxygen is taken out of a breath of air. The air of poorly ventilated rooms will show a slight diminution in the oxygen, accompanied by a corresponding increase in carbon dioxide, organic pollution, and moisture. The poisons in the air due to the presence of too many persons relative to the supply induce a lowering of the vital processes and a loss of muscular strength.

Ordinary outdoor air will contain on an average about four parts of CO_2 in 10000 and fairly good ventilation is ordinarily considered to exist in a room where the air contains not more than from six to eight parts of CO_2 in 10000. That is, if a great amount of CO_2 exists in the air, it is considered as having been breathed too often and unfit for further respiration. The following table gives the amount of air required per hour by the average person, exhaling 0.6 cu. ft. of CO_2 per hour, if it is desired to maintain the corresponding number of parts of CO_2 in the air with outdoor air containing four parts of CO_2 per 10000.

Parts of CO ₂	in 10000	Cu. Ft. Air per Hour
Increase Above Outdoor Air	Total	Per Person
	5 6 7 8 9 10	6000 3000 1500 1200 1000

It is ordinarily the custom to allow for average conditions 1800 cu. ft. of air per hour per person, and this is the factor commonly used for school ventilation. But there are many cases in which the amount of air allowed is varied to suit the circumstances, a few of which are given in the following table:

AIR ALLOWED PER PERSON CU. FT. PER HOUR	
2100 to 2400	
Inspitals (ordinary)	
lospitals (ordinary)	
Vork Shops	
heatres	
Schools (per child)	

Removal of Bodily Heat

In rooms where the glass and wall exposure is considerable, ventilation for the removal of bodily heat need not be considered,

except where the building is artificially cooled. In crowded audience halls, however, and even in school-rooms it is the determining factor. Each adult occupant gives off an average of 400 B. t. u. per hour, of which approximately 150 B. t. u. may be assumed to be latent heat of evaporation, while not more than 250 B. t. u. will be sensible heat given off by the breath and by convection to the surrounding air. On this basis if each occupant is supplied with 30 cu. ft. of air per minute or 1800 cu. ft. per hour there will be a rise of approximately eight degrees above the temperature at which the air is introduced into the room, so that in order to maintain we will say 70 degrees in the room, the air would have to be reduced to 62 degrees. There is evidently a limit to the difference of temperature allowable between incoming air and room temperature, which depends largely on the size and arrangement of inlet openings as effecting the production of cold drafts. The practical limit is found in standard methods of ventilation to be between 5 and 10 degrees. Therefore, the limiting quantity of air required for the removal of bodily heat must be taken approximately between 25 and 50 cu. ft. per minute per adult occupant. This, as may be noted, also gives a very satisfactory standard of purity.

While 1800 cu. ft. of air per hour or 30 cu. ft. per minute (expressed as 30 A. P. M.), when used as a standard for overhead ventilation, is in the average case amply sufficient to take care of the heat and moisture from the body, when the air is supplied through many small openings distributed about the room a smaller quantity of air may often be supplied. Several different systems of this character have been used, such as introducing the air under the seats in a theatre, or through a small opening at each desk in a school. By this means a more uniform distribution of the air is obtained than is possible with the over-head system, with greater assurance that each occupant of the room will receive the desired amount of fresh air.

Carbon Dioxide Determination

Various methods for making analyses of the air to ascertain the CO_2 content have been used, but it is generally considered that the more simple methods are little better than approximations. The more dependable methods require carefully prepared apparatus, and an operator who has had considerable experience in this or similar chemical work. One of the methods quite generally used for this determination is called the Pettenkofer method.

The Pettenkofer method of analyses for carbon dioxide is based on the fact that barium hydroxide will absorb the CO_2 from the atmosphere. A measured bottle or flask is used to collect the sample of air, some form of bellows or air pump being used to force the room air into the bottle. This operation is continued for several seconds, or until the air in the bottle has been changed quite a number of times (six to ten).

After the sample is collected, a definite quantity of standard barium hydroxide is inserted into the bottle to absorb the CO2 from the sample of air contained. At the same time a few drops of penolphthalein is added to the barium hydroxide in the bottle, giving the mixture a reddish color. The sample should then be allowed to stand for at least an hour, being frequently shaken, although the final operation may be left till the next day if desired. The excess of barium hydroxide is then titrated with standard oxalic acid, by dropping the acid into the reddened solution until the color disappears. This oxalic acid should be dropped into the sample bottle from a graduated burette, so that the exact amount of acid required to titrate the barium hydroxide not absorbed by the carbon dioxide may be measured. Previous determinations having been made to find the amount of oxalic acid required to titrate a quantity of barium hydroxide equal to that put into the bottle, the difference in the acid used before and after taking the sample is a measure of the barium hydroxide uniting with the CO2. One c. c. of the oxalic acid is equivalent to 1/10 c. c. of carbon dioxide.

Special Ventilation Requirements

There are other factors that may have to be considered in making a determination of the air quantity to be supplied for ventilating purposes. Some of these special cases are where provision is to be made to care for the heat given off by furnaces or machinery; the effect of gas jets or other lighting apparatus; or to remove the heat radiated from the bodies of the occupants of the building.

The allowance to be made for many sources of heat, such as furnaces, is often a matter of experience and good judgment, but in case of machinery using a known amount of power the heat expended may be determined on the basis of 2545 B. t. u. per hour or 42.416 B. t. u. per minute per horsepower.

The following data concerning the heat given off to the air by various electric lights is based on the standard of 2545 B. t. u. per hour per H. P.; and 1 H. P. = 746 watts, giving 3.41 B. t. u. per watt as the heat radiated. This gives the B. t. u. per hour for the following lamps:

25	watt lan	nps.																							0	-
600	watt end		i		• •	•••	• •	•••	• •	• •	•••	• •	• •	•	•	• •	٠	 •	• •	•	•		 	.1	.36	0
000	watt ent	nosed	are	•••	• •	•••	• •	• •	• •	• •	•		• •			•								.2	04	0

Prof. Kinealy quotes the following values for the heat radiated in B. t. u. per candle power per hour.

Gas, ordinary split burner	~
Gas, Welsbach burner, 16 c. p	Ι,
Petroleum	J
Petroleum	0
Electric, incandescent	4
Electric, arc	3

The following data gives the values commonly quoted as the bodily heat given off in B. t. u. per hour per person.

Child 6 years old
Man 30 years old in an atmosphere with a temperature of 31° F. 600 Adult in old age

The amount of heat in B. t. u. usually assumed as given off per person per hour in an atmosphere at 70° F. is 400 for adults and 200 for children. These are the figures generally used when the heating effect of the occupants of assembly halls, auditoriums, or factories is taken into account.

The proper allowance for the above sources of heat is of especial importance in the design of apparatus used for cooling a building in the summer-time. The heating effect of the direct sun on walls and glass surface has also to be considered, the ordinary factors in B. t. u. per hour per square foot of surface being:

Sun effect—13-inch brick wall, 6.0 B. t. u. per sq. ft. per hr. Sun effect—glass, 150.0 B. t. u. per sq. ft. per hr.

The Fan System for Heating and Ventilating

While for heating purposes the fan heating system may or may not be used, depending on circumstances and the requirements to be met, yet for purposes of ventilation the fan system is practically without competition. The fan system may be

VENTILATION



Three-Quarter Housing Fan, Left-Hand Top Horizontal Discharge, Blowing Air Through and Underneath Heater into Brick Plenum Chamber

used to supply both heat and fresh air for ventilation or it may be used in conjunction with some form of direct radiation which is to care for the heat losses. When used for ventilating purposes the fan will be required to supply whatever amount of air is specified to meet the ventilation requirements.

Arrangement of Apparatus

Fan system apparatus, consisting of a fan and some form of indirect heating coil, may be arranged either to exhaust the air through or to blow through the heater, commonly called the **exhaust-through** or **draw-through** and the **blow-through** apparatus. Each arrangement possesses its own peculiar advantages but the selection depends largely upon the individual requirements of the installation. An exhaust fan is slightly less efficient than a blower, but in a draw-through system the air blows directly from the fan into the piping system with but little, if any, change in velocity. On the other hand when using a blowthrough apparatus the velocity of the air leaving the fan must be reduced through the heater and then raised again through the piping system, both changes entailing a loss in pressure.

The exhaust-through apparatus is usually employed in factory buildings on account of its compactness as well as the advantage gained by connecting directly to the piping system. In this case the temperature of the air delivered will be the same to all parts of the building. The blow-through apparatus is used in public buildings or wherever different temperatures and independent temperature regulation are required for different rooms of the building. The use of the by-pass around the heating coils permits the mixture of hot and cold air in any desired proportions, by the use of a mixing damper at the point where the two ducts from the heater and from the by-pass join to form one duct leading to the room. In the case of public buildings the fan frequently blows the warm air into a space called a plenum chamber, from which the air ducts radiate to the various rooms of the building. For this reason this system is sometimes called the plenum system of heating and ventilating.

Upward and Downward Systems of Ventilation

For audience halls the problems of air distribution and avoidance of drafts are greatly increased owing to the usual large dimensions of such buildings, and the density to which they are peopled. Two plans of ventilation are in vogue, usually distinguished as the upward and the downward systems of ventila-In the upward method the air is admitted through tion. perforations in the floor underneath the seats and is allowed to escape through ventilators in the roof. In the downward system the air is admitted through registers in the walls at a height of several feet above the floor, and removed through vent registers in the walls at the floor line in the same manner as in school buildings. In large auditoriums the upward method is doubtless preferable when the architectural design makes it permissible. A perfect distribution of the air can be secured, and the air flow is upward in accordance with natural currents induced by the heat of the body and the breath, the products of respiration are immediately carried away, and the incoming air is uncontaminated. This method of ventilation is exceedingly efficient, as a high standard of purity can be maintained at the breathing line with a comparatively small air supply.

Upward ventilation to be successful requires a very careful arrangement of the supply openings on account of the greater liability of drafts. The velocities are necessarily low, and the registers are so small that a very large number is needed to convey the necessary air. The plenum chamber for the supply is sometimes out of the question, and on this account the downward system, which is in almost universal use in schools, is extended to churches, theatres and halls with high ceilings. With a proper arrangement of fresh air and vent registers and ample air supply excellent results are obtained. To insure such results exhaust systems are frequently relied upon, the vent registers being connected with suction fans which maintain a steady draft.

Schoolhouse Ventilation

Modern school buildings offer most exacting requirements in heating and ventilation. On account of the large number of pupils seated in one room, a very rapid air change is required, and this must be accomplished without drafts. The temperature must be uniform everywhere, and ventilation must be adequate. Even elaborate systems can not secure entirely perfect distribution of air, and the only practical and successful method of insuring ample ventilation in all parts of the room is to supply air considerably in excess of the theoretical requirements. The necessity of this added capacity, or factor of safety as it may be termed, is often overlooked in writing specifications for school buildings. Thirty cubic feet of air per pupil which is usually specified will allow from six to seven parts CO₂ in 10000. Individually this is ample, but collectively insufficient, since to insure that this per cent. of CO₂ is nowhere exceeded, it would probably be necessary to supply an average of nearly 40 cu. ft. per pupil.

Ventilation of Industrial Buildings

Where an industrial building is heated by means of a fan system apparatus and no special air requirement exists, except in certain cases, it is not customary to provide for ventilation aside from taking the air for heating purposes from the outdoors. Certain industrial processes require ventilation either for cooling or for the removal of obnoxious gases and fumes or of steam. For such cases it is advisable to use an exhaust system where practicable. The air should be exhausted if possible at the point where the heat or objectionable gases escape. It is customary to suspend a hood directly above the source of heat or gases, this hood being connected by a duct or pipe to the inlet of an exhaust fan or to a vent stack. These hoods are usually so proportioned as to obtain a velocity of from 75 to 250 feet per minute over their area, according to the location of the hood. Full directions for the design of such a system, with data on the size of hoods and piping to be used, will be found under "Exhaust Systems" on page 93, and on "Proportioning Piping for Exhaust Systems" on page 129. Data on the design of piping systems for various purposes will also be found under "Air Ducts," Part III.

A few of the more common air changes provided for ordinary conditions are:

Laundry-1 to 3 minute air change depending on the size of the room and the concentration of the heat.

Hotel kitchen—4 minute air supply and 3 minute exhaust. This tends to place the room under a slight vacuum, so that any leakage at the doors is into rather than outward from the kitchen.

Engine and boiler room—3 minute supply and 4 minute exhaust.

Foundry-15 minute air change when air is taken from outside.

Roundhouse—10 to 12 minute supply in order to keep the air free from steam and smoke.

Cooling occupied rooms in summer without refrigeration usually calls for from 4 to 6 minute air supply.

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SECTION III

Air Washing, Cooling, Humidifying,* Drying

AIR WASHING

On account of dust and soot introduced by a ventilating system, some form of air washer or air filter is essential where cleanliness is of importance. The spray type has supersceded cloth screens and other methods of wet cleaning on account of its greater efficiency and is now standard practice for ventilating equipment.

The advantages to be derived both in industrial establishments and in public buildings by maintaining any desired degree of moisture in the air, as well as freeing it from impurities, have become very widely recognized. This process is generally termed air conditioning. This conditioning can be most successfully accomplished by passing the air through a spray type of air washer or humidifier where additional moisture is desired, or by using a spray type dehumidifier when the moisture content of the air is already too great and requires reduction.

Humidity in Heated Buildings

In schools and other public buildings the humidity of the air is of more consequence than is usually supposed. The amount of moisture which air can hold at saturation per unit volume increases rapidly with the temperature as shown by the psychrometric chart on page 35. Air normally has a humidity varying from 40 to 50 per cent. of saturation, while if much above or below these limits it becomes uncomfortable if not actually injurious to the health. Hence air at 70° should contain from 3.5 to 5.5 grains per cubic foot, while at 0° it contains only about 0.3 grains and at 32° about 1.25 grains, so that in the usual systems of heating, with 32° outside, the humidity of the air when heated to 70° would be only 15.5 per cent. The effect of this ex-

^{*}NOTE.—For a general discussion of the subject of Humidity see page 28, Part I. For details of the performance and dimensions of Carrier Air Conditioning Apparatus see Section VI, Part IV.

treme dryness is undoubtedly very harmful to the mucous membrane in the nose, throat and the lungs, and may be considered a contributing source of many throat and pulmonary diseases.

The proper humidity to maintain in public buildings is from 35 to 50 per cent. The humidity to be recommended in good practice is 40 per cent., with a room temperature of 68° F. This corresponds to about three grains of moisture per cubic foot of air and a dew-point of 42°. Even this will cause slight condensation on the windows in extremely cold weather and a lower humidity should be maintained in very cold weather if condensation on the windows is objectionable.

Humidity in Manufacturing Establishments

In the case of industrial installations the amount of moisture required in the air will vary widely according to the nature of the process, some requiring high and others low relative humidity. In textile mills the necessity of humidifying and cooling the air has long been understood. Just as in many instances the fan system has superseded other methods of drying materials, it is to be expected that air conditioning apparatus with automatic control of humidity will find new applications in which economy of operation will justify the expense.

COOLING

One of the special developments in connection with the fan system of ventilating is the cooling of a building so that the indoor temperature in summer will be lower than that outdoors. A limited amount of cooling may be obtained by passing the air through an air washer in which cold water is used, and for many purposes this will be found sufficient. In case a considerable temperature difference is desired, or when a great amount of heat is to be taken care of, as from machinery and other apparatus in a factory, a special form of washer known as a dehumidifier is used. This is generally operated in two stages or sets of sprays, one using cold well water and the second using refrigerated water. With such an apparatus any desired dew-point or per cent. of relative humidity may be maintained in the room to be conditioned, and the air may be delivered as low as 39° or 40°.

It is not generally considered desirable to have too great a difference between the room and outdoor temperatures, on account of the chilling effect to persons coming in from the outdoor air. A difference of from 10° to 15° will generally be found the most desirable. The incoming air must be cooled to a temperature enough lower than the room to take care of any heat generated in the room, as well as the heat transmitted through the walls from the warmer outdoor air. In case the relative humidity of this air is then too great, the moisture content may be reduced by lowering the temperature still further, so condensing a portion of the moisture from the air. The amount of moisture contained at different saturation temperatures may be found from the psychrometric tables on pages 38 to 45.

Relation of Cooling Effect to Percentage of Relative Humidity

In the moist air system of humidifying it is evidently essential, as shown in the table on page 71, that the difference between the dew-point temperature of the incoming air and the room temperature shall not exceed a predetermined value, depending upon the percentage of humidity to be maintained. The minimum temperature at which air can be introduced is evidently the dew-point or saturation temperature at the apparatus. This permissible temperature rise limits the possible cooling effect to be obtained from each cubic foot of air as shown in the table of cooling capacities. This relationship is of primary importance in the design of the humidifying system and the disregard of it has been the chief cause of failure or of unsatisfactory operation.

Per Cent. Humidity in Room	Difference between Dew- point and Room Temperature	Cu. Ft. of Air at 70° Fahr. Required per B. t. u. Cooling Effect
50	20.3	2.71
55	17.7	3.11
60	15.2	3.63
65	12.8	4.31
70	10.8	5.10
75	8.8	6.27
80	6.8	8.11

COOLING CAPACITY OF CARRIER HUMIDIFYING SYSTEM

In the majority of industrial applications the problem during warm weather, and in some instances throughout the entire year, is as much a question of cooling as of humidifying. Indeed, in the moist air system, as has just been shown, one is dependent on the other. In every industrial air conditioning plant there are four sources of heat which must be taken into account in the design of the system:

- (a) Radiation From Outside Owing To The Maintenance Of A Lower Temperature Inside. At ordinary humidities this is negligible, but at high humidities and in dehumidifying plants it is an important factor, owing to the increased temperature difference. This may be calculated from the usual constants of radiation.
- (b) Heating Effect Of Direct Sunlight. This is especially noticeable from window shades and exposed windows and skylights where the entire heat energy of the sunlight is admitted to the room, and from the roof which constitutes the greater amount of sunlight exposure and which in ordinary construction transmits heat much more readily than the walls. Precautions should be taken where high humidities are desired to shade exposed windows and to insulate the roof thoroughly. Ventilators in the roof are of great advantage in removing the hot layer of air next it and those of ample capacity should always be provided.
- (c) Radiation Of Heat From The Bodies Of The Operatives. This amounts to about 400 to 500 B. t. u. per hour per operative, about one-half of which is sensible heat, the other half being transformed into latent heat through evaporation.
- (d) Heat Developed By Power Consumed In Driving Machinery And In Manufacturing Processes In General. According to the laws of conservation of energy, all power used in manufacturing is ultimately converted entirely into its heat equivalent. Each horsepower of energy, therefore, creates 42½ B. t. u. of heat per minute, which must be cared for by ventilation. In high-powered mills this is the chief source of heating and is frequently sufficient to overheat the building even in zero weather, thus requiring cooling by ventilation the year round.

It must be remembered that in cooling moist air the latent heat removed in condensing the moisture is usually of more importance than the reduction in the sensible heat of the air itself. The total heat removed may be determined from the total heat curve of the diagrams on pages 36 and 37. It should also be noted that the total heat of the air is dependent on the wet-bulb temperature only, and the wet-bulb temperature should always be used in such calculations. DEW-POINT TEMPERATURES AND TEMPERATURE DIFFERENCES REQUIRED IN CARRIER SYSTEM OF HUMIDIFVING FOR VARIOUS PERCENTAGES OF HUMIDITY AND ROOM TEMPERATURES

1	1	Point and Room Temp.	.25	
	35	Difference between Dew-	.75 28 .0 29 .0 29	
		Dew-Point Temp.	36.7 41.0	49.7 54.2 59.0 63.2
	40	Difference between Dew-	25.0 25.5 26.0	26.5 27.0 27.5 28.0
		Dew-Point Temp.	40.0 44.5 49.0	53.5 58.0 62.5 67.0
	45	Difference between Dew- Point and Room Temp.	22.0 22.5 22.75	$\begin{array}{c} 23.25\\ 23.75\\ 24.75\\ 24.7\end{array}$
		Dew-Point Temp.	$43.0 \\ 47.5 \\ 52.75$	56.75 61.25 65.75 70.3
	50	Point and Room Temp.	$ \begin{array}{c} 19.2 \\ 19.5 \\ 19.75 \end{array} $	20.25 20.75 21.25 21.65
dity		Dew-Point Temp.	45.8 50.5 55.25	59.75 64.25 68.75 73.35
Percentage Relative Humidity	55	Point and Room Temp.	$ \begin{array}{c} 16.7 \\ 17.0 \\ 17.25 \end{array} $	$17.7 \\ 18.1 \\ 18.1 \\ 18.4 \\ 18.75 \\ 18.75$
elative		Dew-Point Temp.	$\frac{48.3}{53.0}$	62.3 66.9 71.6 76.25
tage R	00	Point and Room Temp.	14.3 14.7 114.7 115.0	$15.2 \\ 15.6 \\ 15.8 \\ 16.2 \\ 16.2 \\ 16.2 \\ 16.2 \\ 10.2 \\ $
Percen		Dew-Point Temp.	50.7 55.3 60.0	64.8 69.4 74.2 78.8
-		Difference between Dew- Point and Room Temp.	$ \begin{array}{c} 12.2 \\ 12.5 \\ 12.75 \end{array} $	12.8 13.25 13.37 13.7
	63	Dew-Point Temp.	52.8 57.5 62.25	67.2 71.75 76.7 81.3
	20	Difference between Dew- Point and Room Temp.	10.25 10.4 10.75	10.75 10.9 11.2 11.4
		Dew-Point Temp.	54.75 59.6 64.3	69.25 74.1 78.8 83.6
	75	Difference between Dew- Point and Room Temp.	8.25 8.4 8.7 8.7	8.8 8.8 9.1 9.25
	1	Dew-Point Temp.	56.75 61.6 66.3	71.2 76.2 80.9 85.75
	•	Room Temperature Deg	65 70 75	95 95 95

Relation of Room Temperature to Outside Wet-Bulb Temperature

During cool weather the dew-point or saturation temperature at the apparatus is secured and controlled artificially at whatever point required. During warm weather however, it is impossible during the greater part of the time to obtain as low a dew-point as desired without refrigeration, which in the majority of cases of humidifying is impracticable. The lowest saturation temperature that can be obtained with an efficient spray system is the same as the outside wet-bulb temperature, as has been shown: therefore the dew-point in the room will always be the same as the outside wet-bulb temperature. Since the difference between the dew-point and the room temperature is dependent upon the percentage of relative humidity maintained, the minimum room temperature and the percentage of humidity required in the enclosure will be as shown in table on page 71. It will be noted that the lower the humidity carried, the lower the dew-point must be for any given room temperature.

Dew-Point Method of Humidity Control

Any one of the three spray types of air conditioners previously described are admirably adapted for humidity control by what is known as the dew-point method. This system is applicable only where the absolute moisture content of the air in the room is unaffected to any great extent by extraneous sources of moisture supply or by moisture absorption. It depends upon supplying the enclosure with conditioned air having a definite dewpoint and maintaining a predetermined relationship between the dew-point temperature and the room temperature. The dew-point of the air supply is determined by saturating the air and removing all free moisture at the apparatus at a definite temperature. This dew-point will evidently remain constant regardless of subsequent variations in air temperature. It may be shown that the percentage of relative humidity in an enclosure is dependent upon the difference between the dewpoint temperature and the room temperature, and that it is substantially constant for any variation in room temperature so long as the difference between the dew-point and room temperature is maintained constant. (See table page 71.)

HEAT REQUIRED TO CONDITION 1000 CU. FT. OF AIR (MEASURED AT 70 DEG. FAHR.) FROM VARIOUS ENTERING WET-BULB TEMPER-ATURES TO VARIOUS DEW-POINT TEMPERATURES

Wet-Bulb Temperature of Entering Air	Per C	Deg. Fa ent. Hun Dew-Poir 5 Deg. 1	midity, It	At 70 Deg. Fahr., 40 Per Cent. Humidity, Dew-Point 44.5 Deg. Fahr.			At 70 Deg. Fahr., 50 Per Cent. Humidity, Dew-Point 50.5 Deg. Fahr.			
Wet-Bulb T of Enter	Sensible Heat	Latent Hcat	Total Hcat	Sensible Heat	Latent Heat	Total Heat	Sensible Heat	Latent Heat	Total Heat	
-10 0 10	856 673 480	338 311 270	1194 984 750	981 802 622	471 444 403	$1452 \\ 1246 \\ 1025$	1086 907 730	567 540 498	$1653 \\ 1447 \\ 1228$	
20 30 40	307 200	203 100	510 300	$443 \\ 263 \\ 82$	336 233 96	779 496 178	550 370 190	433 330 194	983 700 384	
Wet-Bulb Temperature of Entering Air	Per Ce D	Deg. Fa ent. Hun lew-Poin d Deg. Fa	nidíty, t	Per C	Deg. Fa ent. Hun Dew-Poir 5 Deg. Fa	nidity, nt	Per C	Deg. Fa ent. Hur Dew-Poin 5 Deg. F	nt	
Wet-Bulb T of Enter	Sensible Heat	Latent Heat	Total Heat	Sensible Heat	Latent Heat	Total Heat	Sensible Heat	Latent Heat	Total Heat	
-10 0 10 20	$ \begin{array}{r} 1161 \\ 991 \\ 814 \\ 635 \end{array} $	699 672 631 565	$ 1860 \\ 1663 \\ 1445 \\ 1200 $	1243 1066 888 710	801 774 733 667	2044 1840 1621 1377	1310 1131 955 779	935 908 867 802	2245 2039 1822 1581	
30 40 50 60	457 276 83	463 327 137	920 603 220	532 353 154	565 430 240	1097 783 394	600 423 244 63	700 564 375 118	1300 987 619 181	

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It is evident that this system is particularly adapted to thermostatic control of (a) the dew-point (saturation temperature at the apparatus) and the room temperature independently; (b) of the dew-point with reference to a variable room temperature; or (c) of the room temperature with reference to a variable dew-point temperature. System (a) is generally applied to air washers and humidifiers under winter conditions, where the outside temperature is considerably lower than the room temperature and to dehumidifiers where it is possible to maintain a definite dew-point temperature throughout the entire year.

However, during summer conditions the saturation point at the apparatus will frequently and unavoidably be higher than the required minimum dew-point. Under such variable temperature conditions it is necessary to control temperature with reference to the dew-point according to system (c) and a humidifier is employed to give the air complete saturation under these conditions. A differential thermostat effects this control.

Automatic Humidity Control

In many industrial installations where humidifying or dehumidifying systems are used, some means of positively and accurately maintaining the proper temperatures and humidities is essential. While much can be accomplished by hand regulation, this would require the constant attention of a highly skilled operator which in most instances is impracticable. In many processes of manufacturing, as, for example, the weaving of silk and in the conditioning of tobacco for the manufacture of cigars, a uniformity of humidity conditions is quite as essential as the quantity of moisture, as any variation in humidity, either above or below a standard, reduces the output and causes lack of uniformity in the product. In many cases a sensitive automatic humidity control is as important as some means of humidifying. There are three distinct methods by which such automatic control can be secured:

(a) By two separate thermostats, one of which is placed at the humidifier to control the temperature of the dew-point by an automatically operating valve or damper, governing a means of varying the temperature of the spray water, of the entering air, or of both in conjunction. The other thermostat, placed in a room where the humidity is controlled, maintains a constant room temperature, either by controlling the temperature of the air entering the room,

DRYING

or by controlling some source of heat within the room. With these two temperatures maintained constant, the percentage of humidity in the room will remain constant, and will depend upon the difference between the dewpoint temperature maintained at the humidifier and the temperature maintained in the room, as shown by the table on page 71.

- (b) By a differential thermostat. This type of dew-point control is required wherever it is impracticable to maintain either a constant dew-point or a constant room temperature. In this method there are two elements, one of which is exposed to the dew-point temperature, while the other is exposed to the room temperature. They are so connected that they act conjointly upon a single thermostatic valve connected with operating motors arranged to control the dew-point temperature in relation to the variable room temperature, or to control the room temperature with respect to the variable dew-point temperature.
- (c) By means of some form of differential hygrostat. This controls the wet-bulb temperature with respect to the dry-bulb temperature, so as to maintain a constant relative humidity without regard to the dew-point or variation in room temperature.

DRYING

The drying of materials of various kinds may be accomplished either by means of direct radiation from some source of heat, or by means of air currents, depending on the character of the installation or the requirements to be met. Drying by means of air currents may be done either by means of natural circulation, or by the use of some form of fan—either of the disk wheel or steel plate type. This air is usually warmed, either by some form of heating coil or by means of waste heat, the temperature ranging say from 70° to 200° depending entirely on the nature of the substance to be dried. In some cases this temperature is varied at different periods of the operation. The time required may be anywhere from a few minutes to several days. In many cases a combination of the above systems are used—that is, both direct radiation and air circulation.

Dryers are ordinarily built in either the room type or the continuous (or progressive) type. In a room dryer the material to be dried is placed in the room and left for a certain period until drying is accomplished. In the progressive type wet material enters at one end, and is taken from the other in a

dried condition. The entering end of the dryer is termed the green or wet end and the leaving end the dry end. In a continuous dryer it is customary to introduce warm air at the dry end and exhaust it at the wet end, this air being either discharged to the atmosphere or returned to the fan to be recirculated. The apparatus is usually so arranged that any desired proportion of this return air may be recirculated, depending on the varying atmospheric conditions. The drying apparatus itself may take any one of several forms, depending on the material handled, which may be spread on trays, placed in a revolving cylinder, on a traveling conveyor, or in a room or kiln. A drying room or compartment is frequently referred to as a drying tunnel. Except in the case of cylinder driers or continuous conveyors it is customary, whenever practical, to load the material on trucks or small cars in order to facilitate the filling and emptying of the drying tunnel or kiln. The dryer should be so designed that a clear area for the passage of air is provided equal to $\frac{1}{2}$ to $\frac{2}{3}$ the cross sectional area of the dryer.

The amount of moisture carried in the air is of as great importance as is proper temperature in many classes of drying work which require either a high or a low moisture content, or often a varying amount of moisture at different periods of the drying for different substances. Any desired amount of moisture may be obtained by passing the air through a humidifier or a dehumidifier, depending on the conditions desired, or the humidity of the air may frequently be controlled by recirculating varying amounts of the moist air leaving the dryer.

The temperature drop through the dryer or tunnel must be sufficient to care for the following heat losses; (a) Radiation from the walls, (b) Heat required to raise the temperature of the material being dried, including the contained moisture, as well as the trucks or other apparatus from the room to the dryer temperature, (c) Heat required to evaporate the moisture removed by the air, which is the principal requirement. Sufficient quantity of air must be supplied to act as a heat carrier without having the temperature leaving the dryer drop too low. The air quantity must also be sufficient to remove the desired weight of moisture without bringing the air to saturation at the green end of the dryer. The relative humidity of the air leaving the dryer is ordinarily kept below 75 per cent. The quantity of air to be supplied by the fan, or frequency of the air change in the drying chamber, depends upon the rate at which moisture is given up by material. This will vary with every class of installation, in some cases as high as 1/4 minute air change being used. The theoretical amount of moisture which the air will remove is directly proportional to the difference between the wet and dry-bulb temperature of the entering air, while the actual amount absorbed by a given quantity of air is measured by the drop in dry-bulb temperature between the air entering and leaving the dryer, less a slight correction for radiation. For the same reason the higher the temperature of the entering air (the initial moisture content remaining the same) the greater will be the amount of moisture removed per given quantity of air and the greater will be the economy of the dryer.

The temperature of the air will drop approximately $8\frac{1}{2}^{\circ}$ for each grain of moisture absorbed per cubic foot of air measured at 70°, or 0.71 of a degree for each grain of moisture absorbed per pound of air. Approximate calculations may be based on air volume, but for exact determinations the weight of air handled should be used, on account of it being a fixed quantity at all temperatures. Knowing the rate of drying desired and the amount of moisture to be removed, it is a simple matter to determine the quantity of air required.

The following table of drying conditions is given by H. C. Russell* and will show some of the variations required in this work:

Material	Temp. (Deg. F.)	Drying Period
Sole leather hides Thin leather hides Bone glue Starch Apples Leaf tobacco Stem tobacco Stem tobacco Soap Wool Rags Pottery	90 90 70 to 90 70 to 90 180 to 200 140 to 180 85 200 100 105 180 120	4 to 6 days 2 to 3 days 4 days 2 days 12 hours 6 hours 2 days

CONDITIONS FOR DRYING DIFFERENT MATERIALS

*Drying Apparatus by H. C. Russell, Am. Soc. H. & V. Engrs., 1912.

The table on page 79 giving the "Moisture Removing Capacity of Air in Fan System Dryers" will be found especially convenient for use in drying calculations, as it will serve as an indication of the results to be obtained under any given conditions. Two sets of values are given, for air entering the heater either at 50 per cent. or 100 per cent. saturated. It will be noted that the results given are based on the assumption that the air leaves the dryer saturated, but as already explained, in practice the air absorbs only about 60 to 70 per cent. of this theoretical amount. Under these conditions about two-thirds as much moisture will be removed per cubic foot or pound of air as is given in the table, and the air quantity would be increased 50 per cent.

The specific heat of various substances will be found below.

Solids	Solids
Wrought iron 0.1138 Gast iron 0.1298 Steel (soft) 0.1165 Steel (hard) 0.1175 Copper 0.0951 Brass 0.0939 Lead 0.0314 Tin 0.0562 Alumina 0.1970 Zinc 0.0951	Brickwork about 0.200 Masonry about 0.200 Marble 0.210 Coal 0.200 to 0.241 River sand 0.195 Pine (turpentine) 0.467 Oak 0.570 Glass 0.194

SPECIFIC HEAT OF VARIOUS SUBSTANCES*

Liquids	Liquids
Water	Benzine 0.393 Turpentine (density 0.872) 0.472 Ether 0.503

Gases	Constant Pressure	Constant Volume
Dxygen	0.21751 3.40900	$\begin{array}{r} 0.15507 \\ 2.41226 \\ 0.17273 \end{array}$
Vitrogen Carbonic acid	$0.24380 \\ 0.21700 \\ 0.5929$	0.17273 0.17100 0.4683
Marsh gas Blast—furnace gas	0.2277	0.4035

*Kent's Mechanical Engineer's pocket book.

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-	Air E	Entering Heate	er at 70° F. an	d 50% Rel. H	um.
rature g Drye ; F.	Temp. Deg. F. at		f Moisture t Saturation	Cu. Ft. Air at Saturation	Lbs. of Steam at 212° F.
Initial Temperature Entering Dryer Deg. F.	Saturation Leaving Dryer	Grains per Lb. of Air	Grains per Cu. Ft. at 70°	Required to Evaporate I Lb. of Water	Required per Lb. of Water Evaporated
80 90 100	$\begin{array}{c} 62.1 \\ 65.5 \\ 68.7 \end{array}$	28.6 39.7 51.2	$2.12 \\ 2.94 \\ 3.80$	3300 2380 1845	0.455 0.773 0.944
110 120 130	71.7 74.5 77.0	62.5 74.5 87.0	$4.63 \\ 5.52 \\ 6.45$	1515 1270 1085	$1.050 \\ 1.118 \\ 1.152$
140 150 160	79.6 81.8 84.3	99.5 112.0 125.0	7.38 8.30 9.26	950 845 755	$1.187 \\ 1.210 \\ 1.230$
170 180 190	86.4 88.4 90.3	$138.0 \\ 151.0 \\ 164.5$	10.20 11.20 12.20	685 625 575	$1.240 \\ 1.255 \\ 1.260$
200	92.2	178.5	13.20	530	1.260
	Air En	tering Heater	at 70° F. and	Saturated	
80 90 100	72.9 75.6 78.3	$11.6 \\ 23.9 \\ 36.3$	$0.85 \\ 1.75 \\ 2.65$	8240 4050 2640	$1.490 \\ 1.480 \\ 1.470$
110 120 130	80.7 83.0 85.2	48.8 61.8 74.8	$3.56 \\ 4.52 \\ 5.46$	$1965 \\ 1525 \\ 1280$	$1.465 \\ 1.455 \\ 1.440$
140 150 160	87.3 89.3 91.2	87.8 101.8 116.3	6.41 7.44 8.50	1090 934 827	$1.435 \\ 1.418 \\ 1.395$
170 180 190	93.0 94.8 96.5	130.8 145.3 159.8	$9.55 \\ 10.62 \\ 11.68$	732 662 600	$1.380 \\ 1.365 \\ 1.355$
200	98.1	174.3	12.75	562	1.350

MOISTURE REMOVING CAPACITY OF AIR IN FAN SYSTEM DRYERS

Example. The quantity of moisture which a given amount of air may be expected to remove from the contents of a drying chamber may be determined from the psychrometric charts on pages 35 to 37. Let it be assumed that the air to be used as a drying medium contains 50 grains of moisture per pound under the average conditions at which it enters the heater. Here the air is warmed and delivered to the dryer at say 150° Fahr. The moisture content of this air will still be the same as first considered, that is, 50 grains per pound of air.

The amount of moisture which this air will remove may be determined from the high psychrometric chart on page 37. The first step is to find the intersection of the horizontal line through 50 grains per pound with the vertical line through 150° dry-bulb temperature, and by following the diagonal through this point to the saturation curve, we have a wet-bulb temperature of 81°, which is the temperature the air would assume if brought to saturation. Following the horizontal from this point to the left edge of the chart, it will be seen that at saturation this air would be capable of containing 165 grains per pound, or an increase of 115 grains. In practice it is impossible to bring the air to saturation, the limit generally being from 65 to 75 per cent. of the theoretical increase. Assuming that the air under consideration will absorb 70 per cent. of the 115 grains indicated above, gives us 80 grains of moisture absorbed per pound of air.

Inasmuch as a draw-through outfit will generally be used for this class of installation, the fan will handle the air at a temperature enough above 150° to care for the radiation loss from the connections. The quantity of air handled will then be based on 50 grains per pound and a temperature of at least 150°, or, as found from the psychrometric chart, approximately 13.7 cu. ft. per pound. Then 80 ± 13.7 gives 5.85 grains absorbed per cubic foot of air. On the basis that each grain absorbed will reduce the temperature of the air 8.5° , we will have a drop in temperature through the dryer of $8.5 \times 5.85 = 50^\circ$. There will be an additional drop in temperature due to the radiation loss from the walls of the dryer, as well as due to the heat required to raise the contents to the temperature of the dryer.

SECTION IV

MECHANICAL DRAFT

There are two methods in common use for removing smoke and gases from a boiler, by means of a chimney or natural draft, and by means of a steam jet or a fan, commonly called mechanical draft.

Mechanical draft possesses many advantages over natural draft, in that it is independent of atmospheric conditions, and absolute command of the draft enables the boilers to be operated at capacities greatly in excess of that possible when depending on natural draft. Indeed it is directly responsible for the high rates of combustion and the increased efficiency obtained with modern boiler plants. Heat in the escaping gases may be largely used in economizers, since it is not required to create draft, resulting in a considerable saving. It is also possible to burn a cheaper grade of fuel when using the mechanical draft systems.

Mechanical draft produced by a fan is commonly classified under two heads, forced draft and induced draft. Each of these systems has its advantages and each has special features which recommend it for different cases.

Forced Draft

In the case of forced draft, air is forced by the fan through the fire, maintaining a pressure in the ash pit and furnace greater than that of the atmosphere. Forced draft is applied in two ways: The plenum system used in steamships, where forced draft creates a pressure in the entire stoke-hold, and the direct system where the fan discharges directly into the ash pit beneath the grates. Forced draft is always used with underfeed stokers on account of the restricted area of tuyere openings.

With forced draft the blower should be run at a pressure sufficient to overcome the resistance of the grate; the pressure losses in the tubes and breeching all being taken care of by the stack, with an indraft above the fire of from 0.05 to 0.10 of an inch. Hence forced draft requires a higher stack than would an induced draft system, since its action practically ceases at the surface of the fire. If a greater pressure should be carried, the result would be a pressure in the fire-box greater than that existing in the room, so there would be an out-rush of flame and smoke when the fire-door was opened.

Induced Draft

In the induced draft system the fan is placed at the base of the stack and handles the smoke and gases. By this means a partial vacuum is maintained within the furnace, closely imitating the action of a chimney. Induced draft should not be expected to create an excessive vacuum through the fuel bed itself. In case an excessive furnace draft is maintained the loss due to air leakage through the boiler setting is greatly increased. A combination system of both forced and induced draft is frequently used to good advantage where a considerable overload capacity is required of the boilers. Thus it is seen that an induced draft system is intended to either supply the draft ordinarily obtained by means of a stack, or to so increase the capacity of a stack that variable or overload capacities may be carried.

The use of mechanical draft makes a much more flexible system than does any system of natural draft, since the pressure or intensity of the draft is under perfect control of the fireman. Extreme fluctuations of load may be cared for, and peak loads that would be impossible when depending on natural draft may be readily carried.

Draft Requirement

The draft or pressure required for a boiler is due to the combined effect of two causes, the resistance of the fuel bed and the resistance of the boiler itself. In case the breeching and uptake are considered, they will cause an additional pressure loss. The amount or intensity of the draft required varies with the rate of combustion, thickness of the fuel bed, and character of the fuel used. Boiler and economizer losses for which draft is required follow the usual law for frictional resistance. That is, other conditions remaining the same, the draft loss varies as the square of the velocity and therefore approximately as the square of the per cent. of rating developed. For example, an increase of 50 per cent. in capacity requires a draft which is 2.25 times the draft at normal rating, and for forcing to 100 per cent. overload would require four times the draft used at normal rating.

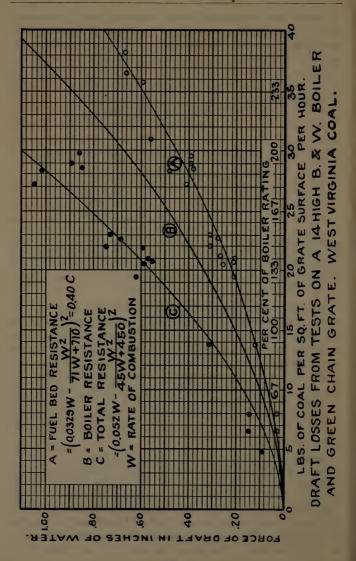
The following table gives some of the commonly accepted values for draft required in the furnace to overcome the resistance of the fuel bed under the different conditions stated:

30 0	Lbs. of Dry Coal Burned per Sq. Ft. of Grate per Hr.						
	15	20	25	30	35	40	45
Eastern bituminous coal Western bituminous coal Semi bituminous coal Anth. buckwheat, No. 1 and	$\begin{array}{c} 0.12 \\ 0.15 \\ 0.15 \\ 0.15 \end{array}$		0.20 0.25 0.28	0.27 0.33 0.37	$0.34 \\ 0.42 \\ 0.48$	$\begin{array}{c} 0.42 \\ 0.52 \\ 0.60 \end{array}$	0.52 0.65 0.80
larger Anth. buckwheat, No. 2 and No. 3	$0.45 \\ 0.75$	$\begin{array}{c} 0.70 \\ 1.30 \end{array}$	1.00		-		

FURNACE DRAFT IN INCHES OF WATER

The diagram on page 84 shows an interesting study of draft losses at different rates of combustion, based on data furnished by Joseph Harrington of the Green Engineering Co. These tests were made on a B. & W. boiler using a Green chain grate, operating at from 50 to 250 per cent. of the rated capacity. The curve "A" shows the resistance of the fuel bed and curve "C" the total resistance of the boiler at the different rates of combustion. It was found from these curves that the fuel bed resistance was 0.4 of the total resistance. The values from curve "A" run a trifle higher than those given for furnace draft in the accompanying table.

Loss of pressure through a boiler will depend in a great measure on the condition of the surfaces in regard to soot, but ordinarily the drop in pressure through a water tube boiler may be taken as 0.25" of water when operating at rated capacity. The loss through horizontal circular or square steel breeching will average about 0.1" per 100 feet of length, and rectangular pipe should not depart far from a square section without increasing this value. The loss of pressure in a brick flue will be



30 per cent. greater than for a steel flue. The loss of draft in an easy right angle bend or elbow will be approximately equal to 0.05" of water. The drop in pressure through an economizer will ordinarily run from 1/4 to 1/2 inch, at rated capacity. Draft intensity of a chimney is proportional to its height.

Draft intensity of a chimney is proportional to its height. For a chimney 100 feet high, with flue gases at 350° above the outside temperature, the draft intensity will average approximately 0.5" of water.

Amount of Air Required

In estimating the amount of air to be supplied, as also the size of fan required, for a forced draft system it is necessary to assume both the rate of combustion and of evaporation for the plant under consideration. These will depend on the size of the plant and the class of equipment installed. The weight of air actually required for the combustion of one pound of coal is approximately 12 pounds, but owing to the fact that it is impossible to perfectly intermingle the air and gases rising from the grate, more air must be provided than is theoretically required. This will vary from 18 to 30 pounds depending on the installation, in the average case between 20 and 25 pounds of air per pound of combustible being allowed.

It is customary practice in selecting apparatus for mechanical draft purposes to allow for 100 per cent. excess air for hand fired boilers, or 16.70 cu. ft. of air per minute at 70° per boiler H. P. for a forced draft fan, and 32.40 cu. ft. per minute at 550° for an induced draft fan. An allowance of 50 per cent. excess air is made where the boiler is equipped with a stoker, or 11.70 cu. ft. per minute at 70° per boiler H. P. for a forced, and 22.80 cu. ft. per minute at 550° for an induced draft fan.

Assuming 20 pounds of air at 70° per pound of coal, and 4.5 pounds coal containing 11450 B. t. u. per pound with a boiler efficiency of 65 per cent. as equivalent to one boiler horsepower, gives 90 pounds of air per hour, or 20 cu. ft. per minute at 70° per boiler horsepower. Then the total horsepower of the boiler multiplied by 20 gives the required capacity of the fan with the air at 70° F. This will be the proper size for a forced draft system, but with induced draft where the fan handles the gases and excess air at flue gas temperature, due allowance must be made for the increased volume to be handled, and a larger fan chosen. A fan for this purpose should be of special design, with bearings protected from the heat of the flue gases handled. There is a definite relation between the analysis of the flue gases passing from the boiler and the quantity of air required or supplied, and, as explained on page 89, the results of the analysis may be used to determine the amount of air or gases being handled by a forced or induced draft system. The method of taking flue gas analysis by means of the Orsat apparatus is quite generally understood, and will be found described in the various standard works on boiler performance.*

A pound of carbon requires for complete combustion 2.67 pounds of oxygen, or a volume of 32.64 cu. ft. at 70° . Considered at 70° , the gaseous product, CO₂, would occupy the same volume as did the oxygen. The volume of the carbon dioxide (CO₂), as also its proportion to the nitrogen, would be the same after combustion as had been the proportions of oxygen and nitrogen originally in the air used. Then the complete combustion of carbon, with no excess of air, would give a volumetric flue gas analysis of

Carbon dioxide.	 $CO_2 = 20.91\%$
Nitrogen	 .N =79.09%

If the supply of air is in excess of that required to supply the oxygen needed, the combined volumes of the carbon dioxide and oxygen are still the same as that of the oxygen before combustion. The action of hydrogen in the coal is to increase the apparent percentage of nitrogen in the flue gases. Thus the sum of the CO_2 and O_2 from flue gas analysis will not be found equal to the theoretical 20.91 per cent., but will approach this amount as the amount of excess air is increased. This is shown by the values given in the table on page 87.

Quantity of air required may be determined approximately by means of the following formula when the ultimate analysis of the fuel is known.

Pounds of air required per pound of fuel

$$= 36.56 \left(\frac{C}{3} + H - \frac{O}{8} \right)$$
(36)

where C, H and O are per cents. by weight of carbon, hydrogen and oxygen in the fuel, divided by 100.

When the proportionate part, by weight, of the carbon in the fuel (C) is known, and also the carbon monoxide (CO), carbon

^{*}Experimental Engineering by R. C. Carpenter. Steam Boiler Economy by Wm. Kent.

iases per r Boiler P.	220 Deg. F.	14.47 17.74 19.37	$\begin{array}{c} 21.10\\ 22.83\\ 24.52\end{array}$	26.38 28.28 30.30	32.40 37.52 42.88	55.85 69.02 87.78
Cu. Ft. Gases p Min. per Boilei H. P.	300 Deg. F.	$\begin{array}{c} 10.89 \\ 13.35 \\ 14.58 \end{array}$	$15.88 \\ 17.18 \\ 18.45$	19.87 21.28 22.80	$\begin{array}{c} 24.39\\ 28.24\\ 32.27\end{array}$	$\begin{array}{c} 42.02\\ 51.94\\ 66.06\end{array}$
	Cu. Ft. Air per l per Boiler H. 70° F.	$7.32 \\ 9.01 \\ 9.85$	10.77 11.68 12.57	13.52 14.53 15.57	$16.68 \\ 19.35 \\ 22.16$	$28.92 \\ 35.81 \\ 45.60$
ur per	Lbs. Gas per Ho Boiler H. P.	35.6 43.4 47.2	51.3 55.4 59.4	$63.8 \\ 68.3 \\ 73.1$	$ \begin{array}{c} 78.1 \\ 90.2 \\ 102.9 \end{array} $	133.6 164.8 209.3
o. nt bet	Lbs. Air per Ho Boiler H. F	32.9 40.5 44.3	48.4 52.5 56.5	60.8 65.3 70.0	$75.0\\87.0\\99.6$	130.0 161.0 205.0
stible r H. P.	Pounds Combu Burned per Boile	$2.74 \\ 2.81 \\ 2.84 $	2.88 2.91 2.94	2.98 3.02 3.07	3.12 3.22 3.32	3.61 3.84 4.28
er Lb.	g səssü sbruoq diysudmoQ	13.0 15.4 16.6	$17.8 \\ 19.0 \\ 20.2 $	21.4 22.6 23.8	$25.0 \\ 28.0 \\ 31.0 $	37.0 43.0 49.0
pəu -moʻʻ	Lbs. Air per Lb. bustible Buri	12.0 14.4 15.6	16.8 18.0 19.2	$20.4 \\ 21.6 \\ 22.8 \\ 22.8 \\ 322.8 \\ $	24.0 27.0 30.0	36.0 42.0 48.0
oiler	Efficiency of B	79.8 77.9 77.0	76.0 75.1 74.2	73.2 72.3 71.3	70.4 68.2 65.8	61.0 56.5 51.6
ss %01	Stack Loss Plus Radiation Lo	20.2 22.1 23.0	24.0 24.9 25.8	26.8 27.7 28.7	29.6 31.8 34.2	39.0 43.5 48.4
ni yay es	Heat Carried As Chimney Gas %	10.2 12.1 13.0	$14.0 \\ 14.9 \\ 15.8 $	16.8 17.7 18.7	$ \begin{array}{c} 19.6 \\ 21.8 \\ 24.2 \\ \end{array} $	29.0 33.5 38.4
ue Gas ysis	Excess Oxygen O2	0 3.6 5.0	6.1 7.1 8.0	8.8 9.5 10.1	10.6 11.8 12.7	14.1 15.1 15.8
From Flue Gas Analysis	Carbon Dioxide CO2 %	18.2 15.1 13.9	12.9 12.0 11.2	10.6 10.0 9.5	9.0 7.9 7.1	5.9 5.1 4.4
	Excess Air %	0 30 30	40 50 60	90 80 80	100 125 150	200 250 300

RELATION OF BOILER EFFICIENCY AND DRAFT REQUIREMENT TO PER CENT. EXCESS AIR WHEN BURNING BITUMINOUS COAL

87

MECHANICAL DRAFT

dioxide (CO₂) and nitrogen (N) in per cent. by volume are determined from the flue gases, the total amount of air supplied may be found from the following formula,

Pounds of air supplied per pound of fue!

$$= 3.032 \left(\frac{\mathrm{N}}{\mathrm{CO}_2 + \mathrm{CO}} \right) \times \mathrm{C} + (1 - \mathrm{A}) \tag{37}$$

where A represents the proportionate part, by weight, of ash in the fuel.

Ratio of air supplied per pound of fuel to the amount theoretically required is

$$\frac{N}{N-3.782 O}$$
(38)

The heat loss in the flue gases is

$$H = 0.24 W (T-t)$$
 (39)

where

H = B. t. u. lost per lb. of fuel.
W = Wt. of flue gas in lb. per lb. fuel.
T = Temperature of flue gas deg. F.
t = Temperature of air deg. F.
0.24 = specific heat of flue gas.

The table on page 87 has been calculated on the basis of burning a good grade of bituminous coal having a combustible containing 87 per cent. carbon and 5.5 per cent. hydrogen. The amount of CO in the flue gas has been considered a negligible quantity, and only the CO₂ and O₂ used in the calculations. This table gives the air required for different dilution coefficients and the air quantities to be allowed for either forced or induced draft work when operating with different amount of excess air. It also gives the per cent. of excess air corresponding to different per cents. of excess oxygen as determined from the flue gas analysis. This may be readily calculated from the formulae on page 89. As explained on page 89 under air measurement, the values in this table give a measure of the air being handled when the flue gas analysis and also either the weight of combustible burned or of water evaporated are known.

On page 87 the column of air quantity at 70° per H. P. would apply to forced draft work; the column headed 300° would apply to the average induced draft conditions where an economizer was in use, while the column headed 550° would be used for induced draft fans handling gases directly from the boiler. These values then indicate the increase in volume of a given weight of air at a constant pressure for the different temperature conditions.

The tables on pages 321 to 330 give the capacity under different conditions, both for standard and for special high efficiency fans when used for induced draft service. The standard Planoidal, Niagara Conoidal and Turbo-Conoidal fan capacity tables in Part IV, Section III, give the required information for forced draft work.

Measurement of Air Used

Amount of air being used by either forced or induced draft systems under different conditions may be determined by either of the three following methods:

1—Pitot tube readings in the breeching or forced draft connection.

2-By weighing the coal and ash and taking the flue gas analysis.

3—Approximately by weighing the water and taking the flue gas analysis, in case of a boiler with a good setting.

The theory and method of using the pitot tube will be found fully given on page 190 under "Fan Testing" and need not be repeated here. If intelligently used this instrument has proven itself to be a simple and accurate method of measuring air or gases. It may be used alone or as a check on either of the other two methods mentioned, and in the case of a forced draft system any difference between determinations made by the pitot tube and from the flue gas analysis would be an indication of air leakage through the boiler setting.

Amount of air used in per cent. of that theoretically required may be determined from the proportions of excess oxygen and carbon dioxide as indicated by the flue gas analysis. The relation between these three factors may be expressed by the following formulae, where $O_2 = \text{excess}$ oxygen and $CO_2 = \text{carbon}$ dioxide from the flue gas analysis, and K = per cent. of excess air being used.

$$\mathbf{K} = \frac{96.6 \ \mathrm{O}_2}{20.9 - \mathrm{O}_2} \tag{40}$$

$$K = \frac{1760}{CO_2} - 96.6 \tag{41}$$

Theoretical amount of O_2 or CO_2 in the flue gas for any per cent. of excess air may be found from the following:

$O_2 = \frac{\frac{20.9 \frac{K}{100}}{0.966 + \frac{K}{100}}}{0.966 + \frac{K}{100}}$	(42)
$CO_2 = \frac{17.60}{K}$	(43)

$$0.966 + \frac{100}{100}$$

Since it requires approximately 12 pounds of air to burn one pound of combustible, in case K as derived from the formulae shows 100 per cent. excess air, we would know at once that 24 pounds of air were being supplied for each pound of combustible burned, or that 25 pounds of gases were being handled if an induced draft system was installed. The table on page 87 gives the pounds of air required per pound of combustible burned for different amounts of excess oxygen in the flue gas.

The table just referred to also shows the cubic feet of air and of chimney gases per boiler H. P. for the different flue gas analyses. Thus we see that if the H. P. developed is known from the weight of water evaporated, the flue gas analysis gives an indication of the amount of air used. Any determinations of this character are subject to corrections on account of varying amounts of leakage through the boiler setting.

Mechanical Draft in Connection with Mechanical Stokers

Mechanical draft may be used in connection with boilers fitted with automatic stokers as readily as with hand fired installations. With some forms of stokers either forced or induced draft may be used while others are only adapted to forced draft, or in some special instances to some form of steam jet blower.

The manufacturers of the Parsons Mechanical Stoker ordinarily install a steam jet blower in connection with their apparatus, although if conditions will permit, forced draft by means of a fan may be used. Their practice is to allow for maximum conditions a pressure in the ash pit of $2\frac{34}{4}$ inches for anthracite, $1\frac{14}{4}$ inches for bituminous coking coals, and 1 inch for noncoking coals. The damper regulators are ordinarily so adjusted as to give a maximum indraft if 0.05 of an inch over the fire, or a condition of minimum inflow at the fire doors or corresponding parts. In special double deck boilers this may be increased to 0.15 of an inch. Forced draft is used in connection with the Jones underfeed stoker system, sufficient pressure being maintained to force the air required for combustion into the air chamber and practically to the top of the fuel bed. The stack is then depended upon to produce the necessary furnace draft and to overcome the resistance through the boiler. To meet the maximum requirements it is customary to provide for supplying 200 cu. ft. of air per pound of coal at a pressure of not less than two ounces in the air chamber. For approximating the probable coal consumption the company's engineers ordinarily assume five pounds of coal per horsepower which will provide a sufficiently large factor of safety and allow for some reserve power. This allows 16.67 cu. ft. of air per minute per boiler horsepower.

Forced draft is used in connection with the Taylor stoker, giving a very wide range of over capacity to the boiler. The pressure required in the tuyere chamber may vary from one to six inches of water according to the conditions and capacity developed. Recent tests on a well known installation of Taylor stokers, with the boilers using an average of approximately 35 per cent. excess air, required the following pressures in inches of water in the tuyere chamber for the corresponding per cent. of rated boiler capacity.

Per Cent. of Rated Boiler Capacity	Air Pressure in Tuyere Chamber
100	1.10 in.
125	1.70 in.
150	2.50 in.
175	3.40 in.
200	4.50 in.

TAYLOR STOKERS

The Murphy automatic smokeless furnace may be used with either forced or induced draft, giving an overload capacity to the boiler. As an instance of this a test on 500 H. P. of watertube boilers may be cited in which a maximum natural draft of 0.45 inch to 0.50 inch above the fire gave a capacity of about 115 to 120 per cent. above normal rating. With a pressure of from $\frac{34}{4}$ inch to 1 inch under the fire the draft suction above the fire was reduced to about 1 to 2 hundredths of an inch and the capacity raised to 200 per cent. above the rating.

Draft requirements in connection with the various chain grates, such as the Green or the B. & W. will not differ materially from each other, or from a stationary grate if it is kept clean and free from clinker, and an interesting study of results obtained from such an installation will be found on page 84. This data was furnished by Joseph Harrington, Chief Engineer of the Green Engineering Company, based on actual tests under the conditions stated. While no one set of curves will give the draft losses for all the various kinds of coal or all the different types of boilers, yet a diagram such as the one referred to is of especial value inasmuch as it gives a basis for a comparative study of other conditions.



Niagara Conoidal Type "N" Fan Direct Connected to Buffalo Double Vertical, Double-Acting Engine

SECTION V EXHAUST SYSTEMS

An extensive field has been developed for the use of exhaust fans of more or less special design, for the removal of refuse and industrial waste in shops and factories, as well as removing the heated or foul air, or gases, resulting from various industrial processes. Such an exhaust system consists of the proper hood or receptacle at the receiving end, the necessary piping to connect to the exhaust fan, and if refuse is handled, some form of dust or refuse collector. In laying out an exhaust or conveying system the usual method of procedure is to determine: (1) the number and size of branch pipes necessary to properly do the work; (2) the design and arrangement of piping to give the best results with the least power consumption; (3) the size and most economical type of exhaust fan, and (4) the disposition of refuse.

Size of Pipe

Proper size of piping required is for the most part a matter of experience, although practice has established standards for the more common applications. The tables on page 94 give the usual sizes of galvanized iron piping to attach to the hoods of the machines indicated. For branch pipes over 25 feet long increase the size 10 per cent. for each additional 20 feet.

Hood Construction

It is almost impossible to give standard practice in hood construction, since there is such a variety of makes and sizes of machines as to obviate the possibility of having any standard design. Furthermore, a hood must be constructed to suit the character of the work to be done. In designing hoods, a principle to keep in mind is to so shape them that the refuse from knives or wheels, due to their centrifugal action, is thrown directly to a point where it will be caught by the highest velocity of air. Hoods should always be made to fit as tight and close as possible, since the suction effect is lost, resulting in poor operation, if this feature is disregarded.

	No. of Pipes	Size of Pipes		No. of Pipes	Size of Pipes
Cut-off Saws, 10-16 inch diameter 18-24 inch diameter Rip Saws and Re-Saws, 10-16 inch diameter 18-24 inch diameter 24-60 inch diameter Band Saws, small Buzz Planer Pony Planer Diagonal Planeer		4 5 4 5 6 3 4-7 4-7 4-7	Matcher Heads, each Moulder Sash and Cabinet Shaper Door Tenoner. Sash Tenoner Sticker, each head. Panel Raiser, each head. Mortiser. Router. Jointer. Jointer. Sand Drum, 24 inch long	1 4 1 1 1 1 1 1 1	5 4-7 4 5 4 4 4 4 4 4 4 4 4 -7 4
Four Sided Planer Bull Planer Planer and Matcher	$4 \\ 2 \\ 4$	4-7 4-7 4-7	Sand Drum, 30 inch long. Sand Belt Floor Sweeps	1	5 4 6

PIPE SIZES FOR WOODWORKING MACHINES

Sizes of pipes for planers, moulders and similar machines with knives or saws.

UPPER I	KNIVES	LOWER KNIVES			
Length, Inches Size of Pipe, Inches		Length, Inches	Size of Pipe, Inches		
			4 5 5 6 7		

For planers handling timber the pipe sizes must be increased 25 per cent. High speed planers and matchers require about 50 per cent. more area than indicated in the above table.

PIPE SIZES FOR EMERY WHEEL EXHAUST SYSTEMS

Diameter of	Size of Pipe,	Diameter of	Size of Pipe,	
Wheel, Inches	Inches	Wheel, Inches	Inches	
36	7	20	4 ½	
30	6	16	4	
26	5	12	3 ½	

For the removal of smoke or fumes it is good practice to make the mouth of the hood extend out over the kettle or furnace at least six inches in every direction, if the hood is not elevated over two feet. For every additional two feet elevation, the size of the hood should be increased six inches each way. The area of the branch pipe should then be made one-sixteenth of the hood mouth. For instance, a furnace 2×4 feet in size, having the bottom of the hood four feet above it, would have a hood 4 ft. x 6 ft. and the area of the pipe should be one-sixteenth of this, or 1.5 sq. ft. This branch should therefore be 17 inches in diameter. The velocity at the mouth for average conditions should be 75 to 250 feet per minute.

In some manufacturing processes it will be found necessary to provide some means for the removal of poisonous and noxious gases that will be more certain in its action than is the common form of open hood or canopy. This can be accomplished by the use of a double hood with about an inch or less of clearance between the edges of the outside and inside hoods. There should also be an opening in the top of the inner hood, located under the exhaust pipes. These openings should be of such a size that a velocity of about 1000 feet per minute will be created through the slot, around the edge and through the central opening.

Size of Main Pipe

It is the common practice in blow-pipe construction to add the area of the branch pipes and make the area of the main pipe equal to their sum. This process should be continued back to the fan, choosing a fan with an inlet equal to or greater in area than the main pipe.

Velocity Required

The subject of the proper velocity of the air throughout the system is an important one, and while sufficient velocity should be provided to insure the removal of the material being handled, any excess means an unnecessary increase in power consumption. It must be borne in mind that the power required increases as the cube of the speed or velocity, hence to double the velocity will require eight times the horsepower.

In planing-mill work, it is customary to allow a velocity of 2400 for light shavings, 3000 for dry saw dust, and from 3600 to 4000 for knots, blocks, etc. This corresponds to operating the exhaust fan at a speed to give approximately $2\frac{1}{2}$ to 5 ounces

of pressure, depending upon the length of the piping and the velocity required. The velocity in the piping should either be uniform throughout the entire system, or else higher in the branches than in the main pipe.

Dust Removal from Grinding and Buffing Wheels

Specifications for the design, construction and operation of exhaust systems for grinding, polishing and buffing wheels to comply with the Labor Law of New York State, have been prepared by William Newell, of the Department of Labor, as follows: Accompanying the specifications are certain recommendations by The Buffalo Forge Company on the design of these systems.

1. Minimum size of branch pipes allowed for different sized emery or other grinding wheels are given in the accompanying table. In case a wheel is thicker than given in the tabulation, or if a disc instead of a regular wheel is used, it must have a branch pipe no smaller than is called for by its grinding surface.

GRINDING WHEELS

Diameter of Wheels	Maximum Grinding Surface, Sq. Ins.	Minimum Diameter of Branch Pipe in Inches		
6" or less, not over 1" thick 7" to 9" inclusive, not over 1 ½" thick 10" to 16" inclusive, not over 2" thick 17" to 19" inclusive, not over 3" thick 20" to 24" inclusive, not over 4" thick 25" to 30" inclusive, not over 5" thick	19 43 101 180 302 472	$ \begin{array}{r} 3 \\ 3 \\ 4 \\ 4 \\ 5 \\ 6 \end{array} $		

BUFFING WHEELS

Diameter of Wheels	Maximum Grinding Surface, Sq. Ins.	Minimum Diameter of Branch Pipes in Inches	
6'' or less, not over 1" thick $7''$ to $12''$ inclusive, not over $1\frac{1}{2}''$ thick	19 57	3 ½ 4	
13" to 16" inclusive, not over 2" thick 17" to 20" inclusive, not over 3" thick 21" to 24" inclusive, not over 4" thick 25" to 30" inclusive, not over 5" thick	$ 101 \\ 189 \\ 302 \\ 472 $	$4\frac{1}{2}$ 5 5 $\frac{1}{2}$	

2. Minimum sizes of branch pipes allowed for different sized buffing, polishing, or rag wheels, as they are variously called, are given in the table.

Buffing wheels six inches or less in diameter used for jewelry work may have a three-inch branch pipe.

The thickness given for buffing wheels applies to the thickness of the wheel at the center. In case the wheel is thicker than given in the tabulation, it must have a branch pipe no smaller than is called for by its grinding surface.

3. Branch pipes must not be less than the sizes specified above throughout their entire length.

4. All branch pipes must enter the main suction duct at an angle not exceeding 45°, and must incline in the direction of the air flow at junction with main.

5. Branch pipes must not project into the main duct.

6. All laps in piping must be made in the direction of the air flow.

7. All bends, turns, or elbows, whether in the main or branch pipes, must be made with a radius in the throat at least equal to $1\frac{1}{2}$ times the diameter of the pipe on which they are connected.

8. The inlet of the fan or exhauster shall be at least 20 per cent. greater in area than the sum of the areas of all the branch pipes, and such increase shall be carried proportionately throughout the entire length of the main suction duct, i. e., the area of the main at any point shall be at least 20 per cent. greater than the combined areas of the branch pipes entering it between such point and the tail end or dead end of the system.

For the convenience of those wishing to use it, the table on page 98 is given, showing what the size of the main suction duct should be at any point for any number of uniform-size branch pipes when the main duct is made 20 per cent. greater than the combined areas of the branches entering it,—the minimum required by these specifications.

9. The area of the discharge pipe from the fan shall be as large or larger than the area of the fan inlet throughout its entire length.

10. The main trunk lines, both suction and discharge, shall be provided with suitable clean-out doors not over ten fect apart, and the end of the main suction duct shall be blanked off with a removable cap placed on the end.

PROPORTIONS OF MAIN DUCT TO ACCOMMODATE BRANCHES

	Diameter of Branch Pipes in Inches									
	3	3 1/2	4	4 1⁄2	5	5 1/2	6	6 1/2	7	
Pipes	Area of Each Branch Pipe in Square Inches									
ranch	7.07	9.62	12.566	15.9	19.635	23.758	28.274	33.183	38.485	
Number of Branch Pipes	Area of Each Branch Pipe Plus 20% (Square Inches)									
Numb	8.484	11.544	15.08	19.08	23.562	28.51	33.93	39.82	46.182	
1 2 3	$3\frac{3}{8}\\4\frac{3}{4}\\5\frac{3}{4}$	$\begin{array}{r} 3 & 7/8 \\ 5 & 1/2 \\ 6 & 5/8 \end{array}$	$ \begin{array}{r} 4 \frac{3}{8} \\ 6 \frac{1}{4} \\ 7 \frac{5}{8} \end{array} $	5 7 8 ⁵ /8	$ 5 \frac{1}{2} \\ 7 \frac{3}{4} \\ 9 \frac{1}{2} $	$\begin{array}{r} 6 \\ 8\frac{5}{8} \\ 10\frac{1}{2} \end{array}$	$\begin{array}{r} 6\frac{5}{8}\\ 9\frac{1}{4}\\ 11\frac{1}{2} \end{array}$	$7\frac{1}{8}\\10\frac{1}{8}\\12\frac{3}{8}$	7 ³ / ₄ 10 ⁷ / ₈ 13 ¹ / ₄	
4 5 6	6 5/8 7 3/8 8 1/3	7 ³ ⁄ ₄ 8 ⁵ ⁄ ₈ 9 ¹ ⁄ ₂	$\begin{array}{r} 8 \frac{3}{4} \\ 9 \frac{7}{8} \\ 10 \frac{3}{4} \end{array}$	$9\frac{7}{8}\\11\\12\frac{1}{8}$	$11 \\ 12\frac{1}{4} \\ 13\frac{1}{2}$	${\begin{array}{*{20}c} 12\frac{1}{8}\\ 13\frac{1}{2}\\ 14\frac{3}{4}\end{array}}$	$13\frac{1}{8}\\14\frac{3}{4}\\16\frac{1}{8}$	$14\frac{1}{14}$ 16 17\frac{1}{2}	$15\frac{3}{8}\\17\frac{1}{8}\\18\frac{3}{4}$	
7 8 9	8 3/4 9 3/8 9 7/8	$10\frac{1}{14}\\10\frac{7}{8}\\11\frac{1}{2}$	${\begin{array}{*{20}c} 11 & {}^{5}\!\!/_8 \\ 12 & {}^{3}\!\!/_8 \\ 13 & {}^{1}\!\!/_8 \end{array}}$	$13\frac{1}{8}\\14\\14\frac{1}{14}\frac{7}{8}$	$\begin{array}{c} 14 \frac{1}{2} \\ 15 \frac{1}{2} \\ 16 \frac{1}{2} \end{array}$	$16 \\ 17\frac{1}{8} \\ 18\frac{1}{8}$	$17\frac{1}{2}\\18\frac{5}{8}\\19\frac{3}{4}$	${}^{18\frac{7}{8}}_{20\frac{1}{8}}_{21\frac{3}{8}}$	$20\frac{1}{4}$ $21\frac{3}{4}$ 23	
10 11 12	$10\frac{1}{2}$ 11 11\frac{1}{2}	${\begin{array}{*{20}c} 12 \frac{1}{8} \\ 12 \frac{3}{4} \\ 13 \frac{3}{8} \end{array}}$	$13 \frac{7}{8} \\ 14 \frac{5}{8} \\ 15 \frac{1}{4}$	${\begin{array}{*{20}c} 15 {}^{5}\!\!\!/8 \\ 16 {}^{3}\!\!\!/8 \\ 17 {}^{1}\!\!\!/8 \end{array}}$	$17\frac{3}{8}$ $18\frac{1}{4}$ 19	19½ 20 20⅔	$\begin{array}{c} 20\frac{3}{4} \\ 21\frac{7}{8} \\ 22\frac{3}{4} \end{array}$	$22\frac{1}{2}\\23\frac{5}{8}\\24\frac{3}{4}$	$24 \frac{1}{4} \\ 25 \frac{1}{2} \\ 26 \frac{5}{8}$	
13 14 15	${}^{11\frac{7}{8}}_{12\frac{3}{8}}_{12\frac{3}{4}}$	$13\frac{7}{8}\\14\frac{3}{8}\\14\frac{7}{8}$	$15\frac{7}{8}$ $16\frac{1}{2}$ 17	$17\frac{7}{8}\\18\frac{1}{2}\\19\frac{1}{8}$	$\begin{array}{c} 19\frac{3}{4} \\ 20\frac{1}{2} \\ 21\frac{1}{4} \end{array}$	$\begin{array}{c} 21\frac{3}{4} \\ 22\frac{5}{8} \\ 23\frac{3}{8} \end{array}$	$\begin{array}{c} 23\frac{3}{4} \\ 24\frac{5}{8} \\ 25\frac{1}{2} \end{array}$	$25\frac{3}{4}$ $26\frac{3}{4}$ $27\frac{5}{8}$	$27\frac{3}{4}\\28\frac{3}{4}\\29\frac{3}{4}$	
16 17 18	$13\frac{1}{4}$ $13\frac{5}{8}$ 14	$15\frac{3}{8}$ $15\frac{7}{8}$ $16\frac{3}{8}$	${ { 175/8 \atop {181/8} \atop {185/8} \atop {185/8} } } $	$19\frac{3}{4}\\20\frac{3}{8}\\21$	$\begin{array}{c} 22 \\ 22 \frac{5}{3} \\ 23 \frac{1}{4} \end{array}$	$24\frac{1}{8}\\24\frac{7}{8}\\25\frac{5}{8}$	$\begin{array}{c} 26\frac{3}{8} \\ 27\frac{1}{8} \\ 27\frac{1}{8} \\ 27\frac{7}{8} \end{array}$	$28\frac{1}{2}\\29\frac{3}{8}\\30\frac{1}{4}$	$\begin{array}{c} 30\frac{3}{4}\\ 31\frac{5}{8}\\ 32\frac{5}{8}\end{array}$	
19 20 21	${}^{14\frac{3}{8}}_{14\frac{3}{4}}_{15\frac{1}{8}}$	$16\frac{3}{4}\\17\frac{1}{8}\\17\frac{5}{8}$	$19\frac{1}{8}\\19\frac{5}{8}\\20\frac{1}{8}$	$21\frac{1}{22}$ $22\frac{1}{8}$ $22\frac{5}{8}$	$\begin{array}{c} 23\frac{7}{8} \\ 24\frac{1}{2} \\ 25\frac{1}{8} \end{array}$	$26\frac{1}{4}\\27\\27\frac{5}{8}$	$\begin{array}{c} 28\frac{3}{4} \\ 29\frac{1}{2} \\ 30\frac{1}{8} \end{array}$	$\begin{array}{c} 31 \frac{1}{8} \\ 31 \frac{7}{8} \\ 32 \frac{3}{4} \end{array}$	$\begin{array}{r} 33 \frac{1}{2} \\ 34 \frac{3}{8} \\ 35 \frac{1}{8} \end{array}$	
22 23 24	${\begin{array}{*{20}c} 15 \frac{1}{2} \\ 15 \frac{3}{4} \\ 16 \frac{1}{8} \end{array}}$	$18\\18\frac{1}{2}\\18\frac{1}{2}\\18\frac{7}{8}$	$\begin{array}{c} 20 \ {}^{5\!/8}_{8} \\ 21 \ {}^{1\!/8}_{1} \\ 21 \ {}^{1\!/2}_{2} \end{array}$	$23{}^{1/_8}_{23}^{3/_4}_{24}^{1/_4}$	$25\frac{3}{4}\\26\frac{3}{8}\\26\frac{7}{8}$	28 ³ ⁄ ₈ 29 29 ⁵ ⁄ ₈	$\begin{array}{c} 30\frac{7}{8} \\ 31\frac{1}{2} \\ 32\frac{1}{4} \end{array}$	$33\frac{1}{2}\\34\frac{1}{4}\\34\frac{7}{8}$	$36 \\ 36 \\ 34 \\ 37 \\ 5/8$	
25 26 27	$16\frac{1}{2}$ $16\frac{3}{4}$ $17\frac{1}{8}$	$19\frac{1}{4}\\19\frac{5}{8}\\20$	$22 \\ 22 \\ 22 \\ 3/8 \\ 22 \\ 7/8 \\ 3$	$24\frac{3}{4}\\25\frac{1}{8}\\25\frac{5}{8}$	$27\frac{1}{2}$ 28 28 $\frac{1}{2}$	$\begin{array}{c} 30 \frac{1}{8} \\ 30 \frac{3}{4} \\ 31 \frac{3}{8} \end{array}$	$\begin{array}{r} 32\frac{7}{8}\\ 33\frac{1}{2}\\ 34\frac{1}{8} \end{array}$	$35\frac{5}{8}$ $36\frac{3}{8}$ 37	$38\frac{3}{8}$ $39\frac{1}{8}$ $39\frac{7}{8}$	
28 29 30	$17\frac{1}{2}$ $17\frac{3}{4}$ 18	$20\frac{3}{3}$ $20\frac{3}{4}$ 21	$23 \frac{1}{4} \\ 23 \frac{5}{8} \\ 24$	$26\frac{1}{8}$ $26\frac{5}{8}$ 27	$29 \\ 29 \frac{1}{2} \\ 30$	$32 \\ 32 \frac{1}{2} \\ 33 $	$34\frac{3}{4}$ $35\frac{1}{2}$ 36	$37\frac{3}{4}$ $38\frac{3}{8}$ 39	40 5/8 41 3/8 42	

11. Sufficient static suction head shall be maintained in each branch pipe within one foot of the hood to produce a difference in level of two inches of water between the two sides of a U-shaped tube. Test is to be made by placing one end of a rubber tube over the small hole made in the pipe, the other end of the tube being connected to one side of a U-shaped water gauge. Test is to be made with all branch pipes open and unobstructed.

In addition to the foregoing specifications, which are compulsory, a number of "Recommendations" are given below, which, if observed, will make for still more efficient operation and longer life of the system.

Recommendations

1. Emery wheel and buffing wheel exhaust systems should be kept separate owing to danger of sparks from the former setting fire to the lint dust from the latter, if both are drawn into the same suction main.

2. In the case of undershot wheels, i. e., the top of the wheel runs toward the operator, which is almost always the direction of rotation of both emery and buffing wheels, the main suction duct should be back of and below the wheels and as close to them as is practicable; or it should be fastened to the ceiling or the floor below, preferably the former. If behind the wheels, it should be not less than six inches above the floor at every point to avoid possible charring of the floor in case of fire in the main duct and also to permit sweeping under it. For similar reasons it should be at least six inches below any ceiling it may run under.

3. Both the main suction and discharge pipes should be made as short and with as few bends as possible, to avoid loss by friction. If one or the other must be of considerable length, it is best to place the fan not far beyond where the nearest branch enters the large end of the main, as a long discharge main is a lesser evil than a long suction main.

4. Avoid any pockets or low places in ducts where dust might accumulate.

5. The main suction duct should be enlarged between every branch pipe entering it, whenever space permits, and in no case should the main duct receive more than two branches in a section of uniform area. All enlargements in the size of the main should be made on a taper and not by an abrupt change.

6. If there is a likelihood of a few additional wheels being installed in the future, it is advisable to leave a space for them between the fan and the first branch and to put in an extra size fan. Or, a space may be left beyond the fan so that the fan may be moved along and the main extended when it is actually decided to install additional wheels, provided the fan is of sufficient size to still comply with these specifications after the additional branches are added.

7. Branch pipes should enter the main on the top or sides —never at the bottom. Two branches should never enter a main directly opposite one another.

8. Each branch pipe should be equipped with a shut-off damper or blast-gate as it is also called, which may be closed, if desirable, when the wheel is not in use. Not more than 25 per cent. of such blast-gates should be closed at one time; otherwise, the air velocity in the main duct may drop too low and let the dust accumulate on the bottom.

9. It is very important that the lower part of the hood shall come far enough forward beneath the front of the wheel so that the dust will enter the hood and not fall outside of it altogether, even if the accomplishment of this result necessitates leavin; considerable space between the wheel and the lower part of the hood in order that the hood shall not interfere with the work.

10. Branch pipes should lead out of the hood as nearly as possible at the point where the dust will naturally be thrown into them by the wheels. This is very important.

11. An objectionable practice sometimes found where small work is polished is the use of a screen across the mouth of the branch pipe where it enters the hood. Such screens are an obstruction to the passage of material, and the ravelings from buffing wheels are held against the screen by the suction, with the result that in a short time the draft is almost entirely cut off.

12. The use of a trap at the junction of the hood and branch pipe is good practice provided it is cleaned out regularly and not allowed to fill up with dust. This will catch the heavier particles and so take some wear off the fan. It will also serve to catch any nuts, pieces of tripoli, etc., dropped by accident, and in the case of work on small articles, will enable them to be recovered when dropped in the hood.

13. All bends, turns, or elbows, whether in the main or branch pipes, should be made with a radius in the throat of twice the diameter of the pipe on which they are connected, wherever space permits.

14. Elbows should be made of metal one or two gauges heavier than the pipe on which they are connected as the wear on them is much greater.

15. The withdrawal of air from a room by an exhaust system naturally tends to create a slight vacuum and for this reason inlets for air at least equal to the sum of the areas of the branch pipes should be left open.

16. Recommendations for the size of the cyclone separator or dust collector, as it is often called, are hard to give, as the separator must be proportioned to suit operating conditions, light dusts requiring a larger separator than heavier dusts. A separator should be selected with an inlet area at least as large as the area of the discharge pipe from the fan.

For light buffing dusts, lint, etc., the air outlet from the top of the separator should be so large that the velocity of discharge will not exceed 300 to 480 feet per minute; then select a separator of which the other dimensions are proportionate. The air outlet should be provided with a proper canopy or elbow to exclude the weather, but should be otherwise unobstructed.

Diam.	Diam.	Dust Outlet	Diam.	Total	Diam.	Diam.	Diam.	Diam.	Total
Inkt	Air Outlet		Collector	Height	Inlet	Air Outlet	Dust Outlet	Collector	Height
6	12	6	24	40	28	56	14	112	175
8	16	7	32	52	30	60	15	120	187
10	20	8	40	64	32	64	16	128	200
12	24	8	48	76	34	68	17	136	212
14	28	8	56	89	36	72	18	144	224
16	32	8	64	101	38	76	19	152	236
18	36	9	72	$ \begin{array}{r} 114 \\ 126 \\ 139 \end{array} $	40	80	20	160	248
20	40	10	80		42	84	21	168	260
22	44	11	88		44	88	22	176	272
24	48	12	96	$\begin{array}{c}151\\163\end{array}$	46	92	23	184	284
26	52	13	104		48	96	24	192	296

DIMENSIONS OF DUST COLLECTORS

Dust Collectors

The air with its contents of shavings and dust should be delivered by the fan into a separator or collector. Whatever heavy matter the air carries here settles to the bottom and is discharged into the proper receptacle, leaving the air to escape to the atmosphere. As usually built they depend on the centrifugal action to accomplish the separation. While the different makes will vary in their dimensions, the table on page 101 will serve to give a general idea of the sizes used. These are built either right or left hand.

A properly designed separator should not cause a resistance of more than one velocity head due to the flow. That is, with a velocity of 4000 feet per minute the resistance would be one inch.

Friction Loss

A complete discussion on the loss in pressure due to friction of the air passing through the piping and elbows will be found on pages 115 to 120. For perfectly smooth piping we may consider that one velocity head, or a pressure corresponding to the velocity, is lost in every 60 diameters of pipes, but for planingmill work it is customary to use a factor of 55 diameters. That is, with a velocity through the pipes of 4000 feet per minute, which corresponds to a pressure or velocity head of one inch, there would be one inch of pressure lost in every 55 diameters. With a pipe 18 inches in diameter, one velocity head would be lost in each 83 feet of length. The fan must operate at a total pressure sufficient to care for all of the losses, and still leave a pressure corresponding to the velocity desired. For the loss in elbows see the diagrams on pages 118 and 119.

Standard and Slow Speed Planing-Mill Exhausters

For conveying refuse from wood working machines and carrying off factory waste of similar nature, fans with steel plate housings and overhung blast wheels are usually employed. These fans are of heavier construction than those used for ventilating, and are built double as well as single for use where a double fan avoids unnecessary length of piping and elbows. A description of these fans and capacity tables will be found in Part IV, Section III. In the ordinary planing-mill the refuse is sufficient to furnish fuel for heating and power. The standard type fan is designed for large capacity, rather than for high efficiency, so wherever it is necessary to buy fuel, a more efficient fan should be used, and proper design makes it possible to combine the features of high efficiency and slow speed. The most efficient type of slow speed planing-mill exhauster has a housing which is very large and narrow in proportion to the size of inlet and outlet connections, and will reduce the power at least 15 per cent. while operating at about two-thirds the speed of the standard fan. Dimension and capacity tables of these fans will be found in Part IV, Section III.

Primarily, the speed of the fan depends upon the suction or vacuum to be maintained at the hoods. To move shavings and saw dust, a velocity in the piping system of from 3000 to 4000 feet per minute is the average requirement, which corresponds approximately to $1\frac{1}{3}$ to 2 inches suction in the pipe near the hood inlets, and a velocity head in the piping of from 0.6 to 1.0 inch. In addition to maintaining this suction at the hoods, the operating pressure at the fan must be sufficient to overcome the friction losses of the system. Piping friction losses, plus collector loss, plus intake and discharge losses, therefore equals the necessary operating pressure of the exhauster.

Examples. As an example, take a planing-mill installation having three 7-inch branch pipes, three 6-inch branch pipes, two 5-inch branch pipes and one 4-inch branch pipe. Assume that the longest run of piping on the suction side of the fan is 57 feet, that there are three right angle elbows in the same (radius of elbows $1\frac{1}{2}$ diameters), and that the fan discharges its refuse into a collector located 60 feet from the fan, with one right angle elbow in this pipe.

Adding the areas of branch pipes, the diameter of the main suction pipe will be 18 inches. Referring to the data on friction losses on page 102 the loss in 55 diameters of pipe equals one velocity head.

57 feet of suction and 60 feet of discharge piping $(1\frac{1}{2})$ foot diameter) is equivalent to

 $\frac{57+60}{1\frac{1}{2}} = 78$ diameters

Referring to the curve of friction loss in round elbows on page 118 it will be seen that the loss in each of the four elbows will be 0.17 of a velocity head. For a perfectly smooth well built system this would mean each elbow was equivalent in friction to 9.5 diameters of pipe, but it is the general custom to allow ten diameters to each elbow. We will then have the four elbows equal to 40 diameters, in addition to the 78 diameters of piping. Allowing the customary 55 diameters as equal to one velocity head lost we have as the loss in the piping and elbows

 $\frac{78 + 40}{55} = 2.15$ velocity heads.

Intake and discharge loss = 1.5 velocity heads.

Loss in refuse collector = 1 velocity head.

Pressure due to the velocity = 1 velocity head.

Total operating head = 5.65 velocity heads.

Assume 4000 feet velocity required, which corresponds to a pressure of one inch or 0.5768 ounces per square inch.

The necessary operating pressure of exhauster will then be $5.65 \times 0.5768 = 3.25$ ounces.

From the dimension and capacity tables, an exhauster having an 18-inch inlet, or the 45-inch size should be used. If a slow speed exhauster were chosen we would find from the table on page 345 that for 3 oz. pressure the necessary speed would be 742 R. P. M., the capacity 6620 cu. ft. per minute and the power required 8.97 H. P. But as the pressure required is 3.25 oz. the accompanying conditions must be calculated from the above factors. That is,

the speed will be $742\sqrt{\frac{3.25}{3.00}} = 770$ R. P. M.

the capacity will be $6620\sqrt{\frac{3.25}{3.00}}=6880$ cu. ft. per min.

and the power will be
$$8.97 \sqrt{\left(\frac{3.25}{3.00}\right)^3} = 10.10$$
 H. P.

If a standard exhauster is used the speed will be 1245 R.P. M.; the capacity the same as above; and the power 12.15 H. P. The power as stated would be maximum, that is, the amount required when all the branch pipes are open. In pattern shops, all of the machines are seldom used at once, which means that less air is handled, with resultant reduction in power.

The capacity tables on pages 343 and 346 which have been compiled with velocity as a basis, will be found more convenient in computing speed and powers than the above method and for most installations will be sufficiently accurate. Assuming the same conditions as in the preceding problem, an example of their use follows:

Length of suction and discharge pipe, 117 feet.

Length of pipe equivalent to four elbows equals

 $4 \times 10 = 40$ diameters.

40 diameters $\times 1\frac{1}{2} = 60$ feet.

Length of pipe equivalent to collector equals one velocity head or 55 diameters.

55 diameters $\times 1\frac{1}{2} = 83$ feet.

Total equivalent length = 260 feet.

The tables are based on an assumption that the system will contain an equivalent of 275 feet of piping, and corrections for 15 feet will be necessary. For each 10 feet difference, the speed must be decreased one per cent., or 1.5 per cent. in this instance, and the power three per cent., or $3 \times 1.5 = 4.5$ per cent.

From tables, pages 343 and 346, the following is obtained:

Slow speed exhauster—Speed 790 less $1\frac{1}{2}\%$ =778 R. P. M. Power 11.1 less $4\frac{1}{2}\%$ =10.60 H. P.

Standard exhauster—Speed 1295 less $1\frac{1}{2}\% = 1275$ R. P. M. Power 13.3 less $4\frac{1}{2}\% = 12.70$ H. P.

SECTION VI MISCELLANEOUS APPLICATIONS

Fans are used for a great variety of purposes, many of which have special engineering features which make it impossible to lay down any easily applied rules for their installation. Even where a standard fan is to be used, a full knowledge of all of the features of the case are necessary before making a selection.

One large field for the use of fans, propellors and disk wheels is in connection with drying and cooling work, a brief discussion of which is given in the following pages. Fans and blowers are used for many purposes requiring air under considerable pressure, such as foundry and furnace service; blast supply for forges; for sand blast machines, pneumatic tube installations, mine ventilation, tunnel work, in glass factories, and many other special applications.

For forge service either the volume blowers listed in the table on page 335 may be used, or the pressure blowers already mentioned, depending on the conditions. For exhausting the smoke and gases from forges a pressure of from one to two ounces is required. The blast is usually run at three to six ounces pressure. Piping should be properly proportioned to allow for friction.

Special blowers and exhausters, either low or high pressure, are built for handling gas at gas works, or for removing acid or other chemical fumes. These latter may be made of special acid-resisting metals. For gas works the low pressure exhausters range in capacity from 30,000 to 1,500,000 cubic feet per hour at a pressure up to 15 inches of water. High pressure exhausters range in capacities from 30,000 to 3,000,000 cubic feet of air.

In connection with blast furnaces a special gas cleaning fan is used, in which the inner surface is kept wet by sprays. The centrifugal force throws the dust particles against the water covered surface of the interior of the fan, so cleansing the gas. In the case of gas producers the same form of fan, or gas scrubber, is used to remove the tar from the gas.

Forge Shop Equipment

Table on page 107 gives sizes of blast and exhaust fans for School Forge Shops and table on page 108 sizes of blast and exhaust tile.

ENI	Forge Shops
P EQUIPMEN	for School
FORGE SHOL	Required
0-	of Fans
	Sizes

H. P. 0.340.765.78 6.99 6.99 8.30 8.30 8.30 8.30 8.30 11.3 Exhaust Fan at 1½ 0z. B Vol. or Planoidal St. Pl. Exhauster R. P. M. $\begin{array}{c} 8848 \\ 7772 \\ 7772 \\ 7707 \\ 77$ A. P. M. per Forge Exhaust Diam. 10 11.11 6¼16′ Fan Main Exh. Duct Н. Р. 622256262 22.7222.70.73R. P. M. 3150 3150 3150 3150 3150 3150 3150 2150 2195 2195 2195 22590 2270 2270 2270 2270 2270 2270 Steel Press. or B Vol. Blower A. P. M. per Forge $\begin{array}{c} 112 \\ 123 \\ 512 \\ 512 \\ 512 \\ 513 \\ 523 \\ 523 \\ 523 \\ 523 \\ 523 \\ 523 \\ 523 \\ 523 \\ 523 \\ 533 \\$ Blast Diam. 77 5 8 " 1 Vol. Vol. Barana and Andrea and A Vol Vol Vol Blower Size mmmmmm mm ~~~~~~~~~ 000000040 Diam. Main Blast Duct 33°_{11} 11°_{11} 11°_{11} Num. of suffalo OJD Forges 32222322 2098765113 21008 2 1/2 Oz. per 5q. In. 20 % E Press. of Blast 'ZO E

SIZE OF BLAST AND EXHAUST TILE FOR FORGE SHOP EQUIPMENT

Sizes of	Blast	Tile		Exhaust Tile	;
Branch Tile	3″	4″	6″	8″	10″
No. of Branch Tile			Size of	Main Tile	
1 2 3 4 5 6 7 8 9 10	345668899	4 6 8 8 9 10 12 12 12		8 12 15 18 18 20 24 24 24 24 30	10 15 18 20 24 27 27 30 30 30
11 12 13 14 15 16 17 18 19 20	9 10 10 12 12 12 12 12 12 12 12 12 15	12 15 15 15 15 15 15 15 15 18 18 18	20 20 24 24 24 24 27 27 27 27 27	30 30 30 36 36 36 36 36 36 36 36	36 36 36 40 x 32 40 x 32 40 x 32 40 x 36 40 x 36 40 x 40 40 x 40
21 22 23 24 25 26 27 28 29 30	15 15 15 15 15 15 15 15 15 15	18 18 18 18 18 20 20 20 20 20 20 20	30 30 30 30 36 36 36 36 36 36 36	40 x 32 40 x 32 40 x 32 40 x 32 40 x 36 40 x 36 40 x 36 40 x 40 40 x 40	$\begin{array}{r} 44 x 44 \\ 44 x 44 \\ 44 x 44 \\ 44 x 44 \\ 50 x 48 \\ 50 x 48 \\ 50 x 48 \end{array}$
31 32 33 34 35 36 37 38 39 40	15 18 18 18 18 18 18 18 18 18 18 18	$ \begin{array}{r} 20 \\ 24 \\$	36 36 36 36 36 36 36 36 36 36 30 36 30 30 30 30 30 30 30 30 30 30 30 30 30	$\begin{array}{r} 44 \times 44 \\ 50 \times 44 \end{array}$	$\begin{array}{c} 50 & x & 48 \\ 50 & x & 54 \\ 50 & x & 54 \\ 50 & x & 54 \\ 60 & x & 54 \\ \end{array}$
41 42 43 44 45 46 47 48 49 50	18 18 18 18 18 20 20 20 20 20 20 20	24 24 24 24 24 27 27 27 27 27 27 27	40 x 30 40 x 30 40 x 30 40 x 34 40 x 34 40 x 34 40 x 34 40 x 34 40 x 34 40 x 36	50 x 44 50 x 44 50 x 48 50 x 48 50 x 48 50 x 48 50 x 54 50 x	$\begin{array}{c} 60 \ x \ 60 \\ 64 \ x \ 64 \\ \end{array}$

Foundry Blower Practice

The air required per ton of iron melted has been variously given at from 30,000 to 33,000 cu. ft. per ton. As it is almost impossible to measure the air directly it is necessary to resort to indirect methods of chemical analysis of the escaping gases. By analyzing a sufficient number of samples, the amount of air used in the combustion of the coke can be determined with considerable exactness. The following weights and volumes of air are required per ton of iron in different melting ratios.

MELTING RATIO	AIR REQUIREMENT
Lbs. of Iron per Lb. of Coke	Cu. Ft. per Ton
7 8 9	31,000 29,000 27,000
10	25,000 22,000

It is customary to provide a blower on a basis of 30,000 cu. ft. of air per ton, which corresponds to from 70 to 80 per cent. of the chemical requirements with coke of average quality and a melting ratio of $7\frac{1}{2}$ to 1. The pressure and quantity of air required for any particular case may be determined by means of the following formulae:

$$W = 2D\gamma p$$
(44)

A. P. M. =
$$\frac{D^2 V p}{2}$$
 (45)

H. P.
$$=\frac{D^2 \sqrt{p^3}}{3800}$$
 (46)

where

W = weight of iron in lbs. per hour.

p = press. at cupola in oz. per sq. in.

D = diam. of cupola in inches.

A. P. M. = cu. ft. of air per minute.

H. P. = horsepower required.

The above formula for A. P. M. allows for an air leakage of 10 per cent.

The table on page 110 of air per minute and H. P. for cupola service gives the cubic feet of air required per minute and horsepower of the fan for various sizes of cupola and at pressures of from 10 to 18 ounces. Knowing the size of cupola and either the pressure to be carried or the weight of metal per hour to be melted, the other factors may be readily determined from the table.

TABLE OF AIR PER MINUTE AND H. P. FOR CUPOLA SERVICE

						1
Inside iam. of Cupola	Stat	ic Pressure a	at Cupola in	Oz. Per Sq.	Inch	
Inside Diam. of Cupola	10 oz.	12 oz.	14 oz.	16 oz.	18 oz.	
30″	5690 1423 7.4	6230 1558 9.7	$6730 \\ 1688 \\ 12.3$	7200 1800 15.0	7640 1910 17.9	CAP. A. P. M. H. P.
35″	$7740 \\ 1935 \\ 10.0$	8480 2120 13.2	9170 2293 16.7	$9800 \\ 2450 \\ 20.4$	$10390 \\ 2773 \\ 25.9$	CAP. A. P. M. H. P.
40″	$10120 \\ 2530 \\ 13.2$	11080 2770 17.3	$11970 \\ 2993 \\ 21.8$	$12800 \\ 3200 \\ 26.6$	$13570 \\ 3393 \\ 31.8$	CAP. A. P. M. H. P.
45″	$12810 \\ 3203 \\ 16.7$	$14030 \\ 3508 \\ 21.9$	$15150 \\ 3788 \\ 27.6$	$16200 \\ 4050 \\ 33.7$	$17180 \\ 4295 \\ 40.2$	CAP. A. P. M. H. P.
50″	$15810 \\ 3953 \\ 20.6$	$17320 \\ 4330 \\ 27.0$	$18700 \\ 4675 \\ 34.0$	$20000 \\ 5000 \\ 41.6$	$21210 \\ 5303 \\ 49.6$	CAP. A. P. M. H. P.
55″	$19130 \\ 4783 \\ 24.9$	$20960 \\ 5240 \\ 32.7$	$22640 \\ 5660 \\ 41.2$	$24200 \\ 6050 \\ 50.3$	$25660 \\ 6415 \\ 60.0$	CAP. A. P. M. H. P.
60″	$22770 \\ 5693 \\ 29.6$	$24940 \\ 6235 \\ 38.9$	$26940 \\ 6735 \\ 49.0$	28800 7200 59.9	30540 7635 71.5	CAP. A. P. M. H. P.
65″	$26730 \\ 6683 \\ 34.8$	$29270 \\ 7318 \\ 45.7$	$31620 \\ 7905 \\ 57.5$	33800 8450 70.3	35840 8960 83.9	CAP. A. P. M. H. P.
70″	30990 7748 40.3	$33950 \\ 8488 \\ 52.9$	36670 9168 66.7	39200 9800 81.5	$41570 \\ 10393 \\ 97.3$	CAP. A. P. M. H. P.
75″	$35580 \\ 8895 \\ 46.3$	$38970 \\ 9743 \\ 60.8$	42090 10523 76.6	$45000 \\ 11250 \\ 93.6$	47720 11930 111.7	CAP. A. P. M. H. P.
80″	$\begin{array}{r} 40480 \\ 10120 \\ 52.6 \end{array}$	$44340 \\ 11085 \\ 69.2$	47890 11973 87.2	$51200 \\ 12800 \\ 106.5$	$54290 \\ 13573 \\ 127.0$	CAP. A. P. M. H. P.

CAP. is lbs. of metal melted per hour. A. P. M. is cu. ft. of air required per minute. H. P. is power required to deliver air at pressure given with steel pressure blowers.

PART III AIR DUCTS

Under the subject of "Air Ducts," will be found detailed information pertaining to the design of various duct or conduit systems used for the conveying of air. The data relating to pressure losses and friction in piping and elbows is based on actual experiments and tests, and in many cases where required information was not to be found, special experiments were made to obtain data for use in this hand-book. The subject of the proper proportions of piping in different systems, as well as the proper velocity of air, is also completely covered.

Material of Air Ducts

One of the essential parts of any heating and ventilating system consists of the ducts or conduits used to convey the air to the desired points in the building. These ducts may go under ground, when they are usually constructed of tile, brick, or of concrete. When the system is an overhead one warm air is usually carried through galvanized iron pipes or ducts, the vertical risers being either of brick or galvanized iron. A very common construction is to run galvanized iron risers inside brick flues. In any event the inside of the duct should be made as smooth as possible, in order to avoid excessive friction and for this reason iron ducts are generally preferred to brick or concrete, unless low velocities are employed.

The piping systems for industrial buildings and those for public buildings are designed according to two distinct methods. In industrial buildings the problem is chiefly to convey heat units with as great an economy of power, material and space as possible, while in public buildings there are the additional requirements of freedom from noise and prevention of drafts. In industrial buildings air is usually conveyed through one or more main lines extending lengthwise of the building, the areas of such pipes decreasing as they extend, to give a uniform distribution of air throughout. On the other hand in public buildings individual ducts are carried from the apparatus to each room, so that it is evident the same method is not applicable to both systems.

in Ft.					Loss o	f Pressui	e per 10	Loss of Pressure per 100 Feet in Inches of Water	Inches	of Wate				
y of Air niM 199						Diar	neter of	Diameter of Pipe in Inches	Inches					
tioolaV I	3 in.	4 in.	5 in.	6 in.	7 in.	8 in.	9 in.	10 in.	12 in.	14 in.	16 in.	18 in.	20 in.	22 in.
200 300 400	.026 .057 .102	.019 .043 .076	.016 .035 .062	.012 .029 .050	.010 .024 .043	.009 .033 .038	.008 .019 .033	.007 .017 .031	.007 .014 .026	.005 .012 .022	.005 .010 .019	.003 .010 .017	.003 .009 .016	.003 .009 .014
500 600 700	.161 .231 .314	.120 .173 .239	.097 .139 .189	.080 .116 .158	.069 .099 .135	.061 .087 .118	.054 .076 .104	.049 .069 .094	.040 .057 .078	.035 .050 .068	.029 .043 .059	.027 .038 .052	.024 .035 .047	.022 .031 .043
800 900 1000	.411 .520 .642	.309 .390 .482	.246 .312 .385	.206 .260 .321	.177 .224 .276	.154 .194 .241	.137 .173 .213	.123 .156 .192	$.102 \\ .130 \\ .160$.088 .111 .137	.076 .097 .120	.069 .087 .108	.062 .078 .097	.056 .071 .088
1500 2000 2500	$\begin{array}{c} 1.444 \\ 2.568 \\ 4.013 \end{array}$	$\frac{1.083}{1.927}$ 3.004	$ \frac{.867}{1.542} $	$.723 \\ 1.285 \\ 2.006$	$\begin{array}{c} .619 \\ 1.101 \\ 1.748 \end{array}$.541 .964 1.505	$ \begin{array}{c} 482 \\ 855 \\ 1.337 \end{array} $	$^{434}_{-770}$.361 .642 1.004	.312 .550 .860	.277 .482 .753	.243 .428 .669	.225 .385 .603	.198 .350 .548
3000 3500 4000	$ \begin{array}{c} 5.774 \\ 7.872 \\ 10.276 \end{array} $	4.335 5.902 7.706	$3.468 \\ 4.722 \\ 6.166$	2.890 3.820 5.138	2.478 3.373 4.405	2.168 2.956 3.853	$ \begin{array}{c} 1.927 \\ 2.624 \\ 3.425 \end{array} $	$ \begin{array}{c} 1.734 \\ 2.360 \\ 3.083 \end{array} $	1.444 1.966 2.568	1.238 1.685 2.202	1.084 1.476 1.926	$ \begin{array}{c} .964 \\ 1.311 \\ 1.713 \end{array} $	$ \begin{array}{c}$	$ \begin{array}{c} .789\\ 1.073\\ 1.401 \end{array} $
4500 5000 5500	$\begin{array}{c} 13.005\\ 16.055\\ 20.643\end{array}$	$\begin{array}{c} 9.754 \\ 12.051 \\ 14.577 \end{array}$	7.803 9.634 11.656	$6.560 \\ 8.084 \\ 9.713$	5.573 6.880 8.340	4.878 5.934 7.288	$ \begin{array}{r} 4.335 \\ 5.351 \\ 6.477 \end{array} $	$3.728 \\ 4.852 \\ 5.827$	$3.251 \\ 4.014 \\ 4.857$	2.787 3.440 4.162	2.438 3.010 3.642	2.168 2.676 3.237	1.951 2.409 2.913	$1.774 \\ 2.190 \\ 2.648$
6000	23.120	17.340	13.871	11.561	9.908	8.670	7.706	6.936	5.780	4.985	4.335	3.853	3.468	3.152

FAN ENGINEERING-BUFFALO FORGE COMPANY

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PRESSURE REQUIRED TO OVERCOME FRICTION OF AIR PASSING THROUGH PIPES (CONTINUED)

				Loss o	f Pressure	Loss of Pressure per 100 Feet in Inches of Water	Feet in In	ches of W	/ater				
	1				Diam	Diameter of Pipe in Inches	pe in Inch	es					r
veloc 17	24 in.	26 in.	28 in.	30 in.	.34 in.	38 in.	42 in.	46 in.	50 in.	54 in.	58 in.	62 in.	RIU.
200 300 400	.00322 .00711 .01281	.00296 .00668 .01183	.00274 .00619 .01099	.00257 .00577 .01025	.00225 .00510 .00905	.00205 .00456 .00810	.00184 .00413 .00732	.00166 .00376 .00668	.00156 .00347 .00607	.00139 .00329 .00572	.00139 .00295 .00538	.00121 .00277 .00486	ITON
500 600 700	.02005 .02890 .03929	.01850 .02667 .03628	.01719 .02476 .03388	.01604 .02311 .03144	.01415 .02039 .02773	.01266 .01826 .02481	.01146 .01651 .02245	.01046 .01491 .02046	.00954 .01387 .01873	.00884 .01283 .01751	.00815 .01179 .01630	.00763 .01127 .01526	1 1 2
800 900	.05134 .06503 .08021	.04741 .06003 .07404	.04401 .05571 .06876	.04108 .05202 .06417	.03624 .04590 .05661	.03243 .04106 .05067	02934 03716 04583	.02670 .03399 .04214	.02462 .03121 .03850	.02289 .02878 .03555	.02133 .02688 .03312	.01994 .02514 .03104	
1500 2000 2500	.18064 .32105 .50129	.16677 .29638 .46300	.15482 .27271 .42995	.14450 .25451 .40129	.12750 .22460 .35402	.11409 .20092 .31678	.10320 .18182 .28660	.09427 .16732 .26167	.08653 .15417 .24069	.08010 .14270 .22281	.07473 .13282 .20740	.06988 .12415 .19403	
3000 3500 4000	.72250 .98330 1.2841	.66695 .90761 1.1853	.61930 .84282 1.1006	.57800 .78661 1.0274	.51000 .69415 .90650	.45631 .62102 .81111	$\begin{array}{c} 41270\\ 56190\\ 73381 \end{array}$.37680 .51295 .66985	.34681 .47181 .61575	.32096 .43700 .57066	.29895 .40680 .53131	.27970 .38051 .49696	~
4500 5000 5500	$\frac{1.6257}{2.0068}$	$\begin{array}{c} 1.5051 \\ 1.8525 \\ 2.2411 \end{array}$	$\begin{array}{c} 1.3934 \\ 1.7201 \\ 2.0814 \end{array}$	$1.3050 \\ 1.5986 \\ 1.9426$	$\begin{array}{c}1.1476\\1.4166\\1.7140\end{array}$	$ \begin{array}{c} 1.0267 \\ 1.2309 \\ 1.5318 \end{array} $	$.92899 \\ 1.1467 \\ 1.3873$	$ \begin{array}{c} .84809\\ 1.0462\\ 1.2667 \end{array} $.78032 .96337 1.1654	.72135 .89178 1.0791	.67106 .83022 1.0046	.62925 .77666 .93980	
6000	2.8900	2,6611	2.4771	2.3121	2.0402	1.8252	1.6473	1.5078	1.3872	1.2844	1.1947	1.1167	
		Powdered	ered	Coal	Engil	1ee	ring &	k Eq	unpm	ent	,0°		

Pressure Losses in Air Ducts

Losses in piping systems are made up of two parts, dynamic losses and friction losses. Dynamic losses are due to changes either in direction or velocity of the air flow, and are composed of loss at entrance and loss in elbows and connections. The first is the pressure required to produce velocity in the pipe, and may vary from 1 to 1.5 times the velocity head, i. e., pressure corresponding to velocity, depending on whether the pipe is connected directly to the fan outlet or through a plenum chamber. It is expressed as a multiple of the pressure corresponding to the average velocity produced in the pipe. Where velocity in the pipe is the same as at the fan outlet this may still be considered a loss, in view of the fact that with a reduction of velocity through a gradually diverging outlet to a larger area the difference between the velocity head at the fan and the velocity head in the pipe is largely utilized by conversion to static pressure.

The other chief source of dynamic loss is in elbows, and depends on the radius of curvature of the elbow and not on its size or on the velocity of the air. This loss may be expressed directly in per cent. of velocity head, and, with a round five-piece elbow, having a center line radius of one diameter, the loss will be 25 per cent. of the average velocity head. With a five-piece elbow having a center line radius of one and one-half diameters the loss will be 17 per cent., or only two-thirds that of the first case. This shows the advantage of an intelligently designed system and the possibility in power saving, for elbows may be of so short a radius as to cause loss of an entire velocity head in each one.

The second source of pressure loss in the piping system is due to friction of air against the sides of the pipe. This loss will vary directly as the length of the pipe, or as the square of the velocity, and inversely as the diameter of the pipe. As length is a fixed quantity for any system, the only factors subject to modification are the diameter and velocity, which determine the relation between power cost and piping cost.

As in the case of heaters, it is the usual engineering practice to proportion piping arbitrarily, either from assumed velocities depending upon the velocity of the air at the fan outlet, or, in better engineering practice, by determining the velocity which will give an assumed resistance considered suitable and within the fan capacity. It is the best practice to gradually decrease the velocity in the main conduit as the latter is decreased in size owing to partial delivery of the air through the branch outlets.

This practice serves three useful purposes:

1. A proper proportioning of the velocity permits a uniform delivery of air through all the branch outlets without dampers and regardless of distance from the fan.

2. By a gradual reduction in velocity a considerable proportion of the velocity pressure is usefully converted to static pressure, thus largely compensating for piping friction.

3. It decreases friction in the smaller piping, where it would otherwise be greatest.

Friction in Air Ducts

Resistance to flow of air through piping varies with several factors such as velocity, roughness of the contact surface, or obstructions such as dampers, deflectors, and elbows. This resistance or loss in pressure is ordinarily expressed as the equivalent head in feet of air; or in velocity heads (that is the ratio of the friction loss to the theoretical pressure corresponding to the average velocity in the pipe); or as the equivalent pressure in inches or ounces. As explained on page 16 under the subject, "Relation of Velocity to Pressure," one velocity head is the pressure corresponding to the velocity of the air.

The formula used by the U.S. Navy Department for loss of head due to friction in a round pipe is

$$H = 4f \frac{L}{D} V^2$$
 (47)

where

H = loss of head in feet of air.

L=length and D=diameter of pipe, both expressed either in feet or in inches.

V = velocity of flow through the pipe in feet per second.

f = 0.00008 for first class piping.

Since in air measurements it is more customary to express velocity as feet per minute, this formula reduces to

$$H = 0.00000089 \frac{L}{D} V^2$$
 (48)

For rectangular ducts the formula becomes

H = 0.000000045
$$\frac{i+n}{n}$$
 $\frac{L}{i}$ V² (49)

where

H = loss of head in feet of air. V = velocity in feet per minute. i = short side of pipe. n = long side of pipe. L = length of pipe. f = assumed as 0.00008.

It will be noted that the loss in head as given by the above formulae is expressed in feet of air, while the head or pressure ordinarily considered in air measurements is expressed either in inches of water or in ounces per square inch. As shown by Equation (12) page 18, the velocity head expressed in feet of air is $\frac{d}{12W}$ times the head in inches of water. Taking a value of d = 62.31 as the density of water we then have

$$H = h' \frac{62.31}{12 W}$$
$$V_0 = \frac{1096.5}{\sqrt{W}} (\text{See page 18})$$

where

 $V_0 = vel.$ in ft. per min. corresponding to one inch of water.

W = weight of air per cubic foot.

From the above and from equation (48)

$$\mathbf{h}' = \frac{\mathbf{L}}{48.6 \,\mathrm{D}} \left(\frac{\mathrm{V}}{\mathrm{V}_0}\right)^2 \tag{50}$$

where

A more general form of the above equation may be expressed

as

$$\mathbf{h}' = \frac{\mathbf{L}}{\mathbf{CD}} \left(\frac{\mathbf{V}}{\mathbf{V}_0} \right)^2 \tag{51}$$

where C=a constant depending on the character of the pipe. The constant C in the above formula represents the length of pipe in diameters causing a loss of one velocity head. For perfectly smooth unobstructed pipe we may take C=60, but for fairly smooth work such as the piping of a planing-mill exhaust system a safe factor would be C=55. For heating and ventilating work where there exist more or less obstructions in the form of dampers, deflectors, etc., and where the piping is usually swedged, we may consider one velocity head lost in from 45 to 50 diameters. For such systems we may usually take C=45. For tile or brick ducts C=40 will meet the average conditions.

From the above we see that if the velocity in a 12-inch pipe is 2832 feet per minute (corresponding to $\frac{1}{2}$ inch) and the pipe is 45 feet long, the loss in pressure will be one velocity head, or $\frac{1}{2}$ inch. If, for instance, a pressure of $\frac{1}{2}$ inch is required at the outlet end of the pipe, a pressure of 1 inch must be maintained at the entering end.

Friction in rectangular pipe may be determined by using the tables on pages 156 and 157 which give the circular equivalent of rectangular pipes computed to give equal friction for the same air quantities. By means of this table the corresponding diameter of round pipe may be found, and the friction loss determined as above.

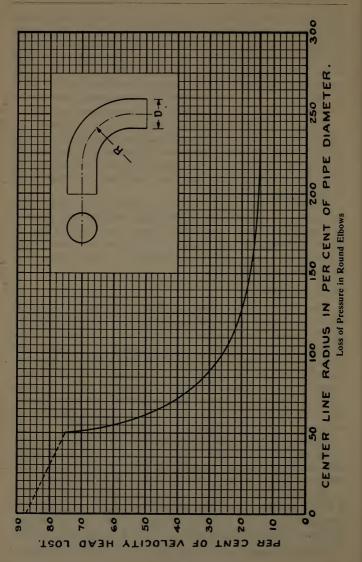
Friction in Elbows

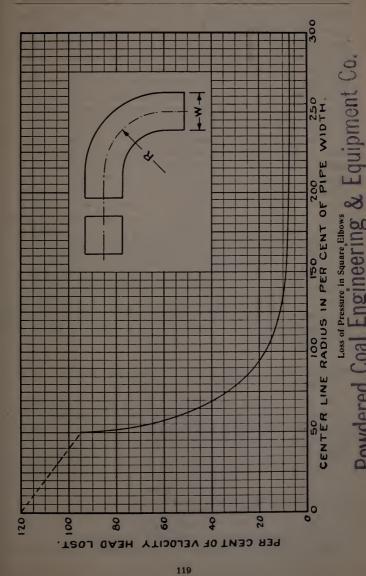
The two diagrams on pages 118 and 119 of pressure loss in elbows show respectively the loss by friction through elbows of either round or square section. These curves are based on data obtained at the testing plant of the Buffalo Forge Company, full details of the tests and of the results obtained being described in a paper presented before the A. S. H. & V. E. on "Loss of Pressure due to Elbows in the Transmission of Air through Pipes or Ducts."* The loss in per cent. of a velocity head is given for elbows of different radii, the center line radius being expressed in per cent. of the pipe diameter or width.

It may be seen from these diagrams that with $R=1\frac{1}{2}D$, or an inside throat radius of one diameter, fairly good results may be obtained without making the elbow unduly long. Practically nothing is to be gained by making R greater than 2D.

It is also evident from an inspection of these diagrams that if it can possibly be avoided an elbow with R less than one D should not be used. Even with these an elbow in a square duct will cause a loss of 17.5 per cent. and in a round duct 25.5 per

^{*}Am. Soc. Heating and Ventilating Engrs., 1913, by Frank L. Busey.





FRICTION I N ELBOWS

cent. of the velocity head. In case $R = \frac{1}{2}D$ (throat of elbow square but outer side rounded to a radius of one diameter) the loss will be 95 per cent. for a square duct and for a round duct 75 per cent. of the velocity head. The loss indicated on the diagram for R = D represents tests on elbows of two-piece construction, or with both inside and outside made square. It is evident that this is a construction that should never be used, since in the case of the square pipe one quarter of the loss may be saved by making the outer side round ($R = \frac{1}{2}D$).

From the curve for round ducts it will be seen that with an elbow having $R = 1\frac{1}{2}D$ the loss will be 17 per cent. of a velocity head. If we consider one velocity head lost in 50 diameters of straight pipe this means that this elbow is equivalent in friction effect to 8.5 diameters of pipe. If the elbow was in a square duct the loss would be equal to 4.5 diameters (or widths) of pipe. With a velocity of 4000 feet per minute through the duct (corresponding to one inch pressure, or a velocity head of one inch) the above elbow in the round pipe would cause a loss in pressure of 0.17 inch and in the square duct of 0.09 inch.

For ordinary calculations one easy long radius elbow in a circular pipe may be considered as equal in friction loss to 10 diameters of straight pipe. This is the factor given by N. S. Thompson in his book, "Mechanical Equipment of Federal Buildings," as applied to elbows having a center line radius of $1\frac{1}{2}$ diameters.

Pressure Losses in Diverging and Converging Nozzles and in Orifices

It may be stated as a general principle in air flow calculations that "The coefficient of pressure loss is the square of the reciprocal of the coefficient of discharge," i. e., the coefficient of pressure loss, m, in terms of the coefficient of discharge, c, may be stated as

$$m = \left(\frac{1}{c}\right)^2 \tag{52}$$

and the loss in static pressure will be

$$p_{s} = m \left(\frac{V}{V_{0}}\right)^{2}$$
(53)

where V = velocity of air flow and $V_0 =$ velocity corresponding

to unit pressure. Then $\left(\frac{V}{V_0}\right)^2$ will be the velocity pressure.

Coefficients of discharge to be used in air measurements will be found below. Coefficients for pressure loss will be

m for sharp edged orifice

m for short length $(2\frac{1}{2}$ to 3 diam.) of pipe 1.47

2.78

1.11

m for short pipe on fan outlet

The coefficient m for converging nozzles having different angles of convergence between the two sides will be

Angle of Convergence	Coefficient m
6 degrees 8 10 12 14 22.5	1.175 1.150 1.140 1.130 1.130 1.130 1.185

In case any of the above factors are to be considered, there will be a loss in static pressure—and the same loss in total pressure—of m times the pressure due to the velocity.

When a diverging nozzle is to be considered, as shown by the diagram on page 123, there will be a certain gain in static pressure as determined by the coefficient e.

The coefficient of loss m will then be (1-e), but in this case the coefficient m is to be applied to the change in velocity head due to the nozzle, and is a measure of the loss in total pressure. That is, the gain in static pressure will be

$$\mathbf{p}_{\mathbf{s}} = \mathbf{e} \left[\left(\frac{\mathbf{V}_1}{\mathbf{V}_0} \right)^2 - \left(\frac{\mathbf{V}_2}{\mathbf{V}_0} \right)^2 \right] \tag{54}$$

The loss in total pressure will be

$$\mathbf{p}_{\mathbf{t}} = (1 - \mathbf{e}) \left[\left(\frac{\mathbf{V}_1}{\mathbf{V}_0} \right)^2 - \left(\frac{\mathbf{V}_2}{\mathbf{V}_0} \right)^2 \right]$$
(55)

In the above formulae the change in velocity head between the entering and leaving end of the nozzle is expressed by

$$\left[\left(\frac{V_1}{V_0} \right)^2 - \left(\frac{V_2}{V_0} \right)^2 \right]$$

 $V_1 =$ velocity of air entering nozzle.

 $V_2 =$ velocity of air leaving nozzle.

 $V_0 =$ velocity corresponding to unit pressure.

e = coefficient from diagram on page 123.

Diverging Nozzle in Air Ducts

A diverging nozzle is used in an air duct when the area is increased in order to reduce the velocity, or when blowing into an enclosed space or plenum chamber. Any change from a higher to a lower velocity is accompanied by a conversion from velocity to static pressure, but inasmuch as there is always some loss in making this conversion, the total pressure is not the same after making the reduction in velocity. That is, there is always a certain portion of this converted static pressure lost in making the change, and the efficiency of conversion is never the full 100 per cent. As will be seen from the chart on page 123, the efficiency of conversion depends on the per cent. of slope of the sides of the diverging nozzle, the more gradual the slope the less the loss in pressure.

The diagram on page 123 shows the efficiency, or ratio of actual to theoretical velocity head obtained with diverging nozzles of different slopes to the sides. That is, while theoretically we should obtain an increase in static pressure equal to decrease in velocity pressure we will really convert only a part of this decreasing velocity pressure to static pressure, depending on the slope of the nozzle. While theoretically we should have

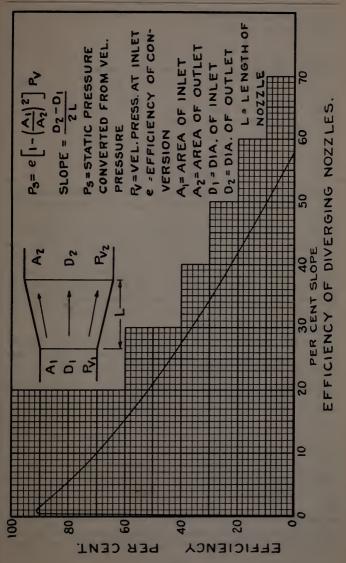
$$p_{s2} - p_{s1} = p_{v1} - p_{v2} = \left(\frac{V_1}{V_0}\right)^2 - \left(\frac{V_2}{V_0}\right)^2$$
 (56)

as a matter of fact we will have

$$p_{s2} - p_{s1} = e \left[\left(\frac{V_1}{V_0} \right)^2 - \left(\frac{V_2}{V_0} \right)^2 \right]$$
(57)

where e represents a factor depending on the proportions of the nozzle.

For instance, if we have a nozzle whose length is five times half the difference between the diameters of the two ends, that is a length of five times the slope or a slope of 0.20, we will have an efficiency of conversion of 51.5 per cent. In case the side of a nozzle makes an angle of say 30 degrees, the slope will be 0.577 and we may see from the curve that there will be no gain from the cone outlet. From the foregoing it may be seen that length of a diverging nozzle should be made as long as the case will permit in order to get the greatest possible benefit from it. The length should be at least from five to ten times the slope, giving a slope of from 0.10 to 0.20 or an angle of approximately 6 to 12 degrees.



Conversion from velocity to static pressure may be determined from the formula

$$\mathbf{p}_{s} = \mathbf{e} \left[1 - \left(\frac{\mathbf{A}_{1}}{\mathbf{A}_{2}} \right)^{2} \right] \mathbf{p}_{\mathbf{v}}$$
(58)

and loss in pressure due to the increase in area will be

$$\mathbf{p}_{t} = (1 - \mathbf{e}) \left[1 - \left(\frac{A_{1}}{A_{2}}\right)^{2} \right] \mathbf{p}_{\mathbf{v}}$$
(59)

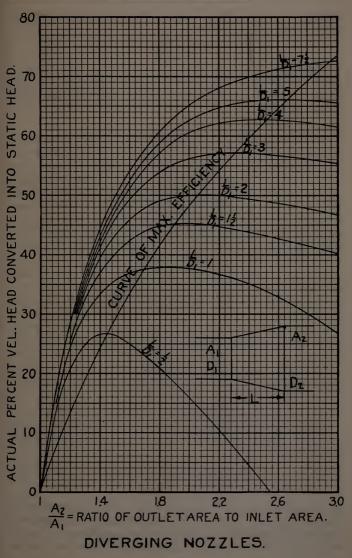
where

 p_s = static press. converted from vel. press. p_t = loss in total press. p_r = velocity press. at inlet of nozzle. e = efficiency of conversion. A_1 = area of inlet to nozzle. A_2 = area of outlet from nozzle.

On page 125 will be found a diagram plotted from actual tests of diverging nozzles, showing the per cent. of velocity head converted into static head by using nozzles having different ratios of length to diameter of outlet, as well as outlet to inlet area. While these tests were made with round pipe, it was found that the same relations held for those of rectangular section. As an example of the use of the diagram we may select a nozzle having a length equal to twice the small or inlet diameter and the outlet area twice the inlet area. From the diagrams we will find that a nozzle of these dimensions will convert 50 per cent. of the velocity head into static head.

The line marked "Curve of Maximum Efficiency" indicates the best ratios of outlet to inlet areas for different fixed lengths of nozzle and inlet diameter. It will be noted that for the different ratios of $\frac{L}{D_1}$ there is a certain ratio of outlet to inlet area that will give maximum conversion from velocity to static pressure.

Example. Assuming a case where a diverging nozzle is to be used on a 24-inch pipe in order to increase the diameter and so decrease the velocity in the pipe, and owing to the limited space the nozzle can be made only six feet long. Then the ratio $\frac{L}{D_1} = 3$, and according to the diagram we will obtain the maximum conversion from velocity to static pressure when the area of the enlarged pipe is made 2.3 times the area of the 24-inch pipe, or 36.5 inches diameter. In this case 57 per cent. of the



change in velocity head will be converted into static pressure at the nozzle outlet. Then

$$\mathbf{p}_{s2} - \mathbf{p}_{s1} = 0.57 \left[\left(\frac{\mathbf{V}_1}{\mathbf{V}_0} \right)^2 - \left(\frac{\mathbf{V}_2}{\mathbf{V}_0} \right)^2 \right]$$

A diverging nozzle on the outlet of multivane fans is often used to advantage, giving a reduction of the comparatively high velocity at the outlet of this type of fan, with a corresponding increase in static pressure.

Theoretical Outlet or Blast Area

It is a well known fact that air (or water) under pressure in passing through an orifice in a thin plate will not deliver the volume indicated by the actual area of the orifice, because the resistance of the orifice, depending on its character, will tend to restrict the flow. It follows then that there will in each instance exist an equivalent or blast area, differing from the actual area in proportion to the resistance. This blast area of an air conveying system is the area which would be theoretically required to deliver the same amount of air at a velocity corresponding to the total pressure resistance offered by the system.

Every point in a fan blast system has its blast area, which, as stated above, is less than the actual area by an amount depending on the resistance at that point. The blast area of the entire system may then be computed, inasmuch as the total resistance is the sum of the various resistances passed in series. In case the air passes through parallel channels the blast area of the system is the sum of the blast area of the separate channels.

Blast area based on the total pressure drop may be determined from

Blast area =
$$\frac{A. P. M.}{4005 \sqrt{\text{total press. drop in inches}}}$$
 (60)

Representing the blast area of an entire system by A_b and the blast area of the various sections by A_{b1} , A_{b2} , etc., we will have the relation

$$A_{b} = \frac{1}{\left(\frac{1}{A_{bl}}\right)^{2} + \left(\frac{1}{A_{b2}}\right)^{2} + \text{ etc.}}$$
(61)

Examples. As an illustration of the above principles, we will assume a case where a fan blows through a short pipe into a heater and thence into a single duct piping system. We may determine the drop in static pressure for the various sections of

the system, and calculate the blast area of each by means of the formula

Blast area = actual area
$$\sqrt{\frac{1}{\text{static loss in vel. heads + 1}}}$$

Assuming the connection between fan and heater to have an area of 4.9 sq. ft. with a loss of entrance of 0.1 vel. head and 0.25 vel. head lost in the connection itself, we find the blast area of this section to be

$$A_{b1} = 4.9 \sqrt{\frac{1}{0.35 + 1.0}} = 4.24$$
 sq. ft.

The blast area of the heater may be found by means of the above general formula. With 10000 A. P. M. and a pressure drop of 0.5 inches through the heater, the blast area will be

$$A_{b2} = \frac{10000}{4005\sqrt{0.5}} = 3.53$$
 sq. ft.

If we assume 0.5 velocity head lost by entrance to the piping system, and two velocity heads lost in the ducts and elbows, we will have as the blast area of this part of the system, if the main pipe is 35 inches in diameter

$$A_{b3} = 6.68 \sqrt{\frac{1}{2.5 + 1.0}} = 3.58 \text{ sq. ft.}$$

The blast area of the entire system may then be found from

$$\mathbf{A}_{b} = \frac{1}{\left(\frac{1}{4.24}\right)^{2} + \left(\frac{1}{3.53}\right)^{2} + \left(\frac{1}{3.58}\right)^{2}} = 4.68 \text{ sq. ft.}$$

Proportioning the Various Losses

In addition to loss of pressure due to friction in piping and elbows, there is a loss of static pressure due to entrance to the piping system of from 0.1 to 0.5 of a velocity head. In addition to this, one velocity head must be maintained to produce the required velocity in the system. In case the piping is connected directly to the fan outlet this loss of entrance is frequently neglected especially if the piping is larger than the fan outlet and is made cone shaped. This is the case in a draw-through system, where the fan draws the air through the heater and blows directly into the piping or ducts. Where the system is a blow-through one, that is, the fan blows into the heater and the air passes through and into the ducts, a considerable loss will occur at the entrance to the piping system, depending on the character of the layout. Where the piping is connected to the heater casing by an easy cone shaped approach, the loss of static pressure may be only 0.2 or 0.3 of a velocity head. In case the fan blows through the heater and into a plenum chamber, from which the pipes radiate to different parts of the building, the loss of entrance to these pipes may be as much as 0.5 of a velocity head. In any case the pressure required at the fan must be one velocity head greater in order to produce the velocity desired in the piping.

It is evident from the above that loss of power due to friction is less in a draw-through than in a blow-through system. Loss of pressure through the heater would be the same in either case, and may be determined from the table on page 446.

In the case of the draw-through system, the sum of all the pressure losses is to be deducted from the total pressure at which the fan is operating, while with the blow-through apparatus this loss is to be deducted from the static pressure.

In an ordinary draw-through system it is usually considered advisable to keep the sum of all piping losses approximately one-third to one-half, and the loss through the heater at less than one-half of the total pressure. The balance is then available for producing velocity. In case a system has been laid out and the pressure loss is found to be greater than desired, the size of the piping may be reproportioned by means of the following formula so as to obtain the desired pressure drop.

$$C_2 = C_1 \sqrt{\frac{p_2}{p_1}}$$
 (62)

where

 $C_1 =$ present pipe area. $C_2 =$ required pipe area. $p_1 =$ present pressure loss. $p_2 =$ desired pressure loss.

Thus, if we have made a layout for a system which it is desired to operate at a total pressure of not more than one and onehalf inches, and find that at the velocity required to handle the air through the sizes of ducts selected the piping loss will be say one inch, we may reproportion the size of the ducts by the above formula. Assuming that a maximum pressure loss of 0.75 inch is to be allowed instead of the above 1.00 inch, we have

$$C_2 = C_1 \sqrt{\frac{1.00}{0.75}} = 1.15 C_1$$

That is, the area of all the ducts in the system must be increased 15 per cent., or the diameters increased 7 per cent. Then if the heater loss is found to be 0.60 inch, and the velocity through the main duct is to be 1800 feet per minute, corresponding approximately to 0.2 inch, the total pressure required at the fan will be 1.55 inches.

Proportioning Piping for Exhaust Systems

It is recommended in the design of piping for an exhaust system where no dampers are provided, to make the area of the main pipe approximately 20 per cent. greater than the sum of the area of the branch pipes at that point. This results in greater uniformity of distribution than where the increase in area is not made.

Where dampers are provided, as in the vent system from buildings, uniform velocity through the system should be maintained by making the area of the main duct equal the area of the branches. Where the exhaust ducts in a public building connect directly to the exhaust fan, a velocity of from 1200 to 1500 feet per minute may be allowed in both branches and main. Where the exhaust register or opening is placed near the floor, a velocity of from 600 to 750 feet per minute should be allowed in the register box. Velocity of the air should be kept uniform throughout the entire system.

For public buildings where a plenum exhaust system (vent stacks connecting into one large chamber, such as an attic) is used and the air discharged from this chamber by means of an exhaust fan, it is customary to allow a velocity of 600 to 750 feet per minute through the vent stacks and remove the same amount of air delivered by the supply fan. When the air is discharged from the exhaust chamber by some other means than an exhaust fan, about two-thirds the amount of air supplied to the building is ordinarily taken as a measure of the air discharged, with a velocity in the exhaust stacks of from 400 to 500 feet per minute. In either case this makes the exhaust or vent stacks the same area as the supply risers.

For industrial buildings, a velocity of from 1500 to 2000 feet per minute may be allowed through the exhaust system, the velocity being made uniform in both the mains and branches. The actual velocities assumed in any case will depend on the best proportion between the first cost and the operating cost. A study of the relation between these two factors will be found on page 130. The design of the piping system as well as the size of branch pipes required for a refuse exhaust system will be found discussed under "Exhaust Systems," Part II, Section V.

Proportioning Piping for Maximum Economy

The subject of the most economical velocity of air through piping systems has been discussed in a paper* presented before the A. S. H. & V. E. at their 1913 annual meeting, some of the more interesting conclusions of which will be here given.

A decrease in velocity increases the size and cost of the air conduit, but decreases cost of power consumed in overcoming the conduit or piping resistance. From a point of economy the question to be determined is what relation between power cost and conduit cost, as determined by the velocity, will give minimum annual total cost.

This relationship may be shown to be

$$\left(\frac{V_{\rm m}}{V_{\rm o}}\right)^{\rm 3} = 0.335 \left(\frac{C_{\rm wo}}{C_{\rm po}}\right) \tag{63}$$

or

$$V_{\rm m} = 0.7 \ V_{\rm o} \left(\frac{C_{\rm wo}}{C_{\rm po}} \right)^{\frac{1}{3}}$$
 (64)

Where C_{po} and C_{wo} represent respectively cost of power to overcome piping resistance and an annual charge for interest and depreciation on piping designed for an assumed velocity V_0 ; and V_m is the relative velocity required for maximum economy.

Comparing these relationships with those obtained for the heater on page 414, it is evident that they are almost identical. It will be seen in this case that for maximum economy the annual cost of power consumed by piping resistance should be practically one-third of the annual interest and depreciation charges based on initial cost of piping. That is $C_p = 0.335 C_{\pi}$ for maximum economy. This annual allowance on the piping system for interest and depreciation may be assumed to be about 25 per cent. of the original cost of the installation.

While these lower velocities and consequently lower resistance would require the use of large fans in order to operate at high efficiency, considering the entire installation of heater, piping and fan, the annual cost of power should be practically

^{*&}quot;The design of Indirect Heating Systems with Respect to Maximum Economy of Maintenance and Operation," by Frank L. Busey and Willis H Carrier.

30 per cent. of the total annual allowance for interest and depreciation. If this allowance is taken at 20 per cent. as an average, we would have approximately 6 per cent. on the first cost as the most economical yearly rate to be allowed for power.

Practical Applications

For the purpose of illustrating the application of the foregoing principles to a system of galvanized iron piping, different cases will be assumed and results shown. A system handling 30000 cu. ft. per minute, at a velocity of 1950 ft. per minute, will require a pipe 53 inches in diameter, or an area of 15.32 sq. ft. These quantities will be taken as a constant condition, but different arrangements considered in the system of piping.

Assuming one straight duct 200 feet long and 53 inches in diameter, delivering all of the air at the end farthest from the fan, we will have two sources of loss to be overcome by the fan.

First, the dynamic loss due to the velocity of 1950 feet per minute (or one velocity head), and second, the loss due to friction, amounting to one velocity head in each 50 diameters of length. The pressure due to the velocity of 1950 feet per minute in the pipe (one velocity) will be 0.237 inch, water gauge. The loss of pressure due to friction will be

 $\frac{200}{4.42\times50} = 0.905 \text{ velocity head}$

This loss expressed in inches of water will be

 $0.237 \times 0.905 = 0.214$ inch

and the total loss will be the sum of these two, or 0.451 inch. In the piping system a part of the velocity is converted to static pressure, hence the power calculated should be based on total pressure with a corresponding fan efficiency of 50 per cent. At a rate of \$20 per H. P. yr., the annual cost due to the piping resistance will be

 $C_{po} = 30000 \times 0.000324 \times 0.451 \times 20 = $48.$

A round galvanized iron pipe, 53 inches in diameter, would be made of No. 18 iron, weighing 2.3 pounds per square foot, and would contain 14.2 sq. ft. per running foot. This would make 32.7 pounds per running foot, or a total of 6540 pounds for the entire pipe. Allowing 25 per cent. annually for interest and depreciation on an initial cost of say 10 cents per pound, the yearly allowance would be 2.5 cents per pound of iron. Then we would have as the yearly allowance for interest and depreciation

$C_{wo} = 6540 \times 0.025 = $163.50.$

From equation (64) we may determine that for the most economical conditions the velocity of air in the pipe should be

$$V_m = 0.7 \times 1950 \left(\frac{163.5}{88.0}\right)^{\frac{1}{3}} = 1670$$
 ft. per min.

Assuming the case where 30000 cu. ft. per minute is to be uniformly distributed by a galvanized iron pipe 200 feet long, with equal openings every 20 feet of its length, each discharging 3000 cu. ft. per minute, we will have an example of another common form of installation. Referring to the chart, page 138, we see that, if the first 20 feet of pipe is 53 inches in diameter, the next 20 feet carrying 90 per cent. of the air should be 51 inches in diameter. Treating each successive section in the same manner we may determine the diameter and weight of each section, and will find the total weight of the piping to be 3922 pounds. Then the yearly total allowance for interest and depreciation on the piping system will be

 $C_{wo} = 3922 \times 0.025 = \98.05

Loss in pressure due to friction will be the same as in the first case considered, or 0.214 inch, but loss due to velocity will be only 40 per cent. of the loss as calculated in the first example, or 0.095 inch. The total pressure loss will then be

0.214 + 0.095 = 0.309 inch.

and the annual power cost at \$20 per H. P. yr. will be $C_{no} = 30000 \times 0.000324 \times 0.309 \times 20 = $60.$

As before from equation (64) we will have as the velocity for the most economical operation

$$V_m = 0.7 \times 1950 \left(\frac{98.05}{60.00}\right)^{\frac{1}{3}} = 1575$$
 ft. per min.

Proportioning Ducts for Public Buildings

In public buildings the sizes of air-conveying ducts from fans or heaters to vertical induction flues, and the sizes of these flues, depend upon the velocity of flow in such ducts and flues. The essential factors in determining these velocities are: Limitations of economical relative speed of fans from the standpoint of power; limitations of air velocities on account of noise or by reason of increasing friction as velocities increase; limitations of velocity of inflowing air through registers into rooms; desirability of as high a velocity of air as is permissible under the limitations referred to in order to get as quick a conveyance of the warmed air as possible; and necessary initial and intermediate velocities to overcome the resistance existing in each particular system or case.

Register Velocity

The size of vertical flues to the registers in the rooms is determined by the maximum velocities allowable in avoiding drafts and noise in the rooms. Practice has shown that the best velocities for the registers should be from 200 to 400 feet per minute over the face of the register, depending upon the size and location; floor registers from 125 to 175 feet. Velocity in the vertical flues leading to the registers should be from 400 to 750. Sizes of these vertical flues are determined largely by the size of register desirable. In general, the velocity in these risers should be low, in order to obtain as uniform a flow as possible over the register area.

Cu. Ft. of	Register	Av. Vel. Over	Size of Riser	Riser Velocity
Air per Min.	Size Inches	Face of Reg.	Inches	Ft. per Min.
160	8 x 13	220	6 x 8	490
230	8 x 18	230	8 x 8	510
290	10 x 18	230	8 x 10	525
360	12 x 18	240	8 x 12	540
430	14 x 18	245	8 x 14	555
510	16 x 18	255	8 x 16	570
580	12 x 30	230	12 x 12	580
690	14 x 24	295	12 x 14	590
810	16 x 28	260	12 x 16	605
925	18 x 27	275	12 x 18	615
1040	20 x 26	290	12 x 20	625
1160	22 x 28	270	12 x 22	635
1290	24 x 27	285	12 x 24	645
1450	20 x 36	290	16 x 20	653
1620	22 x 36	295	16 x 22	663
1790	24 x 36	300	16 x 24	672
1970	24 x 36	330	16 x 26	680
2140	27 x 38	300	16 x 28	687
2310	30 x 36	310	16 x 30	693
2490	30 x 36	330	16 x 32	700

STANDARD SIZES OF REGISTERS AND RISERS FOR PUBLIC BUILDINGS

Duct Velocity

The velocity in horizontal ducts leading from the apparatus to the vertical risers is determined chiefly by the resistance of the duct. In practice these velocities will vary from 700 feet to 1200 feet depending upon size and length of duct, number of elbows, etc. A designer with considerable experience may proportion these ducts so as to give very uniform distribution without going into any extended calculation. However, it is desirable to have a correct method as a basis. For the benefit of engineers and architects we give here the method that may be employed in the determination of duct velocities and sizes.

Allowing for Friction

The principal losses in piping systems for public buildings are in the horizontal ducts where velocity is highest. Losses in these ducts depend upon velocity, size and length of duct, and upon the number of elbows, together with a considerable loss in pressure as the air enters the duct. An ideal system should take all these factors into consideration and so proportion the velocities that the resistance may be practically equal in all ducts regardless of the length, etc. The system above mentioned accomplishes this in a practical manner and at the same time avoids any laborious calculation. For each duct a factor may be obtained by inspection in accordance with the following formula:

$$F = 2\frac{1}{2} + \frac{L}{4W} + \frac{N}{5}$$
 (65)

This factor represents loss by friction in terms of velocity head. The first term, $2\frac{1}{2}$, is approximately the number of times the velocity head is lost by entrance to the pipe, entrance to the vertical flue, and loss in riser and register. The second factor represents loss due to length and size of pipe; L is length in feet and W is approximate width in inches. The third term represents that proportion of the pressure lost in elbows, and N is the number of long radius elbows. One square elbow is considered equal to two long radius elbows. In checking over the piping layout the factors for the various ducts are first found as above and from these factors the velocity in the respective ducts is ascertained directly. In determining these velocities it is usual to allow a loss not exceeding one-quarter of the total fan pressure, which in practice usually amounts to about one-quarter of an inch. The velocity corresponding to a pressure of onequarter of an inch is 2000, and since the velocities vary as the square root of the pressures, the factor F and the velocity V will give a loss of one-quarter of an inch if

$$V = \frac{2000}{\sqrt{F}}$$
(66)

Example. As an example of the above system we will assume a case where the longest run of pipe L=50 feet, W=18 inches, and the number of easy elbows N=4

We will then have

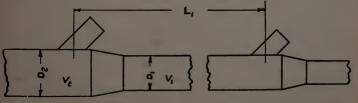
$$F = 2.5 + \frac{50}{72} + \frac{4}{5} = 4.0$$
 velocity heads

Velocity which will cause a loss of one-quarter inch will then be

$$V = \frac{2000}{\sqrt{4}} = 1000$$
 ft. per min.

Proportioning Piping for Industrial Buildings—Supply or Blast System

In proportioning main and branch pipes in industrial buildings, the primary aim is to secure as uniform a distribution as possible without the necessity of dampering, as well as to secure economy of power and economy of material. It has been found good practice in proportioning piping systems to decrease the velocity in the main pipes as the air quantity decreases. As already stated, this principle of proportioning has three advantages. First: It utilizes the velocity of the air in producing static pressure in the system. Second: By this means a nearly uniform static pressure may be secured in all parts of the pipe line, giving a very uniform distribution of air throughout. Third: It reduces the friction in the smaller pipes, which would otherwise be excessive.



Equations giving ideal distribution of static pressure for round pipes are

$$\frac{V_2}{V_1} = \sqrt{\frac{L_1}{40D_1} + \frac{N}{5} + 1}$$
(67)

and

$$\frac{D_1}{D_2} = \sqrt{\frac{C_1}{C_2}} \sqrt[4]{\frac{L_1}{40D_1} + \frac{N}{5} + 1}$$
(68)

These equations for rectangular pipes are

$$\frac{V_2}{V_1} = \sqrt{\frac{(a+b)L_1}{80 \ a \ b} + \frac{N}{5} + 1}$$
(69)

or when the short side a remains constant and the long side \underline{b} changes

$$\frac{b_2}{b_1} = \frac{C_2}{C_1} \frac{1}{\sqrt{\frac{(a+b) L_1}{80 a b} + \frac{N}{5} + 1}}$$
(70)

where

 $V_1 = an$ assumed or predetermined velocity in a length of pipe.

 V_2 = velocity in the preceding length of pipe.

 L_1 =length and D_1 =diameter both expressed in feet of the length of pipe having the velocity V_1 . N=number of easy long radius elbows in section L_1 . C_1 and C_2 =the corresponding air quantities in the pipes D_1 and D_2 .

a = short side and b = long side of a rectangular pipe.

The application of these formulae is clearly shown by a reference to the sketch on page 135, where velocity V_1 is known and velocity V_2 is to be determined. The decrease in velocity between V_2 and V_1 will then be sufficient to care for the static losses of the section having the velocity V_1 .

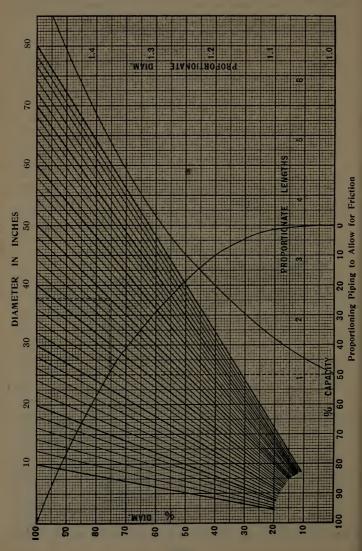
The following method of proportioning piping has been carefully tested and has been found to give a satisfactory distribution when applied to the reduction in size of the main duct with a series of outlets along its length, or to branch pipes of equal length. It also facilitates the calculation of friction. When the branch pipes are of unequal length a correction should be applied as explained under "Equalizing Friction for Unequal Length" on page 139. The principle involved is to so proportion the velocities in the various pipe sizes as to give equal friction in all air pipes per running foot regardless of their size. It may easily be shown that the equation which relates the carrying capacity of a pipe to its size to suit this condition is

$$\frac{\mathrm{d}_2}{\mathrm{d}_1} = \left(\frac{\mathrm{C}_2}{\mathrm{C}^1}\right)^{\frac{2}{5}} \tag{71}$$

Where d_1 and d_2 are the relative diameters of two pipes and C_1 and C_2 are the relative air quantities. As an equation in this form would be difficult of computation, the diagram shown on page 138 may be conveniently employed.

In using this chart commence with the main pipe equal in area to the fan outlet, or larger, as circumstances may require. All sizes are proportioned directly from this main pipe size. It will be noted that the curve is plotted for per cent. capacity and for per cent. diameter according to the formula for constant friction per foot of length. For instance, if we have a branch pipe which is required to carry 50 per cent. of the capacity of the main pipe, we find the point on the curve which corresponds to 50 per cent. capacity and which gives a corresponding point of 76 per cent. diameter; that is, a pipe to carry 50 per cent. of the capacity with the same friction per foot must have 76 per cent. of the diameter, which may be easily calculated or be read directly from the chart for various pipe sizes. It will be seen that straight lines are drawn for pipe sizes from 20 inches up to 80 inches in diameter. Supposing the size of the main pipe is 60 inches in diameter, then following to the line of 60-inch pipe, we find from the scale above a diameter of 46 inches, which is the size of pipe which has half the capacity of a 60-inch pipe with the same friction per foot. By this method the sizes may be read off rapidly without any intermediate calculation.

Example. Let the main pipe from the fan be 48 inches in diameter in the form of a straight duct having ten equal outlets. The first section of piping is 48 inches, the second section has a capacity of 90 per cent., the third section 80 per cent., the fourth 70 per cent. and so on. Corresponding to 90 per cent. we find a diameter of 96 per cent. which for a 48-inch pipe gives us 46 inches for the second section. For the third section we have 80 per cent. capacity corresponding to 91 per cent. diameter, or again following from left to right to the 48-inch line, we find a diameter of approximately 44 inches. For the fourth section we have 70 per cent. capacity with a corresponding pipe size of $86\frac{1}{2}$ per cent. of the main pipe and a diameter of between 41



inches and 42 inches determined as before. For the last section we have 10 per cent. capacity or 40 per cent. diameter, which gives a diameter of between 19 inches and 20 inches.

The sizes of the outlets are not calculated by means of this diagram, but are proportioned so as to give the desired velocity to the air leaving the outlets. This velocity will be determined by the size of the room and consequent distance the air is to be carried, and by the required freedom from drafts due to high velocity of the air leaving the outlets. Outlet velocities varying from 500 to 1400 feet per minute are ordinarily used, depending on the circumstances. The most commonly used velocityat the outlet is about 1000 feet per minute.

As already stated, the above system of proportioning piping applies to the reduction in size of the main pipe where a series of outlets are taken off, or to branch pipes of equal length. When these branch pipes are of unequal length, a correction should be applied as explained in the next paragraph under "Equalizing Friction for Unequal Length."

Equalizing Friction for Unequal Length

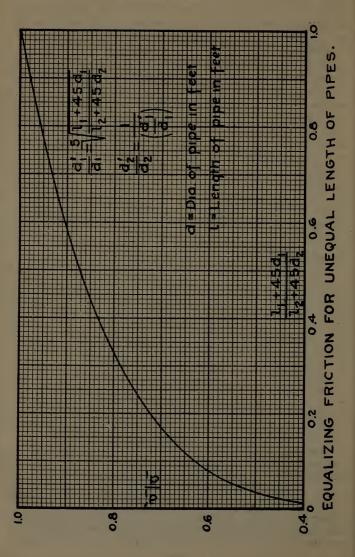
The above system of proportioning piping refers to cases where outlets or branch pipes are of equal length. In case one or more of these branch pipes are of unequal length the shorter pipes will tend to discharge more air than intended. It will then be necessary to so design the various branches that the frictional resistance in each will be equal, or adopt the common practice of placing a damper in each pipe and partly closing it in the pipes which deliver too much air.

The better way of equalizing the friction through a system having runs of unequal length is so to proportion the different runs that the resistance of each is the same. This may be accomplished either by using a smaller pipe and higher velocity in the short pipes, or by making the long run of greater diameter with a corresponding lower velocity and pressure loss.

The change in diameter required to accomplish this equalization of friction loss due to unequal lengths of piping may be computed by means of the following formula,

$$\frac{d_1'}{d_1} = \sqrt[5]{\frac{l_1 + 45 \ d_1}{l_2 + 45 \ d_2}} \tag{72}$$

where d_1 and d_2 are the diameters, and l_1 and l_2 the lengths of the two runs of piping, both expressed in feet, as originally laid out, and d_1' is the diameter d_1 , corrected so as to equalize friction



between the two branches. The regular method of proportioning piping as described on pages 135 to 139 results in equal friction per foot of length, but formula (72) gives equal friction, and therefore the desired distribution, for different lengths of piping.

This formula may be readily solved by means of the curve on page 140, which gives the fifth root of the various ratios of $(l_1+45 d_1)$ to $(l_2+45 d_2)$. This ratio should be applied after the piping has been laid out for equal friction per running foot according to the method explained in the preceding section.

Example. Assuming a piping system has been proportioned for equal friction per foot of length according to the method explained in the example on page 137, and that there are a number of branch pipes ten feet long and one branch pipe to a distant room is 50 feet long. To carry the desired amount of air, according to the method already referred to, we will assume the short pipes are to be 15 inches and the long pipe 12 inches in diameter. While friction in this long run will be the same per lineal foot, owing to the fact that it is longer than the other branches, total friction will be greater and air delivery will be less than desired.

Letting $l_1 = 10$ and $d_1 = 1.25$ as the length and diameter of the short branch, and $l_2 = 50$ and $d_2 = 1$ as the length and diameter of the long branch, we may determine the corrected diameter d_1' by means of the factor obtained from the curve on page 140. We will have

$$\frac{l_1 + 45 d_1}{l_2 + 45 d_2} = \frac{10 + 56.3}{50 + 45} = 0.698$$

and from the curve (page 140) the corresponding ratio

$$\frac{d_1'}{d_1} = 0.93 \text{ or } \frac{d_2'}{d_2} = \frac{1}{0.93} = 1.075$$

In this case diameter of the longer branch should be increased to $d_{2'} = 12 \times 1.075 = 12.9$ inches.

Piping Layout

Values in the tables on pages 144 to 152 are taken from the diagram and for rapid work may be found more convenient than the curves. They give directly the diameter of the branch pipe required to carry, with equal friction, any given percentage of the air carried in the main pipe whose diameter will be found across the top of the table.

In reducing from one pipe size to another the taper should be $1\frac{1}{2}$ inches to the foot until the area is reduced to the size required.

The branches should leave the main at any angle less than 45°, preferably 30°, but it is not necessary to adhere to this rigidly.

Elbows of 90° should be made with a radius of $1\frac{1}{2}$ diameters to the center of the pipe. In mains having high velocity two diameters is a better radius.

Outlets which discharge directly from the main or branches, as is often the case in industrial buildings, should be made about two diameters in length.

By the foregoing method of proportioning piping, it becomes unnecessary to consider the resistance of each section of pipe independently as the friction is constant per foot of length. It is simply necessary to know the length of the longest run of piping in feet, number and sizes of elbows, and diameter and velocity in the largest pipe, as the loss is exactly the same as though the entire amount of air was carried through the largest pipe the entire distance. It is usual to make the area of the largest pipe approximately equal to the area of the fan outlet.

Example. As an example of this method of figuring, assume 120 feet as the length of piping to the farthest outlet with a main pipe of 48 inches diameter and with three reductions of 39, 30 and 20 inches diameter, each containing one 90° elbow. We may then compute the friction in the following manner:

The main pipe is 48 inches or 4 feet in diameter.

120 feet is equivalent to $\frac{120}{4}$ or 30 diameters of 48-inch pipe.

1-48-inch elbow is equivalent to 10 diameters of 48-inch pipe.

1-39-inch elbow is equivalent to 10 diameters of 39-inch pipe or $\frac{3}{48} \times 10 = 8.13$ diameters of 48-inch pipe.

1-30-inch elbow is equivalent to 10 diameters of 30-inch pipe or $\frac{3.6}{4.5} \times 10 = 6.25$ diameters of 48-inch pipe.

1-20-inch elbow is equivalent to 10 diameters of 20-inch pipe or $\frac{20}{48} \times 10 = 4.17$ diameters of 48-inch pipe.

Then the total equivalent length will be 30+10+8.13+6.25+4.17=58.55 diameters of 48-inch pipe.

The equivalent loss in velocity head will then be $58.55 \div 50 = 1.17$

times the velocity head in the 48-inch main. Further, there is a velocity head remaining in the 20-inch pipe which gives an additional loss evidently of 2% of one velocity head or 0.42 times the velocity head in the 48-inch main. This gives a total loss in the piping system, neglecting the loss of entrance of $1.17 \pm 0.42 = 1.59$

times the velocity head in the 48-inch main. If we allow a velocity in the 48-inch main of 2000 feet per minute the corresponding velocity head will be 0.25 inch. The loss in pressure in the piping system is

 $0.25 \times 1.59 = 0.398$ inch.

Carrying Capacity of Pipes

Carrying capacity of round ducts at various velocities may be found from the tables on pages 154 and 155. Capacity of rectangular ducts may be determined from the table of equivalent sizes on pages 156 and 157. Thus if we are to handle 20000 A. P. M. at a velocity of 1800 feet per minute a round pipe 46 inches in diameter should be used. In case a rectangular duct is to be used the size may be found by selecting from the table on page 157 the proper sizes to correspond to the dimension 46 inches in the body of the table. Thus we might use a 35×50 , a 38×46 , a 42×42 , or any one of a number of other combinations.



Three-Quarter Housing Planoidal Type "L" Fan

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		40	$\begin{smallmatrix} & & & & & & \\ & & & & & & \\ & & & & & $
		39	$\begin{smallmatrix} & & & & & & \\ & & & & & & \\ & & & & & $
PIPE		38	88 111 111 111 111 111 111 111
		37	86 86 87 87 87 87 86 86 86 86 86 86 86 86 86 86
		36	860 883 883 883 883 883 883 883 883 883 88
MAIN		35	60 23 25 25 25 25 25 25 25 25 25 25
Z		34	94 111 111 111 111 111 111 111 1
AIR		33	222222200022002200220002202000220200022020
		32	222200 22200 222000 22200 22200 22200 22200 22200 22200 22200 22200 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 20000 20000 2000000
TOTAL		31	7 8 8 8 8 1110 1110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100 11100
0F		30	86 98 98 98 98 98 98 98 98 98 98 98 98 98
		29	76 86 1112 1112 1112 1112 1112 1112 1112
CENTS.	Pipe	28	88888 88888 88888 88888 88888 88888 8888
PER	ain	27	8888746 88888888888888888888888888888888
DIFFERENT PE	of M	26	11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11110 11100 11000 11000 11000 11000 11000 11000 11000 10
	Diameter of Main	25	66 1100 1100 1100 1100 1100 1100 1100 1
HE	iame	24	102 102 102 102 102 102 102 102 102 102
DI	Q	23	
FOR		22	00000000000000000000000000000000000000
		21	44
PIPE		20	333333555555555555555555555555555555555
NCH		10	23656566611111110000000000000000000000000
BRANCH		18	20001111111000000000000888884444000
OF I		17	00000000000000000000000000000000000000
		16	100000000000000000000000000000000000000
DIAMETER		15	000000000000000000000000000000000000000
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		13	COCCON000000000000000000000000000000000
		12	00000000000000000000000000000000000000
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FAN ENGINEERING-BUFFALO FORGE COMPANY

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DIAMETER	OF	BRANCH	PIPES

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	68	44444444444444444444444444444444444444
	67	444440 444440 44440 44440 44440 44440 44440 44440 4400 44000 44000 4400000000
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	65	4440 4400 44000 4400 4400 4400 4400 4400 4400 4400 4400 4400 44000
	64	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4
	63	4 4 1 4 4 1 1 4 1 1
	62	400 440 3333333333333333333333333333333
	61	33333333333333333333333333333333333333
	60	33833335555333335555555555555555555555
	59	33333333333333333333333333333333333333
be	58	33735555757555555555555555555555555555
n Pipe	57	33885555555555555555555555555555555555
Diameter of Main	56	30000000000000000000000000000000000000
	55	33333333333333333333333333333333333333
	54	$1111\\11111111111111111111111111111111$
	53	$\substack{111\\133}\\333333333333333333333333333333$
	52	2210 2220 2200 2000
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	50	$\begin{smallmatrix} & 111 \\ 116 \\ 117 \\ 118 \\ 118 \\ 118 \\ 118 \\ 118 \\ 118 \\ 118 \\ 128 \\ $
	49	$\begin{smallmatrix} & 115\\ & 115\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 116\\ & 226\\ & 225\\ & 226$
	48	$\begin{smallmatrix} & 110\\ & 115\\ & 116$
	47	$\begin{array}{c} 110\\ 110\\ 110\\ 110\\ 110\\ 110\\ 110\\ 110$
	46	$\begin{array}{c} 110\\ 110\\ 110\\ 110\\ 110\\ 110\\ 110\\ 110$
	45	$\begin{array}{c} 100 \\ 110 \\ 111 \\$
	44	90111111111111111111111111111111111111
	43	$\begin{smallmatrix} & 0 \\ & 0 \\ & 112 $
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	41	6 111 111 111 111 111 111 111 111 111 1
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1		98	11 15 12 15 15 15 15 15 15 15 15 15 15 15 15 15
		67	1112 1112 1112 1112 1112 1112 1112 111
		96	661 662 661 661
		95	60000000000000000000000000000000000000
		94	00000000000000000000000000000000000000
		93	00000000000000000000000000000000000000
		92	10000000000000000000000000000000000000
		16	100000004000001444444444446000000000000
		06	40000000000004444444444460000000000000
		68	420000000000000000000000000000000000000
CENTS. OF		88	22222222222222222222222222222222222222
	Pipe	87	21000088888888844444444444446600000000000
		86	112222222222222222222222222222222222222
	f Ma	85	110/0/0/2/2/2/2/2/2/2/2/2/2/2/2/2/2/2/2/
i	Diameter of Main	84	1112 1112
	umet	83	102020202020202020202020202020202020202
:	Dia	82	22222222222222222222222222222222222222
		8	1102020288888884444444444444444444444444
		80	1100002888888888444444444444444444444444
		10	10024202828282828282828282828282828282828
		78	555499 55569 55569 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55699 55695 56695
1		77	1112747373888888888888888888888888888888888
. ,		76	44444444444444444444444444444444444444
		75	444445583333333333321111111111111111111111111
		74	444455 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 44445 4445 4445 4445 4445 4445 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44556 44566 44566 445666 445666 44566666666
		73	44445 48455 48455 48455 48455 48455 48455 48455 48455 48455 48455 485555 485555 485555 485555 485555 485555 48555555 4855555 4855555555
		72	1111 115 115 115 115 115 115 115 115 11
		1	4444 445 445 445 445 445 445 445 445 44
		20	111 114 114 114 114 114 114 114 114 114
	1iA lo	26	333330 333330 333330 333330 333330 333330 333330 333330 333330 333330 333330 333330 33300 33000 30000 3000000

FAN ENGINEERING-BUFFALO FORGE COMPANY

DIAMETER OF BRANCH PIPE FOR DIFFERENT PER CENTS. OF TOTAL AIR IN MAIN PIPE

	DIAMETER	OF BR	ANCH	PIPES
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	40	32422222222222222222222222222222222222
	39	333333333333333333333333333333333333333
	38	333333333333333333333333355555555555555
	37	333333333333333333333333333333333333333
	36	44445555555555555555555555555555555555
	35	83844444888888888888888888888888888888
	34	88888888888888888888888888888888888888
	33	822222222222222222222222222222222222222
	32	212222288883222222222222222222222222222
	31	222222822222222222222222222222222222222
	30	888888888888888888888888888888888888888
	29	10 10 20 20 20 20 20 20 20 20 20 20 20 20 20
Pipe	28	19
ain	27	81288888888888888888888888888888888888
of M	26	88888888888888888888888888888888888888
Diameter of Main Pipe	25	11111111111111111111111111111111111111
iam	24	Level 100 100 100 100 100 100 100 100 100 10
a	23	$\begin{array}{c} 15\\ 166\\ 166\\ 166\\ 117\\ 117\\ 119\\ 119\\ 119\\ 119\\ 119\\ 119$
	22	199991123112511551155115511551155115511551155
	21	11551155115511551155115511551155115511
	20	$\begin{array}{c} 113\\ 1155\\ $
	10	$\begin{array}{c} 113\\ 113\\ 115\\ 115\\ 115\\ 115\\ 115\\ 115\\$
	18	$\begin{array}{c} 1122\\ 1122\\ 1155\\$
	17	
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	12	88889999999999999999999999999999999999
riA îc	2%	3375 2375 2375 2375 2375 2375 2375 2375

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MAIN PIPE		6 9 9 9 9 9 9 9 9 8 8 9 1 1 9 8 9 1
		6 444444444444444444466666666666666666
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		$\begin{array}{c} 6 \\ $
AIR IN		$\begin{array}{ c c c c c c c c c c c c c c c c c c c$
		$\begin{array}{c} 61 \\$
OF TOTAL		$\begin{array}{c} 60 \\$
		$\begin{array}{c} 50 \\$
		58 333333333333333333333333333333333333
DIAMETER OF BRANCH PIPE FOR DIFFERENT PER CENTS.	Diameter of Main Pipe	$\begin{array}{c} & & & & & & \\ & & & & & & \\ & & & & & $
		$\begin{array}{c} 56 \\ 57 \\$
		$\begin{array}{c} 55 \\ 3377 \\ 3373 \\ \mathbf$
	er o	$\begin{array}{c} & \begin{array}{c} & & & \\ & & & & \\ & & & \\ & & & & \\ & & & \\ & & & & $
	amet	$\begin{array}{c} 53\\ 53\\ 55\\ $
	Di	5 5 5 5 5 5 5 5 5 5
		5 5 5 5 5 5 5 5 5 5
		50 51 52 52 53 55 55 55 55 55 55 55
H		64 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65 65
ANC		84 85 85 85 85 85 85 85 85 85 85
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ETE		45 33 33 33 33 33 33 33 3
IAM		$\begin{array}{c} \begin{array}{c} & & & \\ & & & & \\ & & & & & \\ & & & & \\ & & & & & \\ & & & & \\ & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & \\ & & & & & $
0		43
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		4 4 4 4 4 4 4 4 4 4 4 4 4 4
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PIPE		96 653 653 653 655 777	
MAIN		95 665565555555555555555555555555555555	
		94 662 663 665 665 665 665 665 665 665 665 665	
NI		93 660 661 665 665 665 665 665 665 665 665 665	
AIR		92 92 92 92 92 92 92 92 92 92	
TOTAL		991 91 91 91 91 91 91 91 91 91	
TO		90 90 90 90 90 90 90 90 90 90	
OF		765 777 777 777 777 777 777 777 777 777	
CENTS. OF		88825555555555555555555555555555555555	
CEN	ipe	887 6655555555555555555555555555555555555	
PER	Main Pipe	22222222222222222222222222222222222222	
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PIPE			
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9	6 555555555555555555555555555555555555
Pip	8 2222222222222222222222222222222222222
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Diameter of Main Pipe	8 0222222222222222222222222222222222222
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	7 2222222222222222222222222222222222222
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	68	$\begin{array}{c} 55999 \\$
	67	$\begin{array}{c} 573 \\ 553 \\$
	66	$\begin{array}{c} 57\\ 57\\ 55\\ 55\\ 55\\ 55\\ 55\\ 55\\ 55\\ 55\\$
	65	$\begin{array}{c} 56\\ 56\\ 56\\ 56\\ 56\\ 56\\ 56\\ 56\\ 56\\ 56\\$
	64	644663333333355555555555555555555555555
	63	63335555555555555555555555555555555555
	62	62225555555555555555555555555555555555
	61	611
	60	60000000000000000000000000000000000000
	59	55555888714 5555588855555555555555555555555555555
	58	88883333338888888888888888888888888888
4)	57	52225555555555555555555555555555555555
Pipe	56	84 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4
Main	55	55555555555555555555555555555555555555
of l	54	55555555555555555555555555555555555555
Diameter of Main	53	33333333333333333333333333333333333333
Dian	52	52525255555555555555555555555555555555
	51	511 512 512 512 512 512 512 512 512 512
	50	50 50 50 50 50 50 50 50 50 50 50 50 50 5
	49	44444444444444444444444444444444444444
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DIAMETER OF BRANCH PIPE FOR DIFFERENT PER CENTS. OF TOTAL AIR IN MAIN PIPE

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70 71 73 74 75 76 77 78 79 90 91 10 11 72 73 74 75 </th <th></th> <th>93</th> <th>333229999998888888888888888888888888888</th>		93	333229999998888888888888888888888888888
70 71 73 74 75 76 77 78 79 90 81 82 84 85 80 87 85 90 91 71 73 74 75 76 77 78 78 76 77 <th78< th=""> 76 77 78<!--</td--><th></th><td>92</td><td>932999999988888888888888888888888888888</td></th78<>		92	932999999988888888888888888888888888888
70 71 73 74 75 76 77 78 79 80 81 82 83 89 70 71 73 73 74 75 76 77 73 74 74 75 76 77 73 74 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75 76 77 73 74 75<		91	91000000000000000000000000000000000000
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70 71 72 73 74 75 76 77 78 79 80 81 82 83 84 85 86 77 73 74 75 <th75< th=""> 75 75 75<!--</td--><th>-</th><td>80</td><td>$\begin{array}{c} 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77$</td></th75<>	-	80	$\begin{array}{c} 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77\\ 77$
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$		88	$\begin{array}{c} 77\\ 766\\ 777\\ 777\\ 777\\ 777\\ 777\\ 777\\$
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	ipe	87	$\begin{array}{c} 77\\ 755\\ 777\\ 777\\ 777\\ 778\\ 777\\ 778\\ 882\\ 882$
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$		86	$\begin{array}{c} 74\\ 75\\ 75\\ 75\\ 75\\ 75\\ 75\\ 75\\ 75\\ 75\\ 75$
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	W	85	$\begin{array}{c} 7&7\\7&7&7\\7&7&7\\7&7&7&7\\7&7&7&7\\7&7&7&7\\7&7&7&7&7\\7&7&7&7&7\\7&7&7&7&7\\7&7&7&7&7&7\\7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7&7&7&7&7&7\\7&7&7&7&7&7&7&7&7&7&7&7&7&7&7&7&7&7\\7&$
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	er of	84	$\begin{array}{c} & 722\\ & 723\\ & 723\\ & 723\\ & 725\\ & $
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	Diameter of M	83	$\begin{array}{c} & 1\\ & 1\\ & 1\\ & 1\\ & 2\\ & 2\\ & 2\\ & 2\\$
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70 71 72 73 610 61 62 63 64 64 65 65 66 67 71 72 73 73 73 74 75 73 75 73 73 74 75<		75	$\begin{array}{c} 6.65\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 6.55\\ 7.75\\ 7.72\\$
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3 3		73	$\begin{array}{c} 6.3\\ 6.3\\ 6.4\\ 6.5\\ 6.5\\ 6.5\\ 6.5\\ 6.5\\ 6.5\\ 6.5\\ 6.5$
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DIAMETER OF REANCH DIRE FOR DIFFERENT DER CENTS OF TOTAL AID IN MAIN DIRE



CARRYING CAPACITY OF PIPES

This table specifies the diameters of pipes required for the passage of stated volumes of air at given velocities. The column, "Cubic feet of air per minute," indicates various quantities of air to be moved per minute. The figures at top of table give the velocities in feet per minute at which the air is to be moved, and the figures in the body of the table state the required diameters of pipes for the passage of the volumes mentioned at the given velocities.

i.i						Veloci	ties					_
Cubic Ft. of Air per Min.	500	600	800	1000	1200	1500	1800	2000	2500	3000	3500	4000
200 400 800 1200 1200 1200 2200 2200 2200 220	9 13 15 18 20 225 266 288 290 301 33 34 34 34 34 34 34 34 34 34 42 44 44 44	8 11 14 16 18 20 21 23 24 25 27 28 29 30 31 32 29 30 31 32 33 33 34 35 36 37 38 39 90 40	7 10 12 14 16 17 18 20 21 22 23 24 25 26 27 28 28 28 29 30 31 32 24 33 34 35 33 34 35 35 36 37 37 38 38 38 39 9 99 90 40 41 41 41 41 41 41 41 41 41 41 41 41 41	$\begin{array}{c} 7\\ 9\\ 9\\ 11\\ 13\\ 4\\ 15\\ 16\\ 18\\ 19\\ 20\\ 21\\ 22\\ 23\\ 24\\ 25\\ 26\\ 27\\ 28\\ 28\\ 28\\ 28\\ 29\\ 30\\ 30\\ 30\\ 31\\ 31\\ 33\\ 33\\ 33\\ 33\\ 33\\ 33\\ 33\\ 33$	$\begin{array}{c} 6\\ 8\\ 10\\ 12\\ 13\\ 14\\ 15\\ 5\\ 16\\ 17\\ 8\\ 19\\ 20\\ 22\\ 23\\ 22\\ 23\\ 22\\ 22\\ 23\\ 22\\ 22\\ 23\\ 22\\ 22$	6 8 9 9 100 122 13 14 15 15 15 16 16 17 18 19 20 201 221 222 23 24 24 24 25 526 27 7 27 7 28 28 29 29 20 30 30 31 13 22 33 30 33 11 32 23 33 30 33 11 32 23 33 30 33 31 32 23 33 30 33 31 32 33 33 30 33 31 32 33 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 33 30 30	$\begin{array}{c} 6\\ 7\\ 8\\ 9\\ 9\\ 10\\ 11\\ 12\\ 13\\ 14\\ 15\\ 15\\ 16\\ 17\\ 18\\ 19\\ 9\\ 20\\ 21\\ 21\\ 21\\ 22\\ 22\\ 22\\ 22\\ 22\\ 22\\ 22$	$\begin{smallmatrix} 6 & 7 \\ 8 & 9 \\ 9 \\ 10 \\ 11 \\ 12 \\ 13 \\ 13 \\ 14 \\ 15 \\ 15 \\ 16 \\ 16 \\ 16 \\ 17 \\ 18 \\ 19 \\ 19 \\ 20 \\ 20 \\ 21 \\ 21 \\ 22 \\ 22 \\ 23 \\ 23 \\ 24 \\ 24 \\ 24 \\ 25 \\ 25 \\ 26 \\ 26 \\ 26 \\ 26 \\ 27 \\ 27 \\ 28 \\ 28 \\ 28 \\ 28 \\ 28 \\ 28$	$\begin{smallmatrix} 6 & 6 \\ 6 & 7 \\ 8 \\ 9 \\ 101 \\ 111 \\ 123 \\ 133 \\ 144 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 155 \\ 125 \\ 222 \\ 223 \\ 233 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 223 \\ 224 \\ 244 \\ 244 \\ 255 \\ 225 \\ 25$	6 6 6 7 8 8 9 0 10 11 11 12 23 13 14 14 15 15 16 6 16 16 16 16 16 17 17 18 8 18 19 9 20 20 20 21 21 21 22 22 22 23 23	$\begin{array}{c} 6 \\ 6 \\ 6 \\ 7 \\ 8 \\ 9 \\ 9 \\ 9 \\ 9 \\ 9 \\ 10 \\ 11 \\ 11 \\ 12 \\ 13 \\ 13 \\ 14 \\ 15 \\ 15 \\ 15 \\ 16 \\ 16 \\ 16 \\ 16 \\ 17 \\ 17 \\ 8 \\ 18 \\ 18 \\ 18 \\ 18 \\ 18 $	$\begin{array}{c} 6\\ 6\\ 6\\ 7\\ 7\\ 8\\ 9\\ 9\\ 9\\ 10\\ 10\\ 11\\ 11\\ 11\\ 12\\ 12\\ 13\\ 13\\ 13\\ 13\\ 13\\ 13\\ 13\\ 13\\ 13\\ 14\\ 14\\ 15\\ 15\\ 16\\ 6\\ 16\\ 17\\ 7\\ 17\\ 7\\ 18\\ 18\\ 18\\ 18\\ 18\\ 19\\ 19\\ 19\\ 20\\ 20\\ 20\\ \end{array}$

CARRYING CAPACITY OF PIPES

				Vel	oci	ties							Ve	loc	itie	es		- K	3
Cu. Ft.					1					Cu. Ft.								-	-
of Air per	12	9	0	0	0	9	0	0	0	of Air per	12	0	0	0	0	0	0	24	-
Minute	000	200	500	800	2000	2500	3000	3500	4000	Minute	200	500	1800	2200	2500	3000	3500	8	
	1-	-	-	1	R	2	~	3	4		1-	-		2	101	3	3	1	1)
8600	40	37	33	30	29	25	23	21	20	54000	01	82	75	68	63	58	54	50	
8800		37	33	30	29	26	24	22		55000	92	82	75	68	64	58	54	51	2
9000	41		34	31	29	26	24	$\overline{22}$	21	56000	93	83	76	69	65	59	55	51	-
9200			34		30	26	24 24 25 25 25 26 28	22	21	57000	94		77			60			2
9400 9600	42		$\frac{34}{35}$	31 32	30 30	21	24	$\frac{22}{23}$	21 21	58000 59000	95 95		77 78	71		60 60		52 52	0
9800	43		36	32	30	27	25	23	21	60000	96			71	67	61		53	
10000		40	36	32	31	28	25	23	22	61000	97	87	79	72	67	62	57	53	
11000	45			33	31	29	26	24	23	62000	98	88	80	72	68	62	57	54	X
12000	47			35	34	30	28 29	$\frac{25}{27}$	$\frac{24}{25}$	63000 64000				73				54	
13000 14000	51	45 47	40	37 38	$\frac{35}{36}$	$\frac{31}{33}$	30	28	20	65000				73 74			58 59	55 55	50
15000	53	48		40	38	34	31	28	27	66000	1			75			59	56	$\overline{\mathbf{u}}$
16000	55	50		41	39	35	32	29	28	67000			1	75	71	64	60	56	5
17000		51		42	40		33	30	28	68000				76			60	56	2
18000 19000	58 60	$\frac{53}{54}$		43 44	41 42	37 38	$\frac{34}{34}$	$\frac{31}{32}$	29 30	69000 70000				76	71	65	61 61	57 57	a
20000	61				42	39	35	33	31	71000				77	73	66		57	à
21000	63		51		44	40		34	31	72000				78	73	67	62	58	~
22000	64	58	52		45	41	37	34	32	73000				78	74	67		58.	The second secon
23000				49			38	35	33	74000				79	74		63	59	60
24000 25000	67 68	$\frac{61}{62}$		50 51	$\frac{47}{48}$	42 43	39 40	$\frac{36}{37}$	$\frac{34}{34}$	75000 76000				79 80			63 64	59 60	-
26000				52	49			38	35	77000				81					. 1
27000	71	65	58	53	50	45	41	38	36	78000				81	76	70	64	60	
28000	72					46		39	36	79000				82	77		65	61	-
29000 30000	73			$\frac{55}{56}$	52		$\frac{42}{43}$	39 40	$\frac{37}{38}$	80000 81000				82 83	77	70	$\begin{array}{c} 65\\ 66\end{array}$	61^{-}	3
31000	76		62	50 57	53 54	48		40	38	82000				83			66		0
32000	77			57	55		45	41	39	83000				84	79	72			2.3
33000	78			58	56	50	45	42	39	84000				84	79		67		
34000	79			59	56	50	46	43	40	85000				85	79 80		67	63 (63	0
35000 36000	82	74	67	60 61	57 58	$\frac{51}{52}$	47 47	43 44	40 41	86000 87000				85 86	80		68	64	ð
37000	83		68	62	59	52		44	42	88000				86	81	74	68	64	5
38000	84	77	69		60	53	49	45	42	89000	1			87	81			64	0
39000	85		70		60	54		46	43	90000	1			87 88	82	75 75		65	0
40000 41000	86	79 79	71	$\frac{64}{65}$	$\frac{61}{62}$	55 55	50 50	46	43 44	91000 92000				88	83		70 70	$\frac{65}{65}$	5
42000	88			66	63	56		47	44	93000				88		76		66	2
43000	89	82	73	66	63	57	51	48	44	94000				89	84	76	71	66	0
44000	90			67	64	57	52	48	45	95000				89	$\frac{84}{84}$	77	71	66	Q_
45000 46000	91 93		75 75	68 69	$\frac{65}{65}$	58 59	53 53	49 50	46 46	96000 97000				90 90	84 85	77	$\frac{71}{72}$	67 67	
40000	93	84	76	70	05 66	59	54	50 50	40	98000				91	85		72	68	
48000	95	86	77	70	67	60	55	50	47	99000				91	86	78	72	68	
49000	95		78	71	68	60		51	48	100000				92	86	79	73	68	
50000	96		79	72	68	61	56	51	48										
51000 52000	97 98		79 80	73 73	69 70	62 62		52 53	49 49	6. C									
53000		90			70						1								

24	40000000000000000000000000000000000000
23	228.59 238.59 248.59 248.59
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5	22.6 22.6 22.6 22.6 22.6 22.6 22.6 22.6
30	2200 2200 2200 200 200 200 200 200 200
5	2010 2010 2010 2010 2010 2010 2010 2010
2	10.5 10.5
17	118.7 118.7 118.7 119.8 11.8 11.8 11.8 11.8 11.8 11.8 11.
16	1182 1182 1182 1182 1182 1182 1182 1182
15	11176 11176
-	15.4 17.4 17.4 17.4 17.4 17.4 17.4 17.4 17
13	115.2 115.3
12	18.2 18.7 18.7 19.2 19.2 20.6 20.6 20.6 20.6 20.6 20.7 20.6 20.6 20.6 20.6 20.6 20.6 20.6 20.6
=	1210 1210 1210 1210 1210 1210 1210 1210
10	11.0 12.5 12.5 12.5 12.5 12.5 12.5 12.5 12.5
7 8 9 10 11 12	9.0 10.4 11.5 11.5 11.5 11.5 11.5 11.5 11.5 11
8	8.8 9.3 9.3 9.3 9.3 9.3 9.3 111.1 111.1 111.5 11.5 11
~	882 887 987 987 987 987 987 987 987 987 987
0	7.6 8.80 8.80 9.85 9.65 9.65 9.65 9.65 9.65 11.1.4
S	60 887 887 887 887 887 887 887 887 887 88
Side Rect. Duct	880 880 880 880 880 880 880 880

CIRCULAR BOUIVALENTS OF RECTANGULAR DUCTS FOR FOUAL FRICTION

IRCUL	AR EQU	IVAL	ENTS	OFH	LECT	ANGU	LAR	DUCI
48				52.8	54.0 55.0 56.0	57.0 58.0 58.9	59.7 60.6 61.6	62.6 63.5 64.5
46				50.6 51.6	52.9 53.8 54.8	55.9 56.8 57.7	58.5 59.4 60.4	61.3 62.1 63.0
4	1			48.4 49.5 50.5	51.6 52.5 53.5	54.6 55.5 56.4	57.2 58.1 59.1	59.9 60.6 61.3
<u>5</u>			46.2	47.2 48.4 49.3	50.4 51.3 52.3	53.3 54.2 55.0	55.9 56.8 57.6	58.4 59.1 60.0
39 40			44.0 45.1	$rac{46.1}{47.2}$ 48.1	$\begin{array}{c} 49.1\\ 50.1\\ 51.1\end{array}$	52.0 52.9 53.8	54.5 55.4 56.2	56.9 57.7 58.7
38 39			43.4 44.5	45.5 46.6 47.5	$\frac{48.5}{49.5}$	51.3 52.2 53.0	53.9 54.7 55.5	56.2 57.0 57.8
38			$\frac{41.8}{42.9}$	$\begin{array}{c} 44.9 \\ 46.0 \\ 46.9 \end{array}$	47.9 48.9 49.9	50.6 51.5 52.3	53.0 53.9 54.7	55.5 56.2 57.0
37			$\begin{array}{c} 41.2 \\ 42.3 \\ 43.4 \end{array}$	44.3 45.4 46.3	47.1 48.2 49.2	49.9 50.8 51.6	52.4 53.2 53.9	54.6 55.4 56.2
33 34 35 36		39.6	$\begin{array}{c} 40.7 \\ 41.7 \\ 42.7 \end{array}$	43.7 44.8 45.6	46.5 47.5 48.4	49.1 50.0 50.9	51.7 52.4 53.1	53.8 54.5 55.4
35		39.1	$\frac{40.1}{41.1}$	$\begin{array}{c} 43.1 \\ 44.2 \\ 45.0 \end{array}$	45.9 46.8 47.6	$\frac{48.5}{49.4}$	50.9 51.7 52.4	53.1 53.7 54.6
34		37.4 38.5	$39.5 \\ 40.5 \\ 41.5$	42.5 43.5 44.4	45.2 46.1 47.0	47.7 48.5 49.3	50.0 50.9 51.6	$52.2 \\ 52.9 \\ 53.7 \\$
33		36.8 37.9	39.0 39.9 40.9	$\frac{41.8}{42.9}$	44.5 45.4 46.4	46.9 47.8 48.5	$\frac{49.3}{50.0}$	51.4 52.0 52.8
32		35.2 36.3 37.3	$\frac{38.4}{39.3}$	$\frac{41.2}{42.2}$	43.8 44.7 45.5	46.2 47.0 47.8	$\frac{48.4}{49.2}$	50.7 51.3 51.9
31		34.6 35.7 36.7	$\frac{37.7}{38.6}$ 39.6	$\begin{array}{c} 40.5 \\ 41.5 \\ 42.3 \end{array}$	43.0 43.9 44.7	45.4 46.2 46.9	47.6 48.4 49.1	49.7 50.4 51.0
30	33.0	$\frac{34.1}{35.1}$	$\begin{array}{c} 37.1 \\ 38.0 \\ 39.0 \end{array}$	$39.9 \\ 40.8 \\ 41.5$	$\begin{array}{c} 42.3 \\ 43.1 \\ 44.0 \end{array}$	44.6 45.4 46.1	46.8 47.5 48.2	$\frac{48.9}{49.5}$
29	32,5	33.5 34.5 35.5	36.5 37.4 38.3	$39.2 \\ 40.0 \\ 40.8$	41.5 42.3 43.2	43.8 44.5 45.4	46.0 46.7 47.3	48.0 48.7 49.3
28 29	30.8 31.9	$32.9 \\ 33.9 \\ 34.9 \\ 34.9$	35.9 36.7 37.6	38.5 39.3 40.0	40.8 41.6 42.4	43.0 43.8 44.5	$45.1 \\ 45.8 \\ 46.5 \\ 46.5 \\ 100000000000000000000000000000000000$	47.2 47.8 48.4
27	30.2 31.3	32.3 33.3 34.3	35.3 36.0 36.8	37.7 38.5 39.2	$ \begin{array}{c} 40.0 \\ 40.8 \\ 41.5 \end{array} $	$\begin{array}{c} 42.1 \\ 42.9 \\ 43.6 \end{array}$	44.3 44.9 45.6	46.3 46.9 47.5
26	28.6 29.7 30.7	$\frac{31.7}{32.7}$	34.6 35.3 36.0	$\frac{36.9}{37.8}$	$39.2 \\ 40.0 \\ 40.7$	41.3 42.1 42.7	43.4 44.0 44.7	45.3 46.0 46.5
35	28.1 29.1 30.1	$31.1 \\ 32.0 \\ 32.9 \\ 32.9$	$33.8 \\ 34.6 \\ 35.2 \\ 35.2 \\$	36.1 37.0 37.8	38.4 39.1 39.8	40.4 41.2 41.8	42.5 43.1 43.7	44.4 45.0 45.5
Duct.	30855	32 33	38 40 42	44 46 48	5252	56 58 60	62 64 66	68 72 72

Sizes and Weights of Piping

Conduits through which air is conveyed may be either round or rectangular, depending on conditions to be met, and the terms piping or ducts are used for either cross section. The accompanying table gives the gauge of iron generally used for galvanized iron piping in heating and ventilating work, and also the weight per lineal foot of such pipes. For method of proportioning piping see page 135.

WEIGHT PER LINEAL FOOT AND GAUGES FOR GALVANIZED IRON PIPES ORDINARILY USED IN HEATING AND VENTILATING

Diam.	26 Gauge	Diam.	24 Gauge	Diam.	22 Gauge	Diam.	20 Gauge	Diam.	18 Gauge
$10 \\ 11 \\ 12$	$2.70 \\ 2.96 \\ 3.22$	20 21 22	7.02 7.26 7.70	30 31 32	$12.17 \\ 12.54 \\ 12.93$	40 41 42	$18.76 \\ 19.20 \\ 19.61$	$50 \\ 51 \\ 52$	$30.90 \\ 31.40 \\ 32.00$
$\begin{array}{c} 13\\14\\15\end{array}$	$3.48 \\ 3.74 \\ 4.01$	$23 \\ 24 \\ 25$	8.04 8.38 8.72	33 34 35	$13.34 \\ 13.73 \\ 14.10$	43 44 45	$20.30 \\ 20.74 \\ 21.20$	53 54 55	$32.66 \\ 33.20 \\ 34.10$
16 17 18 19	4.27 4.53 4.87 5.14	26 27 28 29	$9.05 \\ 9.40 \\ 9.75 \\ 10.07$	36 37 38 39	$14.50 \\ 14.90 \\ 15.29 \\ 15.60$	46 47 48 49	$\begin{array}{c} 21.62 \\ 22.10 \\ 22.60 \\ 23.00 \end{array}$	56 57 58 59	34.65 35.21 35.84 36.40

GAUGES OF IRON USED FOR PIPING

He	ating and	Planing-Mill and Other Exhaust Systems			
Round Du	cts				
Diam., Inches	Gauge	Width, Inches	Gauge	Diam., Inches	Gauge
6 to 19 20 to 29 30 to 39 40 to 49 50 and above	26 24 22 20 18	4 to 18 19 to 30 31 to 60 61 to 118 118 and above	26 24 22 20 18	Up to 8 9 to 14 15 to 20 21 to 30	24 22 20 18

The tables on pages 160 and 161 give the weight of galvanized iron pipes in pounds per lineal foot for the various gauges ordinarily used in duct work, as also the square feet of surface per lineal foot for pipes from 4 to 86 inches in diameter. The weight per square foot for the different gauges is given at the bottom of the second table. The figures to the right of the heavy line indicate the gauge of iron ordinarily used in heating and ventilating work. Thus a pipe 20 to 29 inches in diameter would be made of 24 gauge and a pipe from 30 to 39 inches of 22 gauge iron. The dotted line indicates the gauge to be used for planing-mill or other exhaust work. Other gauges than those indicated may be used under special circumstances, but those shown as above represent good average practice. The small table on page 158 gives the same information regarding weights of iron in tabular forms as explained above.

In the table on page 162 will be found the weights of black steel pipe of various diameters and gauges in pounds per lineal foot, and also the material used in square feet per running foot for the different sizes. The tables on pages 163 to 167 give the weight in pounds per lineal foot of rectangular galvanized iron ducts. These tables also show the gauge of iron ordinarily used for the different sizes of ducts. Thus a pipe say 20×50 inches would be made of No. 22 gauge iron and would weigh 17.5 pounds per lineal foot, while for a pipe 20×70 inches No. 20 gauge would be used, and the weight would be 26.3 pounds per running foot.



Niagara Conoidal Type "N" Fan

WEIGHT OF GALVANIZED IRON PIPES-POUNDS PER LINEAL FOOT

Diam.	Sq. Ft.		Nu	mber of G	auge, U. S.	. S.	
of Pipe	per Running Ft.	26	24	22	20	18	16
4 5 6	$1.13 \\ 1.39 \\ 1.65$	$1.13 \\ 1.39 \\ 1.65$	$1.47 \\ 1.80 \\ 2.14$	$1.69 \\ 2.08 \\ 2.47$	$1.97 \\ 2.43 \\ 2.89$	$2.56 \\ 3.19 \\ 3.79$	$3.10 \\ 3.82 \\ 4.54$
7 8 9	$1.91 \\ 2.18 \\ 2.44$	$1.91 \\ 2.18 \\ 2.44$	$2.48 \\ 2.83 \\ 3.17$	-2.86 3.27 3.66	$3.34 \\ 3.81 \\ 4.27$	$4.39 \\ 5.01 \\ 5.61$	$5.25 \\ 6.00 \\ 6.71$
10 11 12	$2.70 \\ 2.96 \\ 3.22$	$2.70 \\ 2.96 \\ 3.22$	$3.51 \\ 3.85 \\ 4.18$	$4.05 \\ 4.44 \\ 4.83$	4.72 5.18 5.63	$\begin{array}{c} 6.21 \\ 6.80 \\ 7.40 \end{array}$	7.42 8.14 8.85
13 14 15	$3.48 \\ 3.74 \\ 4.01$	$3.48 \\ 3.74 \\ 4.01$	$4.52 \\ 4.86 \\ 5.21$	$5.22 \\ 5.61 \\ 6.01$	6.09 6.54 7.01	8.00 8.60 9.22	9.57 10.28 10.86
16 17 18	4.27 4.53 4.87	4.27 4.53 4.87	5.55 5.85 6.33	6.40 6.79 7.30	7.47 7.92 8.51	9.82 10.42 11.18	$ \begin{array}{r} 11.74 \\ 12.45 \\ 13.36 \end{array} $
19 20 21	$5.14 \\ 5.40 \\ 5.59$	5.14 5.40 5.59	6.68 7.02 7.26	7.71 8.10 8.39	9.00 9.45 9.78	11.80 12.42 12.85	14.11 14.85 15.36
22 23 24	5.92 6.18 6.45	5.92 6.18 6.45	7.70 8.04 8.38	8.88 9.27 9.67	10.35 10.81 11.30	$12.60 \\ 14.40 \\ 14.84$	16.25 17.00 17.71
25 26 27	$\begin{array}{c} 6.71 \\ 6.97 \\ 7.33 \end{array}$	$6.71 \\ 6.97 \\ 7.33$	8.72 9.05 9.40	$10.06 \\ 10.45 \\ 10.85$	$11.74 \\ 12.20 \\ 12.67$	$15.41 \\ 16.00 \\ 16.62$	18.41 19.15 19.87
28 29 30	7.50 7.75 8.10	7.50 7.75 8.10	9.75 <u>10.07</u> 10.54	$11.27 \\ 11.63 \\ 12.17$	$13.13 \\ 13.58 \\ 14.20$	$17.26 \\ 17.81 \\ 18.62$	$20.60 \\ 21.30 \\ 22.25$
31 32 33	8.36 8.62 8.88	8.36 8.62 8.88	$10.87 \\ 11.20 \\ 11.56$	$12.54 \\ 12.93 \\ 13.34$	$14.63 \\ 15.10 \\ 15.56$	19.20 19.84 20.42	$23.00 \\ 23.70 \\ 24.40$
34 35 36	9.15 9.41 9.67	9.15 9.41 9.67	$11.90 \\ 12.23 \\ 12.57$	$13.73 \\ 14.10 \\ 14.50$	$16.00 \\ 16.48 \\ 16.91$	$21.08 \\ 21.65 \\ 22.22$	$25.18 \\ 25.85 \\ 26.60$
37 38 39	9.93 10.19 10.46	9.93 10.19 10.46	$12.91 \\ 13.25 \\ 13.60$	$14.90 \\ 15.29 \\ 15.60$	17.40 17.81 18.31	$22.84 \\ 23.40 \\ 24.02$	$27.30 \\ 28.00 \\ 28.70$

NOTE: For explanation of heavy and dotted lines, see page 159.

Diam.	Sq. Ft. per		Nui	mber of Ga	uge, U. S.	s.	
of Pipe	Running Ft.	26	24	22	20	18	16
40 41 42	$10.72 \\ 10.98 \\ 11.24$	$10.72 \\ 10.98 \\ 11.24$	$13.95 \\ 14.27 \\ 14.60$	$16.08 \\ 16.47 \\ 16.86$	18.76 19.20 19.61	$24.68 \\ 25.25 \\ 25.86$	29.50 30.20 30.90
43 44 45	11.59 11.85 12.11	11.59 11.85 12.11	$15.06 \\ 15.40 \\ 15.75$	$17.38 \\ 17.78 \\ 18.17$	$20.30 \\ 20.74 \\ 21.20$	26.60 27.25 27.90	31.80 32.60 33.30
46 47 48	$\begin{array}{c} 12.37 \\ 12.63 \\ 12.90 \end{array}$	$12.37 \\ 12.63 \\ 12.90$	$16.10 \\ 16.40 \\ 16.78$	$18.55 \\ 18.95 \\ 19.35$	$21.62 \\ 22.10 \\ 22.60$	28.43 29.00 29.70	$34.00 \\ 34.70 \\ 35.50$
49 50 51	13.15 13.41 13.66	$13.15 \\ 13.41 \\ 13.66$	17.10 17.45 17.75	19.72 20.12 20.49	23.00 23.50 23.90	$30.25 \\ 30.90 \\ 31.40$	36.20 36.90 37.50
52 53 54	$13.94 \\ 14.20 \\ 14.46$	$13.94 \\ 14.20 \\ 14.46$	$\begin{array}{c} 18.12 \\ 18.46 \\ 18.80 \end{array}$	20.97 21.30 21.69	$24.40 \\ 24.90 \\ 25.30$	$32.00 \\ 32.66 \\ 33.20$	38.30 39.00 39.70
55 56 57	$14.81 \\ 15.07 \\ 15.33$	14.81 15.07 15.33	19.28 19.60 19.95	$22.22 \\ 22.61 \\ 23.00$	$25.94 \\ 26.40 \\ 26.80$	$34.10 \\ 34.65 \\ 35.21$	$\begin{array}{r} 40.80 \\ 41.40 \\ 42.10 \end{array}$
58 59 60	$15.58 \\ 15.83 \\ 16.12$	$ \begin{array}{r} 15.58 \\ 15.83 \\ 16.12 \end{array} $	20.30 20.55 20.95	$23.37 \\ 23.74 \\ 24.18$	27.30 27.70 28.20	$35.84 \\ 36.40 \\ 37.00$	42.80 43.50 44.30
62 64 66	$16.65 \\ 17.16 \\ 17.66$	$16.65 \\ 17.16 \\ 17.66$	21.65 22.30 22.97	$24.97 \\ 25.74 \\ 26.49$	29.10 30.00 30.90	$38.20 \\ 39.50 \\ 40.60$	45.70 47.20 48.50
68 70 72	$\begin{array}{c} 18.21 \\ 18.75 \\ 19.25 \end{array}$	$\begin{array}{c} 18.21 \\ 18.75 \\ 19.25 \end{array}$	$23.65 \\ 24.40 \\ 25.02$	$27.31 \\ 28.12 \\ 29.92$	31.83 32.80 33.70	$\begin{array}{c} 41.80 \\ 43.10 \\ 44.30 \end{array}$	$50.00 \\ 51.50 \\ 53.00$
74 76 78	$19.79 \\ 20.41 \\ 21.00$	19.79 20.41 21.00	25.70 26.60 27.30	$29.68 \\ 30.60 \\ 31.50$	$34.65 \\ 35.62 \\ 35.75$	$\begin{array}{r} 45.50 \\ 45.77 \\ 46.96 \end{array}$	$54.50 \\ 54.73 \\ 55.13$
80 82 84	$21.5 \\ 22.0 \\ 22.6$	$21.5 \\ 22.0 \\ 22.6$	28.0 28.6 29.4	32.3 33.0 33.9	36.65 37.57 38.50	$\begin{array}{r} 48.16 \\ 49.40 \\ 50.60 \end{array}$	$56.63 \\ 58.00 \\ 59.40$
86	23.0	23.0	29.9	34.5	39.39	51.77	60.77
W'ght p	ber Sq. Ft.	1.00	1.30	1.50	1.75	2.30	2.70

WEIGHT OF GALVANIZED IRON PIPES-POUNDS PER LINEAL FOOT

NOTE: For explanation of heavy line, see page 159.

WEIGHT OF BLACK STEEL PIPES-POUNDS PER LINEAL FOOT

	per		N	umber o	mber of Gauge, U. S. S.					
of Pipe	Running Ft.	24	22	20	18	16	14	12		
$\begin{array}{c} 4\\ 5\\ 6\\ 7\\ 8\\ 9\\ 10\\ 11\\ 12\\ 13\\ 14\\ 15\\ 16\\ 17\\ 18\\ 9\\ 20\\ 12\\ 23\\ 42\\ 52\\ 26\\ 27\\ 28\\ 9\\ 30\\ 1\\ 32\\ 33\\ 43\\ 56\\ 37\\ 8\\ 39\\ 40\\ 1\\ 42\\ 44\\ 44\\ 55\\ 1\\ 55\\ 46\\ 60\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 64\\ 40\\ 50\\ 51\\ 55\\ 56\\ 86\\ 66\\ 26\\ 66\\ 40\\ 50\\ 50\\ 50\\ 50\\ 50\\ 50\\ 50\\ 50\\ 50\\ 5$	$\begin{array}{c} 1.13\\ 1.39\\ 1.65\\ 1.91\\ 2.18\\ 2.44\\ 2.70\\ 2.96\\ 3.48\\ 3.74\\ 4.01\\ 4.27\\ 4.53\\ 4.87\\ 5.14\\ 5.59\\ 6.18\\ 6.45\\ 6.71\\ 7.23\\ 7.50\\ 8.10\\ 8.86\\ 8.82\\ 8.88\\ 9.15\\ 9.41\\ 9.67\\ 9.93\\ 10.19\\ 10.46\\ 10.72\\ 10.98\\ 11.24\\ 11.55\\ 12.11\\ 12.37\\ 12.63\\ 12.11\\ 12.37\\ 12.63\\ 13.94\\ 11.59\\ 11.58\\ 13.94\\ 11.58\\ 13.94\\ 14.46\\ 15.58\\ 16.12\\ 16.65\\ 17.16\\ 16.58\\ 17.16\\ 16.58\\ 17.16\\ 16.58\\ 17.16\\ 16.58\\ 17.16\\ 10.58\\ 10.12\\ 10.$	$\begin{array}{c} 1.30\\ 1.60\\ 1.90\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 2.50\\ 1.0\\ 3.10\\ 3.70\\ 4.00\\ 4.61\\ 4.91\\ 5.21\\ 5.60\\ 5.91\\ 6.21\\ 6.43\\ 7.11\\ 7.71\\ 8.31\\ 8.62\\ 1.11\\ 7.71\\ 8.31\\ 8.31\\ 8.31\\ 8.31\\ 8.31\\ 8.31\\ 8.31\\ 1.22\\ $	$\begin{array}{c} 1.58\\ 1.95\\ 2.31\\ 2.67\\ 3.05\\ 3.42\\ 3.78\\ 4.15\\ 4.50\\ 4.88\\ 5.23\\ 5.61\\ 5.97\\ 6.35\\ 6.81\\ 7.20\\ 7.56\\ 8.86\\ 9.04\\ 9.40\\ 9.75\\ 10.11\\ 10.50\\ 11.34\\ 9.40\\ 9.75\\ 10.11\\ 10.55\\ 11.34\\ 13.5$	$\begin{array}{c} 1.86\\ 2.29\\ 2.72\\ 3.15\\ 3.60\\ 4.03\\ 4.45\\ 4.88\\ 4.88\\ 5.31\\ 5.74\\ 6.61\\ 7.04\\ 8.03\\ 8.48\\ 8.90\\ 9.22\\ 10.03\\ 11.06\\ 11.93\\ 12.38\\ 14.25\\ 11.02\\ 1.02\\$	$\begin{array}{c} 2.43\\ 2.99\\ 3.54\\ 4.10\\ 4.68\\ 5.25\\ 5.80\\ 6.36\\ 6.91\\ 7.48\\ 8.63\\ 8.61\\ 9.74\\ 9.16\\ 8.61\\ 9.74\\ 10.45\\ 11.04\\ 11.60\\ 12.70\\ 13.29\\ 11.04\\ 11.60\\ 12.70\\ 13.29\\ 11.04\\ 11.60\\ 12.70\\ 13.29\\ 11.04\\ 11.60\\ 12.70\\ 13.29\\ 10.20\\ 22.50\\ 12.2$	$\begin{array}{c} 2.99\\ 3.68\\ 4.36\\ 5.05\\ 5.77\\ 6.47\\ 7.15\\ 7.85\\ 2.9.21\\ 9.90\\ 10.61\\ 11.209\\ 12.00\\ 14.30\\ 14.30\\ 14.30\\ 15.65\\ 16.38\\ 17.08\\ 17.75\\ 22.85\\ 22.15\\ 22.83\\ 23.50\\ 21.45\\ 22.83\\ 23.50\\ 21.45\\ 22.83\\ 23.60\\ 27.74\\ 28.40\\ 25.60\\ 27.74\\ 28.40\\ 25.60\\ 27.74\\ 28.40\\ 25.60\\ 27.74\\ 28.40\\ 25.60\\ 27.00\\ 31.40\\ 32.80\\ 33.45\\ 35.55\\ 36.20\\ 33.420\\ 33.420\\ 33.45\\ 35.55\\ 36.20\\ 36.90\\ 33.420\\ 38.30\\ 39.90\\ 39.90\\ 41.30\\ 42.75\\ 44.10\\ 44.10\\ 42.55\\ 44.10\\ 42.55\\ 50.55\\$	$\begin{array}{c} 3.62\\ 3.62\\ 4.45\\ 5.28\\ 1.0\\ 1.0\\ 1.0\\ 1.0\\ 1.0\\ 1.0\\ 1.0\\ 1.0$	$\begin{array}{c} 5.08\\ 6.25\\ 7.42\\ 8.58\\ 9.80\\ 10.98\\ 9.80\\ 12.15\\ 12.15\\ 13.31\\ 14.48\\ 15.66\\ 16.43\\ 19.17\\ 20.7\\ 23.10\\ 24.30\\ 25.10\\ 23.10\\ 24.30\\ 25.10\\ 23.10\\ 24.30\\ 25.10\\ 30.20\\ 30.20\\ 30.20\\ 30.20\\ 33.750\\ 35$		
66 68 70 72 74	17.1617.6618.2118.7519.2519.79	$ \begin{array}{r} 19.72 \\ 20.30 \\ 20.95 \\ 21.55 \\ 22.15 \\ 22.75 \\ \end{array} $	$\begin{array}{r} 24.00\\ 24.70\\ 25.50\\ 26.25\\ 27.00\\ 27.70\end{array}$	$\begin{array}{r} 28.30 \\ 29.15 \\ 30.00 \\ 30.90 \\ 31.80 \\ 32.65 \end{array}$	36.90 38.00 39.15 40.30 41.40 42.60	45.50 46.80 48.25 49.70 51.00 52.40	$\begin{array}{c} 54.90 \\ 56.50 \\ 58.30 \\ 60.00 \\ 61.60 \\ 63.30 \end{array}$	79.40 81.80 84.30 86.60 89.00		

DUCTS	
RECTANGULAR	
IRON	
GALVANIZED	Standard Gauge
FOR	U. S.
FOOT	
LINEAL	
PER	
VEIGHT	

	81	4.04.04.34	4.67 5.0 5.67 5.67	0.0	30	7.8 8.24 8.24 8.24 8.84 8.84 8.89 9.10 9.91 10.85 11.12 9.95 11.12
	17	3.84 4.0 4.17 4.34	4.5 4.67 5.17 5.5 5.5	10.0	29	2220066252338975859
	16	3.67 3.84 4.0 4.17	4.34 4.5 5.0 5.34 5.67	0.0		7.59 8.24 8.245 8.455 8.455 8.845 8.845 8.845 8.845 8.845 8.845 8.845 8.845 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.824 8.825 8.
	15	3.50 3.67 3.84 4.0	4.17 4.34 5.517 5.57	3	28	$\begin{array}{c} 7.37\\ 7.59\\ 7.58\\ 8.28\\ 8.45\\ 8.45\\ 8.45\\ 8.45\\ 8.45\\ 8.45\\ 9.10\\ 9.54\\ 10.45\\ 10.85\\ 11.729\\ 11.729\\ 11.729\\ 11.729\\ 12.13\end{array}$
	14	3.34 3.50 3.67 3.84	4.0 4.17 4.34 4.34 5.0 5.34		27	$\begin{array}{c} 7.15\\ 7.35\\ 7.59\\ 7.59\\ 7.59\\ 7.59\\ 8.24\\ 8.24\\ 8.32\\ 8.32\\ 8.32\\ 9.32\\ 9.32\\ 9.32\\ 9.32\\ 9.32\\ 9.32\\ 11.6\\$
	13	3.17 3.34 3.50 3.67	5.17 5.17 5.17 5.17	_	26	$\begin{array}{c} 6.94\\ 7.15\\ 7.37\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 7.36\\ 9.57\\ 9.57\\ 10.36\\ 111, 729\\ 111,$
26 Gauge	12	3.0 3.17 3.34 3.50 3.50	3.84 3.84 4.0 4.34 5.0 5.0	Gauge	25	$\begin{array}{c} 6.72\\ 6.94\\ 7.36\\ 7.38\\ 7.58\\ 8.02\\ 8.45\\ 8.45\\ 8.32\\ 9.32\\ 9.76\\ 9.72\\ 9.72\\ 11.6\\ 11.5\\ 11.5\end{array}$
26	=	2.84 3.0 3.17 3.34 3.50	3.67 3.84 4.17 4.5 4.84	24	24	$\begin{array}{c} 6.5\\ 6.72\\ 6.72\\ 7.194\\ 7.157\\ 7.37\\ 7.37\\ 7.37\\ 7.39$
	10	2.67 2.84 3.0 3.34 3.34	3.50 3.67 4.34 4.67		23	6.29 6.5 6.5 6.5 6.5 7.37 7.37 7.37 7.37 7.37 7.37 7.37 7.
	6	2.50 2.67 2.84 3.0 3.17	3.34 3.50 3.84 4.17 4.5		22	6.07 6.29 6.29 6.29 6.29 6.29 6.29 7.37 7.37 7.37 7.37 7.37 7.37 7.37 7.3
	8	2:34 2:50 2:84 3:0	3.17 3.34 3.67 4.0 4.34		21	5.85 6.07 6.07 6.07 6.07 6.12 6.12 7.15 7.15 7.15 7.15 7.15 7.15 8.45 8.45 8.45 8.45 8.45 8.45 8.45 8.4
	2	2.17 2.34 2.50 2.67 2.84	3.0 3.17 3.50 3.84 4.17		20	$\begin{array}{c} 5.64\\ 5.64\\ 6.07\\ 6.07\\ 6.07\\ 6.29\\ 6.72\\ 6.72\\ 6.72\\ 7.337\\ 7.33$
	9	2.17 2.34 2.50 2.50	2.84 3.0 3.67 4.0	-	61	$\begin{array}{c} 5.42\\ 5.64\\ 5.65\\ 5.65\\ 6.07\\ 6.07\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 6.72\\ 10.64\\ 10$
Size of	Duct	00800	2428	Sizeof	Duct	32887555886451-0 ⁰ 870

WEIGHT OF GALVANIZED IRON DUCTS

DUCTS	
RECTANGULAR	
IRON	
GALVANIZED	tondard Games
FOR	2 2 11
FOOT	-
LINEAL	
PER	
VEIGHT	

								<u> </u>		
		45	$12.75 \\ 13.0 \\ 13.25 \\ 13.25$	$13.5 \\ 13.75 \\ 14.0 \\$	$14.25 \\ 14.5 \\ 14.5 \\ 14.75$	$ \begin{array}{r} 15.0 \\ 15.25 \\ 15.5 \\ \end{array} $	$15.75 \\ 16.0 \\ 16.25$	$16.5 \\ 16.75 \\ 17.0 \\$	$17.25 \\ 17.75 \\ 18.25 \\ 18.25$	$ \begin{array}{c} 18.75\\ 19.25\\ 19.75\\ 20.25 \end{array} $
		44	12.5 12.75 13.0	$13.25 \\ 13.5 \\ 13.5 \\ 13.75$	$14.0 \\ 14.25 \\ 14.5 \\ 14.5$	$14.75 \\ 15.0 \\ 15.25$	15.5 15.75 16.0	16.25 16.5 16.75	17.0 17.5 18.0	18.5 19.0 19.5 20.0
		43	$12.25 \\ 12.5 \\ 12.75 \\ 12.75$	$ \begin{array}{c} 13.0 \\ 13.25 \\ 13.5 \end{array} $	$13.75 \\ 14.0 \\ 14.25$	$14.5 \\ 14.75 \\ 15.0 $	$15.25 \\ 15.5 \\ 15.75$	$16.0 \\ 16.25 \\ 16.5 \\ 16.5$	$16.75 \\ 17.25 \\ 17.75$	$\begin{array}{c} 18.25\\ 18.75\\ 19.25\\ 19.75\end{array}$
		42	12.0 12.25 12.5	$12.75 \\ 13.0 \\ 13.25 \\ 13.25$	$13.5 \\ 13.75 \\ 14.0 $	$14.25 \\ 14.5 \\ 14.75$	$15.0 \\ 15.25 \\ 15.5$	$15.75 \\ 16.0 \\ 16.25$	$16.5 \\ 17.0 \\ 17.5$	18.0 18.5 19.0 19.5
		41	$11.75 \\ 12.0 \\ 12.25 \\ 12.25$	12.5 12.75 13.0	$13.25 \\ 13.5 \\ 13.75$	$14.0 \\ 14.25 \\ 14.5$	$\frac{14.75}{15.0}$	$15.5 \\ 15.75 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 10.0 \\$	$\begin{array}{c} 16.25 \\ 16.75 \\ 17.25 \end{array}$	$\frac{17.75}{18.25}$ $\frac{18.25}{19.25}$
		40	$11.5 \\ 111.75 \\ 112.0 $	$12.25 \\ 12.5 \\ 12.75 \\ 12.75$	$ \begin{array}{c} 13.0 \\ 13.25 \\ 13.5 \end{array} $	$\begin{array}{c} 13.75 \\ 14.0 \\ 14.25 \end{array}$	14.5 14.75 15.0	$15.25 \\ 15.5 \\ 15.75$	$16.0 \\ 16.5 \\ 17.0 $	17.5 18.0 18.5 19.0
uge	e	39	$11.25 \\ 11.5 \\ 11.75 \\ 11.75$	12.0 12.25 12.5	$12.75 \\ 13.0 \\ 13.25$	$13.5 \\ 13.75 \\ 14.0 $	$14.25 \\ 14.5 \\ 14.75 \\ 14.75$	$15.0 \\ 15.25 \\ 15.5 \\$	$\begin{array}{c} 15.75 \\ 16.25 \\ 16.75 \end{array}$	$\begin{array}{c} 17.25\\ 17.75\\ 18.25\\ 18.75\\ 18.75\end{array}$
U. S. Standard Gauge	22 Gauge	38	11.0 11.25 11.5	$\begin{array}{c} 11.75 \\ 12.0 \\ 12.25 \\ 12.25 \end{array}$	$12.5 \\ 12.75 \\ 13.0 \\ 13.0 \\ 13.0 \\ 12.75 \\ $	$^{13.25}_{13.5}_{13.75}$	14.0 14.25 14.5	${}^{14.75}_{15.0}_{15.25}$	$15.5 \\ 16.0 \\ 16.5 $	17.0 17.5 18.0 18.5
J. S. Stan		37	10.75 11.0 11.25	$11.5 \\ 11.75 \\ 12.0 \\$	$12.25 \\ 12.5 \\ 12.75 \\ 12.75$	$13.0 \\ 13.25 \\ 13.5$	$\begin{array}{c} 13.75 \\ 14.0 \\ 14.25 \end{array}$	$\begin{array}{c} 14.5 \\ 14.75 \\ 15.0 \\ 15.0 \end{array}$	$\begin{array}{c} 15.25 \\ 15.75 \\ 16.25 \end{array}$	16.75 17.25 17.75 18.25
7		36	10.5 10.75 11.0	$11.25 \\ 11.5 \\ 11.75$	12.0 12.25 12.5	$12.75 \\ 13.0 \\ 13.25$	13.5 13.75 14.0	$\begin{array}{c} 14.25 \\ 14.5 \\ 14.75 \end{array}$	15.0 15.5 16.0	16.5 17.0 17.5 18.0
		35	10.25 10.5 10.75	11.0 11.25 11.5	$11.75 \\ 12.0 \\ 12.25 \\ 12.25$	12.5 12.75 13.0	$\frac{13.25}{13.5}$	14.0 14.25 14.5	14.75 15.25 15.75	$16.25 \\ 16.75 \\ 17.25 \\ 17.75$
		34	$10.0 \\ 10.25 \\ 10.5$	$10.75 \\ 11.0 \\ 11.25$	$11.5 \\ 11.75 \\ 12.0 \\$	$12.25 \\ 12.5 \\ 12.75 \\ 12.75$	13.0 13.25 13.5	$13.75 \\ 14.0 \\ 14.25$	14.5 15.0 15.5	16.0 16.5 17.0 17.5
		33	$\begin{array}{c} 9.75 \\ 9.70 \\ 10.0 \\ 10.25 \end{array}$	$10.5 \\ 10.75 \\ 11.0$	11.25 11.5 11.75	$12.0 \\ 12.25 \\ 12.5 \\$	$12.75 \\ 13.0 \\ 13.25$	13.5 13.75 14.0	14.25 14.75 15.25	$15.75 \\ 16.25 \\ 16.75 \\ 17.2$
		32	$9.5 \\ 9.75 \\ 10.0$	$10.25 \\ 10.5 \\ 10.75$	$11.0 \\ 11.25 \\ 11.5$	$11.75 \\ 12.0 \\ 12.25 \\ 12.25$	$12.5 \\ 12.75 \\ 13.0 \\$	$13.25 \\ 13.5 \\ 13.5 \\ 13.75$	$14.0 \\ 14.5 \\ 15.0 \\ $	15.5 16.0 16.5 17.0
		31	9.25 9.5 9.75	$10.0 \\ 10.25 \\ 10.5$	$10.75 \\ 11.0 \\ 11.25 \\ 11.25$	11.5 11.75 12.0	$12.25 \\ 12.5 \\ 12.5 \\ 12.75$	$ \begin{array}{r} 13.0 \\ 13.25 \\ 13.5 \end{array} $	$13.75 \\ 14.25 \\ 14.75$	15.25 15.75 16.25 16.75
	15U 15U	ri2 [] 10	0 M 00	°011	132	15 17	19 20	23	28 28 28	30 32 36

DUCTS	
I RECTANGULAR	
IRON	
GALVANIZED	Standard Gauge
FOR	U. S.
FOOT	
PER LINEAL	
PER	
VEIGHT	

-										
	09	16.5 16.75 17.0	17.25 17.5 17.75	$ \begin{array}{c} 18.0 \\ 18.25 \\ 18.5 \\ 18.5 \\ \end{array} $	$18.75 \\ 19.0 \\ 19.25 $	$ \begin{array}{c} 19.5 \\ 19.75 \\ 20.0 \end{array} $	20.25 20.5 20.75	21.0 21.5 22.0	22.5 23.0 23.5	24.0
	59	16.25 16.5 16.5	$17.0 \\ 17.25 \\ 17.5 \\$	$17.75 \\ 18.0 \\ 18.25$	18.5 18.75 19.0	$ \begin{array}{c} 19.25 \\ 19.5 \\ 19.75 \\ 19.75 \\ \end{array} $	20.0 20.25 20.5	20.75 21.25 21.75	22.25 22.75 23.25	23.75
	58	16.0 16.25 16.25	16.75 17.0 17.25	$17.5 \\ 17.75 \\ 18.0 \\$	$ \begin{array}{c} 18.25 \\ 18.5 \\ 18.75 \\ 18.75 \\ \end{array} $	$19.0 \\ 19.25 \\ 19.5 \\$	$ \begin{array}{c} 19.75 \\ 20.0 \\ 20.25 \end{array} $	20.5 21.0 21.5	22.0 22.5 23.0	23.5
	57	$\frac{15.75}{16.0}$ 16.25	$16.5 \\ 16.75 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 10.0 \\$		$ \begin{array}{c} 18.0 \\ 18.25 \\ 18.5 \end{array} $	18.75 19.0 19.25	$19.5 \\ 19.75 \\ 20.0$	20.25 20.75 21.25	21.75 22.25 22.75	23.25
	56	15.5 15.75 15.75 16.0	$16.25 \\ 16.5 \\ 16.75 \\ 16.75$	$17.0 \\ 17.25 \\ 17.5$	$17.75 \\ 18.0 \\ 18.25$	$ \begin{array}{c} 18.5 \\ 18.75 \\ 19.0 \\ \end{array} $	$ \begin{array}{c} 19.25 \\ 19.5 \\ 19.75 \end{array} $	20.0 20.5 21.0	21.5 22.0 22.5	23.0
	55	15.25 15.5 15.75	$16.0 \\ 16.25 \\ 16.5 \\ 16.5$	$16.75 \\ 17.0 \\ 17.25 \\ 17.25$	$17.5 \\ 17.75 \\ 18.0$	$ \begin{array}{c} 18.25 \\ 18.5 \\ 18.75 \end{array} $	$ \begin{array}{c} 19.0 \\ 19.25 \\ 19.5 \end{array} $	19.75 20.25 20.75	21.25 21.75 22.25	22.75
e	54	$ \begin{array}{r} 15.0 \\ 15.25 \\ 15.5 \end{array} $	$15.75 \\ 16.0 \\ 16.25 \\ 16.25$	$16.5 \\ 16.75 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 17.0 \\ 10.0 \\$	$17.25 \\ 17.5 \\ 17.75 \\ 17.75$	$ \begin{array}{c} 18.0 \\ 18.25 \\ 18.5 \end{array} $	$ \begin{array}{c} 18.75 \\ 19.0 \\ 19.25 \end{array} $	$ \begin{array}{c} 19.5 \\ 20.0 \\ 20.5 \end{array} $	$21.0 \\ 21.5 \\ 22.0 \\ 22.0 \\ 0$	22.5
22 Gauge	53	$14.75 \\ 15.0 \\ 15.25 \\ 15.25$	$15.5 \\ 15.75 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 16.0 \\ 10.0 \\$	$16.25 \\ 16.5 \\ 16.5 \\ 16.75$	$17.0 \\ 17.25 \\ 17.5$	$17.75 \\ 18.0 \\ 18.25 \\ 18.25$	$ \begin{array}{c} 18.5 \\ 18.75 \\ 19.0 \\ 19.0 \\ \end{array} $	$ \begin{array}{c} 19.25 \\ 19.75 \\ 20.25 \end{array} $	20.75 21.25 21.75	22.25
	52	$ \begin{array}{r} 14.5 \\ 14.75 \\ 15.0 \\ 15.0 \end{array} $	$15.25 \\ 15.5 \\ 15.75 \\ 15.75$	$\frac{16.0}{16.25}$	16.75 17.0 17.25	17.5 17.75 18.0	$ \begin{array}{r} 18.25 \\ 18.5 \\ 18.75 \\ 18.75 \\ \end{array} $	19.0 19.5 20.0	20.5 21.0 21.5	22.0
	51	$14.25 \\ 14.5 \\ 14.75$	$ \begin{array}{c} 15.0 \\ 15.25 \\ 15.5 \end{array} $	$15.75 \\ 16.0 \\ 16.25$	$16.5 \\ 16.75 \\ 17.0 $	$17.25 \\ 17.5 \\ 17.75 \\ 17.75$	18.0 18.25 18.5	$18.75 \\ 19.25 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 19.75 \\ 10.7$	20.25 20.75 21.25	21.75
	50	14.0 14.25 14.5	$\begin{array}{c} 14.75 \\ 15.0 \\ 15.25 \\ 15.25 \end{array}$	$15.5 \\ 15.75 \\ 16.0 \\ 16.0 \\ 16.0 \\ 10.0 \\$	$16.25 \\ 16.5 \\ 16.75$	$17.0 \\ 17.25 \\ 17.5$	$17.75 \\ 18.0 \\ 18.25$	18.5 19.0 19.5	20.0 20.5 21.0	21.5
	49	$13.75 \\ 14.0 \\ 14.25$	14.5 14.75 15.0	$15.25 \\ 15.5 \\ 15.75 \\ 15.75$	$16.0 \\ 16.25 \\ 16.5 \\ 16.5 \\ 16.5 \\ 16.5 \\ 16.5 \\ 16.5 \\ 10.5 \\$	$16.75 \\ 17.0 \\ 17.25$	$^{17.5}_{17.75}$	$ \begin{array}{c} 18.25 \\ 18.75 \\ 19.25 \end{array} $	$ \begin{array}{c} 19.75 \\ 20.25 \\ 20.75 \end{array} $	21.25
-	48	13.5 13.75 14.0	14.25 14.5 14.75	$15.0 \\ 15.25 \\ 15.5 \\$	$15.75 \\ 16.0 \\ 16.25$	$16.5 \\ 16.75 \\ 17.0 \\ 17.0 \\ 17.0 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ $	$17.25 \\ 17.5 \\ 17.75$	18.0 18.5 19.0	$ \begin{array}{c} 19.5 \\ 20.0 \\ 20.5 \end{array} $	21.0
	47	$13.25 \\ 13.5 \\ 13.75 \\ 13.75$	14.0 14.25 14.5	$14.75 \\ 15.0 \\ 15.25 \\ 15.25$	15.5 15.75 16.0	$16.25 \\ 16.5 \\ 16.75$	$17.0 \\ 17.25 \\ 17.5 \\$	$17.75 \\ 18.25 \\ 18.75 \\ 18.75$	$19.25 \\ 19.75 \\ 20.25$	20.75
	46	13.0 13.25 13.5	$13.75 \\ 14.0 \\ 14.25 \\ 14.25$	14.5 14.75 15.0	15.25 15.5 15.75	$16.0 \\ 16.25 \\ 16.5 \\ 16.5 \\ 1$	16.75 17.0 17.25	$17.5 \\ 18.0 \\ 18.5 \\ $	19.0 19.5 20.0	20.5
Size	Duct	810	°01	122	15 16 17	18 19 20	22	24 28 28	32 34 32	36

DUCTS
RECTANGULAR
IRON F
GALVANIZED
FOR
FOOT
LINEAL
PER
VEIGHT

J. S. Standard Gauge

	<u> </u>		H IMU	- 50	FFA L	0 10	JUGE	001	IPAN:
	00	28.0 28.6 29.2	29.8 30.4 30.9	$\frac{31.5}{32.1}$	33.3 33.9 34.4	35.0 35.6 36.2	36.8 37.3 37.9	38.5 39.0 39.6	40.2 40.8 41.4 42.0
	88	27.4 28.0 28.6	29.2 29.8 30.4	30.9 31.5 32.1	32.7 33.3 33.9	34.4 35.0 35.6	36.2 36.8 37.3	37.9 38.5 39.0	39.6 40.2 41.4
	86	26.7 27.4 28.0	28.6 29.2 29.8	$30.4 \\ 30.9 \\ 31.5$	32.1 32.7 33.3	$33.9 \\ 34.4 \\ 35.0$	35.6 36.2 36.8	37.3 37.9 38.5	39.0 39.6 40.2
	84	26.3 26.7 27.4	28.0 28.6 29.2	29.8 30.9 30.9	31.5 32.1 32.7	33.3 33.9 34.4	35.0 35.6 36.2	36.8 37.3 37.9	38.5 39.6 39.6
	82	25.7 26.3 26.7	$27.4 \\ 28.0 \\ 28.6 \\ 28.6 \\ 0$	29.2 29.8 30.4	30.9 31.5 32.1	32.7 33.3 33.9	34.4 35.0 35.6	36.2 36.8 37.3	37.9 38.5 39.0
,	80	$25.1 \\ 25.7 \\ 26.3 \\ $	26.7 27.4 28.0	28.6 29.2 29.8	$30.4 \\ 30.9 \\ 31.5$	32.1 32.7 33.3	$33.9 \\ 34.4 \\ 35.0$	35.6 36.2 36.8	37.3 37.9 38.5
e.	78	24.5 25.1 25.7	26.3 26.7 27.4	28.0 28.6 29.2	29.8 30.4 30.9	31.5 32.1 32.7	33.3 33.9 34.4	35.0 35.6 36.2	36.8 37.3 37.9
20 Gauge	76	$23.9 \\ 24.5 \\ 25.1$	25.7 26.3 26.7	27.4 28.0 28.6	29.2 29.8 30.4	30.9 31.5 32.1	32.7 33.3 33.9	34.4 35.0 35.6	36.2 36.8 37.3
	74	23.4 23.9 24.5	25.1 25.7 26.3	26.7 27.4 28.0	28.6 29.2 29.8	$30.4 \\ 30.9 \\ 31.5$	32.1 32.7 33.3	33.9 34.4 35.0	35.6 36.2 36.8
	72	22.8 23.4 23.9	24.5 25.1 25.7	26.3 26.7 27.4	28.0 28.6 29.2	29.8 30.4 30.9	31.5 32.1 32.7	33.3 33.9 34.4	35.0 35.6 36.2
	70	$22.1 \\ 22.8 \\ 23.4 \\ 23.4$	23.9 24.5 25.1	25.7 26.3 26.7	27.4 28.0 28.6	29.2 29.8 30.4	$30.9 \\ 31.5 \\ 32.1 \\ 32.1$	32.7 33.3 33.9	34.4 35.0 35.6
	68	21.6 22.1 22.8	23.4 23.9 24.5	25.1 25.7 26.3	26.7 27.4 28.0	28.6 29.2 29.8	$30.4 \\ 30.9 \\ 31.5$	32.1 32.7 33.3	33.9 34.4 35.0
	66	$21.0 \\ 21.6 \\ 22.1$	22.8 23.4 23.9	24.5 25.1 25.7	26.3 26.7 27.4	28.0 28.6 29.2	29.8 30.4 30.9	31.5 32.1 32.7	33.3 34.4 24.4 25.4
	64	20.4 21.0 21.6	22.1 22.8 23.4	$23.9 \\ 24.5 \\ 25.1$	25.7 26.3 26.7	27.4 28.0 28.6	29.2 29.8 30.4	30.9 31.5 32.1	32.7 33.3 33.9 34.4
Duct	62	6 19.9 8 20.4 0 21.0	2 22.8 22.8 22.8	23.4 23.9 24.5	4 25.1 5 25.7 8 26.3	26.7 27.4 28.0	28.6 29.2 29.8 29.8	2 30.4 30.9 31.5	32.1
to szi2	1	-	142	18 22 22	58 58 58	30 32 34	36 38 40	444 448	52 52 52

WEIGHT PER LINEAL FOOT FOR GALVANIZED IRON RECTANGULAR DUCTS

U. S. Standard Gauge

Size of Duct							20 Gauge	agu						
	92	94	96	98	100	102	104	106	108	110	112	114	116	110
.00	28.6 20.9	29.2	29.8	30.4	30.9	31.5	32.1	32.7	33.3	33.9	34.4	35.0	35.6	26.9
0	29.8 29.8	30.4	30.9 30.9	30.9	32.15	32.1	32.7	33.3	33.9	34.4	35.0	35.6	36.2	36.8
-		0.00			ļ	į	2	00.9	04.4	0.00	30.0	36.2	36.8	37.3
7 4	30.4 30.9	30.9	32.15	32.1	32.7	33.3	33.9	34.4	35.0	35.6	36.2	36.8	37.3	37.9
16	31.5	32.1	32.7	33.3	33.9	34.4	35.0	35.6	35.6 36.2	36.2 36.8	36.8	37.3	37.9 38.5	38.5
18	32.1	32.7	33.3	33.9	34.4	35.0	35.6	36.2	36.8	37.3	37.0	20 5	0.00	0.60
52	33.3	33.9	33.9 34.4	34.4	35.0 35.6	35.6 36.2	36.2 36.8	36.8	37.3	37.9	38.5	30.0	39.6	40.2 60.2
24	33.9	34.4	35.0	35.6	36.2	36.8	37.3	37.0	30 5	0.00	0.00	0.00	2.0¥	40.8
58 58	34.4 35.0	35.0 35.6	35.6	36.2	36.8	37.3	37.9	38.5	39.0	39.6	40.2	40.2	40.8	41.4
	0.00	0.00	÷.00	0.00	6.10	51.9	38.5	39.0	39.6	40.2	40.8	41.4	42.0	42.6
32	35.6 36.2	36.2 36.2	36.8 37.2	37.3	37.9	38.5	39.0	39.6	40.2	40.8	41.4	42.0	42.6	43.2
34	36.8	37.3	37.9	38.5	39.0	39.6	39.0 40.2	40.2	40.8 41.4	41.4 42.0	42.0 42.6	42.6 43.2	43.2	43.8 44.4
36	37.3	37.9	38.5	39.0	39.6	40.2	40.8	41.4	42.0	42.6	43.9	43.8	44 4	AF O
60	38.5	39.0	39.0	39.6	40.2	40.8	41.4	42.0	42.6	43.2	43.8	44.4	45.0	45.5
4	0.00			3.0F	0.04	F.1F	1.21	42.0	43.2	43.8	44.4	45.0	45.5	46.0
44	39.0 39.6	39.6	40.2	40.8	41.4	42.0	42.6	43.2	43.8	44.4	45.0	45.5	46.0	46.6
46	40.2	40.8	41.4	42.0	42.6	43.2	43.8	44.4	44.4 45.0	45.0 45.5	45.5 46.0	46.0 46.6	46.6	47.2
48	40.8	41.4	42.0	42.6	43.2	43.8	44.4	45.0	45.5	46.0	46.6	47.2	47.8	48.4
22	42.0	42.0	42.6	43.2	43.8	44.4	45.0	45.5	46.0	46.6	47.2	47.8	48.4	49.0
54	42.6	43.2	43.8	44.4	45.0	45.5	46.0	40.0 46.6	40.6	47.2	47.8	48.4	49.0 40.6	49.6
												-	1 DIOL	2.00

PART IV APPARATUS

The essential elements embodied in most installations using fans, more especially those for heating, ventilating, or similar work, are the fan, heater, ducts or piping system, and some form of motive power for driving the fan. In this section will be found complete data relative to the performance and dimensions of fans, heaters and engines, together with detailed directions for making fan tests. Data on the performance and dimensions of cast iron heaters are also given.

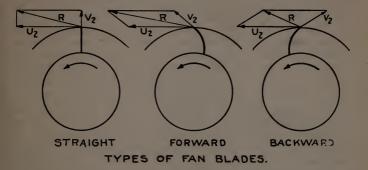
SECTION I FANS

Fan Design

Centrifugal fans may be roughly divided into two classes, those having rotors with straight radial blades, and those having rotors with blades curved with reference to their direction of rotation. Curved blade fans have quite diverse characteristics, depending on whether they are curved forward or backward with reference to their direction of rotation. The mathematical theory of the radial blade fan is very completely and clearly discussed in Prof. Carpenter's book on Heating and Ventilation.

In any centrifugal fan there are two separate and independent sources of pressure. First, pure centrifugal force due to the rotation of an enclosed column of air. Second, kinetic energy contained in the air by virtue of its velocity upon leaving the periphery of the fan rotor. The amount of centrifugal force imparted to the air depends largely upon the ratio of the tangential or rotational velocity of the air leaving the periphery of the rotor to the tangential or rotational velocity of the air entering the fan at the heel of the blades.

When the flow of air through the rotor of a fan is partially obstructed the centrifugal effect in the rotor produces a compression corresponding to the centrifugal force, which is known as static pressure. On the other hand, the kinetic energy of the air leaving the periphery of the rotor must first be converted largely into potential energy in the form of static pressure before being serviceable. This conversion from kinetic energy or velocity into potential energy or static pressure is ordinarily accomplished in the scroll formation of the fan housing. A still further conversion is often secured, where the velocity leaving the outlet is high, by means of a diverging nozzle on the outlet of the fan. The principle covering the design and application of such nozzles is discussed on page 122.



The accompanying diagrams represent the parallelogram of forces for the three general types of blades, the first a straight blade, the second a blade bent forward and the third where the blade is bent backward. The line U_2 represents the tip speed of the wheel and the line V_2 represents the radial velocity of the air leaving the tip of the blade. The diagonal line R then represents the actual velocity of the air with respect to the fan casing.

The amount of total pressure developed by a straight blade fan may be determined by means of the following formula:

$$\mathbf{p} = \frac{(\mathbf{U}_{2}^{2} - \mathbf{U}_{1}^{2}) + \mathbf{M}\mathbf{U}_{2}^{2} - (1 - \mathbf{M}) \, \mathbf{V}_{2}^{2} - (\mathbf{N} \, \mathbf{V}_{n})^{2}}{\mathbf{V}_{p}^{2}}$$
(73)

where

 $\begin{array}{l} p = total \ press. \ developed \ by \ fan. \\ V_o = velocity \ of \ air \ through \ inlet. \\ V_p = vel. \ corresponding \ to \ unit \ press. \\ V_2 = radial \ vel. \ of \ air \ leaving \ tip \ of \ blades. \\ U_1 = lineal \ vel. \ at \ heel \ of \ blades. \\ U_2 = lineal \ vel. \ at \ tip \ of \ blades. \\ M = per \ cent. \ velocity \ pressure \ conversion \ in \ fan \ scroll. \\ N = ratio \ of \ actual \ to \ effective \ area \ of \ inlet. \end{array}$

It will be noticed from the two diagrams of curved blade wheels that when the blade is bent forward an accelerated velocity will be obtained, while with the blades bent backward the opposite effect will be the result. This explains how it is possible to build a fan with a small wheel, such as is used in the multiblade type, and obtain the desired pressure and velocity without using excessive speeds. By curving the blades forward a pressure greater than that due to the peripheral velocity is obtained, as indicated in the diagram.

The velocity of the air leaving the tip of the blades and the corresponding velocity pressure is greatly in excess of that ordinarily required in the piping system, and at the same time the static pressure is too low. By enclosing the wheel in a casing having a properly designed scroll, this velocity is reduced, and a part of the velocity pressure is converted to static pressure. Since the static pressure due to the wheel varies as the difference of the squares of the rotational velocities at the periphery and inlet, it is evident that the shorter the blade the greater must be the dependence on the scroll-shaped housing to obtain the desired static pressure. For this reason the proper design of the housing is of greater importance in the case of a short blade multivane type of fan than with the older styles.

There are frequently cases where a fan is to be direct connected to a high speed unit, where the corresponding pressure obtained would be greater than required. In this case the backward bent blade is used, since, as may be noticed from the diagram, a pressure less than that corresponding to the peripheral velocity is then obtained.

The standard steel plate fan is essentially a straight blade fan, as compared with the later styles of short curved blade multivane type, although, as just shown, when the tips of the blades are bent either forward or backward the fan will have different characteristics from one with straight blades. This fan as ordinarily built does not give as high an efficiency as the multivane type owing to the fact that it is designed for large capacity rather than for high efficiency. But if these long blade fans are built according to special design they may be made to give greater efficiency than may be obtained from the curved short blade fans. This calls for a tall narrow fan with the inlet diameter smaller than that used on the standard fan. It may be readily shown that there is a certain diameter of inlet that will give maximum economy of operation. If the diameter is increased the loss by impact at the heel of the blades is increased as the square of the diameter, and the loss by entrance is decreased as the fourth power of the diameter. The opposite holds true in case the inlet diameter is decreased.

The proper size of the fan inlet depends on the cubic feet of air per revolution handled by the fan. It has been determined both mathematically and experimentally that the most efficient diameter of inlet is given by the simple relationship

$$D_1 = C \sqrt[3]{\frac{Q}{N}}$$
(74)

where

- $D_1 = inlet$ diameter in feet.
 - Q = cubic feet of air per minute.
 - N = revolutions per minute.
 - C=a factor determined experimentally, and is practically a constant for all ratios of inlet diameter to wheel diameter.

COMPARATIVE EFFECT OF BLAST-WHEEL PROPORTIONS UPON THE EFFECT OF STRAIGHT BLADE FANS OPERATING AT THE SAME CAPACITY AND PRESSURE

Ratio of Dia. Inlet to Dia. Wheel	Per Cent. Dian	Relative neter	Per Cent. Relative	Per Cent. Relative	Per Cent. Relative
at Perip.	Wheel	Inlet	Width	Н. Р.	Speed
0.700 0.650 0.625 0.600 0.550 0.500 0.450 0.400 0.350	82.0 93.2 100.0 106.9 123.5 144.9 170.8 206.5 255.0	91.9 97.5 100.0 102.6 108.8 116.6 123.0 132.4 142.8	108.9 102.5 100.0 97.5 92.1 85.9 81.3 75.5 70.1	112.3 104.0 100.0 96.7 91.0 86.8 83.4 80.0 77.5	$123.0 \\109.5 \\100.0 \\92.7 \\78.2 \\64.5 \\53.3 \\43.1 \\34.6$

It may be noted from the accompanying table that the essential factor in the design of straight blade fans is the diameter of the inlet, and that the smaller the inlet as compared to the diameter of the wheel, the greater will be the efficiency obtained. This table is based on the assumption that a value of 62.5 per cent. for the above ratio be used to represent the average standard fan, and the other figures show comparative values for other ratios. It will be seen from the second and fourth columns that the height of the fan increases rapidly while the width decreases. This means, then, that these special high efficiency fans are tall and narrow, which naturally makes them more expensive than the ordinary commercial steel plate fan.

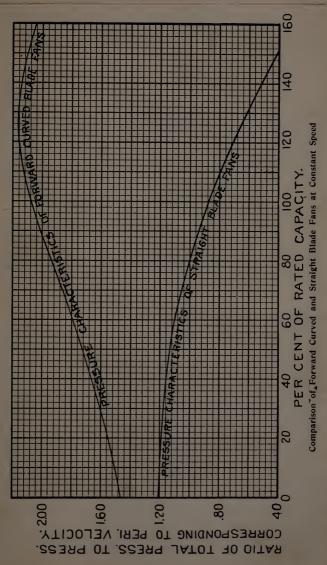
These special tall narrow fans are frequently used for induced draft work, partly because the narrow wheel makes a shorter over-hang on the fan bearing, and partly because they may be operated at lower speed and are therefore more suitable for direct connection to steam engines. A table of special induced draft fans will be found on pages 328 to 330, giving the size of engine and dimensions of fan for various boiler capacities.

Pressure Characteristics

The relative performance of the different styles of fans may be shown by the performance curves given for each style in Section III. The diagrams on pages 214 and 215 or on pages 224 and 225 are typical of the straight blade fan, while the diagram on page 276 shows the performance of the Niagara Conoidal fan, it being typical of the forward curved blade style.

In making the tests on these fans from which the diagrams referred to were computed, the fan was operated at constant speed with varying sized discharge orifices. Horsepower, pressure and capacity readings were taken and the efficiency calculated. The horsepower, pressure and efficiency were then plotted to capacity, giving the performance curves of this test fan. This set of curves shows the power consumption increasing with the capacity, but not at the same ratio. The efficiency increases to a maximum and then decreases to zero. The rating of the fan may be taken at any point adopted as a standard, but the desirable point will generally be determined by the point of maximum efficiency.

As will be noted from the diagrams already referred to, the relative pressure developed by centrifugal fans will differ for fans having straight or curved blades. A further comparison of the two types may be made from the diagram on page 173. The two curves indicate the ratio of the total pressure developed to the pressure corresponding to the peripheral velocity of the wheel, when operating at different per cents. of the fan's rated



FAN CHARACTERISTICS

capacity. Thus we see that at rated capacity the straight blade fan gives a total pressure of 87 per cent. and the forward curved blade type gives 208 per cent. of the pressure corresponding to *the peripheral velocity.

When the Niagara Conoidal fan is operated up to 50 per cent. overload the total pressure increases, but when operating at less than rated capacity the pressure decreases. Just the opposite holds true in the case of the straight blade fan. From this we note that if a forward curved blade fan is intended to operate at a certain pressure and capacity and if for any reason, such as resistance greater than expected, the quantity of air handled is less than the fan's rating for the speed maintained, the total pressure will also be less than that specified. With the straight blade fan just the opposite holds true, for as the capacity is reduced the pressure will increase, at constant speed.

Care should be taken in the selection of a fan with forward curved blades in case it is to be driven with a motor. If for any reason there should be a tendency to operate at over capacity both the air quantity and the pressure will increase, which may overload the motor in case sufficient margin has not been allowed.

Special Types and Features

There are numerous special types of fans intended to meet various requirements. Some of these, as for instance foundry and forge shop blowers and exhausters or planing-mill exhausters, are adaptations of the ordinary straight blade fans. There are other types, such as the disc or propeller wheel, that differ essentially in the principle of their design and operation. These special types will be found described under their proper heading, together with their capacity and dimension tables.

The steel plate fans may be divided into two classes, namely, blower or exhauster, depending on whether they have two inlets or only one. With the double inlet fan, or blower, we have the total inlet area divided between the two sides of the housing, therefore each inlet may be made smaller in diameter for the same size of fan wheel, and so approach the more efficient type of fan as indicated in the table on page 171. For this reason the steel plate blower is a more efficient fan than the single inlet fan, or exhauster. Either may be made full housing or three-quarter housing, depending on the size and requirements. The multivane fan as ordinarily built is a single width fan with but one inlet. These are also built in a double width style, with two inlets, being essentially two fans placed back to back. They have the same characteristics as regards full or three-quarter housing, as also the angle of discharge, as has the steel plate exhauster.

Both the steel plate and the multivane fans are ordinarily built with a bearing on each side of the housing. In the case of the exhauster, where any substance is to be handled that would be injurious to the bearing located in the intake, they are usually made with an overhung wheel, a pedestal supporting an extra bearing being attached to the back of the housing. Special exhausters, as for instance planing-mill exhausters, are built with an overhanging wheel in order to avoid obstructing the inlet of the fan. Induced draft fans are built with an overhung wheel to avoid drawing the hot gases over the bearing. In any fan handling hot gases the bearing attached to the back of the housing should be of a special water cooled type to avoid heating.

The regular discharges of fans and blowers are designated as top or bottom horizontal discharge, up or down blast, and special, which are described by giving the angle of the discharge from the horizontal. The hand of a fan or blower is determined by the side on which the pulley or engine is located. Standing facing or nearest to the discharge outlet, the fan is right or left hand, according to whether the pulley is on the right- or left-hand side.

Horsepower of Fan

Each cubic foot of air per minute moved against a total pressure of one inch water gauge, equivalent to 0.577 oz. per square inch, or 5.19 pounds per square foot, represents the expenditure of 5.19 foot-pounds of work. We then have as the theoretical expenditure of energy in doing this work

 $\frac{5.19}{33000} = 0.000157 \text{ H. P.}$

and also

$\frac{1}{0.000157} = 6370 \text{ A. P. M.}$

That is, with perfect efficiency, it will require 0.000157 H. P. to move one cubic foot of air per minute against a pressure of one

inch, or 6370 cu. ft. of air per minute moved against one inch pressure will require one horsepower. Assuming a fan efficiency of 60 per cent. will give 0.000261 H. P. per cubic foot of air per minute per inch total pressure

H. P. =
$$\frac{A. P. M. \times 0.000157 \times \text{total press. in inches}}{\text{total efficiency}}$$
(75)

or H. P. =
$$\frac{A. P. M. \times 0.000157 \times \text{static press. in inches}}{\text{static efficiency}}$$
 (76)

where total or static efficiency refers to the efficiency based respectively on the total or static pressure. The ratio of total to static pressure will remain constant for any style of fan at rated capacity but will vary for the different types.

In the case of straight blade fans we may determine the horsepower for any given air delivery by assuming twice the pressure corresponding to the peripheral velocity with a corresponding efficiency of 100 per cent. This will give approximately the true horsepower regardless of actual pressure or efficiency obtained. Thus if we have a straight blade fan delivering 30000 A. P. M. at 230 R. P. M. with a fan wheel $83\frac{1}{2}$ inches in diameter, we will have a peripheral velocity of 5040 feet per minute, and twice the pressure corresponding to the peripheral velocity will be 3.17 inches. Then the horsepower required by the fan will be

H. P. = 30000 × 0.000157 × 3.17 = 14.9.

Relations of Total, Static and Velocity Pressure

In fan work air is delivered against a certain static pressure or resistance of the system and in addition has imparted to it a certain velocity at the fan outlet. This velocity is dependent on the amount of air required and on the area of the fan outlet, and the velocity pressure expressed in inches corresponding to this velocity may be determined from the formula (see page 20)

$$p_r = \left(\frac{velocity}{4005}\right)^2 = inches of water$$

where the term velocity refers to the velocity of the air through the fan outlet in feet per minute.

When it is desired to express the velocity pressure in ounces per square inch the following formula should be used:

$$p_v = \left(\frac{velocity}{5273}\right)^2 = oz. per sq. in.$$

The total energy imparted to the air is composed of the static pressure of the system and the energy of discharge corresponding to the velocity pressure or velocity head as it is termed in hydraulics. The total pressure is the sum of the velocity pressure at the fan outlet plus the static pressure produced, and is the pressure upon which the performance and efficiency of the fan is usually based. In the case of an exhaust system, the static head on the fan should be taken as the difference in static pressure at the inlet and outlet of the fan. The method to be used in making these various pressure determinations is fully explained under "Fan Testing," Part IV, Section II.

The ratio of static to velocity pressure at the fan outlet is very important in fan engineering. This ratio varies as the capacity of the fan is varied at constant speed, and bears a definite experimental relationship to the efficiency of the fan. The rated fan performances which represent the most desirable conditions of operation are based on certain relationships of static to velocity pressure. For instance, the rated performance of the Planoidal fan is based on a relationship of

$$\frac{\mathbf{p}_{s}}{\mathbf{p}_{v}}=3.88$$

The performance of the Planoidal fan with reference to this ratio is shown by the diagram on page 215. As an illustration of its use we will assume an 80-inch Planoidal exhauster operating against a static pressure of $\frac{3}{4}$ inch and delivering 12000 cu. ft. air per minute. Since the outlet of this fan is 5.54 sq. ft. (see table on page 207) the velocity at the fan outlet will be $12000 \div 5.54 = 2170$ ft. per minute, and the velocity pressure will be

$$p_r = \left(\frac{2170}{4005}\right)^2 = 0.294$$
 in.

The ratio of static to velocity pressure will then be

$$\frac{p_{s}}{p_{v}} = \frac{0.75}{0.294} = 2.55$$

From the diagram on page 215 we find that with the above ratio, the fan will be operating at 111.5 per cent. of rated capacity, with correspondingly increased power consumption and lowered efficiency. Further examples illustrating the application of these diagrams will be found under "Selection of a Fan" on page 182.

For certain kinds of work a low velocity in the piping system is desired, while in other cases it is necessary to maintain a high velocity. In case a lower velocity is required in the piping system than that maintained at the fan outlet, the area of the main pipe should be gradually increased. This is termed a diverging cone on the fan outlet, and if properly proportioned the loss due to the reduction in velocity at this point will be reduced to a minimum. Rules for the design of cone outlets and their effect in increasing the static pressure will be found given under "Diverging Nozzles in Air Ducts" on page 122.

The Relation Between Pressure, Velocity and Air Density in Fan Work

For low pressures, as in fan work, we may consider that the pressure varies inversely as the absolute temperature and directly as the barometric pressure. The volume of the same weight of air is directly and the weight of the same volume is inversely proportional to the absolute temperature. We will then have

$$\frac{\mathbf{p}_0}{\mathbf{p}} = \frac{\mathbf{T}}{\mathbf{T}_0} \text{ and } \frac{\mathbf{p}_0}{\mathbf{p}} = \frac{\mathbf{b}_0}{\mathbf{b}} \text{ or } \mathbf{p}_0 = \mathbf{p} \times \frac{\mathbf{T}}{\mathbf{T}_0} \times \frac{\mathbf{b}_0}{\mathbf{b}}$$
(77)

where

 $\begin{array}{l} p = \mbox{pressure at absolute temp. T and barom. b.} \\ p_0 = \mbox{pressure at absolute temp. T}_0 \mbox{ and barom. b}_0. \\ T = \mbox{absolute temp. of the air in deg. Fahr.} \end{array}$

b=barometric pressure in in. of mercury.

Then in order to correct any given pressure reading p, at temperature t and barometer b, to the corresponding pressure for standard dry air at 70° F. and 29.92″ barom. we will have

$$p_{o} = p \times \frac{530}{460 + t} \times \frac{b}{29.92} = \frac{0.075 p}{W}$$
 (78)

Since at constant capacity and speed the power consumption will vary as the pressure, and the pressure varies as the density of the air, we will also have

H.P. = (H.P.)₀ ×
$$\frac{460 + t}{530}$$
 × $\frac{29.92}{b}$ = $\frac{(H.P.)_0}{0.075}$ (80)

Thus, if a fan is to operate under some other condition than standard air, corrections can be made for pressure and horsepower by equations (78) and (80) respectively. For illustration see example 5, page 188.

In a centrifugal fan working under a constant orifice condition and at known air density, the theoretical velocity and pressure developed each bears a definite relation to the peripheral or tip velocity of the fan wheel. That is, the air velocity at the fan outlet and capacity is directly proportional to the peripheral velocity and fan speed, and the pressure developed varies directly as the square of the peripheral velocity and therefore as the square of the fan speed. Since the horsepower is proportional to the product of the pressure and capacity, the horsepower evidently varies as the cube of the fan speed. These combined relationships may be expressed by the following formula:

$$\frac{p}{p_0} = \frac{N^2 W}{N_0^2 W_0} \text{ and } \frac{H.P.}{(H.P.)_0} = \frac{N^3 W}{N_0^3 W_0}$$
(81)

where N = revolutions per minute, and W = air density.

Laws of Fan Performance

In the selection and operation of fans, the size, speed, capacity, horsepower, and pressure each has a fixed and definite relation to the other, which may be expressed as follows:

For a given fan size, piping system, and air density-

1-Capacity varies directly as speed.

2-Velocity varies as speed or capacity.

3-Pressure varies as the square of the speed.

4-Speed and capacity vary as square root of the pressure.

5-Horsepower varies as cube of the speed or capacity.

6-Horsepower varies as (pressure)^{3/2}

For a constant pressure and at rated capacity-

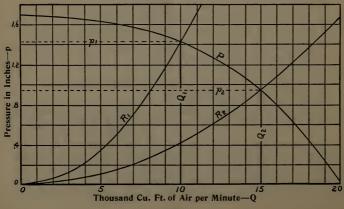
7-Capacity and horsepower vary as square of the size.

8-Speed varies inversely as size.

9—At constant pressure the speed, capacity and horsepower vary as the square root of the absolute temperature.

10—At constant capacity and speed, the horsepower and pressure will vary directly as the density of the air and approximately inversely as the absolute temperature. Thus increasing the temperature from 50° to 550° practically cuts the horsepower and pressure in half if the speed and capacity remain the same. It has been shown that the pressure loss or resistance (p_s) of a given system of air passages varies as the square of the air velocity and therefore as the square of the air quantity, (Q). Also, since the pressure produced by a fan varies as the square of the speed (Law 3) under constant outlet conditions, it is evident that the air quantity delivered by the fan through a given system of air passages will vary directly as the speed, (Law 1). The relation between pressure loss and the air quantity passed through a given system may be termed the coefficient of resistance (R) of that system in the formula $p_s = R Q^2$, and $R = \frac{p_s}{Q^2}$ Also on page 125, it has been shown that each system has an equivalent or blast-area (A), where the pressure loss may also be expressed as $p_s = \left(\frac{Q}{V_0 \cdot A}\right)^2$ and where V_0 is the velocity corresponding to unit pressure. Hence $R = \left(\frac{1}{V_0 \cdot A}\right)^2$

If the coefficient of resistance or blast-area of a system to which a fan is applied should be changed while the fan is operated at constant speed, then the air delivery will undergo a change which is complicated by the fact that the fan pressure also changes with the quantity of air delivered, as shown by the pressure-capacity characteristic. This is best illustrated by the accompanying diagram. In the first case suppose we have a system whose coefficient of resistance is $R_1 = 142/10^{10}$ and in the second case the system is changed so the coefficient of



resistance is reduced to $R_2 = 42/10^{10}$. Curves R_1 and R_2 show how the pressure losses will vary with the air delivery in the respective cases, and curve P shows how the pressure produced by a 90-inch Planoidal exhauster at 330 R. P. M. varies as the air delivery. It is evident that the air delivery will be Q_1 for the first case and Q_2 for the second, with corresponding static pressures p_1 and p_2 .

Selection of a Fan

It is well known and capable of demonstration in practice as well as in theory that of two straight blade fan wheels, the one having longer blades gives greater pressure, and that curving the blades forward in the direction of rotation increases the pressure, the converse also being true.

It is not a fact that a fan with forward curved blades is on that account any more efficient than one with radial blades; the two types have radically different characteristics, and each a field in which it excels; with the short forward curved blades good efficiency requires a greatly increased number as compared with the few blades of the radial type familiar in the steel plate fan.

In both types the need of careful design does not end with the proportions of the blades; the design of the scroll or housing, the area and position of the outlet and the diameter of the inlet are very important factors.

As explained under "Pressure Characteristics," the performance at other than rated capacity of the older style straight blade fan is entirely different from that of the curved blade multivane type. With the straight blade fan the pressure drops off rapidly when operated at overload, but increases when the fan is operated at less than rated capacity. In the case of the multiblade fans, the static pressure is greatest at normal load, and decreases at capacities either above or below this rated point.

Thus we see in the case of a system where a uniform air quantity is desired, whether for heating, ventilating, forced draft or for drying processes, the steel plate fan will come nearer giving this uniform quantity in spite of variations in resistance, throttling effect of closing dampers, and similar conditions.

On the other hand, it is sometimes very desirable to be able to throttle the capacity of a fan without increasing the pressure and velocity, as for instance, if one wing of a building is closed off and it is not convenient to change the speed of the fan, the steel plate fan would deliver an increased amount of air into the remaining part of the system on account of its increased pressure, while the multiblade fan would be more sensitive to the increased resistance and would show only a slight increase in velocity through the ducts which remain open.

In general, the multiblade fans, of which the Niagara Conoidal is a type, require less space than steel plate fans of equal capacity and efficiency. Another important advantage is the fact that the higher speeds of these multiblade fans make them more suitable for direct connection to motors, or at least give better pulley ratios than may be obtained with radial blade fans of equal efficiency.

After determining the style of fan to be used, there are two things to be considered in its selection. It must supply a definite amount of air per minute and it must supply this air at sufficient static pressure to overcome the friction loss of the system, which should be calculated or determined with reasonable accuracy. The performance of the fan under this condition is determined from the capacity tables.

Example 1. Assume that it is required to deliver 16500 cu. ft. air per minute against a static pressure of 0.95 in., and determine the size of Planoidal exhauster to be used, with the corresponding speed and horsepower. From the diagram on page 214 we see that at rated capacity the Planoidal fan gives a static pressure which is 79 per cent. of the rated total pressure. Then the total pressure corresponding to 0.95 in, static will be 1.20 in. From the table on page 208 we see that we may choose between a 90-inch fan operating over capacity or a 100-inch fan operating at less than rated capacity.

A 90-inch Planoidal fan has an outlet area of 7.10 sq. ft. (table page 208) so that the velocity through the outlet will be $16500 \div 7.1 = 2325$ feet per minute. From formula 21 on page 20 we have the pressure varies as the square of the velocity, and from formula 13 on page 18 the velocity for dry air at 70° F. corresponding to one inch pressure is 4005 feet per minute. The velocity head or velocity pressure at the outlet of the 90-inch fan corresponding to a velocity of 2325 feet per minute will then be

$$p_r = (2325 \div 4005)^2 = 0.337$$
 in.

The total pressure against which the 90-inch fan must operate will then be the sum of the static and velocity pressures, or $0.95 \pm 0.337 = 1.287$ inches, and the ratio of static to velocity pressure will be $0.95 \pm 0.337 = 2.82$. Referring to the diagram on page 215, we find a point on the bottom scale corresponding to a ratio of static to velocity pressure of 2.82, and from the intersection of a vertical from this point with the curves above we may, determine the relative performance of the fan from the scale on the left-hand edge of the chart. Thus we find that the fan will be operating at 108 per cent. of the rated capacity, and require 104.5 per cent. of the rated horsepower.

As already stated, the fan is required to deliver 16500 A. P. M.; so that $16500 \div 1.08 = 15300$ A. P. M., the rated capacity of the fan at the speed used. From the table on page 208 we see that this fan will deliver 14890 A. P. M. at 334 R. P. M. and require 6.65 H. P. According to the relations given on page 179 the speed varies directly as the capacity and the power as the cube of the capacity. We will then have for a rated capacity of 15300 A. P. M.

Actual speed =
$$334 \left(\frac{15300}{14890}\right) = 344$$
 R. P. M.
Rated power = $6.65 \left(\frac{15300}{14890}\right)^8 = 7.22$ H. P.

But as already stated, when operating at 108 per cent. of the rated capacity, or 16500 A. P. M., this fan will require 104.5 per cent. of the rated power, so we will have

Actual power = $1.045 \times 7.22 = 7.55$ H. P.

The pressure developed will be 0.95 inch static and 1.287 inches total.

In case a 100-inch Planoidal fan should be selected for this service it will operate at less than the rated capacity, and the power required may be determined in the same manner as for the 90-inch fan. The outlet area of a 100-inch fan is 8.75 sq. ft so the velocity at the outlet will be $16500 \div 8.75 = 1885$ feet per minute and the corresponding velocity pressure will be $(1885 \div 4005)^2 = 0.221$ in. Since the fan is required to develop 0.95 in. static, the total pressure against which it will operate will be $0.95 \pm 0.221 = 1.171$ in., and the ratio of static to velocity pressure will be $0.95 \pm 0.221 = 4.30$. From the diagram on page 215 we find that with a ratio of static to velocity pressure of 4.30 the fan will operate at 97 per cent. of the rated capacity and require 98.5 per cent. of the rated power.

As 16500 is to be 97 per cent. of the fan's rated capacity at the speed used, we have $16500 \div 0.97 = 17000$ A. P. M. as the rated capacity. From the table on page 208 we note that the 100-inch fan at 300 R. P. M. will deliver 18370 A. P. M. andrequire 8.20 H. P. To obtain a rated capacity of 17000 A. P. M it will be necessary to reduce the speed and consequently the power to

Speed =
$$300 \left(\frac{17000}{18370}\right) = 278$$
 R. P. M.
Power = $8.20 \left(\frac{17000}{18370}\right)^3 = 6.50$ H. P.

As determined from the diagram, the power at 97 per cent. capacity will be 98.5 per cent. of the rated, so we will actually require

$$0.985 \times 6.50 = 6.40$$
 H. P.

Thus we see that while the first cost of the 100-inch fan will be greater, the cost for power will be less than with the 90-inch fan.

Example 2. A case frequently met in the application of fans is where the resistance against which the fan must operate is different from any of the pressures given in the fan capacity tables.

We will assume that 12000 A. P. M. is required at 0.20 in. static resistance. What size of fan shall be used and what will be the speed and horsepower? If a fan should be required to operate at rated capacity at a speed corresponding to the 0.20 in. resistance, we may select a Planoidal fan from the table on page 210. We note that the lowest pressure given in the table is $\frac{3}{8}$ inch, but from the ratio given on page 179 we may determine the speed, capacity, and horsepower at 0.20 in. as follows: Since the capacity varies as the square root of the pressure, and we require 12000 A. P. M. at 0.20 in. the corresponding capacity at $\frac{3}{8}$ in. will be 12000 $(0.375 \div 0.2)^{\frac{1}{2}} = 16450$ A. P. M.

We see from the table on page 210 that a 120-inch Planoidal exhauster at % inch static will have a rated capacity of 16030 A. P. M. at 152 R. P. M., and 2.62 H. P. We would use this size and operate it at slightly over the rated capacity to give 16450 A. P. M. at $\frac{3}{8}$ inch or 12000 A. P. M. at 0.20 in. The rated speed of the 120-inch fan at 0.20 inch pressure will be 152 (0.20 $\div 0.375)^{\frac{1}{2}} = 111$ R. P. M. and the rated power will be 2.62 $\left(\frac{111}{152}\right)^3$ = 1.02 H. P. When operating at 16450 \div 16030 = 102 per cent. of the rated capacity, the power required would be 1.08 H. P.

In order to determine the performance of a smaller fan under these conditions we will assume that a 100-inch Planoidal exhauster operating at over capacity is to be used. The outlet area of a 100-inch fan is 8.75 sq. ft. in area so that the velocity through the outlet will be $12000 \div 8.75 = 1370$ ft. per minute and the corresponding velocity pressure will be $(1370 \div 4005)^2 =$ 0.118 in. The ratio of static to velocity pressure will then be $0.20 \div 0.118 = 1.7$, and from the diagram on page 215 we note that with this ratio the exhauster will operate at 118 per cent. of rated capacity and require 110 per cent. of the rated power.

If 12000 A. P. M. is 118 per cent. of the fan's rated capacity at the speed required to meet the assumed conditions, we will have 12000 \div 1.18 = 10150 A. P. M. as the rated capacity. The table on page 210 does not give the speed and power required for 10150 A. P. M., but does give 182 R. P. M. and 1.81 H. P. for 11140 A. P. M. Since the speed varies directly and the power as the cube of the capacity we will have for 10150 A. P. M.,—182 (10150 \div 11140) = 162 R. P. M., and 1.81 (10150 \div 11140)⁸ = 1.28 H. P. as the rated speed and power. As already found from the diagram on page 215 with a ratio of static to velocity pressure of 1.7, the power required will be 110 per cent. of the rated, which gives us under the assumed conditions $1.28 \times 1.10 = 1.41$ H. P. when delivering 12000 A. P. M. against 0.20 in. static resistance at 162 R. P. M.

We see from the table on page 210 that a speed of 182 R. P. M. corresponds to a static pressure of 0.375 inch, and as the pressure varies as the square of the speed, the pressure for 162 R. P. M. will be 0.375 $(162 \div 182)^2 = 0.296$ in. That is, although the resistance of the system is only 0.2 in. and would call for a 120-inch fan, we may reduce the initial cost by using a 100-inch fan operating at a speed corresponding to approximately 0.3 in. with but 30 per cent. increase in the power consumption. Where the fan is to be direct connected to an engine and the exhaust

steam used in the heating coils, this additional power is of little or no consideration.

Selection of a Niagara Conoidal Fan

Example 3. The Niagara Conoidal fan may be selected either from the static pressure tables on pages 232 to 273 or from the total pressure tables on pages 228 to 231. The total pressure tables, like the tables for Planoidal fans, give the performance of this fan at its point of rating only. The static pressure tables give the performance at other than the rated capacity, and give the speed and power required on both sides of the most efficient point. The tables on pages 274 and 275 indicate the efficiencies obtainable under different conditions of pressure and outlet velocity with these fans. Thus we see that there is one point in each pressure column at which the fan will give the highest efficiency. In the selection of these fans it may often be found expedient to operate at other than the most efficient point.

When selecting a fan for use in a public building it is advisable to use a velocity of about 1800 feet per minute through the fan outlet, with a maximum allowable velocity of 2200 for such work. For industrial installations, where higher duct velocities are the rule, outlet velocities up to 4000 may be used, without varying greatly from the most efficient performance.

To illustrate the use of the static pressure tables we will assume that it is required to deliver 17000 cu. ft. of air per minute against a pressure of one inch static. By an inspection of the corresponding tables, we find that we may use a No. 6 at 419 R. P. M., 6.59 H. P., and an outlet velocity of 3200 feet per minute; a No. 7 at 332 R. P. M., 5.19 H. P., and an outlet velocity of 2400 feet per minute or a No. 8 at 291 R. P. M., 4.86 H. P., and an outlet velocity of 1800 feet per minute. For use in a public building the No. 8 should be selected, but in case it is desirable to use higher duct velocities and absolute quietness of operation is not essential, either the No. 7 or No. 6 may be used.

Example 4. A common case of variable resistance in a fan system of heating and ventilating is where a fan is selected to supply a definite amount of air, and during the winter this air is drawn through the heater, but during the summer the damper to the by-pass is open so that the air may be drawn through both the heater and by-pass. As shown by the tables on pages 446 and 447, the resistance due to the heater will depend upon its depth and the velocity of the air through the clear area. From page 457 we see that under average conditions, we may assume two velocity heads lost due to the by-pass. Assuming a case where the heater is four sections deep with a velocity of 1000 feet per minute through the clear area, we find from the table on page 446 that the resistance will be 0.382 in. Allowing a loss of 0.24 in. static in the piping system, the fan will be required to operate against a static pressure of 0.382 + 0.240 = 0.622 in. or $\frac{5}{6}$ in. This is under normal working conditions when the by-pass damper is closed.

We will first assume that a Planoidal exhauster is required to deliver 25000 A. P. M. under the above conditions. With this type of fan at rated capacity the static will be 79 per cent. of the total pressure, so that with a static resistance of 0.622 in. the corresponding total pressure will be $0.622 \div 0.79 = 0.787$ in. or approximately $\frac{34}{4}$ in. From the capacity table on page 210, we find that a 130-inch Planoidal exhauster at $\frac{5}{6}$ inch static pressure has a capacity of 24150 A. P. M. at 180 R. P. M. and will require 6.57 H. P. As this capacity is within a few per cent. of that required, it will be taken as the rated condition.

According to the data given on page 457 the resistance of a standard by-pass is approximately the same as that for four sections of Buffalo heater, so that in the case assumed when the by-pass damper is opened the effective area will be doubled. Since the loss due to the resistance varies as the square of the velocity and the velocity is to be reduced to $\frac{1}{2}$, the resistance for the same air quantity will be $(\frac{1}{2})^2$ or $\frac{1}{4}$ of what it was when all the air passed through the heater. That is, with the by-pass damper open, the resistance at the heater will be one-fourth of 0.382 or 0.095 inch.

With the damper in the by-pass open the static resistance of the system will be reduced to 0.095 + 0.240 = 0.335 in. providing the same air quantity is handled and it will be required to determine the results obtained under this new condition. The area of the outlet of the 130-inch fan is 14.85 sq. ft., so the velocity through the outlet under rated conditions would be $24600 \div 14.85 = 1685$ ft. per minute and the corresponding velocity pressure $(1685 \div 4005)^2 = 0.177$ in. With the by-pass damper open the static pressure based on the same air quantity is 0.335 in. and the ratio of static to velocity pressure will be $0.335 \div 0.177$ in. = 1.89. From the diagram on page 215 we find that with this ratio the actual static pressure will be 65.5 per cent., the capacity 116.5 per cent. and the power 109 per cent. of the rated as given on page 187. That is, we will have

actual pressure = $0.622 \times 0.655 = 0.407$ in. static. actual capacity = $24150 \times 1.165 = 28150$ A. P. M. actual power = $6.57 \times 1.09 = 7.15$ H. P.

Correction for Temperature

Example 5. A case frequently met in selecting a fan is where the air to be handled is specified at some temperature other than the standard of the fan tables (70° F.). For instance, a "B" Volume Exhauster is required to handle 5500 cu. ft. of air per minute at a temperature of 600° F. against a pressure of two ounces. What size exhauster should be used and what will be the speed and horsepower? This fan is to handle the air at 600° while the capacity tables are based on air at 70°.

As explained on page 179, if the speed and capacity are kept constant the pressure and horsepower will vary inversely as the absolute temperature. Thus an increase in temperature from 70° to 600° doubles the absolute temperature $(1060 \div 530 = 2)$ and if we select a fan that will handle 5500 A. P. M. at 70° against four ounces it will have the same capacity at the same speed against two ounces when the temperature is 600° and the power will be half that given in the table for four ounces. From the capacity table of "B" Volume Exhausters on page 335 we find that the nearest size to that required will be No. 8, operating at 1420 R. P. M. and requiring $10.20 \div 2 = 5.1$ H. P.

Another example illustrating the effect of temperature would be to assume a fan is delivering 3500 A. P. M. at 1000° F. against $1\frac{1}{2}$ oz. pressure with a speed of 920 R. P. M. What will be the speed and capacity of this fan at 500° and 2 oz. pressure?

The relative pressure of the air at 1000° and 500° is given by the ratio of the absolute temperature, or $1460 \div 960 = 1.52$. That is, if this fan handles the same volume of air at the same speed, due to the change in the temperature the pressure developed will be $1.5 \times 1.52 = 2.28$ oz. But this fan is required to operate at 2 oz. instead of 2.28 oz., which calls for a lower speed. We may see from page 179 that the speed and consequently the capacity will vary as the square root of the pressure, so the speed at 2 oz. will be 920 $(2 \div 2.28)^{\frac{1}{2}} = 708$ R. P. M. and the capacity will be $3500 (2 \pm 2.28)^{\frac{1}{2}} = 2700$ A. P. M. Thus we see that this same fan will deliver 2700 A. P. M. at 500° against 2 oz. pressure when operated at 708 R. P. M.

Correction for Altitude

Example 6. The following example represents the calculations required to correct the fan performance to a sea-level (29.92 inches barometer) basis. Required a fan to handle 40000 A. P. M. against 0.5 in. static pressure at an altitude of 5000 feet with a temperature of 70°. As the fan tables are based on air at sea-level basis. From the diagram on page 25 we note that the relative pressure for this altitude is 0.835, so that a sea-level pressure corresponding to a pressure of 0.5 in. at 5000 altitude is $0.5 \div 0.835 = 0.6$ in., or approximately $\frac{5}{8}$ in. The horsepower required to operate the fan will be 83.5 per cent. of the rated horsepower as given in the capacity tables for $\frac{5}{8}$ in.

We find from the table of Niagara Conoidal capacities on page 248 that a double No. 8 fan with an outlet velocity of 2200 feet per minute would answer the requirement at $\frac{5}{6}$ in. at 238 R. P. M. and 8.66 H. P. At 5,000 altitude the power consumption will be $8.66 \times 0.835 = 7.23$ H. P.

Another example illustrating the correction for altitude would be to require an induced draft system for 1600 boiler H. P., at an altitude of 5200 feet with flue gases at 550° F. and a static pressure of one inch required. From the diagram on page 25 we find that the factor for 5200 altitude is 0.83. The corresponding pressure at sea-level will then be $1 \div 0.83 = 1.20$ in.

From the table on page 325 we find that a 150-inch Planoidal exhauster operating at 305 R. P. M. will have a capacity of 63110 A. P. M. at 1.25 in. static with a temperature of 550° and require 34.0 H. P. With an allowance of 32.4 A. P. M. at this temperature per boiler H. P. this fan will be capable of supplying draft for 1950 H. P. of boilers at sea-level. The air required per boiler horsepower at an altitude of 5200 feet will be $32.4 \div$ 0.83 = 39.0 A. P. M. so that the draft capacity of this fan at 5200 altitude will be only $63110 \div 39.0 = 1620$ or $1950 \times 0.83 = 1620$ boiler H. P. The power requirements at 5200 altitude will be $34.0 \times 0.83 = 28.2$ H. P.

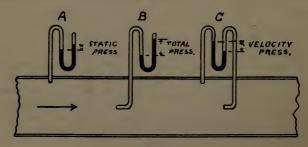
SECTION II FAN TESTING

It is frequently necessary to make a test on a fan installation in order to determine the quantity of air being delivered. There are several methods of making this determination, depending on the degree of accuracy desired, the object of the test, or the conditions under which the system is installed. The velocity and quantity of air delivered by a fan or flowing through a duct may be found by means of a pitot tube, an anemometer, a converging nozzle, an orifice, or a short length of pipe. Each method may be especially applicable under various conditions and a selection should depend on the object and accuracy desired.

The most accurate method for ordinary work is to use the pitot tube, either in an air duct or in connection with a converging nozzle attached to the fan outlet. The anemometer is especially useful in determining the velocity and quantity of air entering a room in order to properly proportion the air distribution in an indirect heating or ventilating system. An orifice or a short length of pipe is frequently used in connection with test work, where a permanent piece of apparatus is desired.

The Pitot Tube

The pitot tube is an instrument used for making velocity measurements of a current of air, the principle of its action being shown by the accompanying diagram. As already explained,



when there exists a flow of air due to a certain pressure, a part of this pressure, termed the velocity head, is transformed into velocity, while the balance, termed pressure of static head, serves to produce pressure. If a bent tube with an open end be inserted in an air duct, as at B in figure on page 190, with the open end facing the air current, a pressure due to both the velocity and static head will be produced in this tube. This is the total or dynamic head, and the amount can be read on an attached gauge or manometer tube. If, instead of a bent tube, a straight tube be inserted as at A, the difference in levels in the manometer tube will indicate the static head or pressure. The velocity head or pressure may then be determined by subtracting the static from the total manometer reading.

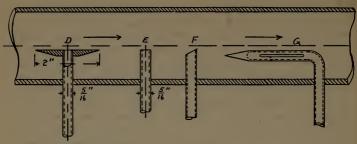
The pitot tube as ordinarily used is an instrument combining the tubes just described, as shown at C, the outer ends being connected to the two legs of the same manometer. By this means the subtraction is made automatically and the difference as shown by the gauge is due to velocity pressure only. These tubes are usually combined in some form as shown in the following figure.



Care should be taken to have all of the connections made tight, especially on the static side, as a very slight leak here will eause considerable error. The small holes as shown above in the static tube should be about 0.02 in. in diameter.

The greatest difficulty to be encountered in air measurements is in obtaining accurate static pressure readings. Many different forms of static tubes have been used, with varying degrees of accuracy. Some of the more common forms are shown on page 192. Charles H. Treat in a paper on "Measurements of Air in Fan Work"* gives the results of his efforts to check the accuracy of some of these forms. He found that tube D was fairly accurate so long as it was set exactly parallel to the air flow, but the open tube E held at right angles to the air flow gave readings as much

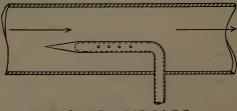
^{*} Am. Soc. Mech. Engrs., Dec., 1912.



DIFFERENT FORMS OF STATIC TIPS,

as 50 per cent. too low. The total pressure, or impact tube, as shown in the sketch representing a pitot tube, will give practically true readings, so that if the static readings are too low the corresponding velocity pressure readings will be too great.

The Gebhardt tube uses a static tip which has the end beveled as at F, in order to avoid the suction of the air flow across the end of the tube, but Prof. Gebhardt states that further experiments are necessary to show whether any fixed angle is applicable to all velocities. A static tube as shown at G is frequently used, having slots on the sides of the tube, the Taylor pitot tube being an adaptation of this form. Mr. Treat found that a slot $\frac{5}{8}$ in. long and 0.01 in. or less wide in a $\frac{1}{4}$ -inch tube gave good results, but it is advisable to cover these slots with a piece of fine mesh wire cloth.



APPROVED FORM OF STATIC TIP

The static tube here shown is the most approved form, and is the one recommended by the A. S. M. E. for fan testing work. It may be combined with the impact tube to form a pitot tube as already shown. Charles H. Treat found that a static tube of this form with clean holes 0.02 in. in diameter in $\frac{1}{4}$ -inch tubing $\frac{1}{42}$ in. thick, gave static readings accurate to within less than one per cent. of the pressure due to the velocity. A hole $\frac{1}{16}$ in. in diameter in this tube gave readings considerably off, while a 2-in. slot $\frac{1}{16}$ in. wide gave velocity readings approximately 10 per cent. too low. Covering the slot with wire cloth improved the results obtained. A $\frac{5}{8}$ -in. slot 0.01 in. or less in width gave fairly accurate results. The tube of the above standard form gave fairly accurate results even though as much as five degrees out of parallel with the air flow.

A very complete series of tests have been made by W. C. Rowse* in which he compared different forms of pitot tubes with the readings of a Thomas electric meter. The author used a pitot tube similar in shape to the one already described, and found that "of the various forms of static openings in the pitot tube itself, very small holes in a perfectly smooth surface give the most accurate results. Slots give erroneous static pressures and beveled-ended tubes for obtaining static pressures are not reliable."

A convenient form of gauge for use with low pressure is the ordinary Ellison differential draft gauge. Mineral seal oil should be used in the Ellison gauge, but it is so graduated that it gives the pressure directly in inches of water, without any correction. The mineral seal oil as ordinarily used for this purpose has a specific gravity of 0.8284.

The theory of the pitot tube is thoroughly discussed by Frank H. Kneeland, together with a study of some of the different forms, in a paper recently read before the American Society of Mechanical Engineers.**

Having determined the velocity head as above explained, the actual velocity may be calculated approximately by means of the formula

$$V = 1096.5 \sqrt{\frac{p}{W}}$$
(84)

where

V = velocity of air in ft. per min.

p = pressure in in. of water.

W = weight of air in lbs. per cu. ft.

*"Pitot Tubes for Gas Measurement" Am. Soc. Mech. Engrs., Sept., 1913.

^{**&}quot;Some experiences with pitot tube on high and low air velocities" Am. Soc. Mech. Engrs., Dec., 1911.

The relationships between velocity and pressure will be found on page 16, from which we see that if we have dry air at 70° F. and 29.92 inches barometer, we will have W = 0.07494, hence the approximate formula (84) becomes

$$V = 4005 \nu p$$

Where the pressure p is expressed in inches of water, or

$$V = 5273 \nu p$$

where p is expressed in ounces per square inch.

The above formulae are only accurate for low pressures, and should not be used for over 10 inches of water. For more accurate work or for high pressures the following formulae should be used. As a matter of ready reference the table of velocity for various pressures as given on page 21 will be found convenient.

Capt. D. W. Taylor in a paper entitled "Experiments with Ventilating Fans and Pipes''* gives the following exact formula for the pitot tube:

$$\frac{V_{1}^{2} - V_{2}^{2}}{2 g} = \frac{y}{y-1} \times \frac{P_{2}}{W} \left[1 - \left(\frac{P_{1}}{P_{2}}\right)^{\frac{y-1}{y}} \right]$$
(85)

where

 V_1 = velocity in ft. per second at a point where the $pressure = p_1$ in lbs. per sq. ft.

p₂ = pressure in lbs. per sq. ft. at any other point.

 $V_2 =$ velocity in ft. per second.

 $W = weight of air in lbs. per cu. ft. where press. = p_a$

 $\mathbf{v} = \mathbf{ratio}$ between specific heats of air under constant pressure and constant volume = 1.408.

g = acceleration due to gravity in ft. per second.

The above formula has been presented in a simplified form by Frank H. Kneeland** as follows:

$$V_1 = 4046.16 \sqrt{\frac{p_2 - p_1}{W} (1 - 0.355k + 0.202k_2 - 0.137k_3)}$$
(86)
here

W

$$\mathbf{k} = \left(\frac{\mathbf{p}_2}{\mathbf{p}_1} - 1\right)$$

The values given above are for a temperature of 70° F., a barometric pressure of 29.92 inches, and a humidity of 70 per cent.

^{*}Society of Naval Arch. and Marine Engrs., 1905, p. 35.

^{**&}quot;Some experiences with pitot tube on high and low air velocities" Am. Soc. Mech. Engrs., Dec., 1911.

From the preceding it is seen that the velocity at 70° F. and 29.92 inches barometer due to one-inch pressure is 4005 feet per minute and the velocity at any other pressure may be determined from the above relation. That is, the velocity varies as the square root of the pressure. For any other temperatures the velocity may be found by inserting the proper values of W in formula (84), or from the ratio of the absolute temperatures or barometric pressure, since at constant pressure the velocity will vary directly as the square root of the barometric pressure.

These formulae may be considered sufficiently accurate for ordinary velocities, say up to 6000 feet per minute. Above that velocity and for very accurate work, various corrections should be made. These corrections, based on the experiments of Capt. D. W. Taylor are discussed by Mr. Kneeland in the paper already referred to.

Use of the Pitot Tube in an Air Duct

For fan testing or in ventilation work the pitot tube may be used to determine the velocity, and hence the quantity, of air flowing through a duct or pipe. The tube should be inserted at a point where the duct is straight and the flow undisturbed. In testing a fan the pitot tube should be placed from 10 to 20 diameters from the fan outlet with the point directly facing the blast. The air pipe should be the same diameter as the fan outlet.

The velocity pressure as shown with the tube in the center of the duct will be higher than the average, and will vary at different points from the center to the sides of the duct. In order to obtain the true or average pressure it is necessary to multiply the velocity pressure reading obtained at the center by the proper coefficient. Various authorities give a coefficient of from 0.81 to 0.82 for circular pipes, by which the velocity pressure readings taken at the center of the pipe should be multiplied to obtain the corrected average pressure. Consequently the velocity based on the observed pressure readings may be multiplied by the coefficient 0.91 to obtain the corrected average velocity.

For more accurate work it is better to make a traverse of the pipe and either determine the coefficient for the case in question or take the average of all of the readings. Where the duct is rectangular it may be divided into a number of small squares or rectangles and a reading taken in the center of each. Then the average of all of the velocities corresponding to these pressures will give the true velocity in the duct. In case the pipe is round its area should be divided into a number of concentric zones or rings of equal area, and four readings taken in each area, readings being taken horizontally and vertically across the pipe.

The position of each successive point may be found by dividing each ring into two equal areas and adding one of these to the sum of the preceding areas. The radius of this resulting area will locate the desired point.

Expressed by means of a series of formulae, these points may be found as follows:

$$R_1 = \sqrt{\frac{a}{6.2832}}$$
(87)

$$R_2 = \sqrt{\frac{a + (a \div 2)}{3.1416}} \tag{88}$$

$$R_3 = \sqrt{\frac{2a + (a \div 2)}{3.1416}}$$
(89)

$$R_4 = \sqrt{\frac{3a + (a \div 2)}{3.1416}} \tag{90}$$

Where R_1 , R_2 , etc., = the distance from the center to the points where the readings should be taken in each successive ring.

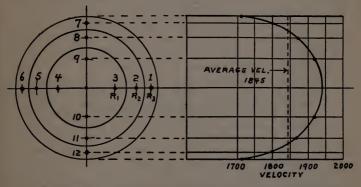
 $\mathbf{a} = \mathbf{the}$ area of each zone or ring.

PIPE TRAVERSE FOR PITOT TUBE READINGS

Distance From Center of Pipe to Point of Reading in Per Cent. of Pipe Diameter

No. of Equal Areas in Traverse	No. of Readings	First R1	Second R2	Third R ₃	Fourth R4	Fifth R ₅	Sixth R ₆	Seventh R_7	Eighth R ₈
3 4 5 6 7 8	12 16 20 24 28 32	$20.4 \\ 17.7 \\ 15.5 \\ 14.5 \\ 13.4 \\ 12.5$	35.3 30.5 27.2 25.0 23.1 21.6	45.5 39.4 35.3 32.3 29.9 28.0	46.6 41.7 38.2 35.3 33.2	47.4 43.3 40.1 37.6	47.9 44.3 41.5	48.2 45.1	48.4

The location of the points on a traverse where readings should be taken are shown in the accompanying sketch. The table on page 196 is based on formulae (87) to (90) for laying out a traverse and will be found very convenient for that purpose. As an example of its use we will assume that a traverse is to be made of a 24-inch pipe, twelve readings to be taken. One reading will be taken at $0.204 \times 24'' = 4.9''$ from the center of the pipe; one at $0.353 \times 24'' = 8.46''$ from the center, and one at $0.455 \times 24'' =$ 10.92'' from the center.



An example of laying out a traverse and finding the average velocity through a round duct is illustrated in the accompanying figure drawn from test results. Twelve readings were taken as shown on the diagram, the points being laid out according to the table on page 196. The velocities were then computed for each point and the average velocity for each area plotted as shown, these points on the lower and upper half of the plot being the same. A curve drawn through these points indicates the velocity at the edge and at the center of the pipe, and these points should be used in calculating the average velocity.

The Anemometer

The anemometer is used in many cases where the velocity of the air is low or extreme accuracy is not required. It is more frequently used to determine the velocity of the air leaving a register or air vent than for testing a fan, although it may be used for either purpose. An anemometer should be frequently calibrated, and when used in a current of hot air the bearings of the instrument are liable to become dry and the readings affected by friction. Such an instrument may vary as much as 10 or 20 per cent. from the true reading.

The space over which the velocity is to be measured should be divided into a considerable number of smaller squares and the velocity readings taken before each square; the average of these readings gives the air velocity in the duct or pipe. Another method frequently used when taking readings before a register or outlet in wall is to take a series of readings along the two diagonals of the openings, each reading being taken during an equal interval of time and similar distances from the center.

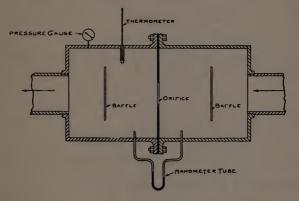
A special committee, appointed by the American Society of Heating and Ventilating Engineers to draft a standard method for measuring air velocities at supply openings by means of an anemometer, reported January 23, 1913, as follows:

- FIRST:—The openings shall be divided into equal rectangular areas, no side of which shall be over 10 inches long excepting where this would require more than ten readings, in which case the opening shall be divided into 12 equal areas.
- SECOND:-Readings are to be taken in every case at the center of every area.
- **THIRD**:—Readings are to be one-half minute duration, the anemometer being held at the register base or in the plane of the opening.
- FOURTH:---Where the diffusers are used, a total area is to be computed on the basis of the periphery of the diffuser.
- FIFTH:—The average of the readings are to be considered as the average velocity at the opening. Where negative velocities are found, they are to be deducted in arriving at the average velocity.
- SIXTH:—In computing volume, the net area of the opening is to be taken, the volume to be considered as the product of the average velocity and the net area of the opening. In case the anemometer is held two inches from the register face, no deduction should be made for the register mesh.

The Orifice

An orifice in connection with some form of testing apparatus is frequently used for fan testing work, usually as a part of a permanent testing plant where the air is blown into a large airtight box and escapes from the box through an orifice. A coefficient of 0.600 applied to the velocity is commonly used with this apparatus. Professor Durley describes in Vol. 27 of the Trans, A. S. M. E. a series of tests where various sized orifices were attached to the end of a gauging box and a set of coefficients determined for the different conditions.

The orifice may also be used for measuring the air delivery in connection with compressed air systems, where the air is under a pressure of several atmospheres. A convenient form of apparatus for such use is here shown, in which the air passes through an enlargement in which the orifice is fastened.



As shown in the sketch, baffles should be provided on each side of the orifice. The pressure, P, should be taken on the leaving side of the chamber, the temperature being taken on either side. The drop in pressure, p_{τ} , between the two sides of the orifice may be measured either in inches of water or of mercury by means of a manometer connected to the two sides of the chamber. The inner ends of these tubes should enter well between the baffle and the orifice plate. Different sizes of orifices may be used in the same apparatus, according to the pressure carried, diaphragms with openings from 1 to $2\frac{1}{2}$ inches in diameter being a suitable range for a chamber having a 4-inch inlet.

The equation for this apparatus would then be

$$Q = 100 A \sqrt{P T p_r}$$
(91)

where

Q = cu. ft. free air per min.

A = area of orifice in sq. ft.

P = absolute pressure in lbs. per sq. in.

T = absolute temperature deg. F.

 $p_{\tau} = drop$ in pressure in inches of mercury.

Orifice at End of Pipe

An orifice may be used on the end of a length of pipe for measuring the air discharged, as shown by Fig. a. The coefficient for such a case is

$$C = \frac{0.60}{\sqrt{1 - \left(\frac{A_2}{A_1}\right)^2}}$$
(92)

where

C = coefficient of discharge.

 $A_1 = area of pipe.$

 $A_2 = area of orifice.$

The quantity of air delivered by a given static pressure in the pipe may be determined by

$$Q = 1096.5 \text{ C A}_2 \sqrt{\frac{p}{W}}$$
 (93)

where

Q = cu. ft. of air per min.

 $C = above \ coefficient \ of \ discharge.$

 $A_2 = area of orifice in sq. ft.$

p=static pressure in inches of water in main pipe.

W = weight of air in lbs. per cu. ft.

For values of W see table on page 17.

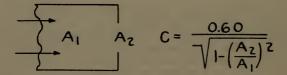


FIG. a ORIFICE AT END OF PIPE.

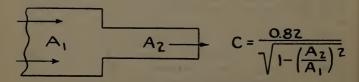


FIG. & SHORT PIPE ATTACHED TO END OF LARGER PIPE.

The orifice may be replaced by a short length of pipe as in Fig. b, in which case the coefficient of discharge becomes

$$C = \frac{0.82}{\sqrt{1 - \left(\frac{A_2}{A_1}\right)^2}}$$
(94)

The above coefficients have been verified experimentally and found to be adapted to measurements of air under low pressures. Short Length of Pipe

A short length of pipe (preferably three diameters long) connected to a box or plenum chamber into which the fan discharges is frequently used instead of an orifice for fan testing, and for several reasons makes a better arrangement. It is used on the outlet of a tight box into which the air is blown by the fan, the air escaping through the short pipe. The static pressure in the box is carefully noted, it being a measure of the fan performance. The box leakage, if any, should be determined.

A coefficient of discharge of 0.825 should be applied to the area of the short pipe to determine the true effective area, or to the velocity of the air. If required, a traverse may be made of the pipe with a pitot tube and the coefficient determined for any special cases.

The quantity of air discharged may be determined by means of the formula:

$$Q = 1096.5 C A \sqrt{\frac{p}{W}}$$

where

Q = cu. ft. of air per min.

C = coefficient of discharge.

A = area of pipe in sq. ft.

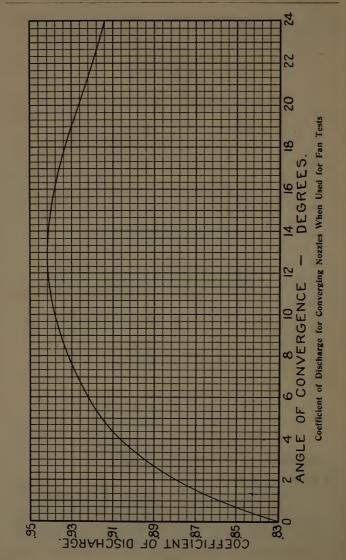
p=static pressure in inches of water in the plenum chamber.

W = weight of air in lbs. per cu. ft.

For values of W see the table on page 17.

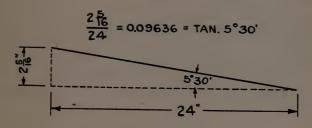
The Converging Nozzle

A method frequently used in commercial work for fan testing, or for testing a special fan before its installation, is by means of a converging nozzle attached directly to the fan outlet. The pressure produced by the velocity of the air is measured at the point of discharge by means of a pitot tube, placed at the center



of the nozzle outlet. Proper correction must be made according to the accompanying curve of coefficients of discharge for converging nozzles. This curve is based on coefficients as given in Merriman's Treatise on Hydraulics.

To illustrate the use of the converging nozzle, we will take the case of a 40-inch planing-mill exhauster at 1780 R. P. M., blowing through a converging nozzle having the inlet and outlet ends 14 and $9\frac{3}{8}$ inches square, with sides sloping at an angle as here shown. The outlet area of the nozzle would be 0.61 sq. ft.



The angle of convergence of the cone outlet would be 11° and from the curve on page 202 the corresponding coefficient is 0.94.

The pressure on the fan will be taken at 3 inches; and the corresponding velocity will be $4005 \sqrt{3} = 6950$ ft. per min. At this velocity through the outlet of 0.61 sq. ft. the fan would handle 4230 A. P. M., but the actual quantity handled will be

$$4230 \times 0.94 = 3980$$
 A. P. M.

Coefficients of Discharge for Air Measurements

Various coefficients are used in the calculation of fan performance or in air measurements, and their derivation and application will be found fully discussed under their proper heading. The following summary is given merely as a matter of convenience, but the factors should not be used without first having an intelligent understanding of their proper application. In case of special requirements it may be found necessary to modify the given coefficient accordingly.

Coefficients of Discharge for Air Measurements

Coefficient for sharp orifice in thin plate - - - - - 0.600

Coefficient for orifice at end of pipe

Coef. for short pipe attached to end of larger pipe For explanation see page 201.

Coefficient for short length of pipe - - (blowing from plenum chamber)

Coefficient for short pipe on outlet of fan (see page 201) - 0.95 Coefficient for round pipe (pitot tube in center) - - - 0.91 Coefficient for converging nozzle (see curve page 202). Coefficient for diverging nozzle (see curve page 223).

0.82

The quantity of air to be measured may be calculated by means of the formula

$$Q = 1096.5 C A \sqrt{\frac{p}{W}}$$

where

Q=cu. ft. air per min. C=coefficient of discharge. A=area of pipe in sq. ft. p=static pressure in inches causing flow of air. W=weight of air in lbs. per cu. ft.

For values of the weight of air in pounds per cubic foot for various atmospheric conditions see the table on page 17.

The coefficients given above are to be applied to velocity, capacity, or to the effective area of pipe or outlet. The proper coefficients to be applied to the pressure readings will be the square of the ones given above. Thus the coefficients for pressure in a round pipe varies from 0.81 to 0.82. These are to be applied to the pressure readings of the pitot tube when taken at the center of the pipe or duct. This coefficient for round pipes is based on test data, but should be decreased for pipes below 12 inches in diameter and increased by a small amount for pipes above 24 inches in diameter.

SECTION III FAN CAPACITIES

The following chapter gives the capacity tables and performance curves for the various styles of Buffalo fans. These are divided into the following divisions: Planoidal Exhausters, Planoidal Blowers, Niagara Conoidal Fans, Turbo-Conoidal Fans, Induced Draft Tables, Miscellaneous fans and blowers. In each case the corresponding performance curves follow the capacity tables. The tables show the rated speed, capacity, and horsepower for fans operating at the different pressures stated, with the exception of the static pressure tables of the Niagara and Turbo-Conoidal fans, which give the performance at other than the rated point.

Use of Performance Curves

In connection with the steel plate and multivane fans, as well as several other styles, are shown relative performance curves, based on actual tests. The scale on the lower edge of each diagram reads per cent. of rated capacity, while the lefthand margin reads directly in per cent. The capacity curves show the relative horsepower, efficiency and pressure at any capacity in per cent. of their respective values at rated capacity. Thus we see from the diagram on page 214 of Planoidal Exhausters, if the fan is operated at say 80 per cent. of the rated capacity, the horsepower required will be 87.5 per cent. and the total pressure 116 per cent. of the rated values as given in the capacity tables. The efficiency will be 6 per cent. greater than at rated capacity.

The use of these diagrams for the analysis of fan performances has been fully covered under the subject of "Fans" (Part IV, Section I) and their application in the selection of a fan may be found on page 182, together with the practical examples explaining the various calculations involved. The relations between static, velocity, and total pressure will be found on page 177.

Combination Fan, Heater and Engine Tables

A series of tables giving combinations of fan, heater, and engine for various duties will be found in Part IV, Section VIII, following the examples on "The Selection of Apparatus." The air capacities given are based on the assumption that an average maximum value for the total pressure, in case of an installation in a public building such as a school or theatre, will be about one inch, and for industrial installations about two inches. A series of heater sizes is given for each fan, and a selection should be made on the basis of allowable velocity through the clear area. For public buildings the larger sizes should be used, and for industrial installations, the smaller. The depth of the heater will depend on the temperature range to be cared for, and may be determined from the heater tables on pages 418 to 431. The low pressure engines were selected on the assumption of 20 to 25 pounds and the high pressure engines on 80 to 100 pounds steam pressure at the throttle. The engines are all suitable for direct connection to the given size of fan.



Planoidal Type "L" Fan Direct Connected to Class "I" Vertical Cylinder Below Shaft Engine CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE EXHAUSTERS (TYPE-L) UNDER AVERAGE WORKING CONDITIONS

					Tempera	iture of 7	Temperature of 70° F., 29.92 Inches Barometer	2 Inches	Baromet	er				
Size	Dlam. Blast-	Area of Outlet	1/2"	Total Press. or 0.288 Oz.	. or	18/2 8/8	Total Press. 0.360 Oz.	s. or	34"	Total Press. or 0.433 Oz.	s. or		Total Press. 0.505 Oz.	s. or
	Wheel		R. P. M.	Vol.	Н. Р.	R. P.M.	Vol.	Н. Р.	R.P.M.	Vol.	Н. Р.	R. P.M.	Vol.	Н. Р.
30 33	19 14" 22 14" 25 34"	$\begin{array}{c} 0.77\\ 1.04\\ 1.36\\ \end{array}$	620 532 465	1030 1400 1820	0.18 0.24 0.31	693 594 520	$1150 \\ 1560 \\ 2040$	0.25 0.34 0.44	760 651 570	1260 1710 2230	$\begin{array}{c} 0.32 \\ 0.44 \\ 0.58 \end{array}$	819 702 614	1350 1840 2410	$\begin{array}{c} 0.41 \\ 0.55 \\ 0.72 \end{array}$
45 55 55	$\frac{29}{32}\frac{7_8''}{1_8''}$	1.75 2.16 2.61	414 372 338	2010 2850 3440	0.40 0.49 0.59	462 415 378	2580 3180 3850	0.55 0.68 0.83	506 456 414	2820 3490 4220	0.73 0.90 1.09	546 492 447	3050 3760 4550	0.91 1.13 1.37
8000	38 ½" 45" 51 ¾	3.13 4.26 5.54	310 266 233	4100 5580 7290	0.71 0.96 1.25	347 297 260	4580 6230 8140	$\begin{array}{c} 0.98 \\ 1.34 \\ 1.75 \end{array}$	380 326 285	5020 6830 8920	$1.30 \\ 1.76 \\ 2.30 \\ 2.30 \\ 1.76 \\ $	410 351 307	5410 7370 9620	1.63 2.21 2.89
0001	57 78" 64 18" 70 34"	$ \begin{array}{c} 7.10 \\ 8.75 \\ 10.57 \end{array} $	207 186 169	9220 11380 13770	$ \begin{array}{c} 1.59 \\ 1.96 \\ 2.37 \end{array} $	231 208 189	10270 12720 15390	$2.21 \\ 2.73 \\ 3.30 \\ 3.30 \\ 3.30 \\ 3.21 \\ 3.30 \\ $	253 228 207	$\frac{11290}{13940}$ 16870	2.92 3.60 4.36	273 246 224	$12180 \\ 15040 \\ 18190$	3.66 4.51 5.46
120	77 14" 83 145" 90"	13.00 14.85 17.20	155 143 133	$16390 \\ 19240 \\ 22310 \\ 22310 \\ 10$	2.82 3.31 3.84	173 160 149	$\frac{18320}{21500}\\24930$	3.90 4.61 5.35	190 175 163	20080 23560 27330	5.18 6.08 7.05	205 189 176	21650 25410 29480	6.50 7.63 8.84
150	96 15" 103" 109 14"	19.70 22.40 25.40	124 116 110	$25610 \\ 29140 \\ 32900$	4.41 5.01 5.66	139 130 122	$28620 \\ 32560 \\ 3670$	6.14 6.99 7.89	152 142 134	$31370 \\ 35690 \\ 40290$	$ \begin{array}{c} 8.10 \\ 9.21 \\ 10.4 \\ \end{array} $	164 154 145	33830 38500 43460	10.2 11.6 13.0
190	$\frac{11534''}{12214''}$	$28.50 \\ 31.70 \\ 35.30$	103 98 93	$36880 \\ 41100 \\ 45540$	6.34 7.07 7.83	116 110 104	41200 45930 50880	$ 8.84 \\ 9.86 \\ 10.9 $	127 120 114	45170 50330 55760	11.7 12.9 14.4	137 129 123	48720 54300 60150	14.6 16.3 18.1
210	$135'' 141 y_{5''} 148'' 148''$	38.7 42.2 46.5	89 85 81	50200 55100 60210	$ \begin{array}{c} 8.64 \\ 9.48 \\ 10.4 \end{array} $	95 95 90	56100 61550 67280	12.0 13.2 14.4	109 104 99	61480 67480 73750	15.9 17.4 19.0	117 112 107	66310 72780 79540	19.9 21.9 23.9
				St	atic Pres	ssure is 7	Static Pressure is 79% of the Rated Total Pressure	e Rated	Total Pr	essure				

CAPACIFIES OF BUFFALO PLANOIDAL STEEL PLATE EXTAUSTERS (TYPE L) UNDER AVERAGE Working State VORTIONS Site Buffalo OF TATIONAL STEEL PLATE EXTAUSTERS (TYPE L) UNDER AVERAGE Site Buffalo OF TATIONAL STEEL PLATE EXTAUSTERS (TYPE L) UNDER AVERAGE Site Blass Outed Tation Colspan="2">(1* Total Press. or 0.337 Os. 1/4" Total Press. or 0.357 Os. 1/4" Total Press. or 0.350 Os. 1/4" Total Press. or 0.351 0s. 1/4" Total Press. or 0.351 0s. 1/4" Total Press. or 0.350 0s. 1/4" Total Press. or 0.351 0s.
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Temperature of 70° E 20.02 Inches Recommendation

CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE EXHAUSTERS (TYPE L) UNDER AVERAGE

Н. Р. 7.34 9.06 3.264.445.80117.5 130.9 145.0 159.9 175.5 191.8 $13.1 \\ 17.8 \\ 23.2 \\$ $29.4 \\ 36.3 \\ 43.9 \\ 43.9 \\ 100 \\$ 52.2 61.3 71.0 81.6 92.8 04.8 3 ½2" Total Press. or 2.019 Oz. 10840147601928043380 50900 59040 67770 77110 87060 97600 108740 120490 132830 145780 159310 24400 30120 364502710 3690 1820 6100 7530 9110 Vol. R. P. M. 1641 1406 1230 1094 984 895 820 703 615 547 492 448 410 379 352 328 308 290 274 259 246 234 224 214 Н. Р. 2.593.524.605.837.19 8.70 $126.9 \\ 139.3 \\ 152.2 \\ 152.$ 64.8 73.6 83.1 $\begin{array}{c} 93.2\\ 103.4\\ 115.1\end{array}$ $23.3 \\ 28.8 \\ 34.8 \\$ 10.4 14.1 18.4 41.448.656.4or 3" Total Press. 1.734 Oz. $\begin{array}{c} 122980 \\ 134970 \\ 147510 \end{array}$ 100401366017850 $22590 \\ 27900 \\ 33740 \\ 33740 \\$ $\begin{array}{r} 40650 \\ 47100 \\ 54750 \end{array}$ 62740 71370 80590 90340 100670 111540 2510 3420 4460 5650 6970 8440 Static Pressure is 79% of the Rated Total Pressure Vol. Temperature of 70° F., 29.92 Inches Barometer R. P. M. 912 829 $519 \\ 302 \\ 139 \\ 139$ 570 570 506 456 414 351 326 304 285 268 253 240 228 217 207 198 Н. Р. 7.88 10.7 14.0 $\begin{array}{c}
 1.97 \\
 2.68 \\
 3.50 \\
 \end{array}$ 4.435.47 6.6296.5 105.9 115.8 17.721.9 26.5 31.537.042.949.3 56.0 63.3 70.9 79.0 87.6 Ы 2 ½ Total Press. 1.442 Oz. 82480 91900 101800 12270123200 134670 9160 12470 16290 20600254603080036660 43020 49890 $57260 \\ 65170 \\ 73570 \\ 73570 \\ \end{array}$ 2290 3120 4070 5160 5360 7700 Vol. R. P. M. 387 189 040 924 832 756 693 594 520 $462 \\ 416 \\ 378 \\ 378 \\$ 347 320 297 277 260 245 231 219 208 98 89 81 Н. Р. $1.41 \\ 1.92 \\ 2.51$ 5.64 7.67 10.0 3.173.924.7412.7 22.626.530.735.3 40.1 45.350.7 56.5 62.7 69.1 75.8 82.9 Total Press. or 1.154 Oz. 184402277027540 $32780 \\ 38470 \\ 44630 \\$ 51220 58270 65790 73760 82180 91060 100390 110170 120420 4610 5690 6890 8200 11540 14570 2050 2790 3630 Vol. R. M. P. č 413 372 338 177 169 162 240 064 930 827 744 676 5320 532 165 310 286 266 248 233 219 207 196 186 Area of Outlet Sq. Ft. 7.10 8.75 10.57 19.7022.40 25.40 28.50 31.70 35.30 0.771.041.36 $1.75 \\ 2.16 \\ 2.61 \\ 2.61$ $3.13 \\ 4.26 \\ 5.54$ 13.0014.8517.20 $\frac{38.7}{42.2}$ Blast-Wheel 135''141 $\frac{1}{12''}$ 148'' 19 14" 22 15" 25 34" 29 7/8" 32 1/8" 35 3/8" 51 3%" 96 ½" 103" 109 ¼" $115'' 122 \frac{1}{128} \frac{1}{12''}$ 38 1/2" 77 14" 83 1/2" 90" Diam. 57 7/8" 64" 70 34" 210 4030 50 55 000 Size 328 882 40 30 30 50

<u> </u>											_			
	ess. or	Н. Р.	0.58 0.79 1.03	$1.30 \\ 1.61 \\ 1.95$	2.32 3.16 4.13	$5.22 \\ 6.44 \\ 7.80$	$\begin{array}{c} 9.35 \\ 10.90 \\ 12.60 \end{array}$	$14.40 \\ 16.45 \\ 18.65$	20.85 23.20 25.75	28.30 31.15 34.00				
TEMPERATURE	Static Press. 0.505 Oz.	Vol.	1535 2075 2730	$3440 \\ 4260 \\ 5140$	6125 8350 10880	$13780 \\ 17020 \\ 20600 $	$24500 \\ 28600 \\ 33350 \\ 33350 \\ \end{array}$	$38250 \\ 43400 \\ 49150$	$55200 \\ 61250 \\ 68200 \\ 68200 \\ c8200 \\ c820$	75000 82200 89900				
MPER	1/8" S	R.P.M.	925 795 695	617 556 505	463 398 347	309 278 253	232 213 198	185 174 164	154 146 138	132 126 121				
AT	ess. of z.	Н. Р.	$\begin{array}{c} 0.46 \\ 0.62 \\ 0.82 \end{array}$	$ \begin{array}{c} 1.03 \\ 1.28 \\ 1.55 \end{array} $	$ \begin{array}{c} 1.84 \\ 2.51 \\ 3.28 \end{array} $	4.15 5.12 6.19	$ \begin{array}{c} 7.40 \\ 8.64 \\ 10.00 \end{array} $	$ \begin{array}{c} 11.40 \\ 13.05 \\ 14.75 \end{array} $	$\frac{16.55}{18.40}$ 20.45	$22.50 \\ 24.75 \\ 27.00$				
(PE L)	Static Press. 0.433 Oz.	Vol.	1420 1925 2530	$3185 \\ 3940 \\ 4765$	5675 7730 10080	$\frac{12750}{15750}$ $\frac{115750}{19100}$	$22700 \\ 26450 \\ 30850$	$35400 \\ 40200 \\ 45500$	51100 56700 63100	$ \begin{array}{c} 69400 \\ 76100 \\ 83300 \end{array} $	e			
RS (TV ETER	34" 5	R. P. M.	857 736 644	571 515 468	429 368 321	286 257 234	$215 \\ 198 \\ 184 \\ 184$	171 161 152	143 135 128	122 117 112	Pressur			
STEEL PLATE EXHAUSTERS (TVPE AND 29.92 INCHES BAROMETER	ess. or	Н. Р.	$\begin{array}{c} 0.35 \\ 0.47 \\ 0.62 \end{array}$	$\begin{array}{c} 0.79 \\ 0.97 \\ 1.18 \end{array}$	$1.40 \\ 1.91 \\ 2.49$	$3.15 \\ 3.89 \\ 4.71$	$5.63 \\ 6.57 \\ 7.60$	$ \begin{array}{c} 8.70 \\ 9.93 \\ 11.25 \end{array} $	$12.60 \\ 14.00 \\ 15.55$	$17.10 \\ 18.85 \\ 20.55 \\ 20.55$	Static Pressure			
TE EXH	Static Press. 0.360 Oz.	Vol.	1300 1755 2310	$2910 \\ 3600 \\ 4350$	5180 7060 9200	$\frac{11640}{14400}$ $\frac{14400}{17400}$	$20700 \\ 24150 \\ 2820$	$32350 \\ 36700 \\ 41600$	46700 51800 57600	63400 69500 75200	Pressure is 126% of the Rated			
PLATE 9.92 INCI	5/8 S	R.P.M.	783 672 588	522 470 427	$391 \\ 336 \\ 293 \\ 293 \\$	261 235 214	196 180 168	157 147 138	130 123 117	111 107 102	% of th			
STEEL AND 29	ess. or	Н. Р.	$\begin{array}{c} 0.25\\ 0.34\\ 0.45\end{array}$	$\begin{array}{c} 0.56 \\ 0.70 \\ 0.84 \end{array}$	$ \begin{array}{c} 1.00 \\ 1.36 \\ 1.78 \end{array} $	2.25 2.78 3.37	4.04 4.70 5.45	$\begin{array}{c} 6.21 \\ 7.08 \\ 8.04 \end{array}$	$\begin{array}{c} 9.00\\ 10.00\\ 11.10\end{array}$	$12.20 \\ 13.45 \\ 14.70$	is 126°			
PLANOIDAL	Static Press. 0.288 Oz.	Vol.	$1160 \\ 1570 \\ 2065$	2600 3220 3890	$4630 \\ 6320 \\ 8230 \\ 8230$	$\begin{array}{c}10410\\12880\\15550\\15550\end{array}$	$\frac{18530}{21600}\\25200$	$\begin{array}{c} 28950\\ 32800\\ 37150\\ 37150 \end{array}$	$\begin{array}{c} 41700\\ 46300\\ 51500\end{array}$	56650 62150 68000	Pressure			
	12" 5	R.P.M.	700 601 526	467 421 382	$350 \\ 301 \\ 262$	233 210 191	$175 \\ 161 \\ 150 $	$140 \\ 132 \\ 124 \\ 124$	117 110 105	100 96 91	Total			
FFALO	ess. or	Н. Р.	$\begin{array}{c} 0.16 \\ 0.22 \\ 0.29 \end{array}$	$\begin{array}{c} 0.37 \\ 0.45 \\ 0.55 \end{array}$	$\begin{array}{c} 0.65 \\ 0.89 \\ 0.89 \\ 1.16 \end{array}$	1.47 1.81 2.19	$2.62 \\ 3.54 \\ 3.54$	4.04 4.61 5.23	$5.86 \\ 6.51 \\ 7.22$	7.95 8.75 9.54				
CAPACITIES OF BUFFALO	tatic Pro	itatic Pro. 0.217 0:	tatic Pre 0.217 02	Static Press. 0.217 Oz.	Vol.	1000 1360 1790	22555 2785 3370	$4010 \\ 5465 \\ 7120$	9020 11140 13480	$ \begin{array}{c} 16030\\ 18700\\ 21830 \end{array} $	25050 28400 32200	$ \begin{array}{r} 36150 \\ 40150 \\ 44600 \\ \end{array} $	$\frac{49100}{53800}$	
CITIES	3,8" S	R.P.M.	606 520 456	404 364 331	303 260 227	202 182 165	152 140 130	121 114 107	101 96 91	86 83 79				
CAPA	A. P. M.	R.P.M.	1.66 2.61 3.93	5.57 7.65 10.18	13.25 21.00 31.38	$\begin{array}{c} 44.60\\ 61.30\\ 81.50\end{array}$	$\begin{array}{c} 105.60 \\ 134.00 \\ 168.00 \end{array}$	$\begin{array}{c} 206.50 \\ 249.50 \\ 300.00 \end{array}$	$\begin{array}{c} 357.50 \\ 420.00 \\ 491.50 \end{array}$	568.50 651.00 745.00				
	Size		30 35 40	45 55	05 80 80	06 001 1100	120 130 140	150 160 170	190 190 200	210 220 230				

CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE EXHAUSTERS (TYPE L) AT TEMPERATURE OF 70° F. AND 29.92 INCHES BAROMETER

	ress. or Oz.	Н. Р.	2.01 2.71 3.56	0 4.50 5.57 6.73	8.00 10.91 14.26	18.05 22.25 26.95) 32.21 37.60 43.60	0 49.75 56.80 64.30	22.15 80.15 89.00	97.80 107.80 117.40
	Static Press. 1.154 Oz.	. Vol.	2320 3140 4135	5210 6440 7780	9260 12630 16450	20850 25750 31100	37050 43250 50400	$57900 \\ 65700 \\ 74300 \\ 74$	83500 92650 103000	$\frac{113300}{124300}$
	2″	R. P. M.	1400 1200 1050	934 842 765	700 601 525	467 420 382	351 323 300	280 263 248	234 221 209	199 191 183
	ress. or)z.	H. P.	1.64 2.22 2.91	3.68 4.55 5.51	$ \begin{array}{c} 6.55\\ 8.93\\ 8.93\\ 11.65 \end{array} $	$14.74 \\ 18.20 \\ 22.05$	26.40 30.75 35.60	40.70 46.50 52.60	59.00 65.55 72.75	80.00 88.15 96.10
	Press. or 134" Static Press. 0z. 1.010 0z.	Vol.	2170 2940 3860	4870 6020 7280	8670 11810 15400	$19500 \\ 24080 \\ 29100$	$34650 \\ 40400 \\ 47200$	54150 61400 69500	78100 86700 96400	106000 116200 195800
		R.P.M.	1310 1125 985	874 787 715	655 562 491	437 393 357	328 302 281	262 246 232	218 206 196	187 178 170
		H. P.	$ \begin{array}{c} 1.31 \\ 1.76 \\ 2.32 \end{array} $	2.93 3.63 4.38	5.21 7.11 9.29	$11.72 \\ 14.45 \\ 17.50$	21.00 24.50 28.40	32.45 37.05 41.90	46.15 52.25 57.95	63.75 70.20 76.50
	Static P 0.865 0	Vol.	2010 2720 3580	4510 5580 6740	$\begin{array}{c} 8030 \\ 10920 \\ 14250 \end{array}$	$\frac{18050}{22300}$ 26950	$32080 \\ 37410 \\ 43700$	50150 56900 64400	72250 80250 89200	98200 107800
	1 1/2"	R.P.M	1212 1041 912	809 729 662	606 521 454	404 364 331	304 279 260	242 228 214	202 191 181	173
	Press. or Oz.	Н. Р.	0.99 1.34 1.76	2.22 2.75 3.33	3.96 5.40 7.05	8.93 11.00 13.35	$15.95 \\ 18.60 \\ 21.55$	$\begin{array}{c} 24.60\\ 28.15\\ 31.80\end{array}$	35.70 39.65 44.00	48.50 53.35 52 95
	Static P 0.721 0	Vol.	1830 2480 3260	4110 5080 6150	7320 99900 13000	$\frac{16480}{20350}$	$\begin{array}{c} 29300\\ 34150\\ 39850\end{array}$	45750 51850 58800	66000 73250 81450	89550 98250 107500
	1 34"	R. P. M.	$ \begin{array}{c} 1110 \\ 950 \\ 831 \end{array} $	738 665 604	554 475 415	369 332 302	277 255 237	221 208 196	184 174 165	158 151 144
	Static Press. or 0.577 0z.	H. P.	$\begin{array}{c} 0.71 \\ 0.96 \\ 1.26 \end{array}$	1.59 1.97 2.38	2.83 3.86 5.04	6.38 7.87 9.53	$11.40 \\ 13.30 \\ 15.40$	$17.60 \\ 20.10 \\ 22.75$	25.50 28.35 31.45	34.60 38.10 41.55
		Vol.	1640 2220 2920	3680 4550 5500	6550 8930 11630	$\frac{14730}{18200}$	$\begin{array}{c} 26200 \\ 30550 \\ 35650 \end{array}$	40900 46450 52550	59000 65500 72850	80150 87900 96150
	3 .1	R.P.M.	990 850 744	660 595 540	495 425 371	330 297 270	248 228 212	198 186 175	165 156 148	141 135
	A. P. M.	R. P. M.	1.66 2.61 3.93	5.57 7.65 10.18	$13.25 \\ 21.00 \\ 31.38$	44.60 61.30 81.50	$\begin{array}{c} 105.60 \\ 134.00 \\ 168.00 \end{array}$	$\begin{array}{c} 206.50 \\ 249.50 \\ 300.00 \end{array}$	$357.50 \\ 420.00 \\ 491.50$	568.50 651.00 745.00
	Size		30 35 40	45 50 55	60 70 80	90 1100	120 130 140	150 160 170	180 190 200	210

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CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE EXHAUSTERS (TYPE L) AT TEMPERATURE	
AT	
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(TYPE	TER
EXHAUSTERS	OF 70° F. AND 29.92 INCHES BAROMETER
BLATE	29.92 INC
STEE	AND
PLANOIDAL	OF 70° F.
BUFFALO	
OF 1	
CAPACITIES	

							o n d			
ress. or)z.	Н. Р.	4.66 6.30 8.26	$\frac{10.43}{12.92}$ 15.60	$\frac{18.55}{25.33}\\33.08$	41.80 51.60 62.50	$ \begin{array}{c} 74.70 \\ 87.20 \\ 101.00 \end{array} $	$115.30 \\ 131.80 \\ 149.20$	$167.10 \\ 185.80 \\ 206.30$	227.00 249.90 272.30	
Static Press. 2.019 Oz.	Vol.	3070 4155 5460	$ \begin{array}{c} 6890\\ 8510\\ 10290\\ 10290\end{array} $	$12250 \\ 16700 \\ 2175$	$27550 \\ 34050 \\ 41200$	$\frac{49000}{57200}\\66700$	76600 86900 98400	$\frac{110400}{122500}$ $\frac{122500}{136300}$	$\frac{150000}{164500}$ $\frac{164500}{179900}$	
3 3/2"	R. P. M.	$ \begin{array}{c} 1852 \\ 1590 \\ 1392 \end{array} $	$1235 \\ 1112 \\ 1010 \\ 100$	926 795 694	617 556 505	464 427 397	371 348 328	309 292 277	264 253 241	
ess. or z.	H. P.	$3.69 \\ 4.99 \\ 6.56$	$ \begin{array}{c} 8.28 \\ 10.24 \\ 12.38 \end{array} $	$ \begin{array}{c} 14.71 \\ 20.08 \\ 26.20 \end{array} $	$33.20 \\ 40.90 \\ 49.60$	59.40 69.25 80.25	$\begin{array}{c} 91.70 \\ 104.50 \\ 118.20 \end{array}$	$\frac{132.60}{147.30}$ 163.70	$179.90 \\ 198.00 \\ 216.00$	
Static Press. 1.734 Oz.	Vol.	2840 3845 5060	6375 7880 9530	$\frac{11340}{15460}$ 20150	$25500 \\ 31530 \\ 38100 \\ 38100$	$\begin{array}{c} 45400\\ 52900\\ 61750\end{array}$	70900 80400 91000	$\frac{102200}{113300}$ $\frac{113300}{126100}$	138800 152200 166500	tre
3" 5	R.P.M.	$1715 \\ 1472 \\ 1288 \\ 1288 \\$	$1143 \\ 1030 \\ 936$	858 736 643	572 515 468	429 395 367	343 322 303	286 270 257	244 234 223	Pressure
2 34" Static Press. or 3" : 1.586 Oz.	Н. Р.	3.24 4.38 5.74	$7.25 \\ 8.98 \\ 10.84$	$12.90 \\ 17.60 \\ 22.88$	29.08 35.85 43.40	51.95 60.60 70.20		$\frac{116.30}{129.20}$ 143.30	$\frac{157.80}{173.50}$ 189.40	I Static
Static Pre 1.586 Oz.	Vol.	$2720 \\ 3680 \\ 4840 $	$6100 \\ 7540 \\ 9120$	$\cdot \begin{array}{c} 10870 \\ 14800 \\ 19300 \end{array}$	$24420\\30200\\36500$	$43400 \\ 50650 \\ 59150$	67800 77000 87200	97800 108700 120800	$\frac{133000}{145800}$ $\frac{132000}{159400}$	of the Rated
2 34"	R.P.M.	1640 1410 1233	$1093 \\ 986 \\ 896$	821 705 615	547 493 448	$\frac{412}{378}$ 352	$\frac{328}{308}$ 290	$274 \\ 259 \\ 246 \\ 246$	234 224 214	
Press. or Oz.	Н. Р.	2.81 3.80 4.98	$ \begin{array}{c} 6.29 \\ 7.78 \\ 9.41 \end{array} $	$11.19 \\ 15.27 \\ 19.92$	25.25 31.10 37.70	$\frac{45.10}{52.60}$ 60.90	69.60 79.50 90.00	$\begin{array}{c} 100.90 \\ 112.00 \\ 124.30 \end{array}$	$\frac{136.80}{150.50}$	Pressure is 126%
Static Pr 1.442 0	Vol.	$2595 \\ 3510 \\ 4620$	5825 7200 8700	10370 14120 18400	23300 28800 34800	$\frac{41400}{48350}$ $\frac{41300}{56400}$	64750 73500 83200	$\begin{array}{c} 93400 \\ 103700 \\ 115100 \end{array}$	$\begin{array}{c} 126800\\ 139000\\ 152100 \end{array}$	Pressure
2 1/2"	R.P.M.	$1565 \\ 1343 \\ 1177 \\ $	$1044 \\ 940 \\ 854$	783 673 587	522 470 427	$392 \\ 361 \\ 335 \\ 335$	313 294 277	261 247 234	223 214 204	Total]
Press. or Oz.	Н. Р.	2.40 3.24 4.26	5.37 6.65 8.04	$ \begin{array}{c} 9.55 \\ 13.04 \\ 17.00 \end{array} $	21.53 26.57 32.15	$38.50 \\ 44.90 \\ 52.00$	$59.40 \\ 67.90 \\ 76.80$	86.10 95.80 106.20	$^{116.80}_{128.60}_{140.20}$	
Static P1 1.298 0	Vol.	$2460 \\ 3330 \\ 4380 \\ 4380 \\ $	5500 6830 8250	9830 13400 17470	22100 27300 33000	$39300 \\ 45800 \\ 53500 \\ 53500 \\$	$\begin{array}{c} 61400 \\ 69700 \\ 78850 \end{array}$	88500 98300 109300	$\frac{120200}{131800}$ $\frac{144200}{144200}$	
2 34"	R. P. M.	$\frac{1485}{1275}$	990 893 810	743 638 557	495 446 405	$\frac{372}{342}$ 318	297 279 263	248 234 222	$212 \\ 203 \\ 194$	
A. P. M.	R. P. M.	$ \begin{array}{c} 1.66 \\ 2.61 \\ 3.93 \end{array} $	5.57 7.65 10.18	13.25 21.00 31.38	44.60 61.30 81.50	$\frac{105.60}{134.00}$ 168.00	206.50 249.50 300.00	$357.50 \\ 420.00 \\ 491.50$	$568.50 \\ 651.00 \\ 745.00$	
Size		30 35 40	45 50 55	60 70 80	90 1100	120 130 140	150 160 170	180 190 200	210 220 230	

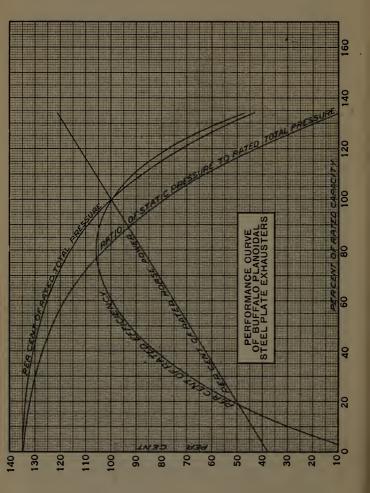
FAN ENGINEERING-BUFFALO FORGE COMPANY

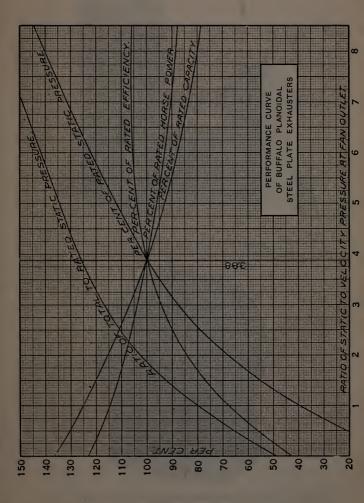
) AT TEMPERATURE	
(TYPE, L	R
EXHAUSTERS (T	ES BAROMETEI
PLATE	92 INCH
STEEL	AND 29.
PLANOIDAL STEEL PLATE E	OF 70° F. AND 29.92 INCHES
S OF BUFFALO	
OF	
APACITIES	

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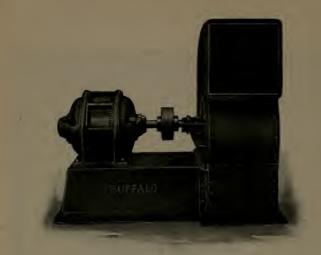
ress. or Dz.	Н. Р.	10.43 14.10 18.52	23.40 29.00 35.00	41.60 56.80 74.10	93.80 115.60 140.00	167.70 195.50 226.40	258.80 295.30 334.50	375.00 416.50 462.50	509.00 560.00 611.00	
Static Press. 3.460 Oz.	Vol.	4030 5440 7150	$\begin{array}{c} 9020\\ 11140\\ 13480\end{array}$	$\frac{16040}{21880}$	36080 44600 53900	64200 74850 87300	$100100 \\ 113700 \\ 128800$	$\frac{144500}{160400}$ $\frac{178400}{178400}$	$\frac{196000}{215300}$	
6"	R.P.M.	2425 2080 1823	$ \begin{array}{c} 1615 \\ 1458 \\ 1323 \\ 1323 \end{array} $	$1212 \\ 1040 \\ 909$	809 728 661	608 559 519	485 456 428	404 382 363	346 331 316	
Préss. or Oz.	Н. Р.	$\begin{array}{c} 9.16 \\ 12.38 \\ 16.25 \end{array}$	20.50 25.40 30.70	36.50 49.80 65.00	82.30 101.50 123.00	$\frac{147.00}{171.80}$ 198.70	227.00 259.30 293.50	329.00 365.90 406.00	446.50 491.50 536.00	
Static P 3.172 0	Vol.	3845 5210 6850	$\begin{array}{c} 8635 \\ 8635 \\ 10680 \\ 12900 \end{array}$	$\frac{15370}{20950}$	$34550 \\ 42700 \\ 51600$	61450 71700 83700	96000 108900 123200	$\frac{138400}{153800}$	$\frac{188000}{206100}$ 225500	re
5 1/2"	R.P.M.	$\begin{array}{c} 2325 \\ 1995 \\ 1745 \end{array}$	$1549 \\ 1395 \\ 1268 \\ $	$\substack{1160\\997\\870}$	774 697 633	582 535 498	464 436 411	387 366 347	331 317 303	ressu
SS. OF Z.	Н. Р.	$ \begin{array}{c} 7.94 \\ 10.73 \\ 14.10 \end{array} $	$17.80 \\ 22.05 \\ 26.60$	$31.65 \\ 43.15 \\ 56.40$	$ \begin{array}{c} 71.40 \\ 88.00 \\ 106.50 \end{array} $	$\frac{127.50}{148.70}$ 172.10	$197.00 \\ 224.80 \\ 254.50$	285.30 317.00 352.00	$387.50 \\ 426.00 \\ 465.00$	Static 1
Static Press. or 2.884 Oz.	Vol.	3670 4965 6530	8230 10180 12300	$\frac{14650}{19980}$ 26000	$32950 \\ 40700 \\ 49200$	58600 68300 79750	$ \begin{array}{c} 91500\\ 103900\\ 117500 \end{array} $	$\frac{132000}{146500}$ $\frac{146500}{163000}$	$\frac{179100}{196600}$ 215000	ne Rated
5" S	R. P. M.	$2215 \\ 1900 \\ 1664$	$1476 \\ 1330 \\ 1208 \\ $	$ \begin{array}{c} 1108 \\ 950 \\ 830 \end{array} $	738 664 604	555 510 474	443 416 391	$ \begin{array}{r} 369 \\ 349 \\ 331 \\ \end{array} $	$315 \\ 302 \\ 289 $	o of th
Press. or Oz.	H. P.	$\begin{array}{c} 6.78 \\ 9.16 \\ 12.03 \end{array}$	$15.18 \\ 18.80 \\ 22.73 \\ 22.73 \\ \end{array}$	27.00 36.83 48.15	60.90 75.10 91.00	$\frac{108.70}{127.00}$ 147.00	$ \begin{array}{c} 168.00\\ 192.00\\ 217.30 \end{array} $	243.50 270.50 300.50	330.00 363.50 397.50	Fotal Pressure is 126% of the Rated Static Pressure
Static P. 2.595 0	Vol.	$ \begin{array}{c} 3480 \\ 4710 \\ 6195 \end{array} $	7805 9650 11680	$\frac{13900}{18950}$ 24680	$31250 \\ 38600 \\ 46650$	55600 64800 75600	$ \begin{array}{c} 86900 \\ 98500 \\ 111400 \end{array} $	$\frac{125200}{139000}$ $\frac{1254500}{154500}$	$\frac{170000}{186400}$ 204000	Pressure
4 1/2	R.P.M.	$2100 \\ 1804 \\ 1579$	1400 1262 1145	$1050 \\ 901 \\ 787$	700 630 573	526 484 450	420 395 371	350 331 314	299 286 274	Total
ess. or z.	Н. Р.	5.68 7.68 10.08	$12.72 \\ 15.76 \\ 19.04$	$22.64 \\ 30.88 \\ 40.30$	51.10 62.96 76.24	$ \begin{array}{c} 91.20 \\ 106.40 \\ 123.20 \end{array} $	$^{140.80}_{160.80}$	204.00 226.80 251.60	276.80 304.80 332.40	
Static Press. 2.307 Oz.	Vol.	3280 4440 5840	$ \begin{array}{c} 7360 \\ 9100 \\ 11000 \end{array} $	$\frac{13100}{17860}\\23280$	29450 36400 44000	52400 61150 71350	$\begin{array}{c} 81800\\92900\\105100\end{array}$	${}^{118000}_{131000}_{145700}$	$\frac{160300}{175800}$ $\frac{175800}{192300}$	
4" S	R. P. M.	1980 1700 1488	$1320\\1190\\1080$	990 850 742	660 594 540	496 456 424	396 372 350	$330 \\ 312 \\ 296 $	$ 282 \\ 270 \\ 258 \\ 258 $	
A. P. M.	K. P. M.	1.66 2.61 3.93	5.57 7.65 10.18	$\begin{array}{c} 13.25 \\ 21.00 \\ 31.38 \end{array}$	44.60 61.30 81.50	$\frac{105.60}{134.00}$ 168.00	206.50 249.50 300.00	$357.50 \\ 420.00 \\ 491.50$	568.50 651.00 745.00	
Size		30 35 40	45 50 55	60 70 80	001 1100	120 130 140	150 160 170	180 190 200	210	

PLANOIDAL EXHAUSTER CAPACITIES





FAN ENGINEERING-BUFFALO FORGE COMPANY



Motor Driven Planoidal Type "L" Fan



Left-Hand Bottom Horizontal Discharge Planoidal Type "L" Fan with Overhung Pulley

		-		- DAL	2110						
	. or	Н. Р.	0.37 0.51 0.66	$\begin{array}{c} 0.84 \\ 1.03 \\ 1.25 \end{array}$	$1.49 \\ 2.02 \\ 2.64$	$3.34 \\ 4.12 \\ 4.99$	$5.94 \\ 6.97 \\ 8.08$	9.28 10.6 11.9	13.4 14.9 16.5	$\begin{smallmatrix}18&2\\20&0\\21&8\end{smallmatrix}$	1
1	Total Press. or 0.505 Oz.	Vol.	$1350 \\ 1840 \\ 2410 \\ 2410 \\ 1350 \\ 2410 \\ 2410 \\ 2410 \\ 35$	3050 3760 4550	5410 7370 9630	$12180 \\ 15040 \\ 18190$	21650 25410 29480	33830 38500 43460	48720 54300 60150	66310 72780 79540	
ETER	7%" T	R.P.M.	795 681 596	530 477 433	397 341 298	265 238 217	199 183 170	159 149 140	133 126 119	114 108 104	
BAROM	5. OF	Н. Р.	$\begin{array}{c} 0.30\\ 0.40\\ 0.53\end{array}$	$ \begin{array}{c} 0.67 \\ 0.82 \\ 1.00 \end{array} $	$ \begin{array}{c} 1.19 \\ 1.61 \\ 2.11 \end{array} $	2.67 3.29 3.98	4.74 5.56 6.45	7.40 8.42 9.50	10.7 11.9 13.2	14.5 15.9 17.4	
INCHES	Total Press. 0.433 Oz.	Vol.	$1260 \\ 1710 \\ 2230$	2820 3490 4220	5020 6830 8920	$11290 \\ 13940 \\ 16870$	20080 23560 27330	$31370 \\ 35690 \\ 40290$	45170 50330 55760	61480 67480 73750	
(D 29.92	34"	R. P. M.	737 632 553	491 442 402	368 316 276	246 221 201	184 170 158	147 138 130	123 116 111	105 101 96	
0° F. AN	s. or	Н. Р.	$\begin{array}{c} 0.22\\ 0.31\\ 0.40\end{array}$	$\begin{array}{c} 0.51 \\ 0.62 \\ 0.76 \end{array}$	$0.90 \\ 1.22 \\ 1.60$	2.02 2.50 3.02	$3.59 \\ 4.22 \\ 4.89 $	5.62 6.38 7.21	8.08 9.01 9.98	11.0 12.1 13.2	F
WORKING CONDITIONS-TEMPERATURE OF 70° F. AND	Total Press. 0.360 Oz.	Vol.	$1150 \\ 1560 \\ 2040$	2580 3180 3850	4580 6230 8140	$10300 \\ 12720 \\ 15390$	$ \begin{array}{c} 18320 \\ 21500 \\ 24930 \end{array} $	$28620 \\ 32560 \\ 36760$	$\frac{41200}{45930}$ $6000000000000000000000000000000000000$	56100 61550 67280	1. 2 MOR
PERAT	5/8	R.P.M.	672 576 504	448 403 367	336 288 252	224 202 183	168 155 144	134 126 119	112 106 101	96 92 88	•
NS-TEM	s. or	Н. Р.	$\begin{array}{c} 0.16 \\ 0.22 \\ 0.29 \end{array}$	$\begin{array}{c} 0.36 \\ 0.45 \\ 0.54 \end{array}$	$\begin{array}{c} 0.65 \\ 0.88 \\ 1.15 \end{array}$	$1.45 \\ 1.79 \\ 2.17$	$2.58 \\ 3.02 \\ 3.51$	4.03 4.58 5.17	5.80 6.46 7.16	7.89 8.66 9.47	
OILION	Total Press. 0.288 Oz.	Vol.	$1025 \\ 1400 \\ 1820$	2310 2850 3440	$\frac{4100}{5580}$ 7290	$ \begin{array}{c} 9220 \\ 11380 \\ 13780 \\ 13780 \\ \end{array} $	$\begin{array}{c} 16390 \\ 19240 \\ 22310 \end{array}$	$25610 \\ 29140 \\ 32900 \\$	$36880 \\ 41100 \\ 45540$	50200 55100 60210	
KING C	1/2"	R.P.M.	602 516 451	401 361 328	301 258 226	201 181 164	150 139 129	120 113 106	100 95 90	86 82 79	
WOR	Area of Outlet	Sq. Ft.	0.77 1.04 1.36	$ \begin{array}{c} 1.75 \\ 2.16 \\ 2.61 \\ 2.61 \end{array} $	$3.13 \\ 4.26 \\ 5.54$	$ \begin{array}{c} 7.10 \\ 8.75 \\ 10.57 \end{array} $	$13.00 \\ 14.85 \\ 17.20$	$ \begin{array}{c} 19.70 \\ 22.40 \\ 25.40 \\ \end{array} $	28.50 31.70 35.30	38.7 42.2 46.5	
	Diam. Blast-	Wheel	$\frac{19}{22} \frac{14}{12}^{"}$	$\begin{array}{c} 29 & 7 \\ 32 & 1 \\ 35 & 3 \\ 38 \\ \end{array}$	$\frac{38}{45}''_{5138''}$	$\begin{array}{c} 57 \ 7_8^{\prime\prime\prime} \\ 64 \ 1_4^{\prime\prime\prime} \\ 70 \ 3_4^{\prime\prime\prime} \end{array}$	77 14" 83 14" 90"	96 ½" 103" 109 ¼"	$\frac{115^{6}4''}{122}$	$\frac{135''}{14112''}$	
	Size		30 35 40	45 50 55	60 70 80	90 1100 110	120 130 140	150 160 170	180 190 200	210 220 230	

CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE BLOWERS (TYPE L) UNDER AVERAGE

Static Pressure is 79% of the Rated Total Pressure

PLANOIDAL BLOWER CAPACITIES

FAN	Εľ	V G	INEE	RING	- B U	FFAI	LOF	ORGI	E CO	MPAN	Y
	6. OF	Н. Р.	$1.05 \\ 1.44 \\ 1.88 \\ 1.88$	2.37 2.93 3.55	4.22 5.74 7.50	$ \begin{array}{c} 9.49 \\ 11.7 \\ 14.2 \end{array} $	16.9 19.8 23.0	26.4 30.0 33.9	38.0 42.3 46.9	51.7 56.7 62.0	
DE	Total Press. 1.010 Oz.	Vol.	1920 2610 3410	$\begin{array}{c} 4310 \\ 5330 \\ 6440 \end{array}$	$ \begin{array}{r} 7670 \\ 10450 \\ 13630 \end{array} $	$17250 \\ 21300 \\ 2577$	$\begin{array}{c} 30670 \\ 36000 \\ 41750 \end{array}$	$\begin{array}{c} 47930 \\ 54510 \\ 61560 \end{array}$	69000 76900 85200	$\begin{array}{c} 93930\\ 103080\\ 112680\end{array}$	
UNDER AVERAGE BAROMETER	1 34"	R. P. M.	$1125 \\ 965 \\ 844$	750 675 614	563 482 422	375 338 307	281 260 241	225 211 199	188 178 169	$161 \\ 154 \\ 147$	
	S. OF	Н. Р.	$\begin{array}{c} 0.84 \\ 1.14 \\ 1.49 \\ 1.49 \end{array}$	$ \begin{array}{c} 1.88 \\ 2.32 \\ 2.81 \\ 2.81 \end{array} $	$3.35 \\ 4.56 \\ 5.95$	$ \begin{array}{c} 7.53 \\ 9.30 \\ 11.3 \\ \end{array} $	13.4 15.7 18.2	20.9 23.8 26.9	30.1 33.6 37.2	41.0 45.0 49.2	
3LOWERS (TYPE L) AND 29.92 INCHES	Total Press. 0.865 Oz.	Vol.	$1770 \\ 2410 \\ 3150$	3990 4930 5960	$ \begin{array}{c} 7100 \\ 9650 \\ 12620 \end{array} $	$15970 \\ 19720 \\ 23860$	28390 33320 38650	44360 50470 56980	63880 71180 78870	$\begin{array}{c} 86950\\ 95430\\ 104300\end{array}$	sure
OWERS ND 29.92	1 15% 1	R. P. M.	$1042 \\ 893 \\ 781$	695 625 568	521 447 391	347 313 284	261 240 223	208 195 184	177 165 156	$\begin{array}{c} 149\\ 142\\ 136\\ 136 \end{array}$	otal Pres
ATE BL 70° F. A	s. or	Н. Р.	$\begin{array}{c} 0.64 \\ 0.87 \\ 1.13 \end{array}$	$1.43 \\ 1.77 \\ 2.14$	2.55 3.46 4.53	$5.73 \\ 7.07 \\ 8.55$	10.2 12.0 13.9	$15.9 \\ 18.1 \\ 20.4$	22.9 25.5 28.3	$31.2 \\ 34.2 \\ 37.4$	Rated T
CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE BLOWERS (TYPE L) WORKING CONDITIONS-TEMPERATURE OF 70° F. AND 29.92 INCHES	Total Press. 0.721 Oz.	Vol.	$1620 \\ 2200 \\ 2880 \\ $	$3640 \\ 4500 \\ 5440$	$6480\\ 8820\\ 11520$	$14580 \\ 18000 \\ 2178$	$25920 \\ 30420 \\ 35280$	$\begin{array}{c} 40500 \\ 46080 \\ 52020 \end{array}$	$\frac{58320}{64980}$	79380 87120 95220	Static Pressure is 79% of the Rated Total Pressure
OIDAL S	1 14"	R. P. M.	951 815 713	634 571 519	476 408 337	$\frac{317}{285}$	238 220 204	190 178 168	159 150 143	136 130 124	ure is 79
0 PLAN	01	Н. Р.	$\begin{array}{c} 0.46 \\ 0.62 \\ 0.81 \end{array}$	$1.03 \\ 1.27 \\ 1.53$	$ \begin{array}{c} 1.82 \\ 2.48 \\ 3.24 \end{array} $	4.10 5.06 6.02	7.29 8.55 9.92	$11.4 \\ 13.0 \\ 14.6 \\ $	$16.4 \\ 18.3 \\ 20.3 \\ 20.3 \\ 10.4 \\ $	22.3 24.5 26.8	tic Press
BUFFAL	1" Total Press. 0.577 Oz.	Vol.	$1450 \\ 1970 \\ 2580$	$3260 \\ 4030 \\ 4870$	$ \begin{array}{c} 5800 \\ 7890 \\ 10300 \end{array} $	$\begin{array}{c} 13040 \\ 16100 \\ 19480 \end{array}$	$23180 \\ 27210 \\ 31560$	$36230 \\ 41220 \\ 46530$	$52160 \\ 58120 \\ 64400$	71000 77920 85170	Sta
TES OF	1 " T	R. P. M.	851 729 638	567 511 464	426 365 319	284 255 232	$ \begin{array}{c} 212 \\ 196 \\ 182 \end{array} $	170 160 150	142 134 128	122 116 111	
CAPACIT	Area	Sq. Ft.	$\begin{array}{c} 0.77 \\ 1.04 \\ 1.36 \end{array}$	$ \begin{array}{c} 1.75 \\ 2.16 \\ 2.61 \end{array} $	$3.13 \\ 4.26 \\ 5.54$	$7.10 \\ 8.75 \\ 10.57 $	$13.00 \\ 14.85 \\ 17.20 $	$ \begin{array}{r} 19.70 \\ 22.40 \\ 25.40 \\ \end{array} $	$\begin{array}{c} 28.50 \\ 31.70 \\ 35.30 \end{array}$	38.7 42.2 46.5	
	Diam. Blast-	Wheel	$\frac{19}{22}\frac{14''}{12''}$	$\begin{array}{c} 28 \ 7_8^{\prime\prime\prime} \\ 32 \ 18^{\prime\prime\prime} \\ 35 \ 38^{\prime\prime\prime} \\ 38^{\prime\prime\prime} \end{array}$	$\frac{38}{45}^{\mu_2}_{n}$	$\begin{array}{c} 57 \ 7_{8''}^{u} \\ 64 \ 1_{4''}^{u} \\ 70 \ 3_{4''}^{u} \end{array}$	77 14" 83 14" 90"	$\frac{96}{103}^{12''}_{109}$	$\frac{11534''}{12214''}\\12812''$	$\frac{135''}{141}$	
	Size	}	30 35 40	45 50 55	80 80 80	90 1100 110	120 130 140	150 160 170	180 190 200	210 220 230	

CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE BLOWERS (TYPE L) UNDER AVERAGE WODKING CONDITIONS_TEMDEDATIDE OF 70° E AND 20 02 INCHES BADOMETED

R. P. M. Vol. H. P. R. P. M. 1345 2290 1.50 1473 1153 3120 2.45 1263 897 5160 4.05 884 897 5160 4.05 884 504 1009 4.05 884 897 5160 6.05 884 504 1050 5.06 883 504 10500 7.20 533 504 10500 12.86 533 448 20600 16.2 401 336 3460 23.8 349 336 49890 33.8 349 288 49890 33.8 346 288 49890 33.8 346 288 49890 33.8 346 288 49890 33.8 346 288 49890 39.2 276 286 57.8 2860 27.8 28		WU Area			WOKNING CONDITIONS-TEMPERATURE OF 70-F.	. or	2 ½"	Total Press. or	70° F. A	3" T	AND 29.92 INCHES BAKOMETEK 3" Total Press. or 3 ½	S BAKU	3 32"	Total Pres	s. or	
R. P.M. Vol. H. P. R. P.M. Vol. H. P. R. P. M. Vol. H. P. R. P. M. Vol. H. P. Nol. H. P. Vol. H. P. Vol. H. P. Vol. H. P. Vol. Vol. H. P. Vol. <	Blast- Outlet 1.154 0z.			1.154 02				1.442 Oz.			1.734 Oz.		:	2.019 Oz.		
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$		R. P. M.	R. P. M.	Vol.		Н. Р.	R. P. M.	Vol.	Н. Р.	R. P. M.	Vol.	Н. Р.	R. P. M.		Н. Р.	
8 550 550 553 1006 6.57 554 7100 501 7105 555 1106 6.57 553 1106 6.57 553 11760 6.57 553 17850 6.57 556 1129 556 1129 556 1129 556 1126 556 1126 556 1126 556 1126 556 1129 556 1126 556 1126 556 1126 556 1126 556 1126 556 1126 556 1126 556 1238 556 1238 556 126 556 556 13280 556 556 556 556 556 556 556 556 556 556 556 556 5578 5576 5578	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	1203 1031 902		$2050 \\ 2800 \\ 3640$		$1.29 \\ 1.75 \\ 2.29$	$1345 \\1153 \\1009$	2290 3120 4070	$ \begin{array}{c} 1.80 \\ 2.45 \\ 3.20 \end{array} $	$1473 \\ 1263 \\ 1105$	$2510 \\ 3420 \\ 4460$	2.36 3.22 4.21	$1590 \\ 1363 \\ 1192$	$2710 \\ 3690 \\ 4820$	2.98 4.06 5.30	
$ \begin{bmatrix} 573 & 9160 & 7.20 & 737 & 10040 & 9.46 & 795 & 10840 \\ 577 & 16290 & 9.30 & 533 & 13560 & 12.9 & 596 & 19280 \\ 448 & 920600 & 16.2 & 491 & 2552 & 21.3 & 530 & 24400 \\ 448 & 20600 & 16.2 & 491 & 22520 & 21.3 & 477 & 3020 \\ 336 & 33660 & 24.2 & 402 & 33740 & 31.8 & 434 & 36450 \\ 336 & 33660 & 24.2 & 402 & 33770 & 31.8 & 434 & 36450 \\ 338 & 43930 & 392 & 316 & 54600 & 51.5 & 341 & 59040 \\ 288 & 49890 & 392 & 316 & 54600 & 51.5 & 341 & 59040 \\ 288 & 49890 & 392 & 316 & 54600 & 51.5 & 341 & 59040 \\ 288 & 49890 & 392 & 316 & 54600 & 51.5 & 341 & 59040 \\ 288 & 49890 & 392 & 316 & 54600 & 51.5 & 298 & 77100 \\ 288 & 57260 & 45.0 & 295 & 62740 & 59.1 & 318 & 67780 \\ 289 & 57580 & 45.0 & 295 & 62740 & 59.1 & 318 & 67780 \\ 280 & 5728 & 55170 & 51.2 & 298 & 77110 \\ 237 & 55170 & 51.2 & 2938 & 100670 & 94.8 & 281 & 20610 \\ 212 & 91900 & 72.2 & 233 & 100670 & 94.8 & 201 & 129400 \\ 212 & 91900 & 72.2 & 231 & 111540 & 105.1 & 239 & 120490 \\ 176 & 13270 & 882 & 211 & 122980 & 1158 & 227 & 132830 \\ 176 & 13260 & 1063 & 192 & 114507 & 1251 & 208 & 13570 & 120490 \\ 176 & 13260 & 1063 & 192 & 114507 & 12518 & 201 & 136730 \\ 176 & 13260 & 105.1 & 203 & 1192 & 13830 & 11588 & 100570 & 120400 \\ 176 & 13260 & 105.1 & 105.1 & 208 & 11588 & 201 & 136730 \\ 176 & 13260 & 105.1 & 122980 & 1158 & 201 & 136730 & 120400 \\ 176 & 13260 & 105.1 & 208 & 1192 & 13830 & 11588 & 100570 & 10057$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	802 722 656		4610 5700 6900		2.90 3.58 4.33	897 807 734	5160 6360 7700	4.05 5.00 6.05	982 884 804	$5650 \\ 6970 \\ 8440$	$5.32 \\ 6.57 \\ 7.95$	1060 954 867	6100 7530 9110	$ \begin{array}{c} 6.71 \\ 8.28 \\ 10.0 \end{array} $	
448 20600 16.2 491 22520 21.3 530 24400 367 25460 20.0 442 22520 21.3 530 24400 366 20.0 24.2 3740 21.3 530 24400 375 3660 28.3 369 40150 37.8 3373 36750 336 3660 28.8 369 40150 37.8 398 43380 336 3760 28.8 369 40150 37.8 398 43380 288 49990 38.3 340 47130 37.8 367 59940 288 49990 39.2 2460 51.5 29940 57.9 29940 237 55170 57.4 59.1 57.9 288 7710 237 55170 57.8 2603 65.9 27780 27780 237 55760 45.8 2603 65.9 27780 57940<	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	602 516 451		$8200 \\ 11150 \\ 14570$		5.15 7.01 9.16	673 577 504	$ \begin{array}{c} 9160 \\ 12460 \\ 16290 \end{array} $	$ \begin{array}{c} 7.20 \\ 9.80 \\ 12.8 \\ \end{array} $	737 632 553	$\begin{array}{c} 10040 \\ 13660 \\ 17850 \end{array}$	$ \begin{array}{c} 9.46 \\ 12.9 \\ 16.8 \end{array} $	795 682 596	$\begin{array}{c} 10840 \\ 14760 \\ 19280 \end{array}$	$11.9 \\ 16.2 \\ 21.2$	
336 36660 28.8 369 40150 37.8 398 43380 310 43020 33.8 340 47130 44.4 367 50040 288 57260 33.2 340 47130 44.4 367 50040 286 57260 45.0 295 62740 591 318 67780 257 75570 51.2 276 80390 75.9 298 87060 257 73570 51.8 2766 80390 75.9 281 87060 251 31990 72.3 233 100670 94.8 265 97600 1 202 101800 80.0 75.9 281 100770 94.8 251 10840 1 10840 1 108740 1 10840 1 1 10840 1 1 108740 1 1 108740 1 1 1 265 97600 1 210440	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	401 18390 361 22770 328 27540	$ \begin{array}{c} 18390 \\ 22770 \\ 27540 \\ \end{array} $		222	11.6 14.3 17.3	448 403 367	$\begin{array}{c} 20600\\ 25460\\ 30800 \end{array}$	16.2 20.0 24.2	491 442 402	$22520 \\ 27900 \\ 33740$	21.3 26.3 31.8	530 477 434	$\begin{array}{c} 24400\\ 30120\\ 36450 \end{array}$	26.8 33.1 40.1	
269 57260 45.0 295 62740 59.1 318 67780 237 65170 51.2 295 62740 59.1 318 7710 237 65170 51.2 295 67780 67.9 296 7710 237 755.9 281 87060 75.9 288 7710 224 82480 64.8 246 90340 85.1 265 97600 212 91900 72.2 233 100670 94.8 251 108740 1 202 101800 80.0 221 111540 105.1 239 120490 1 192 112270 88.2 211 112940 105.1 239 120490 1 176 133200 86.2 211 122980 1138.9 2051 13830 1 134570 176 133670 138.9 206 138.9 206 138350 1 14	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	32880 38470 44630		24 28 28	20.6 24.2 28.1	336 310 288	36660 43020 49890	28.8 33.8 39.2	369 340 316	$\begin{array}{c} 40150 \\ 47130 \\ 54660 \end{array}$	37.8 44.4 51.5	398 367 341	43380 50900 59040	47.7 56.1 64.9	
224 82480 64.8 246 90340 85.1 265 97600 212 91900 72.2 233 100670 94.8 251 108700 202 101800 80.0 221 111540 105.1 233 100470 182 112800 86.2 211 115490 105.1 239 192 11270 88.2 201 134970 1271 132830 176 1134670 105.8 201 12700 135350 12576	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	241 51220 226 58270 212 65790	51220 58270 65790		$32 \\ 36 \\ 36 \\ 41$	0j.0j.4j	269 252 237	$57260 \\ 65170 \\ 73570$	45.0 51.2 57.8	295 276 260	$\begin{array}{c} 62740 \\ 71390 \\ 80590 \end{array}$	59.1 67.2 75.9	318 298 281	67780 77110 87060	74.6 84.8 95.7	
192 112270 88.2 211 122980 115.8 227 132830 183 123200 96.8 201 134970 127.1 217 145780 176 134670 105.8 192 147530 138.9 208 159350	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	73760 82180 91060		512	46.4 51.7 57.3	224 212 202	$\begin{array}{c} 82480\\ 91900\\ 101800 \end{array}$	64.8 72.2 80.0	246 233 221	$\begin{array}{c} 90340 \\ 100670 \\ 111540 \end{array}$	$85.1 \\ 94.8 \\ 105.1$	265 251 239	$\begin{array}{c} 97600\\ 108740\\ 120490\end{array}$	107.3 119.6 132.5	
	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	38.7 172 100390 42.2 164 110170 46.5 157 120420	100390 110170 120420		659	63.1 69.3 75.8	192 183 176	$\frac{112270}{123200}$ $\frac{134670}{134670}$	88.2 96.8 105.8	211 201 192	$\frac{122980}{134970}$ 147530	$115.8 \\ 127.1 \\ 138.9 \\$	227 217 208	$\frac{132830}{145780}$ $\frac{145780}{159350}$	146.1 160.3 175.3	

PLANOIDAL BLOWER CAPACITIES

L TEMPERATURE	
F	
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JFFALO PLANOIDAL STEEL PLATE BLOWERS (TYPE L) AT TI	OF 70° F. AND 29.92 INCHES BAROMETER
F 8	
50	
CAPACITIES OF BUFFALO	

Static Press. or 0.217 Oz. Y ⁴ Static Press. or 0.217 Oz. Vol. H. P. X. M. Vol. H. P. 1790 0.125 508 0.288 0.23 0.217 0.23 1790 0.125 508 1160 0.213 1790 0.215 508 1160 0.23 1790 0.215 508 1160 0.23 1790 0.215 508 1160 0.23 2785 0.34 471 2200 0.52 3770 0.401 2208 1164 0.23 4010 0.603 339 4630 0.25 57465 0.811 2206 10.410 2.06 111440 1.06 238 2.56 1.64 9020 1.35 15550 3.10 2.56 111440 2.01 135 15550 3.10 111440 2.01 135 2.5500 5.76 25050 3.102 2.576 5.76 2.576 251830 3.253<	Matrix Matrix<	Y ^a Static Press. or 0.2388 Oz. Y ^a P. R.P.M. Vol. H. P. R.P.M. 15 578 1150 0.238 568 2.15 568 2055 0.41 568 2.41 2065 0.041 568 568 2.42 407 3330 0.023 758 8.1 2506 0.041 568 265 5.0 369 2053 0.023 378 8.1 2500 0.52 323 333 8.1 2506 10410 2.065 227 0.1 254 8230 1.164 237 8.1 2266 10410 2.06 237 9 1063 12550 3.10 207 132 9 165 15550 3.10 207 132 9 166 1880 2.66 141 175 9 127 1338 2.576	Matrix Matrix<	M_{2}^{*} Static Press. or M_{2}^{*} Static Press. or M_{1}^{*} Static Press. Static Press. Pres	M_{2}^{*} Static Press. or M_{2}^{*} Static Press. or M_{1}^{*} Static Press. Static Press. Pres	Matrix Matrix<	or 1° Static Press. or 9° Static Press. or 9° Static Press. or 3° Static Press. or <th>M' M' <t< th=""><th>or $y_2^{\prime\prime}$ Static Press. or 0.288 Oz.</th><th>Н. Р.</th><th>0.15 678 0.20 580 0.27 508</th><th>0.34 451 0.42 407 0.50 369</th><th>0.60 339 0.81 290 1.07 254</th><th>1.35 226 1.66 203 2.01 185</th><th>2.39 169 2.79 156 3.25 145</th><th>3.73 135 4.26 127 4.81 120</th><th>$\begin{array}{cccc} 5.38 & 112 \\ 6.00 & 107 \\ 6.65 & 102 \end{array}$</th><th>7.33 97 8.05 92 8.80 88</th></t<></th>	M' M' <t< th=""><th>or $y_2^{\prime\prime}$ Static Press. or 0.288 Oz.</th><th>Н. Р.</th><th>0.15 678 0.20 580 0.27 508</th><th>0.34 451 0.42 407 0.50 369</th><th>0.60 339 0.81 290 1.07 254</th><th>1.35 226 1.66 203 2.01 185</th><th>2.39 169 2.79 156 3.25 145</th><th>3.73 135 4.26 127 4.81 120</th><th>$\begin{array}{cccc} 5.38 & 112 \\ 6.00 & 107 \\ 6.65 & 102 \end{array}$</th><th>7.33 97 8.05 92 8.80 88</th></t<>	or $y_2^{\prime\prime}$ Static Press. or 0.288 Oz.	Н. Р.	0.15 678 0.20 580 0.27 508	0.34 451 0.42 407 0.50 369	0.60 339 0.81 290 1.07 254	1.35 226 1.66 203 2.01 185	2.39 169 2.79 156 3.25 145	3.73 135 4.26 127 4.81 120	$\begin{array}{cccc} 5.38 & 112 \\ 6.00 & 107 \\ 6.65 & 102 \end{array}$	7.33 97 8.05 92 8.80 88
½" Static Pres ½" Static Pres B.P.M. Vol. B.P.M. Vol. B.S.B. 02.388 02. 2055 508 11500 508 15700 508 15700 3339 46300 3339 46300 3339 46300 3339 5550 10410 38200 3339 45500 185 15550 185 15550 185 15550 185 15550 185 252000 185 252000 185 32800 185 32800 185 32800 185 32800 185 337150 107 46300 102 46300 102 46300 102 46300 102 55550 102 55550 102 55550 55550	½" Static Press. or 0.288 Oz. ½" Static Press. or 0.288 Oz. ½ R.P.M. Vol. H. P. R.P.M. 5678 1160 0.233 568 5678 1570 0.233 568 5678 1570 0.233 568 451 2505 0.41 568 369 2505 0.641 568 369 3320 0.52 505 369 4930 0.92 378 339 4930 0.92 378 339 4330 0.92 378 254 3220 0.654 337 339 10.6410 2.06 237 254 3220 0.505 227 185 15550 3.10 207 166 21550 3.10 207 167 2550 3.10 175 185 2550 5.76 161 166 21550 3.10 207	½° Static Press. or 0.288 Oz. ½% Static Press. or 0.288 Oz. ½% R.P.M. Vol. H. P. R.P.M. 6578 11760 0.233 558 0.411 568 568 5678 11760 0.233 558 0.411 568 568 451 2505 0.411 568 0.674 415 415 568 369 2905 0.52 505 0.774 415 415 256 232 200 3399 4030 0.92 378 256 232 250 234 257 234 256 232 250 166 126410 2.06 2.09 237 2.00 236 207 116 207 166 12830 2.50 3.10 2.08 237 107 167 166 12830 2.50 5.76 161 177 166 215500 5.74 145 25500 5.74 145 127 33800 6.57 1127 388 0.1025 114 1002 46300 10.25 114 102 114	½" Static Press. or 0.288 Oz. ½" Static Press. or 0.288 Oz. ½" Static Press. or 0.360 Oz. B.P.M. Vol. H. P. P. M. Vol. 6578 11760 0.23 758 1330 5678 1570 0.23 758 1330 5678 1570 0.23 758 1330 5678 1570 0.23 758 1330 5678 1560 0.52 505 2910 3697 3890 0.74 568 2310 369 4630 0.92 378 5180 3755 10410 1.25 324 7060 254 10410 2.06 2.07 14400 169 18530 1.64 2.07 14400 185 15550 3.10 2.07 14400 185 15550 3.10 2.07 14400 185 15550 3.10 2.07 14400 185 15550 3.10	Y'' Static Press. or 0.380 Oz. Y'' Static Press. or 0.288 Oz. Y'' Static Press. or 0.288 Oz. Y'' Net. H - P_1 X_1 R.P.M. Vol. H - P_1 R.P.M. Vol. H - P_1 X'' 8.P.M. Vol. H - P_1 R.P.M. Vol. H - P_1 X_1 558 1570 0.233 758 1300 0.32 830 560 0.55 505 2900 0.37 553 835 451 32200 0.77 415 3550 1.29 415 3899 4630 0.992 378 5180 1.29 415 3899 4630 0.992 378 5180 1.29 415 290 8230 1.64 228 11640 2.29 207 2.29 276 203 1255 310 207 1.7400 3.35 246 207 174 207 177 207 177 207 177 <	Yf Static Press. or Yf Static Press. or Yf B.P.M. Vol. H.P. B.P.M. Vol. H.P. Xf 678 1160 0.233 758 1370 0.321 553 580 1570 0.233 758 1370 0.321 830 678 1570 0.233 758 1370 0.321 830 369 2905 0.411 568 2310 0.73 553 369 3890 0.774 415 3500 1.29 415 378 5180 1.25 378 5180 1.29 315 389 6320 1.64 234 7000 1.75 325 389 5550 3.10 2.07 1.29 315 207 254 10541 2.26 3110 2.07 1.74 327 207 169 18550 3.10 2.07 2.29 207 1.75	Y'' Static Press. or Y'' Static Press. or	Y'' Static Press. or Y'' Statin Y'' Static Press. or	\mathcal{V}'' Static Press. or	½″ Static Press. or 0.288 0z.		678 580 508	451 407 369	339 290 254	226 203 185	169 156 145	135 127 120	112 107 102	97 92 88
Static Press. or 0.288 0z. H. P. Vol. H. P. 1570 0.23 2665 0.41 22600 0.52 38200 0.52 38200 0.52 38200 0.52 38200 0.52 38200 0.52 38200 0.52 38200 0.52 38200 0.52 38200 1.64 15550 3.10 15550 3.10 15550 3.10 15550 3.10 15550 3.10 15550 3.10 15550 3.10 2552000 5.75 38950 5.76 37150 6.57 51500 10.25 51500 10.25 51500 10.25 551500 10.25 551500 10.25 551500 10.25 551500 10.25	% % R.P.M. R.P.M. 6568 5668 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 378 378	% % R.P.M. R.P.M. 568 578 558 415 378 378 378 378 378 378 378 207 189 1161 1161 1134 1134 1134 1134 1134 1134 1134 1134 1138 1134 1134 1138 1138 1134 1134 1134 1134 1134 1134 1134 1134 1134 1134 1134 134 134 134 134 134 134 134 134 134 134 134 138 134	5%" Static Pres 5%" Static Pres 6.360 Oz. 8.P.M Vol. 758 1755 658 2310 568 2310 568 2310 5505 2910 413 4350 413 4350 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 17400 17400 180 2070 180 2070 161 32350 17400 163 265 28400 161 32350 17400 126 411600 114 57600 114 57600 93400 936 63400 938 63400	5% Static Press. or 0.360 Or. 34 R.P.M. Vol. H. P. X 758 1300 0.32 830 758 1370 0.357 623 568 2310 0.357 633 553 553 9415 730 566 2310 0.73 553 413 4350 1.29 415 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 415 2324 7000 1.75 325 2324 7000 3.53 226 17400 3.53 226 192 17400 3.53 236 192 175 24150 6002 192 175 28200 1035 165 17400 <t< td=""><td>5% Static Press. or 0.360 Or. 34 R.P.M. Vol. H. P. X.P.M. 758 1300 0.32 830 758 1370 0.357 623 568 2310 0.357 633 553 553 90 433 413 3350 0.357 633 413 3350 0.373 553 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 315 374 7000 1.75 355 378 5180 1.29 415 237 11640 2.90 276 237 17400 3.55 307 175 24150 602 107 175 28200 7.00 107 175 284150 602 107 176 28350 907 107 175 <</td><td>98" Static Press. or 0.360 Oz. 34" Static Press. 0.433 Oz. R.P.M. Vol. H. P. R.P.M. Vol. 758 1700 0.32 830 1420 568 2310 0.37 553 3185 566 2310 0.37 553 3185 413 455 0.445 523 553 3145 413 4550 0.33 315 1700 1925 378 5180 1.29 415 573 2530 378 5180 1.75 315 17000 234 7060 1.75 315 1700 235 11640 2.90 277 1773 237 117400 3.58 2460 1177 207 17400 3.58 2460 1175 207 17400 3.58 2460 1172 207 17400 3.58 2460 1172 207 1740 2.907</td></t<> <td>94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. R.P.M. Vol. H. P. 74° 558 2310 0.33 533 3185 0.045 567 573 567 573 567 573 567 573 563 567 573 567</td> <td>94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. A.P.M. Vol. H. P. 74° 558 23100 0.332 5313 0.575 673 597 673<td>i </td><th>_</th><td></td><td>888</td><td>46 63 82 82</td><td>1041 1288 1555</td><td>18530 21600 25200</td><td>28950 32800 37150</td><td>$\frac{41700}{46300}$ 51500</td><td>56650 62150 68000</td></td>	5% Static Press. or 0.360 Or. 34 R.P.M. Vol. H. P. X.P.M. 758 1300 0.32 830 758 1370 0.357 623 568 2310 0.357 633 553 553 90 433 413 3350 0.357 633 413 3350 0.373 553 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 315 374 7000 1.75 355 378 5180 1.29 415 237 11640 2.90 276 237 17400 3.55 307 175 24150 602 107 175 28200 7.00 107 175 284150 602 107 176 28350 907 107 175 <	98" Static Press. or 0.360 Oz. 34" Static Press. 0.433 Oz. R.P.M. Vol. H. P. R.P.M. Vol. 758 1700 0.32 830 1420 568 2310 0.37 553 3185 566 2310 0.37 553 3185 413 455 0.445 523 553 3145 413 4550 0.33 315 1700 1925 378 5180 1.29 415 573 2530 378 5180 1.75 315 17000 234 7060 1.75 315 1700 235 11640 2.90 277 1773 237 117400 3.58 2460 1177 207 17400 3.58 2460 1175 207 17400 3.58 2460 1172 207 17400 3.58 2460 1172 207 1740 2.907	94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. R.P.M. Vol. H. P. 74° 558 2310 0.33 533 3185 0.045 567 573 567 573 567 573 567 573 563 567 573 567	94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. A.P.M. Vol. H. P. 74° 558 23100 0.332 5313 0.575 673 597 673 <td>i </td> <th>_</th> <td></td> <td>888</td> <td>46 63 82 82</td> <td>1041 1288 1555</td> <td>18530 21600 25200</td> <td>28950 32800 37150</td> <td>$\frac{41700}{46300}$ 51500</td> <td>56650 62150 68000</td>	i	_		888	46 63 82 82	1041 1288 1555	18530 21600 25200	28950 32800 37150	$\frac{41700}{46300}$ 51500	56650 62150 68000
 ess. or H. P. H. P. 0.411 0.411 0.411 0.411 0.411 0.411 0.52 0.526 3.10 3.10 3.10 5.76 5.76 5.75 5.75 5.75 5.75 5.76 5.76 5.75 5.75<	% % R.P.M. R.P.M. 6568 5668 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 5568 378 378	% % R.P.M. R.P.M. 568 578 558 415 378 378 378 378 378 378 378 207 189 1161 1161 1134 1134 1134 1134 1134 1134 1134 1134 1138 1134 1134 1138 1138 1134 1134 1134 1134 1134 1134 1134 1134 1134 1134 1134 134 134 134 134 134 134 134 134 134 134 134 138 134	5%" Static Pres 5%" Static Pres 6.360 Oz. 8.P.M Vol. 758 1755 658 2310 568 2310 568 2310 5505 2910 413 4350 413 4350 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 378 5180 17400 17400 180 2070 180 2070 161 32350 17400 163 265 28400 161 32350 17400 126 411600 114 57600 114 57600 93400 936 63400 938 63400	5% Static Press. or 0.360 Or. 34 R.P.M. Vol. H. P. X 758 1300 0.32 830 758 1370 0.357 623 568 2310 0.357 633 553 553 9415 730 566 2310 0.73 553 413 4350 1.29 415 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 415 2324 7000 1.75 325 2324 7000 3.53 226 17400 3.53 226 192 17400 3.53 236 192 175 24150 6002 192 175 28200 1035 165 17400 <t< td=""><td>5% Static Press. or 0.360 Or. 34 R.P.M. Vol. H. P. X.P.M. 758 1300 0.32 830 758 1370 0.357 623 568 2310 0.357 633 553 553 90 433 413 3350 0.357 633 413 3350 0.373 553 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 315 374 7000 1.75 355 378 5180 1.29 415 237 11640 2.90 276 237 17400 3.55 307 175 24150 602 107 175 28200 7.00 107 175 284150 602 107 176 28350 907 107 175 <</td><td>98" Static Press. or 0.360 Oz. 34" Static Press. 0.433 Oz. R.P.M. Vol. H. P. R.P.M. Vol. 758 1700 0.32 830 1420 568 2310 0.37 553 3185 566 2310 0.37 553 3185 413 455 0.445 523 553 3145 413 4550 0.33 315 1700 1925 378 5180 1.29 415 573 2530 378 5180 1.75 315 17000 234 7060 1.75 315 1700 235 11640 2.90 277 1773 237 117400 3.58 2460 1177 207 17400 3.58 2460 1175 207 17400 3.58 2460 1172 207 17400 3.58 2460 1172 207 1740 2.907</td></t<> <td>94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. R.P.M. Vol. H. P. 74° 558 2310 0.33 533 3185 0.045 567 573 567 573 567 573 567 573 563 567 573 567</td> <td>94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. A.P.M. Vol. H. P. 74° 558 23100 0.332 5313 0.575 673 597 673<td>i </td><th>Vol.</th><td>160 570 2065</td><td>8000</td><td>888</td><td>000</td><td></td><td></td><td></td><td></td></td>	5% Static Press. or 0.360 Or. 34 R.P.M. Vol. H. P. X.P.M. 758 1300 0.32 830 758 1370 0.357 623 568 2310 0.357 633 553 553 90 433 413 3350 0.357 633 413 3350 0.373 553 378 5180 1.29 415 378 5180 1.29 415 378 5180 1.29 315 374 7000 1.75 355 378 5180 1.29 415 237 11640 2.90 276 237 17400 3.55 307 175 24150 602 107 175 28200 7.00 107 175 284150 602 107 176 28350 907 107 175 <	98" Static Press. or 0.360 Oz. 34" Static Press. 0.433 Oz. R.P.M. Vol. H. P. R.P.M. Vol. 758 1700 0.32 830 1420 568 2310 0.37 553 3185 566 2310 0.37 553 3185 413 455 0.445 523 553 3145 413 4550 0.33 315 1700 1925 378 5180 1.29 415 573 2530 378 5180 1.75 315 17000 234 7060 1.75 315 1700 235 11640 2.90 277 1773 237 117400 3.58 2460 1177 207 17400 3.58 2460 1175 207 17400 3.58 2460 1172 207 17400 3.58 2460 1172 207 1740 2.907	94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. R.P.M. Vol. H. P. 74° 558 2310 0.33 533 3185 0.045 567 573 567 573 567 573 567 573 563 567 573 567	94° Static Press. or 34° Static Press. or 74° Static Press. or 74° Static Press. or R.P.M. Vol. H. P. N.M. Vol. H. P. 74° R.P.M. Vol. H. P. A.P.M. Vol. H. P. 74° 558 23100 0.332 5313 0.575 673 597 673 <td>i </td> <th>Vol.</th> <td>160 570 2065</td> <td>8000</td> <td>888</td> <td>000</td> <td></td> <td></td> <td></td> <td></td>	i	Vol.	160 570 2065	8000	888	000				
	%" S %" S 758 668 648 6568 6568 6568 6568 6568 6568 6568 6568 6568 6568 6568 6568 6568 6568 6568 5505 5055 5055 2027 2031 1038 1114 1114 1116 908	§f Static Prival 95 Static Prival 0.360 0 0.360 0 758 1330 555 568 2310 568 2310 555 505 5910 4350 505 5910 5180 505 2310 2200 505 2310 2200 505 2310 2200 378 5180 2200 252 11640 2200 252 17400 270 17400 277 17400 175 284150 28400 165 28400 160 114 57600 114 57600 103 695000 103 695000	Static Press Static Press Vol. 1300 1755 2310 5180 7260 4350 7260 7260 11640 11440 17440 17440 17440 17440 17440 17460 17460 577600 577600 51800 517600 51800 577600 518000 577600 518000 577600 5777000 5777000 5777000 5777000 5777000 5777000 577700000000	Static Press. or 0.360 Oz. ½/ Vol. H. P. R.P.M. 0.3100 0.57 553 0.321 1300 0.32 1750 0.373 553 2310 0.57 623 2310 0.57 623 2310 0.73 553 2900 0.73 553 3500 1.75 315 7060 1.75 315 11640 3.29 216 17400 4.33 226 24150 5.15 207 2315 7.00 177 241600 11.164 3.33 35700 9.17 165 36700 11.40 1.33 37600 11.40 1.33 37600 1.126 133 37600 1.196 133 37600 1.196 133 37600 1.26 133 37600 1.28 133 <	Static Press. or 0.360 Oz. ½ Vol. H. P. R.P.M. 0.310 Oz. 1300 0.32 330 1750 0.373 553 330 1750 0.367 553 335 2910 0.73 553 355 2910 0.73 553 355 7060 1.75 315 315 7060 1.75 315 315 7060 1.75 325 326 7060 1.75 325 226 7060 1.75 326 276 11640 2.29 315 207 2315 700 177 207 2316700 5.15 207 192 24150 11.06 133 266 357600 12.66 133 315 357600 12.80 133 313 357600 12.80 133 313 357600 12.80 <	Static Press. or 0.360 Oz. ³ /" Static Press. 0.433 Oz. Vol. H. P. R. P. M. Vol. J. 200 Oz. 3/" Static Press. 3/" Static Press. J. 300 Oz. 3/10 U.33 3/10 U.33 1/20 U.33 J. 300 Oz. 3/10 U.33 3/10 U.32 3/10 U.32 J. 300 Oz. 3/3 T.30 1/420 1/20 U.33 J. 300 Oz. 1.29 4/15 T.30 1/420 J. 300 Oz. 1.29 3/35 7/733 2/733 J. 416 Oz. 2.23 31/5 T.008 1/1008 1/1008 11.640 Z.39 2.245 3/1750 1/1008 1/1008 1/1008 11.640 Z.39 2.245 3/1750 1/1008 1/1008 2/1750 11.640 Z.39 2.201 T.29 2/175 2/1750 2/1750 2/1750 2000 Z.2100 T.202 Z.210 2.215 T.202 2/175 2/1750 2/1750 2011 T.440 Z.39 2.216 T.327 2/1750 2/1750 2/1750 2011 T.440 Z.329 2.217 2/1750 2/175	Static Press. or ¾" Static Press. or ¾" O.Jölo Dz.s. ¾" D.Jjä Oz.s. ¾" ½" ¾" ½" ¾" ½" ¾"	Static Press. or ¾" Static Press. or ¾" O.Jölo Dz.s. ¾" P.H. Vol. H.P. X.H. Vol. H.P. R.P.M. Vol. H.P. R.P.M. 1350 0.357 533 0.433 0z.s. 589 591 1350 0.357 533 1420 0.442 587 1350 0.357 533 3185 0.942 587 2500 0.033 553 3185 0.942 588 3500 0.033 553 3185 0.96 597 3500 1.29 415 5675 1.70 448 7060 1.75 355 7730 332 238 116440 3.36 226675 1.77 244 20700 5.15 207 2270 673 224 174400 4.33 2264 19100 5.71 244 23250 1.770 3840 10.60 177 <	2%	H. P.	0.23 0.31 0.41	$\begin{array}{c} 0.52 \\ 0.64 \\ 0.77 \end{array}$	$\begin{array}{c} 0.92 \\ 1.25 \\ 1.64 \end{array}$	2.08 2.56 3.10	3.69 4.31 5.02	5.76 6.57 7.42	$ \begin{array}{c} 8.31 \\ 9.26 \\ 10.25 \end{array} $	11.30 12.40 13.60

CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE BLOWERS (TYPE L) AT TEMPERATURE OF 70° F. AND 29.92 INCHES BAROMETER

		5 5	Static Deace	- 0 -	11/1	Ctatic Deace AP	a0 000	11/1	Static Drace	ace or	13/11	Static Drace	ace or	2" C	Static Deace	00 00
P S	A. P.M. per		0.577 Oz.		*	0.721 Oz.			0.865 Oz.		₹ -	1.010 Oz.			1.154 Oz.	
۹.	W	R. P. M.	Vol.	Н. Р.	R.P.M.	V.ol.	Н. Р.	R.P.M.	Vol.	Н. Р.	R. P. M.	Vol.	Н. Р.	R. P. M.	Vol.	Н. Р.
-044	$\frac{1.71}{2.71}$	958 820 719	1640 2220 2920	$ \begin{array}{c} 0.65 \\ 0.87 \\ 0.87 \\ 1.16 \end{array} $	1070 916 804	$ \begin{array}{c} 1830 \\ 2480 \\ 3260 \\ 3260 \\ \end{array} $	$ \begin{array}{c} 0.91 \\ 1.24 \\ 1.62 \\ 1.62 \end{array} $	$1174 \\ 1005 \\ 880$	2010 2720 3580	$ \begin{array}{c} 1.19 \\ 1.63 \\ 2.13 \end{array} $	1268 1085 951	$2170 \\ 2940 \\ 3860$	$ \begin{array}{c} 1.51 \\ 2.06 \\ 2.69 \\ \end{array} $	$1355 \\1160 \\1018$	2320 3140 4135	$1.84 \\ 2.52 \\ 3.28 \\ 3.28 \\ $
	$ \begin{array}{c} 5.76 \\ 7.92 \\ 10.50 \end{array} $	639 575 522	3680 4550 5500	1.47 1.82 2.19	715 643 584	$\frac{4110}{5080}$ 6150	2.05 2.54 3.06	783 705 640	4510 5580 6740	$2.70 \\ 3.35 \\ 4.03$	845 760 690	4870 6020 7280	3.40 4.21 5.07	904 814 738	$5210 \\ 6440 \\ 7780 $	4.15 5.15 6.19
100	$ \begin{array}{c} 13.70 \\ 21.75 \\ 32.40 \\ \end{array} $	479 410 359	6550 8930 11630	2.61 3.55 4.65	536 459 401	7320 9990 13000	$3.64 \\ 4.96 \\ 6.50$	587 502 440	8030 10920 14250	$\frac{4.80}{6.52}$	634 542 475	$\begin{array}{c} 8670 \\ 11810 \\ 15400 \end{array}$		678 580 508	$\begin{array}{c} 9260 \\ 12630 \\ 16450 \end{array}$	$\begin{array}{c} 7.38\\ 10.02\\ 13.12\end{array}$
TH CO 00	$\begin{array}{c} 46.20\\ 63.40\\ 84.30\end{array}$	319 287 261	$14730 \\ 18200 \\ 22000 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 $	5.88 7.25 8.78	$\frac{357}{321}$	$16480 \\ 20350 \\ 24600 \\ 24600 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 $	$ \begin{array}{c} 8.22 \\ 10.12 \\ 12.28 \end{array} $	391 352 320	$ \begin{array}{c} 18050\\ 22300\\ 26950 \end{array} $	$10.80 \\ 13.32 \\ 16.12$	$\begin{array}{c} 422 \\ 380 \\ 345 \end{array}$	$ \begin{array}{c} 19500 \\ 24080 \\ 29100 \end{array} $	$13.60 \\ 16.80 \\ 20.35$	451 406 369	$\begin{array}{c} 20850\\ 25750\\ 31100\\ \end{array}$	16.60 20.48 24.80
0mh	$\begin{array}{c} 109.50 \\ 138.20 \\ 174.00 \end{array}$	239 221 205	$26200 \\ 30550 \\ 35650 \\ 35650 \\ \end{array}$	10.44 12.20 14.20	267 247 229	$29300 \\ 34150 \\ 39850$	$14.60 \\ 17.04 \\ 19.83$	293 271 251	$32080 \\ 37410 \\ 43700$	$ \begin{array}{c} 19.18 \\ 22.40 \\ 26.10 \end{array} $	$\frac{316}{292}$ 271	$34650 \\ 40400 \\ 47200$	$24.20\\28.25\\32.90$	338 313 290	$37050 \\ 43250 \\ 50400$	29.50 34.50 40.15
	214.00 259.50 311.00	191 179 169	$\begin{array}{c} 40900\\ 46450\\ 52550\end{array}$	$16.30 \\ 18.60 \\ 21.00$	214 200 189	$\begin{array}{c} 45750\\ 51850\\ 58800\end{array}$	22.75 26.00 29.35	234 219 207	50150 56900 64400	29.95 34.15 38.60	$253 \\ 237 \\ 224 \\$	$54150 \\ 61400 \\ 69500$	$37.75 \\ 43.10 \\ 48.60$	270 253 239	$57900 \\ 65700 \\ 74300 \\ 74$	46.10 52.60 59.40
N80	371.00 434.00 505.00	159 151 144	$59000 \\ 65500 \\ 72850$	23.50 26.20 29.00	178 169 161	66000 73250 81450	$32.80 \\ 36.60 \\ 40.50$	195 185 176	$\begin{array}{c} 72250 \\ 80250 \\ 89200 \end{array}$	$\begin{array}{c} 43.15 \\ 48.10 \\ 53.30 \end{array}$	$210 \\ 200 \\ 191$	$ \begin{array}{c} 78100\\ 86700\\ 96400 \end{array} $	$54.40\\60.70\\67.15$	$225 \\ 214 \\ 204$	83500 92650 103000	66.40 74.20 82.00
001-001	585.00 675.50 769.00	137 130 125	80150 87900 96150	32.00 35.10 38.40	153 145 140	$\begin{array}{c} 89550 \\ 98250 \\ 107500 \end{array}$	44.70 49.00 53.65	168 159 153	98200 107800 117850	58.80 64.50 70.50	181 172 165	$\frac{106000}{116200}$ $\frac{1125800}{125800}$	$ \begin{array}{c} 74.10 \\ 81.30 \\ 88.90 \end{array} $	194 184 177	$\frac{113300}{124300}$ $\frac{124300}{136000}$	$ \begin{array}{c} 90.50 \\ 99.40 \\ 108.50 \end{array} $
					Total	Total Pressure is 126% of the Rated Static Pressure	is 1269	% of th	e Rated	Static I	ressur	e				

PLANOIDAL BLOWER CAPACITIES

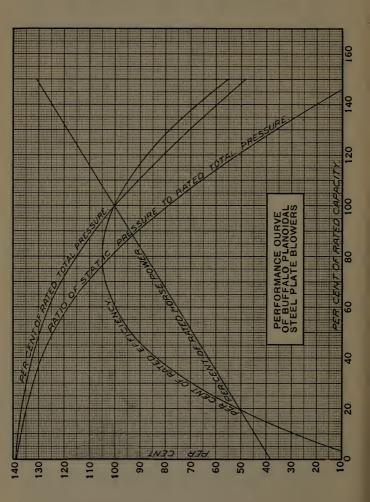
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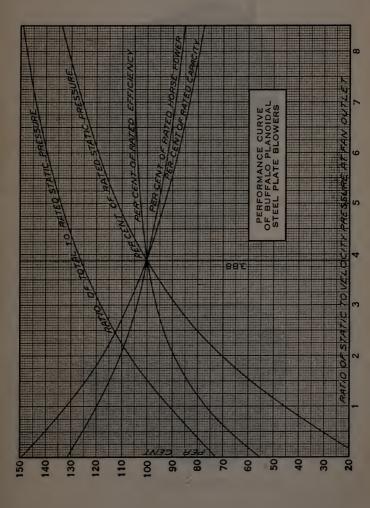
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Press. or 0z.	Н. Р.	4.26 5.83 7.60	9.63 11.91 14.34	$\begin{array}{c} 17.10 \\ 23.25 \\ 30.50 \end{array}$	38.50 47.50 57.50	68.40 80.00 93.00	$\frac{106.80}{121.80}$ 137.50	154.00 171.50 190.00	209.50 230.00 251.50
Static Pr 2.019 O	Vol.	3070 4155 5460	$^{+6890}_{-8510}$	$12250 \\ 16700 \\ 21750$	$27550 \\ 34050 \\ 41200$	$\frac{49000}{57200}\\66700$	$ \begin{array}{c} 76600 \\ 86900 \\ 98400 \\ 98400 \end{array} $	$\frac{110400}{122500}$ $\frac{122500}{136300}$	$\frac{150000}{164500}$
3 1/2"	R. P. M.	$1792 \\ 1534 \\ 1345 \\ 1345 \\$	$1195 \\1076 \\976$	896 767 672	597 537 488	447 413 384	$358 \\ 335 \\ 335 \\ 316 \\ 316$	298 282 269	257 243 234
ss. or	Н. Р.	$3.38 \\ 4.63 \\ 6.03$	$7.63 \\ 9.45 \\ 11.38 $	$\frac{13.55}{18.45}$ 24.20	30.55 37.70 45.60	54.25 63.40 73.80	$\begin{array}{c} 84.70\\ 96.60\\ 109.00\end{array}$	$122.20 \\ 136.00 \\ 150.80$	$\frac{166.30}{182.50}$ 199.50
Static Press. 1.734 Oz.	Vol.	2840 3845 5060	6375 7880 9530	$11340 \\ 15460 \\ 20150$	$25500 \\ 31530 \\ 3810$	45400 52900 61750	$ \begin{array}{c} 70900 \\ 80400 \\ 91000 \end{array} $	102200 113300 126100	$\frac{138800}{152200}$ $\frac{165500}{165500}$
	R. P. M.	1660 1420. 1245	1108 996 904	830 710 621	553 497 452	414 383 355	331 310 293	277 262 250	238 225 217
DAKUMELEK Press. or 3" Oz.	Н. Р.	2.97 4.07 5.30	$ \begin{array}{c} 6.72 \\ 8.32 \\ 10.00 \end{array} $	$ \begin{array}{c} 11.95 \\ 16.23 \\ 21.30 \end{array} $	$26.90 \\ 33.20 \\ 40.15$	47.80 55.80 65.00	$ \begin{array}{c} 74.50 \\ 85.00 \\ 96.00 \end{array} $	107.50 119.80 132.70	$\frac{146.20}{160.50}$
	Vol.	$2720 \\ 3680 \\ 4840 \\ 4840 \\$	6100 7540 9120	$\frac{10870}{14800}$ 19300	$24420\\30200\\36500$	$43400 \\ 50650 \\ 59150$	67800 77000 87200	97800 108700 120800	$\frac{133000}{145800}$ $\frac{145800}{159400}$
234" Static 1.586	R. P. M.	$1589 \\ 1360 \\ 1190 \\ 11190 \\ 11190 \\ 11100 \\ 11100 \\ 110$	1060 954 865	795 680 595	529 476 433	396 366 340	317 297 280	264 250 239	227 216 207
6	Н. Р.	2.57 3.48 4.58	5.81 7.20 8.66	$10.31 \\ 14.03 \\ 18.40 \\ 18.40$	$23.30 \\ 28.70 \\ 34.7$	41.30 48.25 56.15	64.50 73.50 83.00	93.00 103.60 114.70	$126.50 \\ 139.80 \\ 151.90$
Static Press. 1.442 02.	Vol.	2595 3510 4620	5825 7200 8700	10370 14120 18400	$23300 \\ 28800 \\ 3480$	$\begin{array}{c} 41400\\ 48350\\ 56400\end{array}$	64750 73500 83200	$93400 \\ 103700 \\ 115100 \\ 115100 \\ 115100 \\ 10$	126800 139000 152100
2 35"	R. P. M.	1515 1295 1135	1010 910 826	758 648 568	505 454 413	378 350 324	302 283 267	251 239 228	217 206 198
Press. or 0z.	Н. Р.	2.19 3.00 3.92	4.96 6.14 7.40	$ \begin{array}{c} 8.80 \\ 11.98 \\ 15.70 \\ 15.70 \\ \end{array} $	$19.85 \\ 24.50 \\ 29.60$	$35.25 \\ 41.15 \\ 47.90$	$55.00 \\ 62.80 \\ 70.90$	$ \begin{array}{c} 79.30 \\ 88.40 \\ 97.80 \end{array} $	$\frac{108.00}{118.50}$
Static Pre 1.298 Oz.	Vol.	2460 3330 4380	5502 6830 8250	9830 13400 17470	$22100 \\ 27300 \\ 3300$	$39300 \\ 45800 \\ 53500$	61400 69700 78850	88500 98300 109300	$\frac{120200}{131800}$ $\frac{131800}{144200}$
2 34"	R.P.M.	1438 1230 1078	959 863 783	719 615 539	479 430 392	358 332 308	287 269 254	239 227 216	$ \begin{array}{c} 206 \\ 195 \\ 188 \\ \end{array} $
A. P. M.	R.P.M.	$ \begin{array}{c} 1.71 \\ 2.71 \\ 4.06 \end{array} $	5.76 7.92 10.50	$ \begin{array}{c} 13.70 \\ 21.75 \\ 32.40 \end{array} $	$\begin{array}{c} 46.20\\ 63.40\\ 84.30\end{array}$	$\frac{109.50}{138.20}$	214.00 259.50 311.00	$371.00 \\ 434.00 \\ 505.00$	$585.00 \\ 675.50 \\ 679.00 \\ 679.00 \\ $
Size		30 35 40	45 50 55	60 80 80	90 100 110	120 130 140	150 160 170	180 190 200	210 220 230

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CAPACITIES OF BUFFALO PLANOIDAL STEEL PLATE BLOWERS (TYPE L)	

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Ciro	A. P. M.	4" S	Static Press. 2.307 Oz.	ss. or z.	4 35"	Static Press. 2.595 Oz.	ress. or z.	5" S	Static Press. 2.884 0z.	css. or z.	5 1/2"	Static Pre 3.172 Oz.	Press. or 0z.	6" S	Static Press. 3.460 Oz.	SS. OF
2710	R.P.M.	R. P.M.	Vol.	Н. Р.	R. P.M.	Vol.	н. Р.	R.P.M.	Vol.	Н. Р.	R. P.M.	Vol.	Н. Р.	R. P.M.	Vol.	Н. Р.
30 35 40	$ \begin{array}{c} 1.71 \\ 2.71 \\ 4.06 \end{array} $	1916 1640 1438	3280 4440 5840	5.20 7.12 9.28	2035 1740 1525	$ \begin{array}{c} 3480 \\ 4710 \\ 6195 \end{array} $	$ \begin{array}{c} 6.20 \\ 8.50 \\ 10.08 \end{array} $	$\frac{2140}{1833}$	3670 4965 6530	7.27 9.95 12.98	2245 1925 1685	3845 5210 6850		2345 2010 1760	4030 5440 7150	9.55 13.08 17.05
45 55 55	, 5.76 7.92 10.50	$1278 \\ 1150 \\ 1044$	$7360 \\ 9100 \\ 11000$	$11.76 \\ 14.57 \\ 17.52$	1356 1220 1108	$ \begin{array}{c} 7805 \\ 9650 \\ 11680 \\ \end{array} $	14.01 17.37 20.90	1430 1285 1168	8230 10180 12300	16.44 20.35 24.50	$1499 \\ 1349 \\ 1223 \\ 1223 \\$	8635 10680 12900	$\frac{18.90}{23.40}$	$1564 \\ 1410 \\ 1279$	$ \begin{array}{c} 9020 \\ 11140 \\ 13480 \end{array} $	21.60 26.75 32.20
60 70 80	$13.70 \\ 21.75 \\ 32.40$	958 820 718	$\frac{13100}{17860}$	20.88 28.40 37.20	1018 870 762	$\frac{13900}{18950}\\24680$	$24.90 \\ 33.90 \\ 44.40$	$1070 \\ 917 \\ 803$	$\frac{14650}{19980}$	29.20 39.70 52.00	$ \begin{array}{c} 1122 \\ 962 \\ 842 \end{array} $	$15370 \\ 20950 \\ 27280 \\ 27280 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\$	33.60 45.70 59.80	1173 1003 880	16040 21880 28530	38.40 52.10 68.30
90 1100 1110	$\begin{array}{c} 46.20\\ 63.40\\ 84.30\end{array}$	638 574 522	29450 36400 44000	$\begin{array}{c} 47.00\\ 58.00\\ 70.25\end{array}$	677 609 554	$31250 \\ 38600 \\ 46650$	56.10 69.20 83.80	714 642 583	32950 40700 49200	$\begin{array}{c} 65.70 \\ 81.10 \\ 98.20 \end{array}$	749 673 612	$34550 \\ 42700 \\ 51600$	$\begin{array}{c} 75.60\\93.20\\112.90\end{array}$	782 703 640	$ \begin{array}{r} 36080 \\ 44600 \\ 53900 \end{array} $	86.50 106.50 129.00
120 130 140	$\begin{array}{c} 109.50 \\ 138.20 \\ 174.00 \end{array}$	478 442 410	$52400 \\ 61150 \\ 71350$	83.52 97.60 113.80	507 469 435	55600 64800 75600	$\begin{array}{c} 99.60\\ 116.30\\ 135.50\end{array}$	534 494 458	58600 68300 79750	$116.80 \\ 136.30 \\ 158.90$	$561 \\ 518 \\ 481 \\ 481$	61450 71700 83700	$\frac{134.30}{157.00}\\182.70$	585 542 502	64200 74850 87300	153.30 179.20 209.00
150 160 170	214.00 259.50 311.00	358 358 338	\$1\$00 92900 105100	$^{130.40}_{148.80}$	405 380 359	86900 98500 1111400	$\frac{155.50}{177.50}\\200.50$	427 400 378	$ \begin{array}{c} 91500 \\ 103900 \\ 117500 \end{array} $	$ \begin{array}{c} 182.20 \\ 208.00 \\ 235.00 \end{array} $	448 420 396	96000 108900 123200	209.50 239.00 270.00	468 438 414	$\frac{100100}{113700}$ $\frac{1128800}{128800}$	239.50 273.00 308.50
180 190 200	$371.00 \\ 434.00 \\ 505.00$	$318 \\ 302 \\ 288 $	$\frac{118000}{131000}$ $\frac{1145700}{145700}$	$\frac{188.00}{209.60}$ 232.00	338 321 306	$\frac{125200}{139000}$ $\frac{154500}{154500}$	$\begin{array}{c} 224.50\\ 250.00\\ 277.00\end{array}$	356 338 322	$\begin{array}{c} 132000 \\ 146500 \\ 163000 \end{array}$	$\begin{array}{c} 263.00 \\ 293.00 \\ 324.50 \end{array}$	373 354 338	138400 153800 170900	302.00 337.00 373.00	389 370 353	$\frac{144500}{160400}$ $\frac{178400}{178400}$	345.50 385.00 426.00
210 220 230	585.00 675.50 769.00	274 260 250	160300 175800 192300	$\begin{array}{c} 256.00\\ 280.80\\ 307.20\end{array}$	291 276 265	$\frac{170000}{186400}$ $\frac{204000}{204000}$	305.00 335.00 367.00	306 291 279	$\begin{array}{c} 179100 \\ 196600 \\ 215000 \end{array}$	358.00 393.00 429.00	321 305 293	188000 206100 225500	$\begin{array}{c} 412.00\\ 451.50\\ 494.00\end{array}$	$336 \\ 318 \\ 306 \\ 306 $	$\frac{196000}{215300}$ 235500	470.00 516.00 564.00

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Niagara Conoidal Type "N" Fan Wheel



Motor Driven Niagara Conoidal Type "N" Fan

Niagara Conoidal Capacity Tables

The fan capacity tables on pages 228 to 273 refer to the single inlet Niagara Conoidal fans. It will be noted that there are two sets of these tables, the first based on total pressures of from $\frac{3}{8}$ to 4 inches, and the second set for static pressures. The tables on pages 228 to 231 give thespeeds, capacities, and horsepowers for the different sizes when operating approximately at the point of highest total efficiency. Under these conditions the static pressure will be 77.5 per cent. of the total pressure as given in the table. These are termed the rated capacity tables for these fans, and are similar in character to those given for the Planoidal and other fans. Double width fans with two inlets give double the capacities and horsepowers given in the tables.

The static pressure tables on pages 232 to 273 give the capacities, speeds and horsepowers of these fans at static pressures of 0.25 to 2.5 inches of water, and with velocities at the fan outlet of 1000 to 4000 feet per minute. Thus we have the performance not only at the point of maximum efficiency, but at both sides of this point on the performance curve. It will be noted that the peculiar performance of the Niagara Conoidal fan gives a wide range of capacities at constant static pressure with but little variation in speed and but very slight change in total efficiency. The tables on pages 274 and 275 show the total efficiency at various pressures and outlet velocities. While it is generally advisable to operate a fan at or near its most efficient point, it may frequently be necessary to make a slight sacrifice in efficiency in order to meet special conditions.

Particular attention should be used in public building work to keep the fan outlet velocity about 1800 feet per minute in order to insure quietness of operation, with a maximum allowable velocity of 2200 for such work. For industrial installations where higher duct velocities are the rule and absolute quietness of operation is not essential, outlet velocities as high as 4000 may be used. For practical examples in the use of these tables see page 186.

¾" Total Press. or №" Total Press. or •.217 02. •.1 P. •.1 P. </th
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FAN ENGINEERING-BUFFALO FORGE COMPANY

Static Pressure is 77 ½

1 34" Total Press. or 0.721 0z. 0.865 0	°°°
R. P. M. Vol. H. P. R. P. M. Vol. 755 2730 .76 827 299 647 3730 .76 827 299 563 6130 1.71 551 620 510 503 6130 1.71 551 672 503 412 3750 2.11 496 333 503 511 378 10930 2.11 496 451 1004 333 378 10930 2.14 414 1194 354 1034 378 19930 5.41 310 2.134 310 2.134 283 19330 5.41 310 2.134 310 2.134 286 30230 6.85 2.46 3018 2.134 3110 2.134 287 30630 10.2 2.26 3018 2.134 3110 2.134 286 36630 10.2 2.26 3.13	
Vol. H. P. R. P. M. 2730 275 827 3710 1.35 729 3710 1.36 729 3710 1.36 720 3710 1.36 720 1305 6130 1.71 551 7570 2.11 496 411 19300 2.56 411 310 19330 3.04 414 310 38050 0.85 276 236 38050 10.2 2.248 310 3650 18.2 228 236	
Vol. H. P. R. P. M. 2730 76 827 3710 1.04 709 4850 1.35 620 5700 2.11 551 9160 2.56 451 10930 3.04 414 109300 4.14 354	
Vol. H. P. R. P. M. 2730 76 827 3710 1.04 709 1.35 620 1.35 6130 1.131 551 9160 2.56 451	
Vol. H. P. R. P. M. 2730 .76 827 3710 1.04 709 4850 1.35 620	
Vol. H. P. R. P.M.	

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ered 9 CAPACITIES OF BUFFALO NIAGARA CONOIDAL FANS (TYPE N) UNDER AVERAGE WORKING CONDITIONS AT 70° F. AND 29.92 INCHES BAROMETER

Total Press. or 21/2" Total Press. or 1.298 Oz.	Vol. H. P. R.P.M. Vol. H. P.	3660 1.84 1067 2.15 4980 2.50 915 5250 2.05 6500 3.26 801 6850 3.82	8230 4.13 712 8670 4.83 10160 5.09 640 10710 5.96 12290 6.17 582 12960 7.22	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	58510 29.4 267 61680 34.4 68670 34.4 246 72380 40.3 79650 40.0 229 83950 46.8	91420 45.9 214 96380 53.7 104030 52.2 200 109660 61.1 117450 58.9 188 123800 69.0	131660 66.0 178 138770 77.3 146690 73.6 169 154620 86.2 162550 81.5 160 171320 95.5
2 1⁄4" T	R.P.M.	1013 868 760	675 608 552	506 434 380	338 304 276	$253 \\ 234 \\ 217 $	203 190 179	169 160 152
. of	Н. Р.	$ \begin{array}{c} 1.54 \\ 2.09 \\ 2.73 \end{array} $	$3.46 \\ 4.27 \\ 5.17$	$ \begin{array}{c} 6.15 \\ 8.37 \\ 10.9 \end{array} $	$13.8 \\ 17.1 \\ 20.7 \\ 20.7 \\ 13.8 \\ 17.1 \\ $	24.6 28.9 33.5	38.4 43.7 49.4	55.3 61.7 68.3
2" Total Press. or 2 14" To 1.154 Oz.	Vol.	3450 4690 6130	$ \begin{array}{c} 7760 \\ 9580 \\ 11590 \end{array} $	$13790 \\ 18770 \\ 24520$	$ \begin{array}{r} 31020 \\ 38310 \\ 46360 \\ \end{array} $	55170 64730 75090	86200 98060 110720	$\frac{124410}{138280}$
2"T	R.P.M.	955 818 716	636 573 521	477 409 358	318 286 260	239 220 205	191 179 169	159 151 143
	Н. Р.	$ \begin{array}{c} 1.26 \\ 1.71 \\ 2.24 \end{array} $	2.83 3.49 4.23	5.03 6.85 8.95	11.3 14.0 16.9	20.1 23.6 27.4	31.5 35.8 40.4	45.3 50.5
134" Total Press. or 1.010 Oz.	Vol.	3230 4390 5740	$ \begin{array}{c} 7260 \\ 8960 \\ 10840 \end{array} $	$12900 \\ 17560 \\ 22940$	29030 35840 43370	51610 60560 70250	$\begin{array}{c} 80640\\91760\\103590\end{array}$	$\frac{116120}{129380}$ 143360
	R.P.M.	893 766 670	596 536 487	447 383 335	298 268 244	223 206 191	179 168 158	149 141 134
Area	Outlet Sq.Ft.	1.31 1.79 2.33	2.95 3.64 4.41	5.25 7.14 9.33	11.81 14.58 17.64	21.00 24.65 28.68	32.80 37.32 42.14	47.24 52.63 58.32
Mean Dia. of	Blast- Wheel	$\frac{15}{18} \frac{5_{q''}}{18}$ 20 $\frac{12}{20}$	$\frac{23}{26}\frac{1/2^{''}}{1/8^{''}}$ $\frac{28}{34^{''}}$	$31_{36}^{3.8}, 36_{12}^{3.8}, 42^{\circ}$	47" 52" 58"	63" 68" 73"	78" 84" 89"	94" 99" 105"
Fan	No.	88 4 3 8 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	4 10 10 1/2 1/2	0000	•01	227	15	18 19 20

FAN ENGINEERING-BUFFALO FORGE COMPANY

CAPACITIES OF BUFFALO NIAGARA CONOIDAL FANS (TYPE N) UNDER AVERAGE WORKING CONDITIONS AT 70° F. AND 29.92 INCHES BAROMETER

· · ·	Н. Р.	4.35 5.92 7.73	9.78 12.1 14.6	17.4 23.7 30.9	39.1 48.3 58.5	69.6 81.6 94.7	108.7 123.7 139.6	156.5 174.4 193.2
" Total Press. or 2.307 Oz.	Vol.	4880 6640 8670	10970 13550 16390	$\frac{19510}{26550}\\34680$	$\begin{array}{c} 43890 \\ 54180 \\ 65560 \end{array}$	78020 91560 106200	$\begin{array}{c} 121920 \\ 138700 \\ 156600 \end{array}$	$\begin{array}{c} 175550 \\ 195600 \\ 216720 \end{array}$
4"	H. P. R. P. M.	1350 1157 1013	900 810 736	675 579 506	450 405 368	338 312 289	270 253 238	225 213 202
ess.	н, Р.	3.56 4.85 6.32	$ \begin{array}{c} 8.01 \\ 9.87 \\ 12.0 \end{array} $	$14.2 \\ 19.4 \\ 25.3$	32.0 39.5 47.8	57.0 66.8 77.5	89.0 101.2 114.3	128.1 142.7 158.1
3 ½" Total Press. or 2.019 Oz.	Vol.	4560 6210 8110	$\frac{10260}{12670}$ 15330	$\frac{18250}{24840}\\32440$	$\begin{array}{c} 41050\\ 50700\\ 61330\end{array}$	$\begin{array}{c} 72990 \\ 85650 \\ 99340 \end{array}$	$\begin{array}{c} 114050\\ 129750\\ 146490\end{array}$	$\frac{164110}{182970}$ $\frac{202720}{202720}$
3 1/2'	R. P. M.	1263 1083 947	842 758 689	632 541 474	421 379 344	$316 \\ 292 \\ 271$	253 237 223	211 200 190
ss.	н. Р.	2.83 3.85 5.02	6.36 7.84 9.49	$11.3 \\ 15.4 \\ 20.1$	$25.4 \\ 31.4 \\ 38.0$	$45.2 \\ 53.0 \\ 61.5$	70.6 80.3 90.7	101.7 113.3 125.5
3" Total Press. or 1.734 Oz.	Vol.	4220 5750 7510	$\begin{array}{c} 9500\\11730\\14190\end{array}$	$\frac{16890}{23000}\\30040$	$38010 \\ 46930 \\ 56780$	$67570 \\ 79300 \\ 91970$	$\begin{array}{c} 105580\\ 120130\\ 135620\\ \end{array}$	$\begin{array}{c} 152020\\ 169400\\ 187680\end{array}$
3"	R. P.M.	1169 1002 877	780 702 638	585 501 439	390 351 319	292 270 251	234 219 206	195 185 175
ssure z.	н. Р.	2.48 3.38 4.41	5.58 6.88 8.33	9.91 13.5 17.6	22.3 27.5 33.3	39.7 46.5 54.0	62.0 70.5 79.6	89.2 99.4 110.2
2 %4" Total Pressure or 1.586 Oz.	Vol.	4040 5500 7190	$ \begin{array}{c} 9100 \\ 11230 \\ 13590 \end{array} $	$16170 \\ 22020 \\ 28760$	$36390 \\ 44930 \\ 54360$	$64700 \\ 75920 \\ 88060 \\$	$\frac{101080}{115000}$ $\frac{1129840}{129840}$	$\begin{array}{c} 145550\\ 162170\\ 179700\end{array}$
2 34"	R. P.M.	1120 960 840	746 672 610	560 480 420	373 336 305	280 258 240	224 210 198	187 177 168
Area	Outlet Sq. Ft.	$ \begin{array}{c} 1.31 \\ 1.79 \\ 2.33 \end{array} $	2.95 3.64 4.41	5.25 7.14 9.33	$\frac{11.81}{14.58}$ 17.64	21.00 24.65 28.68	32.80 37.32 42.14	47.24 52.63 58.32
Mean	Blast- Wheel	$\frac{155_8''}{181_8''}$ 20 $1_2''$	23 1/2" 26 1/8" 28 34"	31 ³ / ₈ " 36 ¹ / ₂ " 42"	47" 52" 58"	63" 68" 73"	78" 84" 89"	94" 99" 105"
Gan	No.	5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	4 ½ 5 ½ 5 ½	0100	e 011	12 14	15 16 17	18 19 20

Static Pressure is 77 ½% of Total Pressure

NIAGARA CONOIDAL FAN CAPACITIES

FAN	ENC	GINEE	RING	— B U I	FAL	O FO	RGE	СОМ	PANY
	d.	Н. Р.		.52	.54 .56 .50	.62 .66 .71	.76 .81 .87	$^{.94}_{1.02}$	1.36 1.58 1.84
	7,6" S. P.	R.P.M.		743	733 727 723	720 720 720	723 727 733	740 747 767	780 810 833
ES	34" S. P.	Н. Р.		.42 .43	.45 .48 .51	.54 .58 .63	.68 .73 .80	.86 .94 1.10	$ \begin{array}{c} 1.29 \\ 1.50 \\ 1.75 \end{array} $
RESSUR	34"	R.P.M.		687 680	2029 020 020	667 667 670	677 683 690	700 710 730	753 780 807
CAPACITIES AND STATIC PRESSURES (CHES BAROMETER	§∕« S. Ρ.	Н. Р.	-	.32 .33 .35	.37 .40 .43	.47 .52 .56	.61 .67 .73	.80 .88 1.04	$1.22 \\ 1.42$
AND SI METER		R. P. M.		623 617 613	610 607 610	613 617 623	633 643 650	660 673 693	720 747
V) CAPACITIES AND S INCHES BAROMETER	1 <u>/</u> 2" S. P.	Н. Р.	.23	.25 .26 .28	.31 .34 .37	.41 .45 .50	.55 .61 .67	.74 .81 .96	1.14 1.33
N) CAPA		R.P.M.	557	550 547 543	547 550 553	560 570 580	590 600 610	623 633 660	687 717
(TYPE 1 D 29.92	3%" S. P.	Н. Р.	.15 .16 .17	.18 .20 .23	32 32 32 32	.35 .40 .45	.55	.67 .74 .89	1.04
L FAN (T • F. AND		R.P.M.	483 477 477	470 473 477	480 490 500	510 520 530	543 557 570	583 597 623	657
ONOIDAL AT 70°	S. P.	Н. Р.	.09 .11 .12	.14 .16 .18	.21 .24 .28	.31 .35 .39	.44 .49 .55	.60 .67 .81	66.
GARA C	14"	R. P. M.	387 384 387	393 400 410	420 430 443	457 470 483	497 513 527	543 560 590	623
NO. 3 NIAGARA CONOIDAL FAN (TYPE N) AT 70° F. AND 29.92 IN	Add for Total Press.		0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	0.225 0.250 0.275	0.302 0.330 0.360	0.390 0.422 0.489	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
Z	Capacity	Cu. Ft. Air per Min.	1310 1440 1570	1710 1840 1970	2100 2230 2360	2490 2630 2760	2890 3020 3150	3280 3410 3670	3940 4190 4460
	Outlet	Velocity Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

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AL FAN (TYPE N) CAPACITIES AND STATIC I	S BAROMI
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N I A	NIAGARA		OIDA	L FA	N CA	APAC	ITIE	S
S. P.	H.P.		2.13 2.16	2.20 2.24 2.29	2.33 2.38 2.43	2.49 2.54 2.67	$2.82 \\ 3.00 \\ 3.21$	3.48 3.76 4.10
2 1/2"	R.P.M. H.P.		1343 1330	$1317 \\ 1303 \\ 1297$	$1287 \\ 1270 \\ 1263$	1253 1247 1233	1227 1217 1213	1220 1227 1233
P.	Н. Р.		$ \begin{array}{c} 1.53 \\ 1.58 \\ 1.61 \end{array} $	$1.65 \\ 1.68 \\ 1.73$	$1.76 \\ 1.81 \\ 1.85 \\ 1.85$	$1.91 \\ 1.96 \\ 2.10$	2.25 2.47 2.69	2.96 3.28 3.60
2" S. I	R. P. M.		1190 1177 1167	1157 1143 1133	1127 1120 1107	1103 1097 1090	$1087 \\ 1090 \\ 1093$	1107 1117 1133
S. P.	Н. Р.	1.25	$1.29 \\ 1.32 \\ 1.35$	1.39 1.42 1.46	$1.50 \\ 1.54 \\ 1.59 \\ 1.59 \\ 1.59 \\ 1.59 \\ 1.50 \\ $	$1.64 \\ 1.70 \\ 1.84$	2.02 2.23 2.47	2.76 3.04 3.39
1 3.4"	R. P. M.	1110	$1100 \\ 1087 \\ 1077 \\ $	1067 1057 1050	$1040 \\ 1033 \\ 1027$	1023 1020 1013	1020 1023 1033	1050 1067 1087
S. P.	Н. Р.	$1.00 \\ 1.04$	$1.06 \\ 1.09 \\ 1.12$	$ \begin{array}{c} 1.14 \\ 1.17 \\ 1.22 \end{array} $	$1.25 \\ 1.30 \\ 1.35$	$ \begin{array}{c} 1.41 \\ 1.47 \\ 1.63 \\ 1.63 \end{array} $	$1.81 \\ 2.02 \\ 2.26$	2.53 2.84
1 1/2"	R. P. M.	1027 1017	1007 997 983	096 070 960	953 950 947	943 940 943	950 960 980	997 1017
S. P.	Н. Р.	.80 .81	.84 .86 .89	.92 .95 .99	$1.03 \\ 1.08 \\ 1.13 \\ $	$ \begin{array}{c} 1.20 \\ 1.26 \\ 1.43 \end{array} $	$ \begin{array}{c} 1.61 \\ 1.83 \\ 2.06 \end{array} $	2.34
1 }," S.	R. P. M.	920 913	903 893 883	877 873 867	863 860 860	860 863 870	883 900 920	943
1" S. P.	Н. Р.	.58 .59 .62	.64 .66 .68	.71 .75 .79	.89 .89 .95	$1.03 \\ 1.09 \\ 1.25$	$1.44 \\ 1.65 \\ 1.90$	2.18
1" S	R. P. M.	820 810 800	793 783 777	773 770 770	767 770 773	777 783 800	820 837 863	883
Add for	Press.	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
Capacity	Cu. Ft. Air per Min.	1710 1840 1970	2100 2230 2360	2490 2630 2760	2890 3020 3150	3280 3410 3670	3940 4190 4460	4730 4990 5250
Outlet	Velocity Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3200 3200 3400	3600 3800 4000

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J	ENGI	NEEI	RING-	– B U F	FAL) FO	RGE	СОМ	PANY
	à	Н. Р.		.71	.73 .77 .80	85 90: 96:	$1.03 \\ 1.10 \\ 1.18 \\ 1.18$	$1.27 \\ 1.39 \\ 1.59$	1.85 2.16 2.50
	7,8" S.	R. P. M.	_1	637	629 623 620	617 617 617	620 623 629	634 640 657	669 694 714
	ъ.	Н. Р.		.59 .59	.62 .65 .69	.74 .79 .86	$1.00 \\ 1.09$	$1.17 \\ 1.27 \\ 1.50$	$ \begin{array}{c} 1.75 \\ 2.05 \\ 2.38 \\ \end{array} $
	34" S. P.	R. P. M.		589 583	577 574 572	572 572 574	580 586 592	600 609 626	646 669 692
	S. P.	Н. Р.		.43 .45 .48	.51 .55 .59	.64 .70 .76	.83 .91 .99	$1.08 \\ 1.19 \\ 1.41$	$1.65 \\ 1.94$
	5 "S"	R. P. M.		534 529 526	523 520 523	526 529 534	543 552 557	566 577 594	617 640
	s. p.	Н. Р.	.32		.42 .46 .51	.56 .62 .68	.75 .83 .91	$1.01 \\ 1.10 \\ 1.31 \\ 1.31$	$1.56 \\ 1.81$
	1/2"	R. P. M.	477	472 469 466	469 472 474	480 489 497	506 514 523	534 543 566	589 614
	s. P.	Н. Р.	20 23 23	.25 .28 .31	.34 .33 .33	.48 .54 .61	.68 .75 .83	.91 1.01 1.21	1.42
	3/8	R. P. M.	414 409 409	403 406 409	412 422 429	437 446 454	466 477 489	500 512 534	563
	Ŀ.	Н. Р.	.13 .14 .16	.18 .21 .24	.28 .32 .37	.42 .53	.59 .67 .74	.82 .91 1.10	1.35
	14" S.	R.P.M.	332 329 332	337 343 352	360 369 380	392 403 414	426 440 452	466 480 506	534
	Add for Total	Press.	0.063 0.076 0.090	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390\\ 0.422\\ 0.489\end{array}$	0.560 0.638 0.721
	Capacity Cu. Ft.	Air per Min.	$1790 \\ 1970 \\ 2140$	2320 2500 2680	2860 3040 3210	3390 3570 3750	$ \begin{array}{r} 3930 \\ 4110 \\ 4290 \\ \end{array} $	4470 4640 5000	5360 5720 6070
	Outlet Velocity	Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

	NIAGARA		CONC	DIDA.		N CA	FAU	LILES	,
	. P.	H. P.		2.89 2.94	$2.99 \\ 3.05 \\ 3.11$	3.17 3.23 3.31	3.38 3.46 3.63	3.84 4.08 4.36	4.73 5.12 5.59
	2 ½" S.	R.P.M.		1151 1140	1129 1117 1111	1103 1089 1083	1074 1069 1057	$1052 \\ 1043 \\ 1040$	1046 1052 1057
	S. P.	Н. Р.		2.08 2.14 2.19	$2.24 \\ 2.29 \\ 2.35$	$2.40 \\ 2.52 \\ 2.52$	2.60 2.67 2.86	3.06 3.36 3.66	4.03 4.46 4.90
	2" S	R. P. M.		1020 1009 1000	992 980 972	966 960 949	946 940 934	932 934 937	949 957 972
	S. P.	Н. Р.	1.70	$1.75 \\ 1.79 \\ 1.84$	$1.89 \\ 1.94 \\ 1.99 $	2.03 2.10 2.17	2.23 2.32 2.50	2.74 3.04 3.36	3.75 4.14 4.61
AETER	1 34"	R. P. M.	952	943 932 923	914 906 900	892 886 880	877 874 869	874 877 886	900 914 932
BARON	1 ½" S. P.	Н. Р.	$1.36 \\ 1.41$	$ \begin{array}{c} 1.45 \\ 1.48 \\ 1.52 \end{array} $	$1.56 \\ 1.59 \\ 1.65$	$1.70 \\ 1.77 \\ 1.84 \\ 1.84$	$ \begin{array}{c} 1.91 \\ 2.00 \\ 2.22 \end{array} $	2.46 2.75 3.08	3.44 3.86
F. AND 29.92 INCHES BAROMETER		R.P.M.	880 872	863 854 843	837 831 823	817 814 812	809 806 809	814 823 840	854 872
0 29.92	1 ½" S. P.	Н. Р.	1.08 1.10	1.15 1.17 1.21	$1.25 \\ 1.30 \\ 1.35$	$ \begin{array}{c} 1.40 \\ 1.47 \\ 1.53 \end{array} $	$ \begin{array}{c} 1.63 \\ 1.72 \\ 1.95 \end{array} $	2.19 2.49 2.81	3.19
• F. ANI		R. P. M.	789 783	774 766 757	752 749 743	740 737 737	737 740 746	757 772 789	809
AT 70°	l" S. P.	Н. Р.	.78 .81 .84	86. 93. 93. 93.	.97 1.02 1.08	$1.14 \\ 1.22 \\ 1.30 \\ 1.30 \\ 1$	$ \begin{array}{c} 1.40 \\ 1.48 \\ 1.70 \end{array} $	$ \begin{array}{c} 1.96 \\ 2.24 \\ 2.59 \end{array} $	2.97
	1, 5	R.P.M.	703 694 686	680 672 666	663 660 660	657 660 663	666 672 686	703 717 740	757
	Add for Total Press.		$\begin{array}{c} 0.106 \\ 0.122 \\ 0.141 \end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
	Capacity	Cu. Ft. Air per Min.	2320 2500 2680	2860 3040 3210	3390 3570 3750	3930 4110 4290	4470 4640 5000	5360 5720 6070	6430 6790 7140
	Outlet	Velocity Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NO. 3 ½ NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES

NIAGARA CONOIDAL FAN CAPACITIES

1		d.	-	.92	.96 1.00 1.05	1.11	1.35 1.44 1.55	1.67 1.81 2.08	2.42 2.82 3.27
	78" S. P.	H.						1-0	010100
	18/1	R. P. M. H. P.		558	550 545 543	540 540 540	543 545 550	555 560 575	585 608 625
	ď	Н. Р.		.77	.85 .90	$ \begin{array}{c} .96 \\ 1.04 \\ 1.12 \end{array} $	$ \begin{array}{c} 1.21 \\ 1.31 \\ 1.42 \end{array} $	$1.53 \\ 1.67 \\ 1.95$	2.29 2.67 3.11
	34" S. P.	R. P. M.		515 510	505 503 500	500 503 503	508 513 518	525 533 548	565 585 605
	S. P.	Н. Р.		.56 .59 .62	.71 .71 .77	$.84 \\ .92 \\ 1.00$	$1.08 \\ 1.19 \\ 1.30 $	$ \begin{array}{c} 1.41 \\ 1.56 \\ 1.84 \end{array} $	2.16
NELEK	5%" S.	R. P. M.		468 463 460	458 455 458	460 463 468	475 483 488	495 505 520	540 560
BAKUM	; P.	Н. Р.	.41	.44 .47 .50	.55 .60 .66	.73 .81 .89	$^{0.98}_{1.19}$	$ \begin{array}{c} 1.32 \\ 1.43 \\ 1.71 \end{array} $	2.03
INCRES	½″ S. P.	R.P.M.	418	413 410 408	410 413 415	420 428 435	443 450 458	468 475 495	515 538
26.92 (s. P.	Н. Р.	.26 30 30	.33 .36 .40	.45 .50 .56	.63 .71 .80	.88 .98 1.09	$ \begin{array}{c} 1.19 \\ 1.32 \\ 1.58 \end{array} $	1.86
AI 70° F. AND 29.92 INCHES BARUMETER	3 <i>8</i> " S	R. P. M.	363 358 358	355 355 358	360 368 375	383 390 398	408 418 428	438 448 468	493
A1 70	s. P.	Н. Р.	.17 .19 .21	.24 .28 .32	.37 .42 .49	.55 .62 .70	.78 .87 .97	1.07 1.19 1.44	1.76
	M" 5	R.P.M.	290 288 290	295 300 308	$\frac{315}{323}$	343 353 363	373 385 395	408 420 443	468
	Add for Total	Press.	0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	0.225 0.250 0.27 5	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
	Capacity Cu. Ft.	per Min.	2330 2570 2800	3030 3270 3500	3730 3970 4220	4430 4670 4900	5130 5370 5600	5830 6070 6530	7000 7460 7930
	Outlet Velocity	Ht. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

BUFFALO

FORGE

COMPANY

EERING-

NO. 4 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES NT 70° E AND 20 02 INCHES RADOMETED NO. 4 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AND 20 02 INCHES BADOMETED \$

	NIA	GARA	CONC	DIDA	L FA	N CA	PACI	TIES	
	ď	H. P.		3.78 3.84	$3.91 \\ 3.99 \\ 4.07$	4.15 4.23 4.32	4.42 4.51 4.74	5.01 5.33 5.70	6.18 6.69 7.30
	2 1⁄2" S.	R.P.M.		1008 998	988 978 973	965 953 948	940 935 925	920 913 910	915 920 925
	e:	Н. Р.		$2.72 \\ 2.80 \\ 2.87 $	$2.93 \\ 2.99 \\ 3.07$	$3.14 \\ 3.22 \\ 3.30 \\$	$3.39 \\ 3.49 \\ 3.73$	4.00 4.39 4.79	5.27 5.83 6.40
	2″ S. P.	R.P.M.		893 883 875	868 858 850	845 840 830	828 823 818	815 818 820	830 838 850
	S. P.	н. Р.	2.23	$2.29 \\ 2.34 \\ 2.40$	2.47 2.53 2.59	$2.66 \\ 2.74 \\ 2.83 \\ $	2.91 3.03 3.27	$3.59 \\ 3.97 \\ 4.39$	$4.90 \\ 5.41 \\ 6.02$
METER	134"	R. P. M.	833	825 815 808	800 793 788	780 775 770	765 765 760	765 768 775	788 800 815
BARO	1 ½″ S . P.	Н. Р.	$1.78 \\ 1.84$	$ \begin{array}{c} 1.89 \\ 1.94 \\ 1.94 \end{array} $	2.03 2.08 2.16	$2.23 \\ 2.31 \\ 2.40$	$2.50 \\ 2.61 \\ 2.90 $	$3.22 \\ 3.59 \\ 4.02$	4.50 5.04
AT 70° F. AND 29.92 INCHES BAROMETER		R. P. M.	770 763	755 748 738	733 728 720	715 713 710	705 705 708	713 720 735	748 763
D 29.92	S. P.	Н. Р.	1.41 1.44	$1.50 \\ 1.53 \\ 1.58 \\ $	$1.63 \\ 1.70 \\ 1.76$	$ \begin{array}{c} 1.83 \\ 1.92 \\ 2.00 \end{array} $	2.13 2.24 2.55	2.87 3.25 3.67	4.16
F. AN	1 14"	R.P.M.	690 685	678 670 663	655 655 650	645 645 645	645 648 653	663 675 690	208
AT 70	ä	Н. Р.	1.03 1.06 1.09	$1.13 \\ 1.17 \\ 1.22$	1.27 1.33 1.40	$ \begin{array}{c} 1.49 \\ 1.59 \\ 1.70 \end{array} $	$ \begin{array}{c} 1.83 \\ 1.94 \\ 2.23 \end{array} $	2.56 2.93 3.38	3.87
	1" S.	R. P. M.	615 608 600	595 588 583	580 578 578	575 578 580	583 588 600	615 628 648	663
	Add for	Total Press.	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
	Capacity Cu. Ft. Air per Min.		3030 3270 3500	3730 3970 4220	4430 4670 4900	5130 5370 5600	5830 6070 6530	7000 ⁻ 7460 7930	8400 8860 9330
	Outlet Velocity Ft. per Min.		1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

S AND STATIC PRESSURES	
STATIC	
NO. 4 ½ NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND	AT 70° F. AND 29.92 INCHES BAROMETER
FAN (AND
CONOIDAL	AT 70° F.
NIAGARA	
NO. 4 1/2	

ENC	GINEE	RING	- B U I	FAL	O FC	RGE	СОМ	PANY
	Н. Р.		1.17	$1.21 \\ 1.27 \\ 1.33$	$ \begin{array}{c} 1.40 \\ 1.48 \\ 1.59 \end{array} $	$ \begin{array}{c} 1.71 \\ 1.82 \\ 1.96 \end{array} $	$2.11 \\ 2.29 \\ 2.63$	3.06 3.57 4.13
7.8" S.	R. P. M.		496	489 485 482	480 480 480	482 485 489	493 498 511	520 540 556
s. p.	Н. Р.		0.93	$1.02 \\ 1.07 \\ 1.14$	$ \begin{array}{c} 1.22 \\ 1.31 \\ 1.42 \end{array} $	$1.53 \\ 1.65 \\ 1.80$	$ \begin{array}{c} 1.94 \\ 2.11 \\ 2.47 \end{array} $	2.90 3.38 3.93
3.4" 5	R. P. M.		458 453	449 447 445	445 445 447	451 456 460	467 473 487	502 520 538
s. p.	Н. Р.		$\begin{array}{c} 0.71 \\ 0.75 \\ 0.79 \end{array}$	$\begin{array}{c} 0.84 \\ 0.90 \\ 0.97 \end{array}$	$1.06 \\ 1.16 \\ 1.26 $	1.37 1.50 1.64	$ \begin{array}{c} 1.79 \\ 1.97 \\ 2.33 \end{array} $	2.73 3.20
5 %n	R.P.M.		416 411 409	407 405 407	409 411 416	422 429 433	440 449 462	480 498
S. P.	Н. Р.	0.52	0.55 0.59 0.63	$\begin{array}{c} 0.69\\ 0.76\\ 0.84\end{array}$	$\begin{array}{c} 0.92 \\ 1.02 \\ 1.13 \end{array}$	$1.24 \\ 1.37 \\ 1.51$	$ \begin{array}{c} 1.67 \\ 1.81 \\ 2.17 \end{array} $	2.57 3.00
12" -	R. P. M.	371	367 365 362	365 367 369	373 380 387	393 400 407	416 422 440	458 478
³ %" S. P.	Н. Р.	0.33 0.35 0.38	$\begin{array}{c} 0.41 \\ 0.46 \\ 0.51 \end{array}$	$\begin{array}{c} 0.57 \\ 0.64 \\ 0.71 \end{array}$	0.80 0.89 1.01	$1.12 \\ 1.24 \\ 1.38 \\ 1.38 \\ 1.38 \\ 1.128 \\ 1$	$ \begin{array}{c} 1.50 \\ 1.67 \\ 2.00 \end{array} $	2.35
3%"	R.P.M.	322 318 318	313 316 316 318	320 327 333	340 347 353	362 371 380	389 398 416	438
s. p.	Н. Р.	$\begin{array}{c} 0.21 \\ 0.23 \\ 0.27 \end{array}$	$\begin{array}{c} 0.30 \\ 0.35 \\ 0.40 \end{array}$	$\begin{array}{c} 0.46 \\ 0.53 \\ 0.61 \end{array}$	0.69 0.79 0.88	0.98 1.10 1.23	1.35 1.51 1.82	2.23
34"	R.P.M.	258 256 258	262 267 273	280 287 296	$305 \\ 313 \\ 322$	$331 \\ 342 \\ 351 \\ 351 \\$	362 373 393	416
Add for	Total Press.	0.063 0.076 0.090	$\begin{array}{c} 0.106 \\ 0.122 \\ 0.141 \end{array}$	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
Capacity	cu. Ft. Air per Min.	2950 3250 3540	3840 4130 4430	4720 5020 5310	5610 5900 6200	6500 6790 7090	7380 7680 8270	8860 9450 10040
Outlet	Velocity Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

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ETE
AT 70° E AND 20 02 INCHES RADOMETER
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S. P.	Н. Р.		4.78 4.86	4.94 5.04 5.14	5.25 5.35 5.47	5.59 5.71 5.99	6.34 6.74 7.21	7.82 8.46 9.23
2 1/3"	R.P.M.		896 887	878 869 865	858 847 842	836 831 822	818 811 809	813 818 822 822
-i-	Н. Р.		3.44 3.54 3.63	$3.71 \\ 3.79 \\ 3.89$	$3.97 \\ 4.07 \\ 4.17$	4.29 4.42 4.72	5.06 5.55 6.06	6.66 7.37 8.10
2" S.	R. P. M.		793 785 778	771 762 756	751 747 738	736 731 727	725 727 729	738 745 756
S. P.	Н. Р.	2.82	2.90 2.96 3.04	$3.12 \\ 3.20 \\ 3.28 \\ 3.28 \\$	3.36 3.46 3.59	$3.69 \\ 3.83 \\ 4.13$	4.54 5.02 5.55	6.20 6.85 7.61
1.87"	R. P. M.	740	733 725 718	711 704 700	696 689 685	682 680 676	680 682 689	700 711 725
S. P.	Н. Р.	2.25 2.33	$2.39 \\ 2.45 \\ 2.51$	2.57 2.63 2.74	2.82 2.92 3.04	3.16 3.30 3.67	4.07 4.54 5.08	5.69 6.38
1 15"	R.P.M.	685 678	671 665 656	651 647 640	636 633 631	629 627 629	633 640 653	665 678
S. P.	H. P.	$1.79 \\ 1.82$	$ \begin{array}{c} 1.89 \\ 1.93 \\ 2.00 \end{array} $	2.07 2.15 2.23	2.31 2.43 2.53	2.69 2.84 3.22	$3.63 \\ 4.11 \\ 4.64$	5.27
"Fi I	R.P.M.	613 609	602 596 589	585 582 578	576 573 573	573 576 580	589 600 613	629
ď	Н. Р.	$1.30 \\ 1.34 \\ 1.38 \\ $	$ \begin{array}{c} 1.43 \\ 1.48 \\ 1.54 \end{array} $	$1.60 \\ 1.69 \\ 1.78 \\ $	$ \begin{array}{c} 1.89 \\ 2.01 \\ 2.15 \end{array} $	2.31 2.45 2.82	3.24 3.71 4.27	4.90
1" S. P.	R. P. M.	547 540 533	529 522 518	516 513 513	511 513 516	518 522 533	547 558 576	589
Add for	Press.	0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	0.560 0.638 0.721	$\begin{array}{c} 0.810\\ 0.900\\ 1.000\end{array}$
Capacity	Air Air per Min.	3840 4130 4430	4720 5020 5310	5610 5900 6200	6500 6790 7090	7380 7680 8270	8\$60 9450 10040	10630 11220 11810
Outlet	Fit. per Min.	1300	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NIAGARA CONOIDAL FAN CAPACITIES

Н. Р. .44 1.49 1.73 $2.60 \\ 3.25 \\$ $3.78 \\ 4.40 \\ 5.10$ 2.11 2.25 2.41 7.8" S. P. R. P. M. 146 3252 434 436 440 444444444 140 168 188 500 Н. Р. 1.15 1.26 1.50 2.40 3.05 3.05 1.892.222.22 $3.58 \\ 4.18 \\ 4.85$ S. P. R. P. M. 3.4 " $^{412}_{408}$ 401002 0000 406 410 414 420 426 438 452
 468
 484Н. Р. 86.68 1.04 1.31 1.43 1.56 1.69 1.85 2.03 $2.21 \\ 2.88 \\$ 3.38 d, s R. P. M. 18 396 404 416 **132 148** 374 370 368 366366 368 370 374 3863380 Н. Р. 68 73 73 .86 94 03 1.14 $2.24 \\ 2.24 \\ 2.68 \\ 2.68 \\ 3.68 \\$ 3.18 65 ć s R. P. M. 2" 334 330 328 326 328 330 332 $336 \\ 342 \\ 348$ 354 360 366 374 380 396 112 Н. Р. 41.44 51 730 .38 1.862.062.462.90 d, s R. P. M. 38 288 294 300 312 318 318 0630 282 284 286 326 334 342 350 358 374 394 Н. Р. 28 33 33 .38 .43 .50 .57 .76 .98 .97 .09 1.671.862.252.75 21 36 51 ď ŝ R. P. M. 14" 298 308 316 232 232 232 236 240 252 258 266 274 282 290 326 336 354 374 Add for Total Press. 0.390 0.422 0.489 0.063 0.076 0.090 $\begin{array}{c} 0.106\\ 0.122\\ 0.141\\ 0.141 \end{array}$ $\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$ $\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$ $0.302 \\ 0.330 \\ 0.360 \\ 0.360$ $\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$ Capacity Cu. Ft. Air per Min. 3640 4010 4370 4740 51000 5470 5830 6190 6560 6560 7290 7660 8010 8380 8750 9100 9480 0200 0940 1660 2390 Outlet Velocity Ft. per Min. 3000 3200 3400 1500 1700 1900 2200 2500 2600 2800 1000 300 500

(TYPE N) CAPACITIES AND STATIC PRESSURES 29.92 INCHES BAROMETER AND NO. 5 NIAGARA CONOIDAL FAN Ľ. 200 AT

PRESSURES	
STATIC	~
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N) CAPACITIES	BAROMETE
CAP/	INCHES
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IDA	70°
CONOIDAL	AT
NIAGARA	
5	
NO.	

NIAG	ARA	CON	OIDA	LFA	N C	APAC	ITIE	s
P. 1	H.P.		5.90	$6.10 \\ 6.23 \\ 6.35$	6.48 6.60 6.75	6.90 7.05 7.40	7.83 8.32 8.90	9.65 10.5 11.4
2 ½" S.	R. P. M.		806 798	790 782 778	772 762 758	752 748 740	736 730 728	732 736 740
	Н. Р.		4.25 4.38 4.48	4.58 4.68 4.80	$ \frac{4.90}{5.03} $	5.30 5.45 5.83	6.25 6.85 7.48	$ \begin{array}{c} 8.22 \\ 9.10 \\ 10.00 \end{array} $
3, °	R. P. M.		714 706 700	694 686 680	676 672 664	662 658 654	652 656 656	664 670 680
S. P.	Н. Р.	3.48	3.58 3.65 3.75	3.85 3.95 4.05	4.15 4.28 4.44	4.55 4.73 5.10	5.60 6.20 6.85	7.65 8.46 9.40
1 34"	R.P.M.	666	660 652 646	640 634 630	624 620 616	614 612 608	612 614 620	630 640 652
S. P.	Н. Р.	2.78 2.88	2.95 3.03 3.10	3.18 3.25 3.38	3.48 3.60 3.75	3.90 4.08 4.53	5.03 5.60 6.28	7.03 7.88
1 ½" S. P.	R.P.M.	616 610	604 598 590	586 582 576	572 570 568	566 564 566	570 576 588	598 610
	Н. Р.	2.21 2.25	2.34 2.39 2.47	2.55 2.65 2.75	2.85 3.00 3.13	3.33 3.50 3.98	4.48 5.08 5.73	6.50
1 ½" S. P.	R.P.M.	552 548	542 536 530	526 524 520	518 516 516	516 518 522	530 540 552	566
G	Н. Р.	$ \begin{array}{c} 1.60 \\ 1.65 \\ 1.71 \end{array} $	$ \begin{array}{c} 1.76 \\ 1.82 \\ 1.90 \end{array} $	$ \begin{array}{c} 1.98 \\ 2.08 \\ 2.19 \end{array} $	2.33 2.48 2.65	2.85 3.03 3.48	4.00 4.57 5.27	6.05
I" S. P.	R.P.M.	492 486 480	476 470 466	464 462 462	460 462 464	466 470 480	492 502 518	530
Add for Total	Add for Total Press,		$\begin{array}{c} 0.160\\ 0.180\\ 0.202\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	0.302 0.330 0.360	0.390 0.422 0.489	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
Capacity Cu. Ft.	per Min.	4740 5100 5470	5830 6190 6560	6930 7290 7660	8010 8380 8750	9100 9480 10200	$10940 \\ 11660 \\ 12390$	13120 13850 14580
Outlet Velocity	Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NO. 51/2 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

ENG	INEE	RING-	-BUF	FALO	FO FO	RGE	СОМ	PANY
4	H. P.		1.75	$\begin{array}{c} 1.81\\ 1.89\\ 1.98\end{array}$	2.09 2.21 2.37	$2.55 \\ 2.72 \\ 2.92 \\ 2.92 \\ 100 \\ $	3.15 3.42 3.93	4.57 5.33 6.17
7%" S.	R.P.M.		406	400 397 395	393 393 393	395 397 400	404 407 418	426 442 455
34" S. P.	Н. Р.		$1.40 \\ 1.45$	$1.52 \\ 1.60 \\ 1.70$	$ \begin{array}{c} 1.82 \\ 1.96 \\ 2.12 \end{array} $	2.28 2.47 2.68	$2.90 \\ 3.15 \\ 3.69 \\ 3.69$	4.33 5.05 5.87
3.4"	R.P.M.		375 371	367 366 364	364 364 366	369 373 377	382 387 398	411 426 440
S. P.	Н. Р.		1.06 1.12 1.18	$1.26 \\ 1.35 \\ 1.46$	$1.59 \\ 1.73 \\ 1.88 \\ $	2.05 2.24 2.45	2.67 2.94 3.48	4.08 4.78
12 m	R. P. M.		340 336 335	333 331 333	335 336 340	346 351 355	360 367 378	393 407
S. P.	Н. Р.	.78	83 88 85 85	$1.04 \\ 1.13 \\ 1.25$	$ \begin{array}{c} 1.38 \\ 1.53 \\ 1.68 \end{array} $	$ \begin{array}{c} 1.85 \\ 2.05 \\ 2.25 \end{array} $	2.49 2.71 3.24	3.84 4.48
1/2"	R.P.M.	304	300 298 296	298 300 302	306 311 316	322 327 333	340 346 360	375 391
S. P.	Н. Р.	.49 .53 .57	.62 .68 .76	$.85 \\ .95 \\ 1.06$	$ \begin{array}{c} 1.19 \\ 1.34 \\ 1.50 \end{array} $	$ \begin{array}{c} 1.67 \\ 1.86 \\ 2.05 \end{array} $	2.25 2.49 2.98	3.51
3%"	R.P.M.	264 260 260	257 258 260	$262 \\ 267 \\ 273 \\ 273 \\ 273 \\ 273 \\ 273 \\ 267 \\ 273 $	278 284 289	296 304 311	318 326 340	358
S. P.	H. P.	.32 .35 .40	.45 .52 .60	.69 .80 .92	$1.04 \\ 1.17 \\ 1.32 \\ 1.32 \\$	$ \begin{array}{c} 1.47 \\ 1.65 \\ 1.83 \\ 1.83 \end{array} $	$2.02 \\ 2.25 \\ 2.72 $	3.33
14"	R.P.M.	211 209 211	$215 \\ 218 \\ 224 \\ 224$	229 235 242	249 256 264	271 280 287	- 297 306 322	340
Add for Total	Press.	0.063 0.076 0.090	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\\ 0.141 \end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560\\ 0.638\\ 0.721\end{array}$
Capacity Cu. Ft.	Air per Min.	4410 4850 5290	5730 6170 6620	7060 7500 7940	8380 8820 9260	$\begin{array}{c} 9700\\ 10140\\ 10590\end{array}$	$11030\\11470\\12350$	13230 14110 15000
Outlet Velocity	Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

STATIC PRESSURES	
5 ½ NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND 3	AT 70° F. AND 29.92 INCHES BAROMETER
No.	

NIAG	ARA	CON	DIDA	L FA	NCA	APAC	ITIE	S
s. P.	Н. Р.		7.14 7.26	7.38 7.53 7.68	7.84 7.99 8.17	8.35 8.53 8.95	$\begin{array}{c} 9.47 \\ 10.1 \\ 10.8 \\ 10.8 \end{array}$	11.7 12.7 13.8
2 3/2"	R. P. M.		733 726	718 711 707	702 693 689	684 680 673	669 664 662	666 669 673
ď	Н. Р.		$5.14 \\ 5.29 \\ 5.42$	5.54 5.66 5.81	5.93 6.08 6.23	$6.41 \\ 6.59 \\ 7.05$	7.56 8.29 9.04	9.95 11.0 12.1
2" S. P.	R. P.M.		649 642 636	631 624 618	615 611 604	602 598 595	593 595 596	604 609 618
S. P.	Н. Р.	4.21	4.33 4.42 4.54	4.66 4.78 4.90	5.02 5.17 5.35	5.51 5.72 6.17	6.78 7.50 8.29	9.26 10.2 11.4
1 34"	R.P.M.	606	600 593 587	582 576 573	567 564 560	558 557 553	557 558 564	573 582 593
S. P.	Н. Р.	3.36 3.48	3.57 3.66 3.75	$3.84 \\ 3.93 \\ 4.08$	4.21 4.36 4.54	4.72 4.93 5.48	6.08 6.78 7.59	8.50 9.53
1 3/2"	R. P. M.	560 555	549 544 537	533 529 524	520 518 517	515 513 515	518 524 535	544 555
S. P.	Н. Р.	2.67 2.72	2.83 2.89 2.99	$3.09 \\ 3.21 \\ 3.33$	3.45 3.63 3.78	4.02 4.24 4.81	$5.42 \\ 6.14 \\ 6.93$	7.87
1 3%	R. P. M.	502 498	493 487 482	478 476 473	471 469 469	469 471 475	482 491 502	515
P.	Н. Р.	$1.94 \\ 1.99 \\ 2.07$	2.13 2.20 2.30	2.39 2.52 2.65	2.82 3.00 3.21	3.45 3.66 4.21	4.84 5.54 6.38	7.32
1″ S.	R. P. M.	447 442 437	433 427 424	422 420 420	418 420 422	424 427 437	447 456 471	482
Add for Total	Press.	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
Capacity Cu. Ft.	per Min.	5730 6170 6620	7060 7500 7940	8380 8820 9260	9700 10140 10590	$11030 \\ 11470 \\ 12350$	$\begin{array}{c} 13230 \\ 14110 \\ 15000 \end{array}$	$15880 \\ 16760 \\ 17640 \\ 17640 \\ 1$
Outlet		1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

/	7%" S. P.		R. P. M. H. P.	R. P. M. H. P.	R. P. M. H. P.	R. P. M. H. P. 372 2.08 367 2.15 363 2.15 363 2.15	R. P. M. H. P. 372 2.08 367 2.15 360 2.49 360 2.49 360 2.83	R. P.M. H. P. 372 2.08 367 2.15 363 2.25 360 2.49 360 2.63 360 2.82 363 3.04 363 3.04 363 3.04	R. P.M. H. 372 2. 367 2. 3667 2. 3667 2. 3667 2. 3660 2. 367 3. 367 3. 372 3. 367 3. 373 3. 373 3. 374 4. 4. 4. 4. 4. 4. 4. 4. 4.
	34" S. P.	R.P.M. H. P.			344 1.66 340 1.72				
3% S. P. 35" S. P. 5%" S. P.	Н. Р.			1.27 1.33 1.41				· · · · · · · · · · · · · · · · · · ·	
		P. R.P.M.	33		8 312 5 308 3 307				
	s.	R.P.M. H. P.	278 .9		275 .98 274 1.05 272 1.13				
	S. P.	Н. Р.	.59 .63 .67		.73 .81 .91	$\begin{array}{c} .73\\ .81\\ .91\\ .91\\ 1.01\\ 1.13\\ 1.26\end{array}$.73 .81 .91 1.01 1.13 1.26 1.79	.73 .81 .91 .91 .1.13 1.26 1.26 1.26 1.59 1.79 1.79 2.21 2.45	.73 .81 .91 .01 1.26 1.26 1.29 1.29 1.29 1.29 1.29 2.45 2.45 2.45 2.26 2.26 2.26 2.26 3.55
	38/1	R. P. M.	242 238 238		235 237 238				
	J₄" S. P.	M. H. P.	37 37 37 37 37 37 37 37 37 37 37 37						
		Press. R. P.M.	0.063 193 0.076 193 0.090 193						
		per Min.			6820 7350 7870				
		Ft. per Min.	1000 1100 1200		1300 1400 1500	1300 1500 1500 1700 1800	1300 1500 1500 1700 1800 22000 2100	1300 11400 11500 11500 11500 11700 11700 11700 11700 2200 22000 22000 22000 22000	1300 11400 11500 11500 11500 11500 1200 22000 22000 22500 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 22000 222000 2200 2200 2200 2200 2000 2000 2000000

-BUFFALO FORGE COMPANY

NO. 6 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 700 E AND 20 02 INCHES BADOMETED NGIN

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NO. 6 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMOTER

NIA	GARA	CON	UTDA		AN C	APAC	TTTE	ä
S. P.	H. P.		$8.50 \\ 8.64$	$8.78 \\ 8.96 \\ 9.14$	$9.32 \\ 9.50 \\ 9.72$	$ \begin{array}{c} 9.94 \\ 10.2 \\ 10.7 \end{array} $	11.3 12.0 12.8	$13.9 \\ 15.1 \\ 16.4$
2 1/2" S	R.P.M.		672 665	659 652 649	644 635 632	627 624 617	614 609 607	610 614 617
ď	Н. Р.		$6.12 \\ 6.30 \\ 6.45$	$6.59 \\ 6.73 \\ 6.91$	7.06 7.24 7.42	7.63 7.85 8.39	$ \begin{array}{c} 9.00 \\ 9.86 \\ 10.8 \end{array} $	11.9 13.1 14.4
2" S.	R. P. M.		595 589 584	579 572 567	~ 564 560 554	552 549 545	544 545 547	554 559 567
s. P.	Н. Р.	5.00	5.15 5.26 5.40	5.55 5.69 5.83	$5.98 \\ 6.16 \\ 6.37$	$6.55 \\ 6.81 \\ 7.34$	8.06 8.93 9.86	$11.0 \\ 12.2 \\ 13.5 \\ 13.5 \\ 13.5 \\ 12.2 \\ 13.5 \\ $
1 3,4″ S.	R.P.M.	555	550 544 539	534 529 525	520 517 514	512 510 507	510 512 517	525 534 544
S. P.	Н. Р.	4.00 4.14	4.25 4.36 4.47	4.57 4.68 4.86	5.00 5.18 5.40	$5.62 \\ 5.87 \\ 6.52$	7.24 8.06 9.04	10.1 11.3
1 1/2"	R.P.M.	513 509	504 499 492	489 485 480	477 475 474	472 470 472	475 480 490	499 509
S. P.	Н. Р.	3.18 3.24	3.36 3.44 3.56	3.67 3.82 3.96	$4.11 \\ 4.32 \\ 4.50$	4.79 5.04 5.73	$6.45 \\ 7.31 \\ 8.24$	9.36
	R. P.M.	460 457	452 447 442	439 437 434	432 430 430	430 432 435	442 450 460	472
Ρ.	Н. Р.	2.31 2.37 2.46	$2.54 \\ 2.62 \\ 2.73 $	2.85 3.00 3.16	3.35 3.57 3.82	$\frac{4.10}{4.36}$	5.76 6.59 7.60	8.71
1″ S.	R.P.M.	410 405 400	397 392 389	387 385 385	384 385 387	389 392 400	410 419 432	442
Add for	Total Press.	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
Capacity C. Et	Air per Min.	6820 7350 7870	8400 8920 9450	9970 10500 11030	$11550 \\ 12070 \\ 12600 $	13120 13650 14700	$15750 \\ 16790 \\ 17850$	18900 19950 21000
	Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

FIC PRESSURES	
AND STATIC	TER
CAPACITIES AN	AT 70° F. AND 29.92 INCHES BAROMETER
N) CAPA	INCHES
L FAN (TYPE N) C	29.92
FAN	ANI
ONOIDAL	AT 70° F
VIAGARA CO	
NO. 7	

NGI	NEE	RING-	- B U F	FALO) FO	RGE	СОМ	PANY
S. P.	H.P.		2.83	$2.93 \\ 3.07 \\ 3.21 \\ 3.21$	3.39 3.58 3.84	4.13 4.40 4.73	5.10 5.54 6.37	7.40 8.62 10.0
S "8/L	R.P.M.		319	314 312 310	309 309 309	310 312 314	$317 \\ 320 \\ 329$	334 347 357
s. P.	Н. Р.		2.26 2.34	2.46 2.60 2.75	2.95 3.18 3.43	3.70 4.00 4.34	$\frac{4.70}{5.98}$	7.01 8.18 9.51
34" 5	R.P.M.		294 292	289 287 286	286 286 287	290 293 296	300 304 313	323 334 346
s. P.	Н. Р.		$1.73 \\ 1.81 \\ 1.91 \\ 1.91$	2.03 2.18 2.36	2.56 2.80 3.05	3.31 3.63 3.97	4.33 4.77 5.64	6.62 7.74
2%	R.P.M.		267 264 263	262 260 262	263 264 267	272 276 279	283 289 297	309 320
s. p.	Н. Р.	1.26	$ \begin{array}{c} 1.34 \\ 1.43 \\ 1.53 \end{array} $	$ \begin{array}{c} 1.68 \\ 1.83 \\ 2.02 \end{array} $	2.23 2.47 2.73	3.00 3.31 3.64	4.03 4.39 5.24	6.22 7.25
1 ² " S	R.P.M.	239	236 234 233	234 236 237	240 244 249	253 257 262	267 272 283	294 307
ď	Н. Р.	0.80 0.85 0.92	1.00 1.10 1.24	1.37 1.54 1.72	$ \begin{array}{c} 1.93 \\ 2.17 \\ 2.44 \end{array} $	2.70 3.01 3.33	3.64 4.03 4.83	5.68
3 <i>«</i> " Ş. P.	R.P.M.	207 204 204	202 203 204	206 210 214	219 223 227	233 239 244	250 256 267	282
Ū.	Н. Р.	$\begin{array}{c} 0.51 \\ 0.57 \\ 0.65 \end{array}$	$\begin{array}{c} 0.74 \\ 0.85 \\ 0.98 \end{array}$	$ \begin{array}{c} 1.12 \\ 1.29 \\ 1.49 \end{array} $	1.68 1.90 2.13	2.38 2.67 2.97	3.27 3.64 4.41	5.39
J∡" S. P.	R.P.M.	166 164 164 166	169 172 176	180 184 190	196 202 207	213 220 226	233 240 253	267
Add for	Press.	0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\\ 0.202 \end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	0.560 0.638 0.721
Capacity Cu. Ft.	Air per Min.	7140 7860 8570	9290 10000 10720	$\frac{11430}{12150}$	$\frac{13570}{14290}$ 15000	$\frac{15720}{16430}$ 17150	17860 18580 20000	21430 22860 24290
Outlet Velocity	Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

	S. P.	H. P.		11.6 11.8	12.0 12.5 12.5	12.7 12.9 13.2	13.5 13.8 14.5	15.3 16.3 17.4	18.9 20.5 22.4
	2 1/3" S	R. P. M.		576 570	564 559 556	552 544 542	537 534 529	526 520 520	523 526 529
	S. P.	H. P.		8.33 8.58 8.77	8.97 9.16 9.41	$ \begin{array}{c} 9.60 \\ 9.85 \\ 9.85 \\ 10.1 \end{array} $	10.4 10.7 11.4	12.3 13.4 14.7	16.1 17.8 19.6
	2" S	R. P. M.		510 504 500	496 490 486	483 480 474	473 470 467	466 467 469	474 479 486
	1 34" S. P.	Н. Р.	6.81	7.01 7.15 7.35	7.55 7.74 7.94	8.13 8.38 8.67		11.0 12.2 13.4	15.0 16.6 18.4
METER	1 34"	R.P.M.	476	472 466 462	457 453 450	446 443 440	439 437 434	437 439 443	450 457 466
AT 70° F. AND 29.92 INCHES BAROMETER	S. P.	Н. Р.	5.44 5.64	5.78 5.93 6.08	$6.22 \\ 6.37 \\ 6.62$	6.81 7.06 7.35	7.64 7.99 8.87	$ \begin{array}{c} 9.85 \\ 11.0 \\ 12.3 \end{array} $	13.8 15.4
	.5/1	R.P.M.	440 436	432 427 422	419 416 412	409 407 406	404 403 404	407 412 420	427 436
D 29.92	1 ½" S. P.	Н. Р.	4.33 4.41	4.58 4.68 4.85	5.00 5.39	5.59 5.88 6.13	6.52 6.86 7.79	$ \begin{array}{c} 8.77 \\ 9.95 \\ 11.2 \end{array} $	12.7
° F. AN		R.P.M.	394 392	387 383 379	376 374 372	370 369 369	369 370 373	$379 \\ 386 \\ 394$	404
AT 70	. P.	H. P.	$3.14 \\ 3.23 \\ 3.35$	3.46 3.57 3.72	3.88 4.08 4.30	$4.56 \\ 4.86 \\ 5.19$	5.59 5.93 6.81	$ \begin{array}{c} 7.84 \\ 8.97 \\ 10.3 \end{array} $	11.9
	I" S.	R.P.M.	352 347 343	340 336 333	332 330 330 330	332 332 332	333 336 343	352 359 370	379
	Add for	Press.	$\begin{array}{c} 0.106 \\ 0.122 \\ 0.141 \end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$ \begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array} $	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	$\begin{array}{c} 0.810\\ 0.900\\ 1.000\end{array}$
	Capacity Cu. Fr	Air per Min.	9290 10000 10720	$11430 \\ 12150 \\ 12860$	13570 14290 15000	15720 16430 17150	17860 18580 20000	21430 22860 24290	25720 27150 28580
		Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NO. 7 NIAGARA CONOIDAL FAN (TYPE_N) CAPACIFIES AND STATIC PRESSURES and output A NID OO 5 ----

NIAGARA CONOIDAL FAN CAPACITIES

FAN	ENC	GINEE	RING	— B U I	FFAL	O FC	RGE	COM	IPANY
NO. 8 NIADARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES At 70° F. AND 29.92 INCHES BAROMETER	7,6" S. P.	Н. Р.		3.69	3.82 4.01 4.19	4.42 4.68 5.02	$5.40 \\ 5.75 \\ 6.18$	6.66 7.23 8.32	9.66 11.3 13.1
		R. P. M.		279	275 273 271	270 270 270	271 273 275	278 280 288	293 304 313
	34" S. P.	Н. Р.		2.95 3.06	3.21 3.39 3.59	3.85 4.15 4.48	4.83 5.22 5.67	6.13 6.66 7.81	9.15 10.7 12.4
		R. P. M.		258 255	253 251 250	250 250 251	254 256 259	263 266 274	283 293 303
	§∕ 8 ″ S. P.	НР.		2.25 2.36 2.50	$2.66 \\ 2.85 \\ 3.08 \\ $	$3.34 \\ 3.66 \\ 3.98$	4.33 4.74 5.19	5.65 6.23 7.36	8.64 10.1
		R.P.M.		234 231 230	229 228 229	230 231 234	238 241 244	248 253 260	270 280
ACITIE:	<u>}</u> 4″ S. P.	Н. Р.	1.65	$1.75 \\ 1.87 \\ 2.00$	2.19 2.39 2.64	$2.91 \\ 3.23 \\ 3.56 \\ $	3.92 4.33 4.76	5.26 5.73 6.85	8.13 9.47
N) CAP		R.P.M.	209	206 205 204	205 206 208	210 214 218	221 225 229	234 238 248	258 269
(TYPE ND 29.93	3,4" S. P.	Н. Р.	$1.04 \\ 1.11 \\ 1.20 \\ 1.20$	1.31 1.44 1.61	$ \begin{array}{c} 1.79 \\ 2.01 \\ 2.25 \end{array} $	$2.52 \\ 2.83 \\ 3.18 \\ 3.18$	$3.53 \\ 3.93 \\ 4.35$	4.75 5.26 6.31	7.42
DAL FAN 70° F. Al		R. P. M.	181 179 179	176 178 179	180 184 188	191 195 199	204 209 214	219 224 234	246
CONOID	}√" S. P.	Н. Р.	.67 .74 .85	$ \begin{array}{c} .96\\ 1.11\\ 1.27 \end{array} $	1.47 1.69 1.94	2.20 2.48 2.79	$3.11 \\ 3.48 \\ 3.87 \\ 3.87 \\$	4.28 4.76 5.76	7.04
NO. 8 NIADARA (R.P.M.	145 144 145	148 150 154	$158 \\ 161 \\ 166 $	171 176 181	186 193 198	204 210 221	234
	Add for Total Press.		0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
	Capacity Cu. Ft. Air per Min.		9330 10270 11200	12130 13060 14000	$\frac{14930}{15860}$ 16800	17730 18660 19600	20530 21460 22400	$23330 \\ 24260 \\ 26130$	28000 29860 31720
	Outlet Velocity Ft. per Min.		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

NO. 8 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

NIAGARA CONOIDAL FAN CAPACITIES								s
S. P.	H. P.		15.1 15.4	15.6 15.9 16.3	16.6 16.9 17.3	17.7 18.1 19.0	20.0 21.3 22.8	24.7 26.8 29.2
2 35" 5	R.P.M.		504 499	494 489 486	483 476 474	470 468 463	460 456 455	458 460 463
S. P.	Н. Р.		10.9 11.2 11.5	11.7 12.0 12.3	12.6 12.9 13.2	13.6 14.0 14.9	16.0 17.5 19.1	21.1 23.3 25.6
2" S	R.P.M.		446 441 438	434 429 425	423 420 415	414 411 409	408 409 410	415 419 425
s. P.	H. P.	8.90	9.15 9.34 9.60	$ \begin{array}{c} 9.86 \\ 10.1 \\ 10.4 \end{array} $	10.6 11.0 11.3	11.7 12.1 13.1	14.3 15.9 17.5	19.6 21.6 24.1
1 34"	R.P.M.	416	413 408 404	400 396 394	390 388 385	384 383 380	383 384 388	394 400 408
S. P.	Н. Р.	7.10 7.36	7.55 7.74 7.94	8.13 8.32 8.64	8.90 9.22 9.60	9.98 10.4 11.6	12.9 14.3 16.1	18.0 20.2
1 35"	R. P. M.	385 381	378 374 369	366 364 360	3558 3558 355	354 353 354	356 368 368	374 381
S. P.	Н. Р.	5.65 5.76	5.98 6.11 6.33	6.53 6.78 7.04	7.30 7.68 8.00	$8.51 \\ 8.96 \\ 8.96 \\ 10.2$	11.5 13.0 14.7	16.6
1 14"	R.P.M.	345 343	339 335 331	329 328 325	324 323 323	323 324 326	331 338 345	354
ď	Н. Р.	4.10 4.22 4.37	4.51 4.66 4.86	5.06 5.33 5.61	5.96 6.35 6.78	7.30 7.74 8.90	10.2 11.7 13.5	15.5
1″ S. P.	R.P.M.	308 304 300	298 294 291	290 289 289	288 289 290	291 294 300	308 314 324	331
	Add for Total Press.		$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560\\ 0.638\\ 0.721\end{array}$	0.810 0.900 1.000
Capacity	Outlet Capacity Velocity Cu. Ft. Ft. per Min.		14930 15860 16800	17730 18660 19600	20530 21460 22400	23330 24260 26130	28000 29860 31720	33590 35460 37330
Outlet			1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

FAN	ENG	INEE	RING-	- B U F	FAL	O FO	RGE	COM	PANY
NO. 9 NIAGARA CONOIDAL FAN (TVPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	7,6" S. P.	Н. Р.		4.67	4.84 5.07 5.30	5.60 5.92 6.35	6.83 7.27 7.82	$ \begin{array}{c} 8.43 \\ 9.15 \\ 10.5 \end{array} $	12.2 14.3 16.5
		R.P.M.		248	244 242 241	240 240 240	241 242 244	247 249 256	260 270 278
	34" S. P.	Н. Р.		3.74 3.87	4.07 4.29 4.55	4.87 5.25 5.67	6.10 6.61 7.18	7.76 8.42 9.88	11.6 13.5 15.7
		R.P.M.		229	225 223 222	222 222 223	226 228 230	233 237 243	251 260 269
	5∕8″ S. P.	Н. Р.		2.85 2.99 3.16	3.36 3.60 3.90	4.23 4.64 5.04	5.47 6.00 6.56	7.15 7.88 9.30	10.9 12.8
		R.P.M.		208 206 205	203 203 203	205 206 208	211 215 217	220 224 231	240 249
	½" S. P.	Н. Р.	2.09	2.21 2.37 2.54	2.77 3.03 3.35	3.69 4.08 4.51	4.96 5.48 6.02	6.66 7.25 8.67	10.3
N) CAP INCHE		R.P.M.	186	183 182 181	182 183 185	187 190 193	197 200 203	208 211 220	229
(TYPE D 29.92	3%" S. P.	Н. Р.	$ \begin{array}{c} 1.32 \\ 1.41 \\ 1.52 \end{array} $	1.65 1.82 2.04	2.27 2.54 2.84	3.19 3.58 4.03	4.47 4.97 5.50	6.01 6.66 7.98	9.40
AL FAN P F. AN		R.P.M.	161 159 159	157 158 159	160 163 167	170 173 177	181 186 190	195 199 208	219
CONOID	∭" S. P.	Н. Р.	0.84 0.94 1.07	$1.22 \\ 1.40 \\ 1.61$	$ \begin{array}{c} 1.86 \\ 2.14 \\ 2.45 \end{array} $	2.78 3.14 3.52	$3.93 \\ 4.41 \\ 4.90$	5.41 6.02 7.28	8.91
NO. 9 NIAGARA C		R. P. M.	129 128 129	131 133 137	140 143 148	152 157 161	166 171 176	181 187 197	208
	Add for Total Press.		0.063 0.076 0.090	0.106 0.122 0.141	0.160 0.180 0.202	0.225 0.250 0.275	0.302 0.330 0.360	0.390 0.422 0.489	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
	Capacity Cu. Ft. Air per Min.		11810 12990 14170	15360 16530 17720	$\frac{18900}{20080}$ 21250	22440 23620 24800	$25980 \\ 27160 \\ 28340$	29520 30710 33070	35430 37790 40150
	Outlet Velocity Ft. per Min.		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

PRESSURES	
STATIC F	9
ANI	ADOMETE
SILVING CAPACITIES	C RADO
CAP	BHUN
Z	Ē
TYPE	20 02
FAN (AND
CONOIDAL	AT 70° E AND 20 02 INCHES B
NIAGARA C	
0	
N0.	

NIA	GARA	CON	OIDA	L FA	N C	A P A C	ITIE	S
s. P.	H. P.		19.1 19.4	19.8 20.2 20.6	21.0 21.4 21.9	22.4 22.8 24.0	25.4 27.0 28.8	31.3 33.9 36.9
2 35"	R.P.M.		448 443	439 435 432	429 423 421	418 416 411	409 406 405	407 409 411
ď	Н. Р.		13.8 14.2 14.5	14.8 15.2 15.6	$15.9 \\ 16.3 \\ 16.7$	$17.2 \\ 17.7 \\ 18.9$	20.3 22.2 24.2	26.7 29.5 32.4
2" S. P.	R.P.M.		397 392 389	386 381 378	376 373 369	368 366 363	362 363 364	369 372 378
S. P.	Н. Р.	11.3	11.6 11.8 12.2	12.5 12.8 13.1	13.4 13.7 14.3	$14.8 \\ 15.3 \\ 16.5$	$ \begin{array}{c} 18.2 \\ 20.1 \\ 22.2 \\ \end{array} $	24.8 27.4 30.5
13.4"	R. P.M.	370	367 362 359	356 352 350	347 344 342	341 340 338	340 341 344	350 356 362
S. P.	Н. Р.	8.99 9.31	$ \begin{array}{c} 9.56 \\ 9.80 \\ 10.0 \end{array} $	10.3 10.5 10.9	11.3 11.7 12.2	12.6 13.2 14.7	16.3 18.1 20.3	22.8 25.5
1 35"	R.P.M.	342 339	336 332 328	326 323 320	318 317 316	314 313 314	317 320 327	332 339
1 yé" S. P.	H. P.	7.15	7.57 7.73 8.01	8.26 8.59 8.91	$9.23 \\ 9.72 \\ 10.1$	10.8 11.3 12.9	14.5 16.4 18.6	21.1
1 34"	R.P.M.	307 304	301 298 294	292 291 289	288 287 287	287 288 290	294 300 307	314
a.	Н. Р.	5.18 5.34 5.53	5.71 5.90 6.15	6.41 6.74 7.10	7.54 8.04 8.59	9.23 9.80 11.3	13.0 14.8 17.1	19.6
1" S.	R.P.M.	273 270 267	264 261 259	258 257 257	256 257 258	259 261 267	273 279 288	294
Add for	Total Press.	0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	0.390 0.422 0.489	0.560 0.638 0.721	0.810 0.900 1.000
Capacity C. Er	Air per Min.	15360 16530 17720	18900 - 20080 21250	22440 23620 24800	25980 27160 28340	29520 30710 33070	35430 37790 40150	42510 44880 47240
	Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

FAN	ENGI	NEE	RING	— B U I	FAL	O FO	RGE	СОМ	PANY
	7,8" S. P.	Н. Р.		5.77	5.97 6.26 6.55	6.91 7.31 7.84	8.43 8.98 9.65	10.4 11.3 13.0	15.1 17.6 20.4
		R. P. M. H. P.		223	220 218 217	$216 \\ 216 \\ 216 \\ 216$	217 218 220	222 224 230	234 243 250
RES	Ч.	Н. Р.		4.61 4.78	5.02 5.30 5.61	$\begin{array}{c} 6.01 \\ 6.48 \\ 7.00 \end{array}$	$7.54 \\ 8.16 \\ 8.86 \\ 8.86$	$ \begin{array}{c} 9.58 \\ 10.4 \\ 12.2 \end{array} $	$14.3 \\ 16.7 \\ 19.4$
PRESSU	3⁄4" S. P.	R. P. M.		206 204	201 201 200	200 201 201	203 205 207	210 213 219	226 234 242
TATIC I	S. P.	Н. Р.		3.52 3.69 3.90	4.15 4.45 4.81	$5.22 \\ 5.72 \\ 6.22 \end{cases}$	6.76 7.40 8.10	8.83 9.73 11.5	13.5 15.8
N) CAPACITIES AND STATIC PRESSURES INCHES BAROMETER	5 ⁸ " S	R. P. M.		187 185 184	183 182 183	184 185 187	190 193 195	198 202 208	216 224
N) CAPACITIES AND INCHES BAROMETER	. L	Н. Р.	2.58	2.73 2.92 3.13	$3.42 \\ 3.74 \\ 4.13 $	4.55 5.04 5.56	6.12 6.76 7.43	$^{8.22}_{8.95}_{10.7}$	12.7 14.8
N) CAP.	<u>}∕</u> 2" S. P.	R.P.M.	167	$165 \\ 164 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 163 \\ 164 $	$\begin{array}{c}164\\165\\166\end{array}$	168 171 174	177 180 183	187 190 198	206 215
(TYPE) 29.92	S. P.	Н. Р.	$ \begin{array}{c} 1.63 \\ 1.74 \\ 1.87 \end{array} $	2.04 2.25 2.52	2.80 3.14 3.51	3.94 4.42 4.97	5.51 6.14 6.79	$7.42 \\ 8.22 \\ 9.85$	11.6
AL FAN (³ /" S. I	R.P.M.	145 143 143	141 142 143	144 147 150	153 156 159	163 167 171	175 179 187	197
AT 70°	S. P.	Н. Р.	$1.04 \\ 1.16 \\ 1.32 $	$1.50 \\ 1.73 \\ 1.99 \\ $	2.29 2.64 3.03	3.43 3.88 4.35	4.85 5.44 6.05	6.68 7.43 8.99	11.0
GARA C	14" S	R.P.M.	116 115 116	118 120 123	126 129 133	137 141 145	149 154 158	163 168 177	187
NO. 10 NIAGARA CONOIDAL FAN (TYPE AT 70° F. AND 29.92	Add for Total	Press.	0.063 0.076 0.090	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
Z	Capacity Cu. Ft.	per Min.	14580 16040 17500	$\frac{18960}{20410}\\21870$	23330 24790 26240	$\begin{array}{c} 27700\\ 29160\\ 30620 \end{array}$	$32080 \\ 33540 \\ 34990$	$36450 \\ 37910 \\ 40830$	43740 46660 49570
	Outlet Velocity Et port	Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

	S. P.	Н. Р.		23.6 24.0	24.4 24.9 25.4	25.9 26.4 27.0	27.6 28.2 29.6	31.3 33.3 35.6	38.6 41.8 45.6
	. "źł Z	R. P. M.		403 399	395 391 389	386 381 379	376 374 370	368 365 364	366 368 370
	S. P.	н. Р.		17.0 17.5 17.9	18.3 18.7 19.2	$19.6 \\ 20.1 \\ 20.6 \\ 20.6 \\ 19.6 \\ 20.6 \\ $	21.2 21.8 23.3	$25.0 \\ 27.4 \\ 29.9$	32.9 36.4 40.0
	5"	R. P. M.		357 353 350	347 343 340	338 336 332	331 329 327	326 327 328	332 335 340
	S. P.	Н. Р.	13.9	$14.3 \\ 14.6 \\ 15.0 $	$15.4 \\ 15.8 \\ 16.2 \\ 16.2 \\ 1$	$16.6 \\ 17.1 \\ 17.7 \\ 17.7 \\ 117.7 \\ $	$ \begin{array}{c} 18.2 \\ 18.9 \\ 20.4 \end{array} $	22.4 24.8 27.4	30.6 33.8 37.6
METER	1 34"	R. P. M.	333	330 326 323	320 317 315	312 310 308	307 306 304	306 307 310	315 320 326
F. AND 29.92 INCHES BAROMETER	S. P.	Н. Р.	11.1 11.5	11.8 12.1 12.4	12.7 13.0 13.5	$13.9 \\ 14.4 \\ 15.0 $	15.6 16.3 18.1	$20.1 \\ 22.4 \\ 25.1$	28.1 31.5
INCHE	1 1/2"	R. P. M.	308 305	302 299 295	29 3 291 288	286 285 284	283 283 283	285 288 294	299 305
D 29.92	S. P.	Н. Р.	8.83 9.00	9.34 9.54 9.89	10.2 10.6 11.0	$11.4 \\ 12.0 \\ 12.5 \\ $	13.3 14.0 15.9	17.9 20.3 22.9	26.0
)° F. AN	1 34"	R. P. M.	276 274	271 268 265	263 262 260	259 258 258	258 259 261	265 270 276	283
AT 70°	S. P.	Н. Р.	6.40 6.59 6.83	7.05 7.28 7.59	7.91 8.32 8.77	9.31 9.92 10.6	11.4 12.1 13.9	16.0 18.3 21.1	24.2
	1.	R.P.M.	246 243 240	238 235 233	232 231 231	230 231 232	233 235 240	246 251 259	265
	Add for Total	Press.	0.106 0.122 0.141	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
	Capacity Cu. Ft.	per Min.	18960 20410 21870	$23330 \\ 24790 \\ 26240 $	27700 29160 30620	32080 33540 34990	$36450 \\ 37910 \\ 40830$	43740 46660 49570	52490 55400 58320
	Outlet Velocity Fr. ner	Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NO. 10 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES

	EINC	JINCE	RING	- B U F	FAL	0 F 0	RGE	COM	PANY
	s. P.	Н. Р.	[6.98	$7.22 \\ 7.58 \\ 7.93 \\$	8.36 8.85 9.49	10.2 10.9 11.7	$12.6 \\ 13.7 \\ 15.7 $	$ \begin{array}{c} 18.3 \\ 21.3 \\ 24.7 \end{array} $
	7/8" S	R.P.M.		203	200 198 197	196 196 196	197 198 200	202 204 209	213 221 227
ES	.P.	Н. Р.		5.58 5.78	$\begin{array}{c} 6.08 \\ 6.41 \\ 6.79 \end{array}$	7.27 7.84 8.87	$^{9.12}_{9.87}_{10.7}$	11.6 12.6 14.8	$17.3 \\ 20.2 \\ 23.5$
RESSUR	34″ S. P.	R.P.M.		187 186	184 183 182	182 182 183	185 186 188	191 194 199	206 213 220
(TYPE N) CAPACITIES AND STATIC PRESSURES 29.92 INCHES BAROMETER	S. P.	H. P.		4.26 4.47 4.72	5.02 5.39 5.82	$6.32 \\ 6.92 \\ 7.53$	8.18 8.95 9.80	10.7 11.8 13.9	16.3 19.1
LETER	5%" S	R.P.M.		170 168 167	166 166 166	167 168 170	173 176 177	180 184 189	196 204
BAROM	S. P.	H. P.	3.12	3.30 3.53 3.79	4.14 4.53 5.00	$5.51 \\ 6.10 \\ 6.73$	7.41 8.18 8.99	9.95 10.8 13.0	15.4 17.9
N) CAP INCHES	32" 2	R. P. M.	152	150 149 148	149 150 151	$153 \\ 156 \\ 158 \\ 158 \\ .$	161 164 166	170 173 180	187 196
	3 ₈ " S. P.	Н. Р.	$ \begin{array}{c} 1.97 \\ 2.11 \\ 2.26 \end{array} $	2.47 2.72 3.05	3.39 3.80 4.25	4.77 5.35 6.01	6.67 7.43 8.22	8.98 9.95 11.9	14.0
AL FAN F. AND	3/11	R.P.M.	132 130 130	128 129 130	131 134 136	139 142 145	148 152 156	159 163 170	179
AT 70°	S. P.	Н. Р.	$1.26 \\ 1.40 \\ 1.60$	$1.82 \\ 2.09 \\ 2.41$	2.77 3.20 3.67	$\begin{array}{c} 4.15 \\ 4.70 \\ 5.26 \end{array}$	5.87 6.58 7.32	8.08 8.99 10.9	13.3
NUARA	34"	R.P.M.	106 105 106	107 109 112	115 117 121	125 128 132	136 140 144	148 153 161	170
NO. II NIAUAKA CONOIDAL FAN AT 70° F. AND	Add for	Total Press.	0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	0.225 0.250 0.275	0.302 0.330 0.360	0.390 0.422 0.489	0.560 0.638 0.721
Z	Capacity	Air per Min.	$\frac{17640}{19410}$ 21170	$22930 \\ 24700 \\ 26460 \\ 2640 \\ 26460 \\ 26460 \\ 2640 \\ 2640 \\ 26460 \\ 2640 \\ 26$	$28230 \\ 29990 \\ 31750$	33520 35280 37050	$38810 \\ 40580 \\ 42340$	$\begin{array}{c} 44100 \\ 45870 \\ 49400 \end{array}$	52910 56450 59980
1	Outlet	Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

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NIAGARA	
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	NIA	GARA	CONC	IDA	L FA	N C A	PAC	TIES	3
	S. P.	H. P.		28.6 29.0	29.5 30.1 30.7	31.3 32.0 32.7	33.4 34.1 35.8	37.9 40.3 43.1	46.7 50.6 55.2
	2 1/2" S	R.P.M.		366 363	359 356 354	351 346 345	342 340 336	335 332 331	333 335 336
	. P.	Н. Р.		20.6 21.2 21.7	22.2 22.6 23.2	23.7 24.3 24.9	25.7 26.4 28.2	30.3 33.2 36.2	39.8 44.1 48.4
	2" S.	R. P. M.		325 321 318	316 312 309	307 306 302	301 299 297	296 297 248	302 305 309
	S. P.	Н. Р.	16.8	$17.3 \\ 17.7 \\ 18.2$	18.6 19.1 19.6	20.1 20.7 21.4	22.0 22.9 24.7	27.1 30.0 33.2	37.0 40.9 45.5
	1 34"	R.P.M.	303	300 296 294	$291 \\ 288 \\ 286 $	284 282 280	279 278 276	278 279 282	286 291 296
L' VIND 27:74 INCHES DUVOILLEN	S. P.	Н. Р.	$13.4 \\ 13.9$	$14.3 \\ 14.7 \\ 15.0 $	$15.4 \\ 15.7 \\ 16.3 \\ 16.3$	$16.8 \\ 17.4 \\ 18.2$	$ \begin{array}{c} 18.9 \\ 19.7 \\ 21.9 \end{array} $	24.3 27.1 30.4	34.0 38.1
	1 1/3"	R.P.M.	280 277	$275 \\ 272 \\ 268 $	265 265 262	260 259 258	257 256 257	259 262 267	272 277
44.44 0	l \v_" S. P.	Н. Р.	10.7 10.9	11.3 11.6 12.0	12.4 12.8 13.3	13.8 14.5 15.1	16.1 17.0 19.2	21.7 24.6 27.7	31.5
	114"	R.P.M.	251 249	246 244 241	239 238 236	236 235 235	235 236 237	241 246 251	257
N/ IV	.P.	Н. Р.	7.74 7.97 8.26	$ \begin{array}{c} 8.53 \\ 8.81 \\ 9.18 \\ \end{array} $	9.57 10.1 10.6	11.3 12.0 12.8	13.8 14.6 16.8	19.4 22.1 25.5	29.3
	1″ S.	R.P.M.	224 221 218	216 214 212	211 210 210	209 210 211	212 214 218	224 228 236	241
	Add for	Total Press.	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
	Capacity	cu. Ft. Air per Min.	22930 24700 26460	28230 29990 31750	33520 35280 37050	38810 40580 42340	44100 45870 49400	52910 56450 59980	63510 67030 70560
		Velocity Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

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76" S. P.	H. P.		8.31	8.60 9.02 9.43	9.95 10.5 11.3	12.2 12.9 13.9	15.0 16.3 18.7	21.8 25.4 29.4
S #%1	R. P. M.		186	183 182 181	180 180 180	181 182 183	185 187 192	195 203 208
34" S. P.	Н. Р.		6.64 6.88	7.23 7.63 8.08	$ \begin{array}{c} 8.66 \\ 9.33 \\ 9.33 \\ 10.1 \end{array} $	10.9 11.8 12.8	13.8 15.0 17.6	20.6 24.1 27.9
1. J. C.	R.P.M.		172 170	168 168 167	167 167 168	169 171 173	175 178 183	188 195 202
s. P.	Н. Р.		5.07 5.31 5.62	5.98 6.41 6.93	7.52 8.24 8.96	$ \begin{array}{c} 9.74 \\ 10.7 \\ 11.7 \end{array} $	$12.7 \\ 14.0 \\ 16.6$	19.5 22.8
METER	R. P. M.		156 154 153	153 152 153	153 154 156	158 161 163	165 168 173	180 187
1NCHES BAROMETER 1/2" S. P.	Н. Р.	3.72	3.93 4.21 4.51	4.93 5.39 5.95	$6.55 \\ 7.26 \\ 8.01$	$ \begin{array}{c} 8.81 \\ 9.74 \\ 10.7 \end{array} $	11.8 12.9 15.4	18.3 21.3
	R.P.M.	139	138 137 136	137 138 138	140 143 145	148 150 153	156 158 165	172 179
4D 29.92 S. P.	H. P.	2.35 2.51 2.69	2.94 3.24 3.63	4.03 4.52 5.06	5.67 6.37 7.16	7.94 8.84 9.78	10.7 11.8 14.2	16.7
AT 70° F. AND P. 3%" S.	R.P.M.	121 119 119	118 118 119	120 123 125	128 130 133	136 139 143	146 149 156	164
AT 70 14" S. P.	H. P.	1.50 1.67 1.90	2.16 2.49 2.87	3.30 3.80 4.36	4.94 5.59 6.27	6.99 7.83 8.71	9.62 10.7 13.0	15.9
M"	R. P. M.	97 96 97	98 100 103	105 108 111	114 118 121	124 128 132	136 140 148	156
	Add for Total Press.	0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	0.225 0.250 0.275	0.302 0.330 0.360	0.390 0.422 0.489	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
	Capacity Cu. Ft. Air per Min.	21000 23090 25190	$27290 \\ 29390 \\ 31490$	33600 35690 37790	$39890 \\ 41990 \\ 44090$	46190 48290 50390	52490 54590 58790	62980 67180 71380
	Uutlet Velocity Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

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Add for Air Add for Posal Add for Air Press R. P. M. Per Min. Press R. P. M. 27290 0.1105 205 9.22 23600 0.1122 203 9.29 33600 0.1122 203 9.49 33600 0.1160 196 102 33690 0.2225 193 10.4 39890 0.2225 193 10.5 39890 0.2255 193 11.4 41990 0.275 193 11.4 44090 0.2330 193 12.6 45390 0.2365 193 12.6 45390 0.3300 193 14.3 53490 0.3300 193 14.3 53490 0.4422 194 16.4 534500 0.4422 196 17.4 534500 0.5560 205 23.0 53400 0.5560 2050 23.0	R.P.M. 1 230 228 228 228 228 228 228 228 228 228 22	R. P. M. H.			2" S.	S. P.	2 1/2" 5	S. P.
0.106 0.1122 0.1122 0.1122 0.1122 0.1120 0.1120 0.1120 0.1120 0.1120 0.1120 0.1100 0.1100 1.141 0.1202 1.194 1.193 1.1	230 228 221 221 221		H. P. R. P.M.	A. H. P.	R. P. M.	Н. Р.	R. P. M. H. P.	Н. Р.
0.160 198 0.150 198 0.225 194 0.225 193 0.225 193 0.226 193 0.269 193 0.330 193 0.330 194 0.423 194 0.423 196 0.443 200		257 16 254 16	16.0 16.6 278	20.0				
0.225 193 0.256 193 0.275 193 0.2302 192 0.330 193 0.380 194 0.459 194 0.459 200 0.560 200		252 17 249 17 246 17	17.0 275 17.4 272 17.9 269	20.6 21.0 21.6	298 294 292	24.5 25.2 25.8	336 333	34.0 34.6
0.302 192 0.330 193 0.330 193 0.330 194 0.422 196 0.455 200	218 15.3 217 15.8	244 18 243 18 240 19	18.3 267 18.7 264 19.5 263	22.2 22.8 23.3	289 286 283	$26.4 \\ 26.9 \\ 27.7$	329 326 324	$35.1 \\ 35.9 \\ 36.6$
0.390 194 0.422 196 0.489 200 0.560 205 0.638 205	216 16.4 215 17.3 215 18.0	238 20 238 20 237 21	20.0 260 20.7 258 21.6 257	23.9 24.6 25.5	282 280 277	$28.2 \\ 29.0 \\ 29.7 \\ $	322 318 316	$\frac{37.3}{38.9}$
0.560 205 0.638 209	215 19.2 216 20.2 218 22.9	236 235 236 236 236 26	22.5 256 23.5 255 26.1 255	26.2 27.2 29.4	276 274 273	30.5 31.4 33.6	313 312 308	39.8 40.6 42.6
0.721 216	221 25.8 225 29.2 230 33.0	238 29 240 32 245 36	29.0 255 32.3 256 36.2 258	32.3 35.7 39.5	272 273 273	$36.0 \\ 39.5 \\ 43.1$	307 304 303	45.1 48.0 51.3
75580 0.810 221 34.9 79780 0.900 1.000 83980 1.000	236 37.5	249 40 254 45	40.5 263 45.4 267 272	44.1 48.7 54.2	277 279 283	47.4 52.4 57.6	305 307 308	$55.6 \\ 60.2 \\ 65.7 \\ $

NO. 12 NIAGADA CONDIDAT EAN (TVDE N) CADACITIES AND STATIC DDESSIDES

utlet	Capacity	A 4.4 600	14" S	S. P.	3%" S. P.	. P.	1/2" 5	S. P.	58" 5	S. P.	34" S. P.	Ŀ.	7,8" S	S. P.
Velocity Ft. per Min.	Cu. Ft. Air per Min.	Total Total Press.	R. P. M.	Н. Р.	R.P.M.	H. P.	R. P. M.	Н. Р.	R. P. M.	H. P.	R. P. M.	Н. Р.	R.P.M.	Н. Р.
1000	24650 27110 29570	0.063 0.076 0.090	8 8 8 8	$ \begin{array}{c} 1.76 \\ 1.96 \\ 2.23 \end{array} $	112 110 110	2.76 2.94 3.16	129	4.36						
1300	32040 34500 36960	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	91 92 95	$2.54 \\ 2.92 \\ 3.36$	100 1109 110	3.45 3.80 4.26	127 126 125	$4.61 \\ 4.94 \\ 5.29$	144 142 142	5.95 6.24 6.59	159 157	7.79 8.08	172	9.75
1500	39430 41900 44350	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	97 99 102	3.87 4.46 5.12	111 113 115	4.73 5.31 5.93	126 127 128	5.78 6.32 6.98	141 140 141	$7.01 \\ 7.52 \\ 8.13$	156 155 154	8.48 8.96 9.48	169 168 167	10.1 10.6 11.1
1900 2000 2100	46810 49280 51740	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	105 109 112	5.80 6.56 7.35	118 120 122	6.66 7.47 8.40	129 132 134	$7.69 \\ 8.52 \\ 9.40$	142 142 144	$^{8.82}_{9.67}_{10.5}$	154 154 155	10.2 11.0 11.8	166 166 166	11.7 12.4 13.3
2200 2300 2400	54210 56680 59130	0.302 0.330 0.360	115 119 122	$ \begin{array}{c} 8.20 \\ 9.19 \\ 10.2 \end{array} $	125 129 132	$ \begin{array}{c} 9.31 \\ 10.4 \\ 11.5 \end{array} $	136 139 141	10.4 11.4 12.6	146 149 150	11.4 12.5 13.7	156 158 159	12.8 13.8 15.0	167 168 169	14.3 15.2 16.3
2500 2600 2800	61600 64060 69000	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	125 129 136	11.3 12.6 15.2	135 138 144	12.6 13.9 16.7	144 146 152	13.9 15.1 18.1	152 156 160	14.9 16.5 19.4	162 164 169	$16.2 \\ 17.6 \\ 20.6$	171 172 177	$17.6 \\ 19.1 \\ 22.0 \\ 22.0 \\ 17.6 \\ 19.1 \\ 22.0 \\ 10.1 \\ $
3000 3200 3400	73920 78850 83770	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	144	18.6	152	19.6	$159 \\ 166$	21.5 25.0	166 172	22.8 26.7	174 180 186	24.2 28.2	180 187	25.5 29.8 24.8

NO. 13 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES

AT 70° F. AND 29.92 INCHES BAROMETER

S. P.	Н. Р.		39.9 40.6	41.2 42.1 42.9	43.8 44.6 45.6	46.7 47.7 50.0	52.9 56.3 60.2	65.2 70.6 77.1
2 1/2"	R.P.M.		310 307	304 301 299	297 293 292	289 289 285	283 281 280	282 283 285
. P.	Н. Р.		28.7 29.6 30.3	$30.9 \\ 31.6 \\ 32.5$	$33.1 \\ 34.0 \\ 34.8 \\ $	35.8 36.8 39.4	42.3 46.3 50.5	55.6 61.5 67.6
3" S.	R.P.M.		275 272 269	267 264 262	260 259 255	255 253 252	251 252 252	255 258 262
34" S. P.	Н. Р.	23.5	$24.2 \\ 24.7 \\ 25.4$	26.0 26.7 27.4	28.1 28.9 29.9	30.8 31.9 34.5	37.9 41.9 46.3	51.7 57.1 63.5
n *ć 1	R.P.M.	256	254 251 249	246 244 242	240 239 237	236 235 234	235 236 239	$242 \\ 246 \\ 251 \\ 251 \\$
S. P.	H. P.	18.8 19.4	20.0 20.5 21.0	21.5 22.0 22.8	23.5 24.3 25.4	26.4 27.6 30.6	34.0 37.9 42.4	47.5 53.2
1 1/2"	R.P.M.	237 235	232 230 227	225 224 222	220 219 219	218 217 218	219 222 226	230 235
l t ₄ " S. P.	Н. Р.	14.9 15.2	15.8 16.1 16.7	$17.2 \\ 17.9 \\ 18.6$	$ \begin{array}{c} 19.3 \\ 20.3 \\ 21.1 \end{array} $	23.5 23.7 26.9	30.3 34.3 38.7	44.0
"F1 I	R.P.M.	212 211	209 206 204	202 202 202	199 199 199	199 199 201	204 208 212	218
1" S. P.	Н. Р.	10.8 11.1 11.6	11.9 12.3 12.8	13.4 14.1 14.8	15.7 16.8 17.9	$ \begin{array}{c} 19.3 \\ 20.5 \\ 23.5 \end{array} $	27.0 30.9 35.7	40.9
	R. P. M.	189 187 185	183 181 179	179 178 178	177 178 179	179 181 185	189 193 199	204
Add for Total	Press.	0.106 0.122 0.141	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	0.225 0.250 0.275	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
Capacity Cu. Ft.	per Min.	32040 34500 36960	39430 41900 44350	46810 49280 51740	54210 56680 59130	61600 64060 69000	73920 78850 83770	88700 93620 98560
Outlet Velocity	Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

1	<u>a</u> :	Н. Р.		11.3	11.7 12.3 12.8	$13.6 \\ 14.3 \\ 15.4$	16.5 17.6 18.9	20.4 22.2 25.5	29.6 34.5 40.0
	7,% S. P.	R.P.M.		159	157 156 155	$154 \\ 154 $	155 156 157	159 160 164	167 174 179
RES	. P.	Н. Р.		9.04 9.37	$ \begin{array}{c} 9.84 \\ 10.4 \\ 11.0 \end{array} $	$11.8 \\ 12.7 \\ 13.7$	$14.8 \\ 16.0 \\ 17.4$	$ \begin{array}{c} 18.8 \\ 20.4 \\ 23.9 \end{array} $	28.0 32.7 38.0
RESSUI	^{3,4} " S. P.	R.P.M.		147 146	144 144 143	143 143 144	145 147 148	150 152 157	162 167 173
TATIC H	5, ⁸ S. P.	Н. Р.		6.90 7.23 7.65	8.14 8.72 9.43	$10.2 \\ 11.2 \\ 12.2 \\ $	$13.3 \\ 14.5 \\ 15.9$	$17.3 \\ 19.1 \\ 22.6$	26.5 31.0
, FAN (TVPE N) CAPACITIES AND ST F. AND 29.92 INCHES BAROMETER	18/1	R.P.M.		$134 \\ 132 \\ 132 \\ 132$	131 130 131	132 132 134	136 138 139	142 144 149	154 160
ACITIES ES BARG	½" S. P.	Н. Р.	5.06	5.35 5.72 6.14	$6.70 \\ 7.33 \\ 8.10$	$ \begin{array}{c} 8.92 \\ 9.88 \\ 10.9 \end{array} $	12.0 13.3 14.6	$16.1 \\ 17.6 \\ 21.0 \\ 21.0 \\ 21.0 \\ 31.0 \\ $	24.9 29.0
N) CAP.	<u>}</u>	R.P.M.	119	118 117 117	117 118 119	120 122 124	127 129 131	$134 \\ 136 \\ 142 $	147 154
(TYPE VD 29.92	_{3%} " S. P.	Н. Р.	$3.20 \\ 3.41 \\ 3.67$	4.00 4.41 4.94	$5.49 \\ 6.16 \\ 6.88$	$\begin{array}{c} 7.72 \\ 8.66 \\ 9.74 \end{array}$	$10.8 \\ 12.0 \\ 13.3 \\ 13.3 \\ 12.0 \\ $	14.6 16.1 19.3	22.7
IDAL FAN 70° F. AN	3."	R.P.M.	104 102 102	101 102 102	103 105 107	109 112 114	117 119 122	125 128 134	141
CONOID AT 70	14" S. P.	Н. Р.	2.04 2.27 2.59	$2.94 \\ 3.39 \\ 3.90 \\$	$ \begin{array}{r} 4.49 \\ 5.18 \\ 5.94 \\ \end{array} $	$6.72 \\ 7.61 \\ 8.53$	$ \begin{array}{c} 9.51 \\ 10.7 \\ 11.9 \end{array} $	13.1 14.6 17.6	21.6
NGARA	14"	R.P.M.	83 83 83 83	86 86 88 88	90 92 95	98 101 104	107 110 113	117 120 127	134
NO. 14 NIAGARA CONOIDAL FAN (TYPEN) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	Add for Total	Press.	0.063 0.076 0.090	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\\ 0.141 \end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.432 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
Z	Capacity Cu. Ft.	per Min.	$28680 \\ 31440 \\ 34290$	$37150 \\ 40000 \\ 42860$	$\begin{array}{c} 45720 \\ 48580 \\ 51420 \end{array}$	54290 57150 60010	62880 65720 68580	71430 74290 80010	85730 91440 97150
	Outlet Velocity	Ain.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

PRESSURES	
STATIC	
CAPACITIES AND	BAROMETER
N) CAPAC	INCHES E
(TYPE	29.92
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CONOIDAL	AT 70° I
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I* S. P. R. P. M. H. P. I70 122.6 I71 122.6 I70 13.3 I66 15.5 I65 14.9 I66 15.5 I65 12.0 I66 15.5 I66 15.5 I65 15.5 I66 15.5 I67 23.7 I67 22.4 I67 22.4 I67 23.7 I67 22.4 I67 23.7 I77 35.9 I78 35.9 I78 35.4 I78 35.4

FAN	ENG	INEER	I N G —	BUF	FALC	FO	RGE	COM	PANY
	S. P.	Н.Р.		13.0	13.4 14.1 14.7	15.6 16.5 17.7	19.0 20.2 21.7	23.4 25.4 29.3	34.0 39.6 45.9
NO. IS NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	7/8" S.	R. P.M.		149	147 145 145	144 144 144	145 145 147	148 149 153	156 162 167
	S. P.	Н. Р.	-	10.4 10.8	11.3 11.9 12.6	13.5 14.6 15.8	17.0 18.4 19.9	21.6 23.4 27.5	32.2 37.6 43.7
	3.4.5.6	R.P.M.		137 136	135 134 133	133 133 134	135 137 138	140 142 146	151 156 161
	5,8" S. P.	Н. Р.		7.92 8.30 8.78	$9.34 \\ 10.0 \\ 10.8 \\ $	11.8 12.9 14.0	15.2 16.7 18.2	19.9 21.9 25.9	30.4 35.6
		R.P.M.		125 123 123	122 121 122	123 123 125	127 129 130	132 135 139	144 149
	}≦" S. P.	Н. Р.	5.81	6.14 6.57 7.04	7.70 8.42 9.29	$10.2 \\ 11.4 \\ 12.5$	$13.8 \\ 15.2 \\ 16.7 $	$ \begin{array}{c} 18.5 \\ 20.1 \\ 24.1 \\ \end{array} $	28.6 33.3
		R. P. M.	111	110 109 109	100 111 111	112 114 116	118 120 122	125 127 132	137
	3,8" S. P.	Н. Р.	3.67 3.92 4.21	4.59 5.06 5.67	6.30 7.07 7.90	8.87 9.95 11.2	12.4 13.8 15.3	$ \begin{array}{c} 16.7 \\ 18.5 \\ 22.2 \end{array} $	26.1
DNOIDAL FAN (TYPE AT 70° F. AND 29.92		R. P. M.	97 95 95	94 95 95	96 98 100	102 104 106	109 111 114	117 119 125	131
CONOID. AT 70	S. P.	Н. Р.	2.34 2.61 2.97	3.38 3.89 4.48	5.15 5.94 6.82	7.72 8.73 9.79	10.9 12.2 13.6	$ \begin{array}{c} 15.0 \\ 16.7 \\ 20.2 \end{array} $	24.8
). IS NIAGARA C	Man 5	R. P. M.	77 77	79 80 82	84 86 89	91 94 97	99 103 105	109 112 118	125
	A44 600	Add for Total Press.		$\begin{array}{c} 0.106 \\ 0.122 \\ 0.141 \end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	0.225 0.250 0.275	0.302 0.330 0.360	$0.390 \\ 0.432 \\ 0.489$	0.560 0.638 0.721
Ň.	Canacity	Cu. Ft. Air per Min.	32800 36080 39360	42650 45920 49210	52490 55760 59040	62320 65610 68900	72160 75450 78720	82010 85300 91850	98420 104970 111520
	Outlet	Velocity Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

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	s. P.	Н. Р.		53.1 54.0	54.9 56.0 57.2	58.3 59.4 60.8	62.1 63.5 66.6	70.4 74.9 80.1	86.9 94.1 102.6
NO. 15 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	2 1/2"	R.P.M.		269 266	263 261 259	257 254 253	251 249 247	245 243 243	244 245 247
	S. P.	H. P.		38.3 39.4 40.3	41.2 42.1 43.2	44.1 45.2 46.4	47.7 49.1 52.4	56.3 61.7 67.3	74.0 81.9 90.0
	5"	R.P.M.		238 235 233	231 229 227	225 224 221	221 219 218	217 218 219	221 223 227
	S. P.	Н. Р.	31.3	32.2 32.9 33.8	34.7 35.6 36.5	37.4 38.5 39.8	41.0 42.5 45.9	50.4 55.8 61.7	68.9 76.1 84.6
	134	R. P. M.	222	220 217 215	213 211 210	208 207 205	205 204 203	204 205 207	210 213 217
	s. P.	Н. Р.	25.0 25.9	26.6 27.2 27.9	28.6 29.3 30.4	31.3 32.4 33.8	$35.1 \\ 36.7 \\ 40.7$	45.2 50.4 56.5	63.2 70.9
	1 1.2"	R. P. M.	205 203	201 199 197	195 194 192	191 190 189	189 188 189	190 192 196	199 203
	I ½"S. P.	Н. Р.	19.9 20.3	21.0 21.5 22.3	23.0 23.9 24.8	25.7 27.0 28.1	29.9 31.5 35.8	40.3 45.7 51.5	58.5
D° F. AN	5X.1	R.P.M.	184 183	181 179 177	175 175 173	173 172 172	172 173 174	177 180 184	189
AGARA CONOIDA AT 70°	S. P.	Н. Р.	14.4 14.8 15.4	$15.9 \\ 16.4 \\ 17.1$	17.8 18.7 19.7	21.0 22.3 23.8	25.7 27.2 31.3	$ \begin{array}{r} 36.0 \\ 41.2 \\ 47.5 \end{array} $	54.5
	2	R.P.M.	164 162 160	159 157 155	155 154 154	153 154 155	155 157 160	164 167 173	177
10. 15 NI	Add for Total	Add for Total Press.		$\begin{array}{c} 0.160\\ 0.180\\ 0.202\\ 0.202 \end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$ \begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array} $	0.560 0.638 0.721	0.810 0.900 1.000
2	Capacity Cu. Ft. Air	per Min.	42650 45920 49210	52490 55760 59040	62320 65610 68900	72160 75450 78720	82010 85300 91850	98420 104970 111520	118100 124650 131210
	Outlet Velocity Ft. per	Min.	1300 1400 1500	1600 1700 1800	-1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

FAN	ENGI	NEEH	RING-	– B U F	FALO) FO	RGE	СОМ	PANY
	S. P.	Н. Р.		14.8	15.3 16.0 16.8	17.7 18.7 20.1	21.6 23.0 24.7	26.6 33.3 33.3	38.7 45.1 52.2
	1%" S.	R. P. M.		139	138 136 136	135 135 135	136 136 138	139 140 144	146 152 156
ES	. P.	Н. Р.		$11.8 \\ 12.2$	12.9 13.6 14.4	15.4 16.6 17.9	19.3 20.9 22.7	24.5 26.6 31.2	36.6 42.8 49.7
PRESSU	34" S. P.	R.P.M.		129 128	126 126 125	125 125 126	127 128 129	131 133 137	141 146 151
NO. 16 NIADARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	۶٬۳ S. P.	Н. Р.		9.01 9.45 9.98	10.6 11.4 12.3	13.4 14.7 15.9	17.3 19.0 20.7	22.6 24.9 29.5	34.6 40.5
		R. P. M.		117 116 115	114 114 114	115 116 117	119 121 122	124 126 130	135
	½″ S. P.	Н. Р.	6.61	$6.99 \\ 7.48 \\ 8.01$	$ \begin{array}{c} 8.76 \\ 9.58 \\ 10.6 \end{array} $	11.7 12.9 14.2	15.7 17.3 19.0	21.1 22.9 27.4	32.5 37.9
N) CAP INCHES		R. P. M.	104	$103 \\ 103 \\ 102$	103 103 104	105 107 109	111 113 114	117 119 124	128 134
(TYPE D 29.92	_{3%"} S. P.	Н. Р.	4.17 4.46 4.79	$5.22 \\ 5.76 \\ 6.45$	7.17 8.04 8.99	10.1 11.3 12.7	14.1 15.7 17.4	$ \begin{array}{c} 19.0 \\ 21.1 \\ 25.2 \end{array} $	29.7
AL FAN • F. AN		R. P. M.	91 89 89	8888 8888 8888 8888 8888 8888 8888 8888 8888	92 94 94	96 86 86	102 104 107	109 112 117	123
AT 70	₩" S. P.	Н. Р.	2.66 2.97 3.38	3.84 4.43 5.10	5.86 6.76 7.76	$ \begin{array}{c} 8.78 \\ 9.93 \\ 11.1 \end{array} $	12.4 13.9 15.5	17.1 19.0 23.0	28.2
), 16 NIAGARA C	M" :	R.P.M.	73 72 73	74 75 77	79 81 83	86. 88 91	8988 8988	102 105 111	117
	Add for	Press.	0.063 0.076 0.090	0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390\\ 0.422\\ 0.489\end{array}$	0.560 0.638 0.721
Ż	Capacity Cu. Ft.	Air per Min.	37320 41060 44790	48520 52250 55980	59720 63450 67170	70910 74640 78380	82110 85840 89570	93300 97040 104500	$\begin{array}{c} 111970\\ 1119430\\ 126900\end{array}$
	Outlet Velocity		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

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STATIC PRESSURES	a
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CAPACITIES	INCHES BARON
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DAL	AT 70° F.
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NIA	NIAGARA CONOIDAL FAN CAPACITIES									
	H.P.		60.4 61.4	62.5 63.8 65.0	66.3 67.6 69.1	70.7 72.2 75.8	80.1 85.3 91.1	98.8 107.0 116.7		
2 ½" S. P.	R.P.M.		252 249	247 244 243	241 238 237	$235 \\ 234 \\ 231 \\ 231 $	230 228 228	229 230 231		
S. P.	Н. Р.		43.5 44.8 45.8	46.9 47.9 49.2	50.2 51.5 52.7	54.3 55.8 59.7	64.0 70.2 76.6	84.2 93.2 102.4		
2" S	R. P. M.		223 221 219	217 214 213	211 210 208	207 206 204	204 204 205	208 209 213		
S. P.	Н. Р.	35.6	36.6 37.4 38.4	39.4 40.5 41.5	42.5 43.8 45.3	46.6 48.4 52.2	57.4 63.5 70.2	78.3 86.5 96.3		
137,	R.P.M.	208	206 204 202	200 198 197	195 194 193	192 191 190	191 192 194	197 200 204		
S. P.	Н. Р.	28.4 29.4	30.2 31.0 31.8	32.5 33.3 34.6	35.6 36.9 38.4	$ \begin{array}{r} 39.9 \\ 41.7 \\ 46.3 \end{array} $	51.5 57.4 64.3	71.9		
1 1/2"	R. P. M.	193 191	189 187 184	183 182 180	179 178 178	177 176 177	178 180 184	187 191		
S. P.	H. P.	22.6 23.0	23.9 24.4 25.3	26.1 27.1 28.2	$29.2 \\ 30.7 \\ 32.0 \\ 32.0 \\$	34.1 35.9 40.7	45.8 52.0 58.6	66.6		
1 14"	R. P.M.	171 171	169 168 166	164 164 163	162 161 161	161 162 163	166 169 173	177		
s. P.	H. P.	16.4 16.9 17.5	18.1 18.6 19.4	20.3 21.3 22.5	23.8 25.4 27.1	29.2 31.0 35.6	41.0 46.9 54.0	62.0		
1" S	R. P. M.	154 152 150	149 147 146	145 144 144	144 144 145	146 147 150	154 157 162	166		
Add for	Add for Total Press.		$\begin{array}{c} 0.160\\ 0.180\\ 0.202\\ 0.202 \end{array}$	0.225 0.250 0.275	0.302 0.330 0.360	0.390 0.422 0.489	0.560 0.638 0.721	0.810 0.900 1.000		
Capacity Cut. Ft.	Air per Min.	48520 52250 55980	59720 63450 67170	70910 74640 78380	82110 85840 89570	93300 97040 104500	111970 119430 126900	134380 141810 149300		
Outlet	Ft. per Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000		

	18" S. P.	Н. Р.		16.7	17.3 18.1 18.9	20.0 21.1 22.7	24.4 26.0 27.9	$30.1 \\ 32.7 \\ 37.6 \\$	43.6 50.9 59.0
F. AND 29:02 INCHES BAROMETER	1/8	R. P. M.		131	130 128 128	127 127 127	128 128 130	131 132 135	138 143 147
	ď	Н. Р.		13.3 13.8	14.5 15.3 16.2	$17.4 \\ 18.7 \\ 20.2 $	$21.8 \\ 23.6 \\ 25.6$	$\begin{array}{c} 27.7 \\ 30.1 \\ 35.3 \end{array}$	41.3 48.3 56.1
	34" S. P.	R. P. M.		121 120	119 118 118	118 118 118	120 121 122	124 125 129	133 138 142
	S. P.	Н. Р.		$10.2 \\ 10.7 \\ 11.3 $	12.0 12.9 13.9	15.1 16.5 18.0	$ \begin{array}{c} 19.5 \\ 21.4 \\ 23.4 \end{array} $	25.5 28.1 33.2	39.0 45.7
	2 8/1	R.P.M.		110 109 108	108 107 108	108 109 110	112 114 115	117 119 122	127 132
	<u>1∕</u> 2″ S. P.	Н. Р.	7.46	$7.89\\8.44\\9.05$	9.88 10.8 11.9	13.2 14.6 16.1	17.7 19.5 21.5	23.8 25.9 30.9	36.7 42.8
		R.P.M.	98	96 96	97 97 98	99 101 102	104 106 108	110 112 117	121 127
D 29.92	S. P.	Н. Р.	4.71 5.03 5.41	$5.90 \\ 6.50 \\ 7.28 \\ 7.28 \\ \end{array}$	$ \begin{array}{c} 8.09 \\ 9.08 \\ 10.2 \end{array} $	$11.4 \\ 12.8 \\ 14.4 \\ 14.4 \\ 1$	$15.9 \\ 17.8 \\ 19.6 \\ 19.6 \\ 19.6 \\ 19.6 \\ 10.6 \\ $	$21.5 \\ 23.8 \\ 28.5 \\ 28.5 \\ 22.5 \\ $	33.5
• F. AN	3,8"	R.P.M.	85 84 84	83 84 84	85 87 88	90 92 94	96 98 101	103 105 110	116
AT 70°	S. P.	Н. Р.	$3.01 \\ 3.35 \\ 3.82 \\ 3.82$	4.34 5.00 5.75	$6.62 \\ 7.63 \\ 8.76$	$9.91 \\ 11.2 \\ 12.6 \\ $	14.0 15.7 17.5	$ \begin{array}{c} 19.3 \\ 21.5 \\ 26.0 \\ \end{array} $	31.8
	1 <u>4</u> "	R.P.M.	68 88 88 88	69 71 72	74 76 78	81 83 85	88 91 93	96 99 104	110
	Add for	Add for Total Press.		$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
	Capacity Cu. Ft.	Air per Min.	42140 46350 50560	54780 58980 63200	67430 71630 75840	80050 84270 88490	92690 96900 101130	$\frac{105340}{109560}$	$\begin{array}{c} 126410\\ 134820\\ 143260\\ \end{array}$
	Outlet Velocity	Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3200 3200 3400

NO. 17 NIAGARA CONOIDAL FAN (TVPE N) CAPACITIES AND STATIC PRESSURES

	S. P.	Н. Р.		68.2 69.4	70.5 72.0 73.4	74.9 76.3 78.0	79.8 81.5 85.6	$90.5 \\ 96.2 \\ 102.9$	111.6 120.8 131.8
	2 1/2" 5	R. P. M. H. P.		237 235	232 230 229	227 224 223	221 220 218	217 215 214	215 217 218 218
SES	S. P.	Н. Р.		49.1 50.6 51.7	52.9 54.1 55.5	56.7 58.1 59.5	61.3 63.0 67.3	72.3 79.2 86.4	95.1 105.2 115.6
RESSUR	2" S	R.P.M.		210 208 206	204 202 200	199 198 195	195 194 192	192 192 193	195 197 200
LATIC P	S. P.	Н. Р.	40.2	41.3 42.2 43.4	44.5 45.7 46.8	48.0 49.4 51.2	52.6 54.6 59.0	64.7 71.7 79.2	88.4 97.7 108.7
AND ST	1 34"	R. P. M.	196	194 192 190	188 187 185	184 182 181	181 180 179	180 181 182	185 188 192
N) CAPACITIES AND INCHES BAROMETER	S. P.	Н. Р.	32.1 33.2	$\begin{array}{c} 34.1\\ 35.0\\ 35.8\\ \end{array}$	36.7 37.6 39.0	40.2 41.6 43.4	45.1 47.1 52.3	58.1 64.7 72.5	81.2 91.0
N) CAPA	1 3%	R.P.M.	181 180	178 176 174	172 171 170	168 168 167	167 166 167	168 170 173	176 180
(TYPE) 29.92	S. P.	Н. Р.	25.5 26.0	$27.0 \\ 27.6 \\ 28.6$	29.5 30.6 31.8	33.0 34.7 36.1	$38.4 \\ 40.5 \\ 46.0$	51.7 58.7 66.2	75.1
F. AND	1 14"	R.P.M.	162 161	160 158 156	155 154 153	$152 \\ 152 $	152 152 154	156 159 162	167
AT 70°	S. P.	Н. Р.	18.5 19.1 19.7	20.4 21.0 21.9	22.9 24.1 25.4	26.9 28.7 30.6	33.0 35.0 40.2	46.2 52.9 61.0	6.9.9
UAKA C	*- -	R.P.M.	145 143 141	140 138 137	137 136 136	135 136 137	137 138 141	145 148 152	156
NO. 17 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	Add for Total	Press.	0.106 0.122 0.141	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	0.302 0.330 0.360	$\begin{array}{c} 0.390 \\ 0.432 \\ 0.489 \end{array}$	0.560 0.638 0.721	0.810 0.900 1.000
Z	Capacity Cu. Ft.	per Min.	54780 58980 63200	$\begin{array}{c} 67430\\ 71630\\ 75840\end{array}$	80050 84270 88490	92690 96900 101130	$\begin{array}{c} 105340 \\ 109560 \\ 117990 \end{array}$	$\frac{126410}{134820}$ 134820	151700 160100 168550
	Outlet Velocity Et. ner	Min.	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

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	S. P.	Н. Р.		76.5 77.8	79.1 80.7 82.3	83.9 85.5 87.5	$89.4 \\ 91.4 \\ 95.9$	$101.4 \\ 107.9 \\ 115.3$	$125.1 \\ 135.4 \\ 147.7$
	2 1/2"	R.P.M		224 222	220 217 216	$215 \\ 212 \\ 211 \\ 211$	209 208 206	205 203 202	203 205 206
	S. P.	Н. Р.		55.1 56.7 58.0	59.3 60.6 62.2	63.5 65.1 66.8	68.7 70.6 75.5	81.0 88.8 96.9	106.6 117.9 129.6
	5, 2	R.P.M.		198 196 195	193 191 189	188 187 185	184 183 182	181 182 182	185 186 189
	S. P.	Н. Р.	45.0	46.3 47.3 48.6	49.9 51.2 52.5	53.8 55.4 57.4	59.0 61.2 66.1	72.6 80.3 88.8	99.2 109.5 121.8
METER	1 3," S.	R. P. M.	185	183 181 180	178 176 175	173 172 171	171 170 169	170 171 172	175 178 181
F. AND 29.92 INCHES BAROMETER	I ½″ S. P.	Н. Р.	36.0 37.3	$38.2 \\ 39.2 \\ 40.2$	41.2 42.1 43.8	45.0 46.7 48.6	50.6 52.8 58.7	$65.1 \\ 72.6 \\ 81.3$	$ \begin{array}{c} 91.0 \\ 102.1 \end{array} $
		R. P. M.	171 170	168 166 164	163 162 160	159 158 158	157 157 157	158 160 163	166 170
D 29.92	S. P.	Н. Р.	28.6 29.2	30.3 30.9 32.1	$33.1 \\ 34.4 \\ 35.7$	$ \begin{array}{r} 36.9 \\ 38.9 \\ 40.5 \end{array} $	43.1 45.4 51.5	58.0 65.8 74.2	84.2
P F. AN	1 14"	R. P. M.	153 152	151 149 147	146 146 145	144 143 143	143 144 145	147 150 153	157
AT 70°	. P.	Н. Р.	20.7 21.4 22.1	22.9 23.6 24.6	25.6 27.0 28.4	30.2 32.2 34.4	$36.9 \\ 39.7 \\ 45.0$	51.8 59.3 68.4	78.4
	1″ S.	R. P. M.	137 135 133	132 131 130	129 128 128	128 128 129	130 131 133	137 140 144	147
	Add for Total Press.		0.106 0.122 0.141	$\begin{array}{c} 0.160\\ 0.180\\ 0.202\end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.432 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
	Capacity Cu. Ft.	per Min.	61420 66130 70860	$\begin{array}{c} 75590 \\ 80300 \\ 85010 \end{array}$	89750 94480 99200	$\begin{array}{c} 103910 \\ 108650 \\ 113370 \end{array}$	$\frac{118100}{122820}$ $\frac{132260}{132260}$	141710 151160 160600	$\frac{170070}{179500}$ 188950
	Outlet Velocity Et ner		1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NO. 18 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES

	4	Н. Р.		20.8	21.6 22.6 23.7	25.0 26.4 28.3	$30.4 \\ 32.4 \\ 34.8 \\ $	37.6 40.8 46.9	54.5 63.5 73.6
	7,8" S. P.	R. P. M.		117	116 115 114	114 114 114	114 115 116	117 118 121	123 128 132
IRES	34" S. P.	Н. Р.		16.7 17.3	18.1 19.1 20.3	21.7 23.4 25.3	$27.2 \\ 29.5 \\ 32.0 \\$	34.6 37.6 44.1	51.6 60.3 70.0
PRESSI	34"	R.P.M.		109 107	106 106 105	105 105 106	107 108 109	111 112 115	119 123 127
NO. 19 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	5,« S. P.	Н. Р.		12.7 13.3 14.1	15.0 16.1 17.4	$ \begin{array}{c} 18.9 \\ 20.7 \\ 22.5 \end{array} $	24.4 26.7 29.2	$31.9 \\ 35.1 \\ 41.5$	48.7 57.0
		R. P. M.		98 97 97	96 96 96	97 98 98	100 102 103	104 106 110	114 118
	½″ S. P.	Н. Р.	9.31	9.86 10.6 11.3	12.4 13.5 14.9	$16.4 \\ 18.2 \\ 20.1 $	$22.1 \\ 24.4 \\ 26.8 \\ $	29.7 32.3 38.6	45.9 53.4
		R.P.M.	88	87 86 86	86 87 87	89 90 92	93 95 96	99 100 104	109 113
N (TYPE	<u>у</u> " S. P. 3 ₈ " S. P.	Н. Р.	5.88 6.28 6.75	7.36 8.12 9.10	10.1 11.3 12.7	$14.2 \\ 16.0 \\ 18.0$	$ \begin{array}{c} 19.9 \\ 22.2 \\ 24.5 \end{array} $	26.8 29.7 35.6	41.9
DNOIDAL FAN (TYPE AT 70° F. AND 29.92		R.P.M.	76 75 75	74 75 75	57 77 79	81 82 84	86 88 90	92 94 98	104
CONOIE AT 70		Н. Р.	3.76 4.19 4.77	$5.42 \\ 6.25 \\ 7.18$	$ 8.27 \\ 9.53 \\ 10.9 $	$12.4 \\ 14.0 \\ 15.7$	$17.5 \\ 19.6 \\ 21.8 \\ 21.8 \\ 31.8 \\ $	24.1 26.8 32.5	39.7
0. 19 NIAGARA		R.P.M.	61 61 61	62 63 65	66 68 70	72 74 76	79 81 83	86 89 89	66
	Add for Total Press.		0.063 0.076 0.090	$\begin{array}{c} 0.106 \\ 0.122 \\ 0.141 \end{array}$	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	0.560 0.638 0.721
4	Capacity Cu. Ft.	Air per Min.	52630 57900 63150	68430 73680 78950	84220 89470 94720	$\begin{array}{c} 999990 \\ 105270 \\ 110520 \end{array}$	$\frac{115780}{121050}$ 126310	$\begin{array}{c} 131580\\ 136840\\ 147390\end{array}$	$\begin{array}{c} 157890 \\ 168420 \\ 178950 \end{array}$
		Ft. per Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

	S. P.	Н. Р.		85.2 86.6	88.1 89.9 91.7	93.5 95.3 97.5	99.6 101.8 106.9	113.0 120.2 128.5	139.3 150.9 164.6
	2 3/2"	R. P. M.		212 210	208 206 205	203 201 200	$\begin{array}{c} 198\\ 197\\ 195\end{array}$	$194 \\ 192 \\ 192 $	193 194 195
	s. p.	Н. Р.		$61.4 \\ 63.2 \\ 64.6$	66.1 67.5 69.3	70.8 72.6 74.4	76.5 78.7 84.1	90.3 98.9 107.9	$118.8 \\ 131.4 \\ 144.4$
	2" S.	R. P. M.		188 186 184	181 181 179	178 177 175	$174 \\ 173 \\ 172$	$172 \\ 172 \\ 173$	175 176 179
	S. P.	Н. Р.	50.2	51.6 52.7 54.2	55.6 57.0 58.5	59.9 61.7 63.9	65.7 68.2 73.6	80.9 89.5 98.9	110.5 122.0 135.7
ETER	1 34"	R. P. M.	175	174 172 170	169 167 166	$164 \\ 163 \\ 162$	162 161 160	161 162 163	166 168 172
BAROM	S. P.	Н. Р.	40.1 41.5	42.6 43.7 44.8	45.9 46.9 48.7	50.2 52.0 54.2	56.3 58.8 65.3	72.6 80.9 90.6	101.4
F. AND 29.92 INCHES BAROMETER	1 3/2"	R. P. M.	162 161	159 157 155	154 153 152	151 150 150	149 149 149	150 152 155	157 161
29.92	S. P.	н. Р.	31.9 32.5	33.7 34.4 35.7	36.8 38.3 39.7	$41.2 \\ 43.3 \\ 45.1$	48.0 50.5 57.4	64.6 73.3 82.7	93.9
F. AND	5 "1/1	R.P.M.	145 144	143 141 140	139 138 137	136 136 136	136 136 137	140 142 145	149
AT 70°	S. P.	Н. Р.	23.1 23.8 24.7	25.5 26.3 27.4	28.6 30.0 31.7	33.6 35.8 38.3	41.2 43.7 50.2	57.8 66.1 76.2	87.4
	1" S	R. P. M.	130 128 126	125 124 123	122 122 122	121 122 122	123 124 126	130 132 136	140
	Add for Total Press.		$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225\\ 0.250\\ 0.275\end{array}$	0.302 0.330 0.360	0.390 0.422 0.489	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$	0.810 0.900 1.000
	Capacity Cu. Ft.	per Min.	68430 73680 78950	84220 89470 94720	999990 105270 110520	115780 121050 126310	$\begin{array}{c} 131580\\ 136840\\ 147390\end{array}$	$\frac{157890}{168420}$ $\frac{168420}{178950}$	$\frac{189490}{199990}$ 210530
	Outlet Velocity		1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

NO. 19 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES

FAN	ENG	INEE	RING	— B U I	FFAL	O FC	DRGE	COM	IPANY
	e.	Н. Р.		23.1	23.9 25.1 26.2	27.7 29.3 31.4	33.7 35.9 38.6	41.6 45.2 52.0	60.4 70.4 81.6
	7,8" S. P.	R.P.M.		112	110 109 109	108 108 108	109 109 110	111 112 115	117 122 125
SES	. P.	Н. Р.		$18.5 \\ 19.1$	$20.1 \\ 21.2 \\ 22.5 \\ 22.5 \\ 32.5 \\ $	$24.1 \\ 25.9 \\ 28.0 \\$	$30.2 \\ 32.7 \\ 35.5$	$38.3 \\ 41.6 \\ 48.8 \\ 48.8 \\ 1000 \\ $	57.2 66.8 77.6
N) CAPACITIES AND STATIC PRESSURES INCHES BAROMETER	34" S.	R.P.M.		103 102	101 101 100	100 101	102 103 104	105 107 110	113 117 121
TATIC	S. P.	Н. Р.		$14.1 \\ 14.8 \\ 15.6 \\ 15.6$	16.6 17.8 19.3	20.9 22.9 24.9	$27.1 \\ 29.6 \\ 32.4$	$35.3 \\ 38.9 \\ 46.0$	54.0 63.2
AETER	5 / S	R.P.M.		94 93 92	92 91 92	92 93 94	95 97 98	99 101 104	108
ACITIES BAROA	Р.	Н. Р.	10.3	$10.9 \\ 11.7 \\ 12.5$	$13.7 \\ 15.0 \\ 16.5$	$ \begin{array}{c} 18.2 \\ 20.2 \\ 22.3 \end{array} $	24.5 27.1 29.7	$32.9 \\ 35.8 \\ 42.8 \\ $	50.8 59.2
N) CAPACITIES AND INCHES BAROMETER	₩. S. P.	R. P. M.	84	82 82 82 83	8357 8358 837	84 86 87	92 92 92	94 95 99	103 108
AN (TYPE AND 29.92	S. P.	Н. Р.	$6.52 \\ 6.96 \\ 7.48$	8.16 9.00 10.1	11.2 12.6 14.1	15.8 17.7 19.9	$22.1 \\ 24.6 \\ 27.2 $	29.7 32.9 39.4	46.4
AL FAN F. ANI	3%" S	R.P.M.	73 72 72	71 71 72	72 74 75	77 78 80	82 86 86	88 94 94	66
CONOIDA AT 70°	S. P.	Н. Р.	$4.16 \\ 4.64 \\ 5.28$	$\begin{array}{c} 6.00 \\ 6.92 \\ 7.96 \end{array}$	$^{9.16}_{10.6}$	13.7 15.5 17.4	$ \begin{array}{c} 19.4 \\ 21.8 \\ 24.2 \end{array} $	26.7 29.7 36.0	44.0
GARA (14"	R. P. M.	58 58 58	59 60 62	63 65 67	69 71 73	75 77 79	82 84 89	94
NO. 20 NIAGARA CONOIDAL FAN (TYPE AT 70° F. AND 29.92	Add for Total	Press.	$\begin{array}{c} 0.063\\ 0.076\\ 0.090\end{array}$	$\begin{array}{c} 0.106 \\ 0.122 \\ 0.141 \end{array}$	$\begin{array}{c} 0.160 \\ 0.180 \\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	$\begin{array}{c} 0.560 \\ 0.638 \\ 0.721 \end{array}$
Z	Capacity Cu. Ft.	per Min.	58320 64150 69980	$\begin{array}{c} 75820 \\ 81640 \\ 87480 \end{array}$	$\begin{array}{c} 93320\\ 99140\\ 104960 \end{array}$	$\frac{110800}{116640}$ $\frac{122480}{122480}$	$\begin{array}{c} 128300\\ 134140\\ 139960\end{array}$	$\frac{145800}{151650}$ 163300	$\frac{174960}{186620}$ $\frac{198300}{198300}$
	Outlet Velocity	Min.	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400

NGINEERING-BUFFALO FORGE

COMPANY

	S. P.	Н. Р.		94.4 96.0	97.6 99.6 101.6	$103.6 \\ 105.6 \\ 108.0$	110.4 112.8 118.4	$125.2 \\ 133.2 \\ 142.4$	154.4 167.2 182.4
	2 1⁄4" S. P.	R.P.M.		202 200	198 196 195	193 191 190	188 187 185	184 183 182	183 184 185
	S. P.	H. P.		68.0 70.0 71.6	73.2 74.8 76.8	78.4 80.4 82.4	84.8 87.2 93.2	100.0 109.6 119.6	$131.6\\145.6\\160.0$
	2" S	R.P.M.		179 177 175	174 172 170	$\substack{169\\168}166$	166 165 164	163 164 164	166 167 170
	S. P.	Н. Р.	55.6	$57.2 \\ 58.4 \\ 60.0$	61.6 63.2 64.8	66.4 68.4 70.8	$72.8 \\ 75.6 \\ 81.6$	89.6 99.2 109.6	$122.4 \\ 135.2 \\ 150.4$
29.92 INCHES BAROMETER	1 34" S. 1	R.P.M.	167	165 163 162	160 159 158	156 155 154	154 153 152	153 154 155	158 160 163
S BARC	1 <u>)</u> 2" S. P.	Н. Р.	44.4 46.0	47.2 48.4 49.6	50.8 52.0 54.0	55.6 57.6 60.0	62.4 65.2 72.4	80.4 89.6 100.4	112.4 126.0
INCHE	1 1/3"	R.P.M.	154 153	151 150 148	147 146 144	143 143 142	142 141 142	143 144 147	150 153
AND 29.92	S. P.	Н. Р.	35.3 36.0	$37.4 \\ 38.2 \\ 39.5$	40.8 42.4 44.0	45.6 48.0 50.0	53.2 56.0 63.6	71.6 81.2 91.6	104.0
70° F. AN	11%	R.P.M.	138 137	136 134 133	132 131 130	130 129 129	129 130 131	133 135 138	142
AT 7(ď	Н. Р.	25.6 26.4 27.3	$28.2 \\ 29.1 \\ 30.4$	$\frac{31.6}{33.3}$	37.3 39.7 42.4	45.6 48.4 55.6	64.0 73.2 84.4	96.8
	l" S. P.	R.P.M.	123 122 120	119 118 117	116 116 116	115 116 116	117 118 120	123 126 130	133
	Add for Total	Press.	$\begin{array}{c} 0.106\\ 0.122\\ 0.141\end{array}$	$\begin{array}{c} 0.160\\ 0.180\\ 0.202 \end{array}$	$\begin{array}{c} 0.225 \\ 0.250 \\ 0.275 \end{array}$	$\begin{array}{c} 0.302 \\ 0.330 \\ 0.360 \end{array}$	$\begin{array}{c} 0.390 \\ 0.422 \\ 0.489 \end{array}$	0.560 0.638 0.721	0.810 0.900 1.000
	Capacity Cu. Ft.	per Min.	75820 81640 87480	$\begin{array}{c} 93320\\ 99140\\ 104960\end{array}$	$\frac{110800}{116640}$ $\frac{1122480}{122480}$	$\frac{128300}{134140}$ 139960	145800 151650 163300	$\frac{174960}{186620}$ $\frac{186620}{198300}$	209960 221600 233300
	Outlet Velocity		1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2800	3000 3200 3400	3600 3800 4000

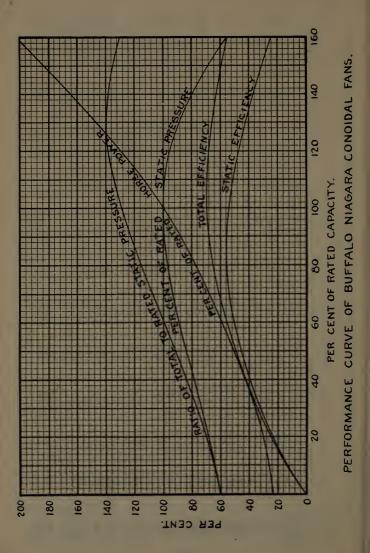
NO. 20 NIAGARA CONOIDAL FAN (TYPE N) CAPACITIES AND STATIC PRESSURES

VELOCITIES	
OUTLET	
) FOR VARIOUS OUTL	
Z.	
FANS (TYPE]	SURES
FANS	PRE
CONOIDAL	AND TOTAL
VITH NIAGARA	
WITH	
EFFICIENCIES	
TOTAL	

E N) FOR VARIO	5%" Static	Total Total Total Press.	701 54.1 715 58.1	.731 61.9 .747 64.7 .766 67.5	.785 69.1 .805 70.4 .827 70.8	.850 70.8 .875 70.0 .900 69.5	.927 69.0 .955 68.5 .985 66.8	1.015 65.7 1.047 64.2 1.114 62.0	.185 60.3 263 58.6 346 57.4 .435 56.7
TOTAL EFFICIENCIES WITH NIAGARA CONOIDAL FANS (TYPE N) FOR VARIOUS OUTLET VELOCITIES AND TOTAL PRESSURES	142" Static	Total Eff.	55.2 59.0 63.0	66.0 68.5 70.4	70.7 70.7 70.2	69.5 68.3 66.9	66.0 64.8 63.6	62.0 61.2 59.3	57.2 56.2 55.0
NIAGARA CONO AND 1	3%" Static	Total Total Eff. Press	61.5 .563 65.2 .563 68.1 .590	70.4 .606 70.6 .622 70.7 .641	69.9 .660 68.9 .680 67.7 .702	67.2 .725 64.7 .750 62.9 .775	61.7 .802 60.5 .830 59.5 .860	. 59.0 .890 57.6 .922 56.2 .989	54.9 1.060 54.0 1.138 1.221
CIENCIES WITH	Static 3%"	Total Total Eff.	68.8 .438 70.6 .451 70.7 .451	70.6 .481 68.7 .497 67.2 .516	65.6 .535 63.3 .555 61.4 .577	60.2 .600 59.0 .625 58.0 .650	57.2 .677 56.1 .705 55.4 .735	54.8 .705 53.8 .797 52.6 .864	1.013
TOTAL EFFI	M"	Ft. per Min. Press.	1000 .313 1100 .326 1200 .340	1300 .356 1400 .372 1500 .301	1600 .410 1700 .430 1800 .452	1900 .475 2000 .500 2100 .525	2200 ¹ .552 2300 .580 2400 .610	2500 .640 2600 .672 2800 .739	3000 3200 3400 3600

I.V. Static I.Y. Static I.Y. Static I.Y. Static Z. Static			-			AND TOTAL PRESSURES	PRESSU	RES					
Total Total <th< th=""><th>1" Static</th><th>atic</th><th></th><th>114"</th><th>Static</th><th>1 1/3" S</th><th>tatic</th><th>1 34" S</th><th>itatic</th><th>2" St</th><th>atic</th><th>2 3/2" 5</th><th>tatic</th></th<>	1" Static	atic		114"	Static	1 1/3" S	tatic	1 34" S	itatic	2" St	atic	2 3/2" 5	tatic
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	Total Total Press. Eff.	Total Eff.		Total Press.	Total Eff.	Total Press.	Total Eff.	Total Press.	Total Eff.	Total Press.	Total Eff.	Total Press.	Total Eff.
	.106 51.4 .122 54.6 .141 57.5	51.4 54.6 57.5		1.372 1.391	49.8 53.0	1.622 1.641	46.9 49.2	1.891	46.5				
	160 60.3 180 63.1 .202 65.1	60.3 63.1 65.1		1.410 1.430 1.452	55.2 58.0 60.4	1.660 1.680 1.702	51.2 54.1 56.7	1.910 1.930 1.952	48.9 51.2 53.5	2.160 2.180 2.202	46.4 48.5 50.6	2.680 2.702	44.1
	.225 67.3 .250 68.5 .275 70.0	67.3 68.5 70.0		1.475 1.500 1.525	63.1 65.0 66.8	$ \begin{array}{c} 1.725 \\ 1.750 \\ 1.775 \\ 1.775 \end{array} $	58.8 61.4 63.5	1.975 2.000 2.025	55.9 58.0 60.0	2.225 2.250 2.275	53.0 55.1 56.8	2.725 2.750 2.775	48.5 50.6 52.5
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$.302 70.5 .330 70.5 .360 70.6	70.5 70.5 70.6		1.552 1.580 1.610	68.3 69.5 70.5	1.802 1.830 1.860	65.0 66.9 68.1	2.052 2.080 2.110	62.1 64.0 65.5	2.302 2.330 2.360	58.9 61.0 62.9	2.802 2.830 2.860	54.5 56.5 58.1
	.390 70.6 .422 70.0	70.6 70.0 68.6		1.640 1.672 1.739	70.6 70.8 70.2	$ \begin{array}{c} 1.890 \\ 1.922 \\ 1.989 \end{array} $	69.2 70.2 70.4	2.140 2.172 2.239	67.0 68.2 70.1	2.390 2.422 2.489	64.5 65.9 68.4	2.890 2.922 2.989	59.7 61.6 64.5
65.0 2.310 67.5 2.560 68.9 2.810 70.2 3.310 63.5 2.400 66.0 2.650 68.1 2.900 69.3 3.400 63.5 2.500 65.0 2.750 68.1 2.900 69.3 3.400	.560 67.0 .638 65.5 .721 63.6	67.0 65.5 63.6		1.810 1.888 1.971	69.5 68.0 66.8	2.060 2.138 2.221	70.2 69.8 68.9	2.310 2.388 2.471	70.8 70.5 70.0	2.560 2.638 2.721	70.1 70.7 70.6	3.060 3.138 3.221	67.1 69.0 70.5
	1.810 61.5	61.5		2.150	65.0 63.5	2.310 2.400 2.500	67.5 66.0 65.0	2.560 2.650 2.750	68.9 68.1 65.9	2.810 2.900 3.000	70.2 69.3 68.4	3.310 3.400 3.500	70.6 70.6 70.0

TOTAL EFFICIENCIES WITH NIAGARA CONOIDAL FANS (TYPE N) FOR VARIOUS OUTLET VELOCITIES



Turbo-Conoidal Capacity Tables

For high speed, high efficiency fans suitable for direct connection to motors or turbines, see Turbo-Conoidal capacity tables on pages 278 to 319 inclusive. These fans have speeds for corresponding capacities and pressures which are nearly double those of the Niagara Conoidal of the same size. The dimensions of the housing are identical with those of the Niagara Conoidal. Complete and separate tables of capacities, speeds and horsepowers at various static pressures and outlet velocities are given for each size of single inlet fan as in the Niagara Conoidal tables. This enables the engineer to select a fan for a fixed direct connection speed and for any condition of static pressure and capacity.

It will be noted from the performance curves on page 320 that the pressure builds up rapidly with decreased capacity and increased resistance. In this respect it is in direct contrast with pressure capacity characteristic of the Niagara Conoidal.

For public building work where extreme quietness of operation is essential the following may be taken as conservative conditions of operation of the Turbo-Conoidal fans:—

At 1 in. static pressure, 1600 outlet velocity.

At 34 in. static pressure, 1800 outlet velocity.

At 1/2 in. static pressure, 2000 outlet velocity.

At 1/4 in. static pressure, 2200 outlet velocity.

For exhausting and for systems blowing through heaters, these velocities may be considerably increased.

For industrial work any desired outlet velocity may be used for static pressure up to 6 or 7 inches.

Double width fans with two inlets give double the capacities and horsepowers given in the tables.

1	ď.	H.P.	.24 .25 .28	.35 .35 .38	.42 .47 .51	.56 .61 .67	.73 .79 .86	$.93 \\ 1.00 \\ 1.08 $	1.16 1.25 1.34
	1 " S.	R.P.M.	$1304 \\ 1324 \\ 1352 \\ $	$1380 \\ 1408 \\ 1440 \\ 1440 \\ 1$	$1472 \\ 1508 \\ 1540 \\ $	$1576 \\ 1608 \\ 1644 \\ 1644$	$1684 \\ 1724 \\ 1760$	1796 1836 1876	1916 1956 1996
1	ď	H.P.	20 22 25	.28 .31 .35	.39 .43	.52 .56 .62	.68 .74 .80	.87 .94 1.01	$1.09 \\ 1.17 \\ 1.26 \\ 1.26$
~	7.8" S.	R. P.M.	$1232 \\ 1256 \\ 1284 \\ 1284 \\$	1316 1344 1376	1408 1444 1480	$1516 \\ 1552 \\ 1588 \\ $	$1628 \\ 1668 \\ 1704$	$1744 \\ 1780 \\ 1820$	$1860 \\ 1904 \\ 1948$
	ď.	H.P.	.17 .20	.25 .31 .31	.35 .39 .43	.47 .52 .57	.62 .68 .74	.81 .87 .94	$1.02 \\ 1.10 \\ 1.18 \\ 1.18$
METER	34" S.	R.P.M.	1160 1188 1216	$1248 \\ 1280 \\ 1312 \\ $	$1344 \\ 1380 \\ 1420$	$1456 \\ 1492 \\ 1532$	$1568 \\ 1608 \\ 1648 \\ $	1688 1732 1772	1812 1852 1896
BAROMETER	Ъ.	H.P.	.15	.22 .25 .28	.31 .35 .38	.43 .52	.57 .62 .68	.74 .80 .87	$^{.95}_{1.10}$
	5,8" S.	R. P. M.	1084 1112 1140	$1176 \\ 1208 \\ 1244 \\ 1244 \\$	$1280 \\ 1316 \\ 1352$	$1392 \\ 1428 \\ 1468 \\ 1468 \\ 1200 \\ $	1508 1548 1588	$1632 \\ 1672 \\ 1712 $	1756 1800 1840
INCHES	ď	H.P.	.12 .14 .16	.19 .21	.27 .30 .34	.38 .42 .46	.51 .56 .61	.67 .73 .80	.87 .94 1.02
29.92	1⁄2" S.	R.P.M.	$ \begin{array}{c} 996 \\ 1032 \\ 1064 \end{array} $	1096 1132 1172	$1208 \\ 1244 \\ 1284$	1324 1364 1404	1444 1484 1528	$1568 \\ 1608 \\ 1652 \\ 1652 \\ 1$	1700 1744 1788
F. AND	ď	H.P.	.12	.16 .18 .21	.23 .26 .30	.33 .37 .41	.45 .50 .55	.61 .66 .73	.80 .88 .95
AT 70° F. AN	3,8" S.	R. P. M.	908 944 980	1016 1052 1088	$1128 \\ 1168 \\ 1168 \\ 1208 $	$\begin{array}{c} 1248\\ 1288\\ 1328\\ 1328\end{array}$	1372 1416 1460	1504 1548 1596	$1640 \\ 1688 \\ 1732$
	Ŀ.	H.P.	80. 11.	.13 .15	.19 .22	.32 .32 .36	.40 .44 .49	.60 .60	.73 .80 .87
	14" S.	R. P. M.	804 840 876	$ \begin{array}{c} 916 \\ 956 \\ 1000 \end{array} $	$1040 \\ 1084 \\ 1124$	1164 1208 1256	1300 1348 1392	1440 1484 1532	1576 1628 1676
		Add for Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	910 1000 1090	1190 1280 1370	$1460 \\ 1550 \\ 1640$	1730 1820 1910	2010 2100 2190	2270 2370 2460	2550 2640 2730
	locity. Min.	Outlet Ve Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

22 25 25 25 25 25 25 Н.Р. 1.39 1.671.88 2.24 2.372.502.642.77 3.08 3.41 S. P. R. P. M. 3 1/2" 2488 2516 2544 2572 2600 2632 2344 2364 2384 2404 2424 2444 2464 2664 2696 2728 2756 2824 2888 4 97 .03 .20 1.471.561.66.77 88. 99 2.2362.2362.362.482.773.08Ĥ. à ŝ R. P. M. ň 2188 2208 2232 2252 2272 2296 2320 2344 2372 2400 2432 2464 2496 2560 2592 2528 2624 2696 2764 Н. Р. 71 $1.02 \\ 1.18 \\$ 82 88 95 .35 $1.85 \\ 1.96 \\ 2.08 \\ 2.08 \\ 1.08 \\$ $2.20 \\ 2.47 \\ 2.75$ à ŝ R. P. M. 2 15" INCHES BAROMETER 2040 2064 2088 2112 2140 2168 2288 2320 2352 2384 2420 2452 2488 2556 2632 1984 2000 2196 2224 2226 ď 54 57 62 .73 .73 95 99 99 1.14 1.31 1.40 .20 1.932.17 2.44 Ĥ. ď ŝ R. P. M. ň 1796 1816 840 1860 1884 1912 1940 1968 2000 $2032 \\ 2060 \\ 2092 \\ 2092 \\ 002 \\$ $2124 \\ 2160 \\ 2196 \\ 2196$ 2232 2268 2300 2336 2412 2488 29.92 Н. Р. 45 45 48 53 68 74 80 .93 .00 .34 .53 .53 1.64 4 15" S. AND R. P. M. $\frac{752}{784}$ 848 884 916 1952 1988 2024 $612 \\ 636$ 664 692 720 2096 2136 2060 Ľ, 70° Н. Р. 3741 545 59 65 70 76 83 90 .05 .13 30 .49 AT S. P. R. P. M. 1 14" 1972 2012 2048 472 500 528 556 588 616 644 680 716 752 788 824 860 896 936 208821682244122 122 141 160 180 202 225 2250 $275 \\ 302 \\ 330 \\ 330 \\$ 360 390 422 455 489 525 560 638 721 Press. Add for Total Capacity Cu. Ft. Air per Min. $370 \\ 460 \\ 550$ 1640 1730 1820 1910 2010 2100 2190 2270 2370 2460 2550 2640 2730 2920 3100 090 190 280 Ft. per Min. 1200 500 600 700 1800 2100 2200 2300 2400 2500 2600 2700 2800 2900 3200 Outlet Velocity

T) CAPACITIES AND STATIC PRESSURES

NO. 2 % TURBO-CONOIDAL FAN (TYPE

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FAN (TYPE	AT 70° F. AND 29.92 INCHES F
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N	ENO	GINEE	RING	- B U I	FFAL	O FO	RGE	COM	I P A N Y
	ď	H.P.	.34 .36 .40	.45 .50 .55	.61 .70 .73	.80 88. 96	$1.05 \\ 1.14 \\ 1.23 \\ 1.23 \\$	$1.34 \\ 1.44 \\ 1.55$	1.67 1.79 1.93
	1 <i>"</i> S.	R.P.M.	1087 1103 1127	$1150 \\ 1173 \\ 1200 $	1227 1257 1283	1313 1340 1370	1403 1437 1467	1497 1530 1563	$1597 \\ 1630 \\ 1663 \\ $
	ď	H.P.		.40 .45 .50	.55 .61 .67	.7 4 .81 .89	$ \begin{array}{c} .98\\ 1.06\\ 1.15 \end{array} $	$ \begin{array}{r} 1.25 \\ 1.35 \\ 1.46 \end{array} $	$ \begin{array}{c} 1.57 \\ 1.69 \\ 1.82 \end{array} $
	7.°" S.	R.P.M.	1027 1047 1070	$1097 \\ 1120 \\ 1147$	$1173 \\ 1203 \\ 1233$	$1263 \\ 1293 \\ 1323$	1357 1390 1420	$1453 \\ 1483 \\ 1483 \\ 1517$	1550 1587 1623
	ď	H.P.	.25 .28 .32	.36 .40	.50 .55 .61	.68 .75 .82	.90 .98 1.06	$ \begin{array}{c} 1.16 \\ 1.26 \\ 1.36 \end{array} $	$ \begin{array}{c} 1.47 \\ 1.58 \\ 1.70 \end{array} $
	·34" S.	R.P.M.	967 990 1013	$1040 \\ 1067 \\ 1093$	1120 1150 1183	1213 1243 1277	1307 1340 1373	1407 1443 1477	1510 1543 1580
	ď	H.P.	.21 .24 .28	.31 .35 .40	.45 .50 .55	.61 .68 .75	.82 .89 .98	$1.06 \\ 1.16 \\ 1.25$	$ \begin{array}{c} 1.36 \\ 1.47 \\ 1.59 \end{array} $
INVILLA UNIVERSE	5," S.	R.P.M.	903 927 950	980 1007 1037	$1067 \\ 1097 \\ 1127$	$1160 \\ 1190 \\ 1223$	$1257 \\ 1290 \\ 1323$	1360 1393 1427	1463 1500 1533
	ď	H.P.	.18 .21 .24	.27 .31 .35	.39 .44 .49	.54 .60 .67	.74 .80 .88	$^{.97}_{1.05}$	$ \begin{array}{c} 1.25 \\ 1.36 \\ 1.47 \end{array} $
4/1/4	<u>}∕</u> 2" S.	R.P.M.	830 860 887	913 943 977	1006 1037 1070	1103 1137 1170	1203 1237 1273	1307 1340 1377	1417 1453 1490
	4	H.P.	.15 .17 .20	.2 3 .26 .29	.33 .38 .42	.47 .53 .59	.65 .72 .79	.87 .96 1.05	$ \begin{array}{c} 1.15 \\ 1.26 \\ 1.37 \end{array} $
	3,8" S.	R.P.M.	757 787 817	847 877 907	940 973 1007	$1040 \\ 1073 \\ 1107$	1143 1180 1217	1253 1290 1330	1367 1407 1443
	ъ.	H.P.	.11 .13 .15	.18 .21 .24	.28 .31 .36	.40 .45 .51	.57 .64 .71	.78 .87 .96	$ \begin{array}{c} 1.05 \\ 1.15 \\ 1.26 \\ 1.26 \end{array} $
	₩ S.	R.P.M.	670 730	764 797 833	867 903 937	970 1007 1047	1083 1123 1160	1200 1237 1277	1313 1357 1397
		τοί bbA Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	$\frac{1310}{1440}$ 1580	$1710 \\ 1840 \\ 1970 $	2100 2230 2360	$2490 \\ 2630 \\ 2760 \\ 0$	2890 3020 3150	$3280 \\ 3410 \\ 3540 \\ 3540 \\ \end{array}$	3670 3810 3940
	elocity Min.	Outlet Vo Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	S. P.	Н. Р.	1.67	$1.75 \\ 1.82 \\ 1.89 $	$1.99 \\ 2.12 \\ 2.26$	2.40 2.55 2.71	2.88 3.05 3.23	3.41 3.60 3.79	$3.99 \\ 4.43 \\ 4.90$
	3 ½″ S	R.P.M.	1953	1970 1987 2003	2020 2037 2053	2073 2097 2120	2143 2167 2193	2220 2247 2273	2297 2353 2407
	ď.	Н. Р.	1.39	$1.45 \\ 1.52 \\ 1.61$	$1.72 \\ 1.85 \\ 1.98 \\ $	$2.11 \\ 2.25 \\ 2.39 $	$2.55 \\ 2.70 \\ 2.86 $	3.03 3.21 3.39	3.57 3.99 4.43
	3" S.	R.P.M.	1823	1840 1860 1877	1893 1913 1933	1953 1977 2000	2027 2053 2080	2107 2133 2160	2187 2247 2303
	S. P.	Н. Р.	1.02 1.07 1.12	$1.18 \\ 1.27 \\ 1.36 \\ 1.36$	$1.48 \\ 1.59 \\ 1.70$	$ \begin{array}{c} 1.82 \\ 1.95 \\ 2.07 \end{array} $	2.21 2.36 2.50	2.66 2.82 2.99	3.17 3.55 3.96
METER	2 35"	R. P. M.	1653 1667 1683	1720 1720 1740	1760 1783 1807	1830 1853 1880	1907 1933 1960	1987 2017 2043	2073 2130 2193
BARO	S. P.	Н. Р.	.78 .82 .89	$ \begin{array}{c} .96 \\ 1.05 \\ 1.14 \end{array} $	$ \begin{array}{c} 1.23 \\ 1.33 \\ 1.43 \end{array} $	$1.54 \\ 1.65 \\ 1.76 \\ $	$1.88 \\ 2.02 \\ 2.15 $	$2.30 \\ 2.44 \\ 2.60 $	2.77 3.13 3.51
29.92 INCHES BAROMETER	2, 2	R.P.M.	1497 1513 1533	1550 1570 1593	1617 1640 1667	$1693 \\ 1717 \\ 1743 \\ 1743$	1770 1800 1830	$1860 \\ 1890 \\ 1917 \\ $	1947 2010 2073
	s. P.	Н. Р.	.57 .65	.76 .83 .90	$^{.98}_{1.07}$	$1.25 \\ 1.34 \\ 1.45$	$1.56 \\ 1.68 \\ 1.80 $	$1.93 \\ 2.06 \\ 2.21$	2.35 2.67 3.02
° F. AND	1 35	R.P.M.	1327 1343 1363	1387 1410 1433	$ \begin{array}{c} 1460 \\ 1487 \\ 1513 \end{array} $	1540 1570 1597	1627 1657 1687	1717 1747 1780	1813 1877 1940
AT 70°	S. P.	H. P.	.59 .59	.65 .72 .78	$.85 \\ .93 \\ 1.01$	$1.10 \\ 1.19 \\ 1.29 \\ 1.29$	1.39 1.51 1.62	$ \begin{array}{c} 1.74 \\ 1.87 \\ 2.01 \end{array} $	2.14 2.43 2.77
	1 14"	R. P. M.	1227 1250 1273	$1297 \\ 1323 \\ 1347$	1370 1400 1430	$1460 \\ 1490 \\ 1520$	1550 1580 1613	1643 1677 1707	1740 1807 1870
	Total s.	Add for Pres	.106	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	Cu. Ft.	Capacity Air per	1580 1710 1840	1970 2100 2230	$2360 \\ 2490 \\ 2630$	2760 2890 3020	$3150 \\ 3280 \\ 3410 $	$3540 \\ 3670 \\ 3810$	3940 4200 4460
	slocity Min.	Outlet Ver	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 3 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES

NO. 3 ½ TURBO-CONOIDAL FAN (TVPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

	JINEE	RING	<u>– в о і</u>	FAL	U FC	RGE	COM	PANI
ď	Н. Р.	.46 .49 .55	.61 .68 .75	$^{-83}_{-91}$	$ \begin{array}{c} 1.10 \\ 1.20 \\ 1.31 \end{array} $	$ \begin{array}{r} 1.43 \\ 1.55 \\ 1.68 \\ \end{array} $	$\frac{1.82}{1.96}$	2.28 2.44 2.62
1" S.	R.P.M.	932 946 966	986 1006 1029	$\begin{array}{c} 1052 \\ 1077 \\ 1100 \end{array}$	1126 1149 1174	$1203 \\ 1232 \\ 1257 \\ $	1283 1312 1340	1369 1397 1426
s. P.	H. P.		.55 .61 .68	.76 .83 .92	1.01 1.11 1.21	$ \begin{array}{c} 1.33 \\ 1.44 \\ 1.57 \\ 1.57 \end{array} $	$ \begin{array}{c} 1.70 \\ 1.83 \\ 1.98 \end{array} $	2.13 2.30 2.47
1 ⁸ /2	R.P.M.	880 897 917	940 960 983	$1006 \\ 1032 \\ 1057 \\ $	1083 1109 1134	$1163 \\ 1192 \\ 1217$	$1246 \\ 1272 \\ 1300 \\ 1000 \\ $	1329 1360 1392
S. P.	Н. Р.	.38 .38 .43 .53	.49 .55 .61	.68 .75 .83	$^{.92}_{1.11}$	$ \begin{array}{c} 1.22 \\ 1.33 \\ 1.45 \end{array} $	$ \begin{array}{c} 1.58 \\ 1.71 \\ 1.85 \end{array} $	2.00 2.16 2.31
34" 5	R. P. M.	829 849 869		960 986 1014	1040 1065 1094	1120 1149 1177	$1206 \\ 1237 \\ 1266 \\ 1266$	1294 1323 1354
S. P.	Н. Р.	.29 .33 .38	.43 .48 .54	.61 .68 .75	.83 .92 1.01	$ \begin{array}{c} 1.11 \\ 1.22 \\ 1.33 \end{array} $	$ \begin{array}{c} 1.45 \\ 1.57 \\ 1.71 \end{array} $	$ \begin{array}{c} 1.85 \\ 2.00 \\ 2.16 \\ \end{array} $
5%" 5	Н. Р. R. P. M.	774 794 814	840 863 889	$\begin{array}{c} 914\\ 940\\ 966\end{array}$	994 1020 1049	1077 1106 1134	$1166 \\ 1194 \\ 1223$	1254 1286 1314
ď	Н. Р.	.24 .28 .32	.37 .42 .47	.53 .60 .67	.74 .82 .91	$1.00 \\ 1.10 \\ 1.20 \\ $	$ \begin{array}{c} 1.31 \\ 1.43 \\ 1.56 \\ 1.56 \end{array} $	$ \begin{array}{c} 1.70 \\ 1.84 \\ 2.00 \end{array} $
₩, S.	R.P.M.	712 737 760	783 809 837	863 889 917	$ \begin{array}{c} 946 \\ 974 \\ 1003 \end{array} $	$1032 \\ 1060 \\ 1092$	1120 1149 1180	1214 1246 1277
Ъ.	H. P	.20 .23 .27	.31 .35 .40	.46 .51 .58	.65 .72 .80	$^{.88}_{.98}_{.98}_{1.08}$	$ \begin{array}{c} 1.19\\ 1.30\\ 1.43\\ 1.43 \end{array} $	1.57 1.71 1.87
3.8" S.	R.P.M.	649 674 700	726 752 777	806 834 863	892 920 949	980 1012 1043	1074 1106 1140	1172 1206 1237
S. P.	Н. Р.	.15 .18 .21	.25 .29 .33	.38 .43 .48	.55 .62 .69	.78 .87 .96	1.07 1.18 1.31 1.31	$ \begin{array}{c} 1.43 \\ 1.56 \\ 1.71 \end{array} $
34" S	R.P.M.	574 600 626	654 683 714	743 774 803	831 863 897	929 963 994	1029 1060 1094	1126 1163 1197
	roî bbA Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Capacity Air per	$1790 \\ 1970 \\ 2140$	2320 2500 2680	2860 3040 3220	3390 3570 3750	3930 4110 4290	4470 4650 4820	5000 5180 5360
elocity Min.	Outlet V Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

NO. 3½ TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F, AND 29.92 INCHES BAROMETER

TUF	R B O - (CONOI	DAL	FAN	CAH	PACI	TIES	
<u>.</u>	Н. Р.	2.28	2.38 2.48 2.58	2.71 2.88 3.07	3.27 3.47 3.69	$3.92 \\ 4.15 \\ 4.39$	4.64 4.90 5.16	5.43 6.03 6.68
3 1/2" S.	R.P.M.	1674	1689 1703 1717	1732 1746 1760	1777 1797 1817	1837 1857 1880	1903 1926 1949	1969 2017 2063
ď	Н. Р.	1.90	$ \begin{array}{c} 1.98 \\ 2.07 \\ 2.20 \end{array} $	$2.34 \\ 2.52 \\ 2.69 $	$2.88 \\ 3.07 \\ 3.26$	3.47 3.68 3.90	4.13 4.37 4.62	4.86 5.43 6.03
3" S.	R. P. M.	1563	1577 1594 1609	1623 1640 1657	$1674 \\ 1695 \\ 1714$	1737 1760 1783	1806 1829 1852	1874 1926 1975
S. P.	Н. Р.	$ \begin{array}{c} 1.39 \\ 1.45 \\ 1.53 \end{array} $	$1.61 \\ 1.73 \\ 1.86 \\ 1.86$	$2.01 \\ 2.16 \\ 2.31 \\ 2.31$	2.48 2.65 2.82	3.01 3.21 3.41	3.62 3.84 4.07	4.31 4.84 5.39
2 1/2"	R.P.M.	1417 1429 1443	1457 1474 1492	$1509 \\ 1529 \\ 1549$	$1569 \\ 1589 \\ 1612 \\ $	1634 1657 1680	1703 1729 1752	$1777 \\1826 \\1880 $
ď	Н. Р.	1.07 1.12 1.21	$ \begin{array}{c} 1.31 \\ 1.43 \\ 1.55 \end{array} $	$ \begin{array}{c} 1.68 \\ 1.81 \\ 1.94 \end{array} $	2.09 2.24 2.40	2.57 2.74 2.93	3.12 3.32 3.54	3.77 4.26 4.77
2" S.	R. P. M.	1283 1297 1314	$1329 \\ 1346 \\ 1366$	1386 1406 1429	$1452 \\ 1472 \\ 1494$	1517 1543 1569	1595 1620 1643	1669 1723 1777
S. P.	Н. Р.	.78 .88 .94	$ \begin{array}{c} 1.03 \\ 1.13 \\ 1.23 \end{array} $	1.33 1.45 1.57	$ \begin{array}{c} 1.70 \\ 1.83 \\ 1.97 \end{array} $	$2.12 \\ 2.28 \\ 2.45 $	$2.62 \\ 2.81 \\ 3.00$	$3.20 \\ 3.64 \\ 4.10$
1 1/2"	R.P.M.	1137 1152 1169	1189 1209 1229	1252 1274 1297	$1320 \\ 1346 \\ 1369$	$1394 \\ 1420 \\ 1446 \\ $	1472 1497 1526	1555 1609 1663
S. P.	Н. Р.	.66 .73 .81	.89 .98 1.07	$ \begin{array}{c} 1.16 \\ 1.27 \\ 1.38 \end{array} $	$1.50 \\ 1.62 \\ 1.76$	$ \begin{array}{c} 1.89 \\ 2.05 \\ 2.21 \end{array} $	2.37 2.55 2.73	$2.92 \\ 3.31 \\ 3.77$
1 14"	R.P.M.	1052 1072 1092	$1112 \\ 1134 \\ 1154 \\ $	1174 1200 1226	1252 1277 1303	1329 1355 1383	1409 1437 1463	1492 1549 1603
or Total ess.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
ty Cu. Ft. er Min.	isegeð d tið	2140 2320 2500	2680 2860 3040	3220 3390 3570	3750 3930 4110	4290 4470 4650	. 4820 5000 5180	5360 5720 6070
Velocity er Min.	Outlet Ft. p	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 4 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

N E	N G	INEE	RING-	- B U I	FFAL	O FC	RGE	СОМ	IPANY
		Н.Р.	.60 .63 .71	8. 88. 88. 86.	$1.08 \\ 1.19 \\ 1.31$	$1.43 \\ 1.56 \\ 1.71$	$ \begin{array}{c} 1.86 \\ 2.02 \\ 2.19 \end{array} $	2.37 2.56 2.76	2.97 3.19 3.43
2 # C		R.P.M.	815 828 845	863 880 900	920 943 963	$ \begin{array}{c} 985 \\ 1005 \\ 1028 \end{array} $	$1053 \\ 1078 \\ 1100 \\ $	1123 1148 1173	1198 1223 1248
-		H.P.	.50 .57 .64	.72 .80 .89	$^{.99}_{1.20}$	$ \begin{array}{c} 1.32 \\ 1.44 \\ 1.59 \end{array} $	$ \begin{array}{c} 1.74 \\ 1.88 \\ 2.05 \end{array} $	$2.22 \\ 2.40 \\ 2.59 $	2.79 3.00 3.22
7/n C	° 8/	R.P.M.	770 785 803	823 840 860	880 903 925	948 970 993	1018 1043 1065	1090 1113 1138	1163 1190 1218
-		Н. Р.	.44 .50	.64 .71 .80	.89 .98 1.09	$ \begin{array}{c} 1.20 \\ 1.33 \\ 1.46 \end{array} $	$ \begin{array}{c} 1.59 \\ 1.74 \\ 1.89 \end{array} $	2.06 2.23 2.42	2.61 2.82 3.01
3/11 C	° */	H.P. R.P.M.	725 743 760	780 800 820	840 863 888	910 932 958	980 1005 1030	$1055 \\ 1083 \\ 1108 \\ $	1133 1158 1185
0			.38 .43 .49	.56 .63 .71	.79 .88 .98	$ \begin{array}{c} 1.09 \\ 1.20 \\ 1.32 \end{array} $	$ \begin{array}{c} 1.45 \\ 1.59 \\ 1.74 \end{array} $	$ \begin{array}{c} 1.89 \\ 2.05 \\ 2.23 \end{array} $	$2.42 \\ 2.61 \\ 2.82 $
5.11 C		H.P. R.P.M.	678 695 713	735 755 778	800 822 845	870 893 918	943 968 993	$1020 \\ 1045 \\ 1070$	1098 1125 1150
-			.32 .37 .42	.48 .55 .62	.69 .78 .87	$^{.97}_{1.07}$	$ \begin{array}{c} 1.31 \\ 1.43 \\ 1.57 \\ 1.57 \end{array} $	$ \begin{array}{c} 1.71 \\ 1.87 \\ 2.03 \end{array} $	2.23 2.41 2.61
17n C		R.P.M.	623 645 665	685 708 733	755 778 802	828 853 878	903 928 955	980 1005 1032	1062 1090 1118
6		Н. Р.	.26 .30 .35	.40 .46 .52	.59 .67 .75	$.84 \\ .94 \\ 1.04$	$ \begin{array}{c} 1.15 \\ 1.28 \\ 1.41 \\ 1.41 \end{array} $	$1.55 \\ 1.70 \\ 1.87 \\ $	2.05 2.24 2.44
3./" C		R.P.M.	568 590 613	635 658 680	705 730 755	780 805 830	858 885 912	940 968 998	1025 1055 1082
6		H.P.	.20 .23	.32 .37 .43	.49 .56	.71 .81 .91	$1.01 \\ 1.13 \\ 1.26 \\ 1.26$	$ \begin{array}{c} 1.39 \\ 1.55 \\ 1.71 \end{array} $	1.87 2.04 2.23
17" C		R.P.M.	503 525 548	573 598 625	650 678 703	728 755 785	813 843 870	900 928 958	985 1018 1048
ls	Outlet Velocity Pt. per Min. Capacity Cu. Ft. Air per Min. Press.		.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
 			2330 2570 2800	$3030 \\ 3270 \\ 3500 $	$3760 \\ 3970 \\ 4200 $	4430 4670 4900	5130 5370 5660	5830 6070 6300	6530 6770 7000
			1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

NO. 4 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

10	n D O - C	JONOI	<u> </u>	1	0 11 1			
Ъ.	H. P.	2.98	3.11 3.23 3.37	3.55 3.76 4.01	4.27 4.54 4.82	5.12 5.43 5.74	$6.06 \\ 6.40 \\ 6.75$	7.10 7.87 8.72
3 ½″ S.	R.P.M.	1465	1478 1490 1503	$1515 \\ 1528 \\ 1540 $	1555 1573 1590	$1608 \\ 1625 \\ 1645$	$1665 \\ 1685 \\ 1705 \\ $	1725 1765 1805
4	Н. Р.	2.47	2.58 2.71 2.87	3.06 3.29 3.51	$3.76 \\ 4.00 \\ 4.26$	4.53 4.80 5.09	5.39 5.71 6.03	6.35 7.09 7.87
3" S.	R. P. M.	1368	1380 1395 1408	1420 1435 1450	1465 1483 1500	1520 1540 1560	1580 1600 1620	$1640 \\ 1685 \\ 1728 \\ -$
S. P.	Н. Р.	1.81 1.90 1.99	$2.11 \\ 2.26 \\ 2.43 \\ 2.43$	2.62 2.82 3.02	$3.24 \\ 3.46 \\ 3.69$	3.94 4.19 4.45	4.73 5.02 5.31	5.63 6.32 7.04
2 1/2"	R.P.M.	1240 1250 1263	1275 1290 1305	1320 1338 1355	1373 1390 1410	1430 1450 1470	1490 1513 1533	1555 1598 1645
S. P.	Н. Р.	$1.39 \\ 1.47 \\ 1.58 \\ $	$1.71 \\ 1.86 \\ 2.02$	$2.19 \\ 2.54 \\ 2.54$	2.73 2.93 3.14	3.35 3.55 3.58 3.83	4.08 4.34 4.62	4.93 5.56 6.23
2" S	R.P.M.	1123 1135 1150	1163 1178 1195	1213 1230 1250	1270 1288 1308	1328 1350 1373	1395 1418 1438	1460 1508 1555
S. P.	Н. Р.	$1.01 \\ 1.15 \\ 1.23$	$1.35 \\ 1.47 \\ 1.61 \\ $	$1.74 \\ 1.89 \\ 2.05$	$2.21 \\ 2.39 \\ 2.57$	$2.77 \\ 2.98 \\ 3.19$	3.42 3.67 3.92	4.19 4.75 5.36
1 1/2"	R.P.M.	995 1008 1023	1040 1058 1075	1095 1115 1135	1155 1178 1198	1220 1243 1265	1288 1310 1335	1360 1408 1455
S. P.	Н. Р.	.86 .95 1.05	$1.16 \\ 1.27 \\ 1.39 \\ 1.39$	$1.52 \\ 1.65 \\ 1.80$	$1.96 \\ 2.12 \\ 2.29$	2.47 2.68 2.88	$3.10 \\ 3.33 \\ 3.56 \\ 3.56$	3.81 4.32 4.92
1 14"	R.P.M.	920 938 955	973 993 1010	1028 1050 1073	$1095 \\ 1118 \\ 1140$	1163 1185 1210	1233 1258 1280	1305 1355 1403
	noi bbA Pres	.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	Capacity Air per	2800 3030 3270	3500 3730 3970	4200 4430 4670	4900 5130 5370	5660 5830 6070	6300 6530 6770	7000 7460 7930
Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

D STATIC PRESSURE	
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T) CAPACITIES	AT 70° F. AND 29.02 INCHES RADOMETER
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7 TURBO-CONOIDAL FAN (TYPE T) C	AT
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	ď	H.P.	.76 .80 .90	1.01 1.12 1.24	1.37 1.51 1.65	$ \begin{array}{c} 1.81 \\ 1.98 \\ 2.16 \end{array} $	2.36 2.56 2.78	3.00 3.24 3.50	3.76 4.01 4.33
	1" S.	R. P. M.	725 736 751	767 782 800	818 838 856	876 893 913	936 958 978	998 1020 1042	$1064 \\ 1087 \\ 1109 $
	7, 8 S. P.	H.P.	.63 .72 .81	$ \begin{array}{c} .90 \\ 1.01 \\ 1.12 \end{array} $	$ \begin{array}{c} 1.25 \\ 1.38 \\ 1.52 \end{array} $	$ \begin{array}{c} 1.67 \\ 1.83 \\ 2.01 \end{array} $	$2.20 \\ 2.38 \\ 2.59 $	2.81 3.03 3.28	3.53 3.79 4.08
		R.P.M.	685 698 713	731 747 765	782 802 822	842 862 882	904 927 947	969 989 1011	$1033 \\ 1058 \\ 1082 \\ $
	34" S. P.	H.P.	.56 .63 .72	$^{-81}_{-90}$	$ \begin{array}{c} 1.12 \\ 1.25 \\ 1.38 \end{array} $	$ \begin{array}{c} 1.52 \\ 1.68 \\ 1.84 \end{array} $	$2.02 \\ 2.20 \\ 2.39 \\ 2.39$	$2.60 \\ 2.83 \\ 3.06$	3.30 3.56 3.82
		R. P. M.	645 660 676	693 711 729	747 767 789	809 829 851	871 893 916	933 962 985	$1007 \\ 1029 \\ 1053$
	5%" S. P.	H.P.	.48 .55 .63	.71 .79 .89	$ \begin{array}{c} 1.00 \\ 1.12 \\ 1.24 \end{array} $	$ \begin{array}{c} 1.38 \\ 1.52 \\ 1.68 \end{array} $	$ \begin{array}{c} 1.83 \\ 2.01 \\ 2.20 \end{array} $	$2.39 \\ 2.60 \\ 2.82 $	3.06 3.31 3.56
		R. P. M.	602 618 633	653 671 691	711 731 751	$\begin{array}{c} 773\\793\\816\end{array}$	838 860 882	907 929 951	976 1000 1022
	½″ S. P.	H.P.	.40 .46	.60 .69 .78	$^{.88}_{.98}$	$ \begin{array}{c} 1.22 \\ 1.36 \\ 1.50 \end{array} $	$ \begin{array}{c} 1.65 \\ 1.81 \\ 1.99 \end{array} $	2.18 2.37 2.57	2.82 3.05 3.30
		R. P. M.	553 573 591	609 629 651	671 691 713	736 758 780	802 825 849	871 893 918	945 969 993
	38" S. P.	H.P.	.33 .38 .44	.51 .58 .66	.75 .85 .96	$1.07 \\ 1.19 \\ 1.32 \\ 1.32$	$\begin{array}{c} 1.46\\ 1.62\\ 1.78\end{array}$	$ \frac{1.97}{2.15} $	2.59 2.83 3.09
		R.P.M.	505 525 545	565 585 605	627 649 671	693 716 738	762 787 811	836 860 887	911 938 962
	}₄" S. P.	H.P.	.25 .29 .35	.41 .47 .54	.62 .70 .80	$^{.90}_{1.15}$	$ \begin{array}{c} 1.28 \\ 1.43 \\ 1.59 \end{array} $	$1.76 \\ 1.96 \\ 2.16$	2.37 2.58 2.83
		R.P.M.	447 467 487	509 531 556	578 602 625	647 671 698	722 749 773	800 825 851	876 905 931
		Add for Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	2950 3250 3540	3840 4130 4430	4720 5020 5310	5610 5910 6200	6500 6790 7090	7380 7680 7970	8270 8560 8860
	Outlet Velocity Pt. per Min.		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

 $3.94 \\ 4.09 \\ 4.26 \\ 4.26 \\ 100 \\$ 4.49 4.76 5.07 5.41 5.74 6.10 $6.48 \\ 6.87 \\ 7.26$ 7.678.10 8.54 8.98 9.96 1.0 H.P. 3.77 3 ½" S. P. R. P. M. 382 395 413 429 445 462 302 313 323 336 1347 1358 1358 1480 1498 1516 1531 1569 1605 H. P. 3.13 $3.26 \\ 3.42 \\ 3.63 \\ 3.63 \\$ 8.94 9.96 3.87 4.16 4.45 4.75 5.07 5.39 5.73 5.07 5.44 5.83 7.23 7.64 ď ŝ R. P. M. ž 1404 1422 1440 216 1227 1240 1251 1262 1274 289 1302 1318 1333 351 369 387 458 498 536 Н. Р. 2.292.402.522.662.2.863.07 $3.32 \\ 3.57 \\ 3.82 \\ 3.82 \\$ L.10 L.38 L.66 4.98 5.31 5.63 5.98 5.35 5.72 7.13 8.00 8.91 4 ŝ 2 1/2" R. P. M. INCHES BAROMETER $102 \\ 111 \\ 122$ $325 \\ 345 \\ 362 \\ 362 \\$ 1382 1420 1462 133 147 160 173 1220 1236 1253 271 289 308 ď $1.76 \\ 1.86 \\ 2.00 \\ 2.00 \\ 1.76 \\$ 2.172.362.562.772.983.213.453.703.974.24 4.53 4.84 5.165.495.846.247.04 7.89 ÷ ď ŝ R. P. M. à 1033 1047 062 $129 \\ 144 \\ 162$ 180 200 220 240 260 278 $298 \\ 340 \\ 382 \\ 382$ 998 1009 1022 078 093 111 F. AND 29.92 Н. Р. $1.71 \\ 1.86 \\ 2.03 \\ 2.03$ $2.20 \\ 2.40 \\ 2.59$ 2.803.023.253.50 3.77 4.04 5.30 6.01 6.73 1.28 4.33 4.64 4.96 1 1/2" S. P. R. P. M. 144 1165 884 896 909 924 940 956 973 991 009 027 047 065 1085 1105 1125 209 251 293 200 ď .208.333 .47 .61 .76 $1.92 \\ 2.09 \\ 2.28 \\$ 2.472.682.903.133.393.654.825.476.233.92 1.21 AT 114" S. P. Ĥ R. P. M. 818 833 849 864 882 898 913 933 953 973 993 013 033 053 076 1118 $160 \\ 205 \\ 247$ 275 302 330 $360 \\ 390 \\ 422$ $141 \\ 160 \\ 180$ 202 225 2250 455 489 525 560 638 721 090 122 Press. Add for Total Capacity Cu. Ft. Air per Min. 5310 5610 5910 5200 5500 5790 7090 7380 7680 7970 8270 8560 SS60 9450 0040 3540 3840 4130 4430 4720 5020 200 300 400 500 800 1900 2100 22000 2300 2400 2500 2600 2700 2800 2900 3200 Outlet Velocity Ft. per Min.

NO. 41/2 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES

DAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES	AT 70° F. AND 29.92 INCHES BAROMETER
. 5 TURBO-CONOIDAL FA	AT 70° F.
SC	

							001	
<u> </u>	H.P.	$.94 \\ .99 \\ 1.11$	$ \begin{array}{c} 1.24 \\ 1.38 \\ 1.53 \end{array} $	$ \begin{array}{c} 1.69 \\ 1.86 \\ 2.04 \end{array} $	2.24 2.44 2.67	$2.91 \\ 3.16 \\ 3.43$	3.71 4.00 4.32	4.65 4.98 5.35
1″ S.	R. P.M.	652 662 676	690 704 720	736 754 770	788 804 822	842 862 880	898 918 938	958 978 998
Р.	H.P.	.78 .89 1.00	$ \begin{array}{c} 1.12 \\ 1.25 \\ 1.39 \end{array} $	$1.54 \\ 1.70 \\ 1.87 \\ $	$2.06 \\ 2.26 \\ 2.48 \\ 2.48 \\$	$2.71 \\ 2.94 \\ 3.20$	3.47 3.74 4.05	4.36 4.68 5.04
7,8" S.	R. P. M.		$658 \\ 672 \\ 688 \\ 088 $	704 722 740	758 776 794	814 834 852		930 952 974
. P.	H.P.	.69 .78 .89	$1.00 \\ 1.11 \\ 1.24 \\ 1.24$	$ \begin{array}{c} 1.38 \\ 1.54 \\ 1.70 \end{array} $	$ \begin{array}{c} 1.88 \\ 2.08 \\ 2.27 \end{array} $	$2.49 \\ 2.72 \\ 2.95$	$3.22 \\ 3.49 \\ 3.78 \\ 3.78 \\$	4.08 4.40 4.72
34" S.	R. P. M.	580 594 608	$624 \\ 640 \\ 656$	672 690 710	728 746 766	784 804 824	844 866 886	906 926 948
ď	H.P.	.59 .68 .77	$^{-87}_{-98}$	$ \begin{array}{c} 1.24 \\ 1.38 \\ 1.53 \end{array} $	${1.70 \\ 1.88 \\ 2.07 }$	2.26 2.48 2.71	2.95 3.21 3.48	$3.79 \\ 4.08 \\ 4.40$
.5%" S.	R. P. M.	542 556 570	588 604 622	640 658 676	696 714 734	754 774 794	816 836 856	878 900 920
Р.	H.P.	.50 .57 .66	.75 .85 .96	$ \begin{array}{c} 1.08 \\ 1.21 \\ 1.36 \\ 1.36 \end{array} $	$ \begin{array}{c} 1.51 \\ 1.68 \\ 1.85 \\ 1.85 \end{array} $	$2.04 \\ 2.23 \\ 2.45$	$2.68 \\ 2.93 \\ 3.18 \\$	$3.48 \\ 3.76 \\ 4.08 \\ 4.08 \\ 108 \\ $
<u>}∕</u> 2″ S.	R. P. M.	$\frac{498}{516}$	$548 \\ 566 \\ 586$	604 622 642	662 682 702	722 742 764	784 804 826	850 872 894
ď	H.P.	.40 .47 .54	.63 .72 .82	$^{.93}_{1.05}$	$ \begin{array}{c} 1.32 \\ 1.47 \\ 1.63 \end{array} $	$ \begin{array}{c} 1.80 \\ 2.00 \\ 2.20 \end{array} $	$2.43 \\ 2.66 \\ 2.91$	3.20 3.50 3.81
³ / ₈ " S.	R. P. M.	454 472 490	508 526 544	564 584 604	624 644 664	686 708 730	752 774 798	820 844 866
P.	H.P.	.31 .36 .43	.50 .58 .67	.77 .87 .99	$ \begin{array}{c} 1.12 \\ 1.26 \\ 1.42 \end{array} $	$1.58 \\ 1.77 \\ 1.96 \\ 1.96$	$2.18 \\ 2.41 \\ 2.66 \\ 2.66$	2.93 3.19 3.49
1√" S.	R. P.M.	402 420 438	458 478 500	520 542 562	582 604 628	650 674 696	720 742 766	788 814 838
	Add for Pres	.060 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
Capacity Cu. Ft. Air per Min.		3650 4010 4380	$4740 \\ 5100 \\ 5470 \\$	5830 6200 6560	6930 7290 7660	8020 8380 8750	$\begin{array}{c} 9110\\ 9480\\ 9840\\ 9840 \end{array}$	$10200 \\ 10570 \\ 10940$
elocity Min.	Outlet Ver	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

S. P.	Н. Р.	4.65	4.87 5.05 5.26	5.54 5.88 6.26	6.68 7.09 7.53	8.00 8.48 8.96	$ \begin{array}{c} 9.46 \\ 10.0 \\ 10.5 \end{array} $	11.1 12.3 13.6
3 35"	R. P. M. H.	1172	1182 1192 1202	1212 1222 1232	1244 1258 1272	1286 1300 1316	1332 1348 1364	1378 1412 1444
S. P.	Н. Р.	3.87	4.03 4.23 4.48	4.78 5.14 5.49	5.87 6.26 6.65	7.95 7.95	8.43 8.93 9.43	9.93 11.1 12.3
S. P. 3" S	R.P.M.	1094	1104 1116 1126	1136 1148 1160	1172 1186 1200	1216 1232 1248	1264 1280 1296	1312 1348 1382
	Н. Р.	2.83 2.97 3.11	3.29 3.53 3.79	4.10 4.41 4.72	5.06 5.41 5.76	6.15 6.55 6.96	7.39 7.84 8.30	$ 8.80 \\ 9.87 \\ 11.0 $
2 3/5"	R.P.M.	992 1000 1010	$1020\\1032\\1044$	$1056 \\ 1070 \\ 1084 $	1098 1112 1128	1144 1160 1176	1192 1210 1226	$1244 \\ 1278 \\ 1316 \\ 1316 \\ 1316 \\ 1218 \\ $
S. P.	н. Р.	2.18 2.29 2.47	$2.68 \\ 2.91 \\ 3.16$	3.42 3.68 3.96	4.26 4.57 4.90	5.23 5.60 5.98	6.38 6.78 7.21	7.70 8.69 9.74
2" 5	R. P. M.	898 908 920	930 942 956	970 984 1000	1016 1030 1046	1062 1080 1098	1116 1134 1150	$1168 \\ 1206 \\ 1244$
S. P.	Н. Р.	$1.58 \\ 1.79 \\ 1.91 \\ $	$2.11 \\ 2.30 \\ 2.51 \\ 2.51 \\ 2.51 \\ 3.61 \\ $	$2.72 \\ 2.96 \\ 3.20$	3.46 3.73 4.01	4.33 4.65 4.99	5.35 5.73 6.12	6.54 7.43 8.38
1 35"	R.P.M.	796 806 818	832 846 860	876 892 908	924 942 958	976 994 1012	1030 1048 1068	1088 1126 1164
S. P.	Н. Р.	$1.34 \\ 1.49 \\ 1.65$	$1.81 \\ 1.99 \\ 2.18$	2.37 2.58 2.81	3.06 3.31 3.58	3.87 4.19 4.50	4.84 5.20 5.57	5.95 6.76 7.69
"}{ I	R.P.M.	736 750 764	778 794 808	$\begin{array}{c} 822 \\ 840 \\ 858 \end{array}$	876 894 912	930 948 968	986 1006 1024	1044 1084 1122
Add for Total Press.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
Capacity Cu. Ft. Air per Min.		4380 4740 5100	5470 5830 6200	6560 6930 7290	7660 8020 8380	8750 9110 9480	9840 10200 10570	10940 11660 12390
	Outlet / Ft. per	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

E TUDBO CONOLDAL BAN

IC PRESSURES	
STATIC	×
AND	METE
ITIES	BAROME
FAN (TYPE T) CAPACITIES	AT 70° F. AND 29.92 INCHES E
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TYPE	29.92
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AL	.0
TURB0-CONOIDA	AT 7
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NO. 5	

N	ENO	GINEE	RING	- B U I	FFAL	0 F0	RGE	СОМ	PANY
	Ŀ.	Н.Р.	$ \frac{1.14}{1.20} $	$ \begin{array}{c} 1.50 \\ 1.67 \\ 1.85 \end{array} $	2.05 2.25 2.47	2.71 2.95 3.23	$3.52 \\ 3.82 \\ 4.14$	4.49 4.84 5.22	$5.62 \\ 6.02 \\ 6.47$
	1″ S.	R.P.M.	593 602 615	627 640 655	669 686 700	716 731 747	766 784 800	816 835 853	871 889 907
	ď	H.P.	.95 1.08 1.21	$ \begin{array}{c} 1.36 \\ 1.51 \\ 1.68 \\ 1.68 \end{array} $	$ \begin{array}{c} 1.86 \\ 2.05 \\ 2.26 \end{array} $	$2.49 \\ 2.73 \\ 3.00$	3.28 3.56 3.87	4.20 4.53 4.90	5.27 5.67 6.10
	7,8" S.	R.P.M.	560 571 584	598 611 626	640 656 673	689 706 722	740 758 775	793 809 827	846 866 886
	P.	н.Р.	.83 .95 1.07	$ \begin{array}{c} 1.20 \\ 1.35 \\ 1.50 \end{array} $	$ \begin{array}{c} 1.67 \\ 1.86 \\ 2.06 \end{array} $	2.28 2.51 2.75	$3.01 \\ 3.29 \\ 3.57 \\ 3.57 \\$	$3.89 \\ 4.22 \\ 4.57 \\ 4.57 \\ $	4.93 5.32 5.71
4	34" S.	R.P.M.	527 540 553	567 582 596		662 678 696	713 731 749	767 787 806	824 842 862
	ď	H.P.	.71 .82 .93	$ \begin{array}{c} 1.05 \\ 1.19 \\ 1.34 \end{array} $	$1.50 \\ 1.67 \\ 1.86 \\ 1.86$	2.05 2.27 2.50	$2.74 \\ 3.00 \\ 3.28 \\ $	3.57 3.88 3.88 4.21	4.58 4.94 5.32
	58" S.	R.P.M.	493 506 518	535 549 566	582 598 615	633 649 667	686 704 722	742 760 778	798 818 836
	<u>.</u>	H.P.	.79 .79	$ \begin{array}{c} .90 \\ 1.03 \\ 1.16 \end{array} $	1.31 1.47 1.64	$ \begin{array}{c} 1.83 \\ 2.03 \\ 2.24 \end{array} $	2.47 2.70 2.97	$3.24 \\ 3.54 \\ 3.85 \\ 3.85$	4.21 4.55 4.93
1107 744	12" S.	R.P.M.	453 469 484	498 515 533	549 566 584	602 620 638	656 675 695	713 731 751	773 793 813
:	Ъ.	H.P.	.49 .56 .65	.76 .87 .99	$ \begin{array}{c} 1.12 \\ 1.27 \\ 1.43 \end{array} $	$ \begin{array}{c} 1.59 \\ 1.78 \\ 1.97 \\ 1.97 \end{array} $	2.18 2.42 2.66	2.94 3.21 3.53	3.87 4.23 4.61
	3″" S.	R.P.M.	413 429 446	462 478 495	513 531 549	567 585 604	624 644 664	684 704 726	745 767 787
	4.	H.P.	.37 .44 .52	.61 .70 .81	$ \begin{array}{c} .93\\ 1.05\\ 1.19\end{array} $	$ \begin{array}{c} 1.35 \\ 1.53 \\ 1.71 \\ 1.71 \end{array} $	$ \begin{array}{c} 1.91 \\ 2.14 \\ 2.37 \end{array} $	$2.64 \\ 2.92 \\ 3.22 \\$	$3.54 \\ 3.86 \\ 4.22 \\ 4.22 \\ 1.22 \\ $
	¥" S.	R. P. M.	366 382 398	416 435 455	473 493 511	529 549 571	591 613 633	655 675 697	716 740 762
	Outlet Velocity Ft. per Min. Capacity Cu. Ft. Air per Min. Press.		.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
			4410 4850 5290	5730 6170 6620	7060 7500 7940	8380 8820 9260	9700 10140 10590	11030 11470 11910	12350 12790 13230
			1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

PRESSURES	
STATIC	
S AND	OMETER
CAPACITIES	BALON
CAPA	CHES
F	Z
(TYPE	29.92 INCHES
FAN	AND .
-	Ω,
CONOIDA	AT 70° F.
TURB0-CON	AT
5 3%	
NO.	

S. P.	H. P.	5.63	$5.89 \\ 6.11 \\ 6.36$	6.70 7.11 7.58	8.08 8.58 9.11	9.68 10.3 10.9	11.5 12.1 12.8	13.4 14.9 16.5
3 3/2"	R. P. M.	1066	1075 1083 1093	11102 11111 11120	1131 1144 1156	1169 1182 1197	1211 1226 1240	1253 1284 1313
P.	H. P.	4.68	4.88 5.11 5.43	5.78 6.21 6.64	7.10 7.57 8.05	$ \begin{array}{c} 8.56 \\ 9.08 \\ 9.62 \end{array} $	10.2 10.8 11.4	12.0 13.4 14.9
3″ S.	R. P. M.	995	1004 1015 1024	1034 1044 1055	1066 1078 1091	1106 1120 1135	1149 1164 1178	1193 1226 1257
S. P.	Н. Р.	3.42 3.59 3.77	3.98 4.27 4.58	4.96 5.33 5.71	6.12 6.54 6.97	7.44 7.93 8.42	8.94 9.48 10.1	10.7 12.0 13.3
2 3/5"	R.P.M.	902 909 918	927 938 949	960 973 986	998 1011 1026	1040 1055 1069	1084 1100 1115	1131 1162 1196
e.	Н. Р.	2.63 2.77 2.99	3.24 3.52 3.82	4.14 4.46 4.80	5.16 5.53 5.93	6.33 6.77 7.23	7.72 8.20 8.73	9.32 10.5 11.8
2″ S.	R. P. M.	816 826 836	846 856 869	882 895 909	924 936 951	966 982 998	1015 1031 1045	1062 1097 1131
S. P.	Н. Р.	$ \begin{array}{c} 1.91 \\ 2.17 \\ 2.31 \\ \end{array} $	$2.55 \\ 2.78 \\ 3.03 \\$	3.29 3.58 3.87	4.18 4.51 4.86	5.23 5.63 6.04	6.47 6.93 7.41	7.91 8.99 10.1
1 1/2"	R.P.M.	724 733 744	756 769 782	796 811 826	840 856 871	887 904 920	936 953 971	989 1024 1058
S. P.	Н. Р.	$ \begin{array}{c} 1.62 \\ 1.80 \\ 1.99 \end{array} $	2.19 2.41 2.63	2.87 3.13 3.40	3.70 4.01 4.33	4.68 5.07 5.45	5.85 6.29 6.74	7.20 8.17 9.29
1 1/4 1	R.P.M.	669 682 695	707 722 735	747 764 780	796 813 829	846 862 880	896 915 931	949 986 1020
Add for Total Press.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
Capacity Cu. Ft. Air per Min.		5290 5730 6170	6620 7060 7500	7940 8380 8820	9260 9700 10140	10590 11030 11470	11910 12350 12790	13230 14110 15000
elocity Min.	Outlet V Ft. per	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

D M C	JINEE	RINU.	D U 1	TAL	0 1
å	H.P.	1.60	$ \begin{array}{c} 1.79 \\ 1.99 \\ 2.20 \end{array} $	2.43 2.68 2.93	3.22 3.51 3.84
l" S.	R. P. M.	563	575 587 600	613 628 642	657 670 685
ď	H.P.	$ \begin{array}{c} 1.13 \\ 1.28 \\ 1.44 \end{array} $	$ \begin{array}{c} 1.61 \\ 1.80 \\ 2.00 \end{array} $	$2.22 \\ 2.45 \\ 2.69 $	2.97 3.25 3.57
7.8" S.	R.P.M.	513 523 535	548 560 573	587 602 617	632 647 662
ď	H.P.	$^{+}_{-1.28}$	$ \begin{array}{c} 1.43 \\ 1.60 \\ 1.79 \end{array} $	$ \begin{array}{c} 1.99 \\ 2.22 \\ 2.45 \end{array} $	$2.71 \\ 2.99 \\ 3.27 \\ 3.27 \\$
34" S.	R.P.M.	483 495 507	520 533 547	560 575 592	607 622 638
-i	H.P.	.85 .98 1.11	$ \begin{array}{c} 1.25 \\ 1.41 \\ 1.59 \end{array} $	$ \begin{array}{c} 1.78 \\ 1.98 \\ 2.21 \end{array} $	2.45 2.70 2.98
5,8" S	R. P. M.	452 463 475	490 503 518	533 548 563	580 595 612
NO. 6 TURBO-CONOIDAL FAN (TVPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER AT Y" S. P. CURPE Float Y" S. P. CURPE Each U Y" S. P. Y" S. P. Y" S. P. Y" S. P. CURPE Each U P. P. M. H.P. R. P. M. H.P.	$ \begin{array}{c} 1.56 \\ 1.75 \\ 1.96 \end{array} $	2.17 2.41 2.67			
	R.P.M.	415 430 443	457 472 488	503 518 535	552 562 585
	.58 .67 .78	$^{.90}_{1.03}$	$ \begin{array}{c} 1.34 \\ 1.51 \\ 1.70 \end{array} $	$ \begin{array}{c} 1.89 \\ 2.12 \\ 2.34 \end{array} $	
	R.P.M.	378 393 408	423 438 453	470 487 503	520 537 553
	H.P.	0.44 0.52 0.62	$\begin{array}{c} 0.72 \\ 0.84 \\ 0.96 \end{array}$	$ \begin{array}{c} 1.10 \\ 1.25 \\ 1.42 \end{array} $	$ \begin{array}{r} 1.61 \\ 1.82 \\ 2.04 \end{array} $
	R.P.M.	335 350 365	382 398 417	433 452 468	485 503 523
		.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275
Cu. Ft.	Сарасіtу Аіт рег	5250 5770 6300	6820 7350 7870	8400 8920 9450	9970 10500 11020
Min.	Outlet Vo Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100
	Іі Ії Ії	HeHeMinMinMinMinHeMinMinMinMinMinMinMaterityMin	Hú Hú Hú Ná" S. P. Ná" S. P.	Hit Hit <th>$\begin{array}{ c c c c c c c c c c c c c c c c c c c$</th>	$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$

6.697.17 7.71

798 315 332 332

 $6.27 \\ 6.74 \\ 7.25 \\ 7.25 \\$

775 793 793 312

 $5.87 \\ 6.34 \\ 6.80$

755 772 790

5.455.886.34

732

5.015.425.87

727

4.61 5.04 5.49

683 703 722

4.214.595.02

657 678 698

489 525 560

4700 5220 5750

2800 2900 3000

4.1944.93

718733

 $3.90 \\ 4.23 \\ 4.61 \\ 4.61 \\ 100 \\$

578 595 710

 $3.58 \\ 6.91 \\ 4.25$

5553 570 587

3.263.583.91

328 545 562

 $2.94 \\ 3.22 \\ 3.53 \\$

502 518 337

 $2.59 \\ 2.87 \\ 3.17 \\ 3.17 \\$

572 590 308

 $2.282 \\ 2.55 \\ 2.82 \\ 2.82 \\ 2.82 \\ 3.82 \\$

542 562 580

302 330 360

15502070 2600

2200 2300 2400

5.345.766.21

748 765 782

5.005.395.83

727 742 758

4.635.035.44

722 738

 $4.25 \\ 4.62 \\ 5.01 \\ 5.01 \\$

580 597 713

 $3.85 \\ 4.21 \\ 4.58 \\ 4.58 \\ 158 \\ 120 \\$

653 670 688

 $3.50 \\ 3.82 \\ 4.20 \\ 1$

627 645 665

 $3.14 \\ 3.47 \\ 3.83 \\ 3.83$

600 618 638

 $\frac{390}{422}$

13120 13650 14170

2500 2600 2700

-									
	S. P.	Н. Р.	6.70	7.01 7.27 7.57	7.98 8.46 9.02	$9.61 \\ 10.21 \\ 10.84$	$ \begin{array}{c} 11.52 \\ 12.20 \\ 12.91 \end{array} $	$13.63 \\ 14.40 \\ 15.17$	15.97 17.71 19.62
	3 ½" S. P.	R. P. M.	277	$ \begin{array}{c} 985 \\ 993 \\ 1002 \end{array} $	$1010 \\ 1018 \\ 1027 \\ 1027 \\$	1037 1048 1060	$1072 \\ 1083 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1097 \\ 1008 \\ $	1110 1123 1137	1148 1177 1203
FAN (TYPE T) CAPACITIES AND STATIC PRESSURES F. AND 29.92 INCHES BAROMETER	S. P.	Н. Р.	5.57	$5.80 \\ 6.09 \\ 6.46 $	6.88 7.39 7.91	$ \begin{array}{c} 8.45 \\ 9.01 \\ 9.58 \end{array} $	$10.19 \\ 10.80 \\ 11.45$	12.13 12.85 13.57	$14.29 \\ 15.95 \\ 17.71$
	3" 5	R.P.M.	910	920 930 938	947 957 967	977 988 1000	1013 1027 1040	1053 1067 1080	1093 1123 1152
ATIC PI	S. P.	Н. Р.	4.07 4.27 4.48	4.74 5.08 5.46	$5.90 \\ 6.34 \\ 6.80 \\ 6.80 \\$	$7.28 \\ 7.78 \\ 8.29 \\ 8.29$		10.64 11.29 11.95	12.67 14.21 15.84
AND ST METER	2 1/2"	R.P.M.	827 833 842	850 860 870	880 892 903	$ \begin{array}{c} 915 \\ 927 \\ 940 \end{array} $	953 967 980	993 1008 1022	1037 1065 1097
VPE T) CAPACITIES AND ST 29.92 INCHES BAROMETER	S. P.	Н. Р.	3.13 3.30 3.56	$3.85 \\ 4.19 \\ 4.55$	4.93 5.30 5.71	6.14 6.58 7.06	$7.54 \\ 8.06 \\ 8.61 \\ 8.61$	9.18 9.76 10.39	$11.09 \\ 12.51 \\ 14.02$
) CAPA	2" S	R. P. M.	748 757 767	775 785 797	808 820 833	847 858 872	885 900 915	930 945 958	973 1005 1037
TYPE 1 D 29.92	½" S. P.	Н. Р.	2.29 2.58 2.76	3.03 3.31 3.61	$3.92 \\ 4.26 \\ 4.61$	4.98 5.37 5.78	6.23 6.70 7.18	7.70 8.24 8.82	$9.42 \\ 10.69 \\ 12.06$
	1 1%	R. P. M.	663 672 682	693 705 717	730 743 757	770 785 798	813 828 843	858 873 890	907 938 970
AT 70°	S. P.	Н. Р.	$ \begin{array}{c} 1.93 \\ 2.14 \\ 2.37 \end{array} $	2.61 2.87 3.13	3.42 3.72 4.05	$4.40 \\ 4.77 \\ 5.16$	5.57 6.03 6.48	6.96 7.49 8.02	$ \begin{array}{c} 8.57 \\ 9.73 \\ 9.73 \\ 11.06 \end{array} $
6 TURBO-CONOIDAL AT 70°	1 1/4"	R.P.M.	613 625 637	648 662 673	685 700 715	730 745 760	775 790 807	822 838 853	870 903 935
NO. 6 TU	IstoT .28	rot bbA Pres	.090 .106 .122	.141 .160 .180	202 225 250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	Cu. Ft.	Capacity Air per	6300 6820 7350	7870 8400 8920	9450 9970 10500	11020 11550 12070	12600 13120 13650	$14170 \\ 14700 \\ 15220 \\ 15220 \\ 1$	15750 16790 17850
	elocity. Min.	Outlet V Ft. per	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3200 3200 3400

T) CAPACITIES AND STATIC PRESSURES INCHES BAROMETER 29.92 NO. 6 ½ TURBO-CONOIDAL FAN (TYPE AND Ľ. 20° AT

R. P. M. H. P. $3.78 \\ 4.12 \\ 4.50$ $6.27 \\ 6.76 \\ 7.29 \\ 7.29$ 1.591.671.88 $2.10 \\ 2.33 \\ 2.59$ 2.863.14 3.44 4.91 5.34 5.79 7.85 8.41 9.04 ď 1″ S. 606 619 632 531 542 554 566 592 592 648 663 677 691 722 722 737 752 768 502 R.P.M. H.P. $3.48 \\ 3.81 \\ 4.18 \\ 1.18 \\$ 4.58 4.97 5.40 1.321.511.70 $1.89 \\ 2.11 \\ 2.35 \\ 2.35 \\ 1.89 \\$ $2.60 \\ 2.87 \\ 3.16$ $5.87 \\ 6.32 \\ 6.84$ 7.367.91 8.51 d, ŝ .8 174 506517 542569 583 597 311 326 342 355 371 385 700 715 732 749 R. P. M. H. P. $\frac{1.68}{1.88}
 2.10$ 4.204.594.99 $5.44 \\ 5.90 \\ 6.38$ $6.89 \\ 7.44 \\ 7.98 \\ 7.98 \\$.16 2.342.602.87 $3.18 \\ 3.51 \\ 3.84 \\ 3.84$ 4 ŝ 34" 492 505 697 712 729 146 157 168 517 531 546 560 574 589 503 519 534 649 666 682 R. P. M. H. P. .15 1.471.661.862.092.332.592.873.173.50 $3.82 \\ 4.20 \\ 4.58 \\ 4.58 \\ 100 \\$ $4.99 \\ 5.42 \\ 5.88 \\ 5.88 \\$ $6.39 \\ 6.90 \\ 7.44$ à ŝ 18 580 595 611 417 428 439 152 165 179 492 506 520 535 549 565 628 643 659 676 692 708 R. P. M. H. P. 84.96 1.261.441.621.832.052.302.552.833.133.135.87 6.36 6.89 $3.45 \\ 3.77 \\ 4.14 \\ 4.14$ 4.524.945.37à ŝ 2 383 397 409 422 436 451 465 479 494 509 525 540 555 571 588 503 519 535 654 671 688 Н. Р. 1.21 2.222.492.753.043.373.72 $4.10 \\ 4.49 \\ 4.92$ 1.57 5.415.916.442 ŝ R. P. M. 38" 391 405 480 511 349 363 377 434 449 465 528 545 562 579 595 614 631 649 666 R. P. M. H. P. $\frac{52}{61}$.85 .98 .13 1.29 $1.89 \\ 2.13 \\ 2.39 \\ 2.39 \\ 1.89 \\$ 2.672.993.31 $3.68 \\ 4.08 \\ 4.50 \\ 4.50 \\ 1.50 \\$ 4.945.395.89à ŝ 148 14 337 352 368 385 #17 #17 500 519 536 554 571 589 306 326 345 Press. 063 076 090 106 122 141 160 180 202 225 250 275 302 330 360 390 422 455 489 525 560 Add for Total 11700 2320 2940 13550 14170 14780 6160 6780 7390 8010 8620 9240 9860 0470 1090 5400 6020 6630 7250 7860 8480 Air per Min. Capacity Cu. Ft. 1600 1700 2000 2200 2300 2400 Outlet Velocity Ft. per Min. 2000 300 400 500 2500 2600 2700 0002

FAN ENGINEERING-BUFFALO FORGE COMPANY

	S. P.	H.P.	7.86	8.22 8.54 8.88	9.36 9.93 10.6	11.3 12.0 12.7	13.5 14.3 15.2	16.0 16.9 17.8	18.7 20.8 23.0
	3 ½″ S.	R.P.M.	902	909 917 925	932 940 948	957 968 979	989 1000 1012	$1025 \\ 1037 \\ 1049 \\ 1049 \\$	1060 1086 1111
	ъ.	Н. Р.	6.53	6.81 7.14 7.58	8.08 8.68 9.28	9.92 10.6 11.2	12.0 12.7 13.4	14.2 15.1 15.9	16.8 18.7 20.8
	3" S.	R.P.M.	842	849 859 866	874 883 892	902 912 923	936 948 960	972 985 997	1009 1037 1063
	S. P.	Н. Р.	4.78 5.01 5.26	5.56 5.96 6.40	6.92 7.45 7.98	8.55 9.13 9.73	10.4 11.1 11.8	12.5 13.3 14.0	14.9 16.7 18.6
	2 1/2"	R.P.M.	763 769 777	785 794 803	812 823 834	845 856 868	880 892 905	917 931 943	957 983 1012
	d.	Н. Р.	3.68 3.87 4.18	4.52 4.91 5.34	5.78 6.22 6.70	$7.20 \\ 7.72 \\ 8.23 \\ 8.23$	8.84 9.46 10.1	10.8 11.5 12.2	$13.0 \\ 14.7 \\ 16.5$
	2" S.	R.P.M.	691 699 708	716 725 735	746 757 769	782 792 805	817 831 845	859 872 885	899 928 957
	S. P.	Н. Р.	2.67 3.03 3.23	3.56 3.89 4.24	4.60 5.00 5.41	$5.84 \\ 6.30 \\ 6.79$	7.31 7.86 8.43	$9.03 \\ 9.68 \\ 10.4$	11.1 12.6 14.2
	1 1/2" 5	R.P.M.	613 620 . 629	640 651 661	674 686 699	711 725 737	751 765 779	792 806 822	837 866 896
	S. P.	Н. Р.	2.26 2.51 2.78	3.06 3.36 3.68	4.01 4.37 4.75	5.16 5.59 6.05	6.53 7.08 7.61	8.17 8.78 9.41	10.1 11.4 13.0
	114"	R.P.M.	566 577 588	599 611 622	632 646 660	674 688 702	716 729 745	759 774 788	803 834 863
T	Capacity Cu. Ft. Air per Min. Add for Total Press.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
3,			7390 8010 8620	9240 9860 10470	$11090 \\ 11700 \\ 12320$	$12940 \\ 13550 \\ 14170$	14780. 15400 16020	$16630 \\ 17250 \\ 17860$	$18480 \\ 19710 \\ 20940$
£1	Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 61/2 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

FAN	ENG	INEER	. I N G –	-BUF	FALO) FO	RGE	СОМ	PANY
		Н.Р.	$ \begin{array}{c} 1.84 \\ 1.94 \\ 2.18 \end{array} $	2.44 2.71 3.00	3.31 3.64 3.99	4.38 4.78 5.22	5.70 6.19 6.71	7.27 7.84 8.46	$9.10 \\ 9.76 \\ 10.5$
	1" S.	R. P. M. H. P.	466 473 483	493 503 514	526 539 550	563 574 587	602 616 629	642 656 670	684 699 713
10	Ŀ.	Н. Р.	$ \begin{array}{c} 1.53 \\ 1.75 \\ 1.97 \end{array} $	$2.20 \\ 2.45 \\ 2.72 \\ 2.72 \\$	$3.01 \\ 3.33 \\ 3.67 \\$	4.04 4.42 4.85	5.31 5.76 6.27	6.80 7.33 7.93	8.54 9.18 9.87
TURBO-CONOIDAL FAN (TVPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER	7, ["] S.	R. P. M.	440 449 459	470 480 491	503 516 529	542 554 567	582 596 609	623 636 650	664 680 696
C PRE	S. P.	H.P.	$ \begin{array}{c} 1.35 \\ 1.53 \\ 1.74 \end{array} $	$ \begin{array}{c} 1.95 \\ 2.18 \\ 2.44 \end{array} $	$2.71 \\ 3.01 \\ 3.33$	$3.69 \\ 4.07 \\ 4.46$	4.88 5.32 5.78	6.30 6.84 7.40	7.99 8.62 9.25
d stati fer	3.4" S.	R. P. M.	414 424 434	446 457 469	480 493 507	520 533 547	560 574 589	603 619 633	647 662 677
ITIES AND S BAROMETER	. P.	H.P.	$ \begin{array}{c} 1.16 \\ 1.33 \\ 1.51 \\ 1.51 \end{array} $	$ \begin{array}{c} 1.71 \\ 1.92 \\ 2.16 \end{array} $	$2.42 \\ 2.70 \\ 3.00 $	$3.33 \\ 3.68 \\ 4.05$	4.44 4.87 5.32	$5.78 \\ 6.29 \\ 6.82 \\ 6.82 \\$	$ \begin{array}{c} 7.41 \\ 8.00 \\ 8.62 \end{array} $
PACITII IES BAI	5,8" S.	R. P. M.	387 397 407	420 432 444	457 470 483	497 510 524	539 553 567	583 597 611	627 643 657
T) CAPAC INCHES	S. P.	H.P.	.97 1.12 1.28	$ \begin{array}{c} 1.46 \\ 1.67 \\ 1.88 \\ 1.88 \end{array} $	$2.12 \\ 2.38 \\ 2.66$	2.96 3.28 3.63	4.00 4.38 4.80	$5.24 \\ 5.73 \\ 6.23$	6.81 7.38 7.99
AN (TYPE T AND 29.92	1⁄2" S	H.P. R.P.M.	356 369 380	$392 \\ 404 \\ 419$	432 444 459	473 487 502	$516 \\ 530 \\ 546 \\$	560 574 590	607 623 639
FAN F. AN	Ъ.		.78 .91 1.06	$ \begin{array}{c} 1.23 \\ 1.41 \\ 1.60 \\ \end{array} $	$ \begin{array}{c} 1.82 \\ 2.05 \\ 2.31 \end{array} $	2.58 2.88 3.19	$3.53 \\ 3.91 \\ 4.31 \\ 4.31$	$\frac{4.76}{5.20}$	6.27 6.86 7.47
NOIDAL AT 70°	3 ₈ " S.	R. P. M.	324 337 350	363 376 389	403 417 432	446 460 474	490 506 521	537 553 570	586 603 619
B0-C0	ď	н. Р.	.60 .71 .84	$.98 \\ 1.14 \\ 1.31$	$1.50 \\ 1.70 \\ 1.93$	$2.19 \\ 2.47 \\ 2.77 \\ 2.77 \\$	$3.10 \\ 3.47 \\ 3.84 \\ 3.84$	$4.27 \\ 4.73 \\ 5.22$	5.73 6.25 6.84
7 TUR	14" S.	R.P.M.	287 300 313	327 342 357	372 387 402	416 432 449	464 482 497	514 530 547	563 582 599
NO. 7	Total s.	tot bbA estq	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 360 360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	7140 7860 8580	9290 10000 10720	$11430 \\ 12150 \\ 12860$	$13570 \\ 14290 \\ 15000$	$\frac{15720}{16430}$ 17150	17860 18580 19290	20000 20720 21430
	slocity Min.	Outlet Ver	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

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NO. 7 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

10	IURBO-CONOIDAL TAN OATAOTTES										
S. P.	Н. Р.	9.12	$9.54 \\ 9.90 \\ 10.3 $	10.9 11.5 12.3	13.1 13.9 14.8	15.7 16.6 17.6	18.6 19.6 20.7	21.7 24.1 26.7			
3 1/2" 2	R.P.M.	837	844 852 859	866 873 880	889 899 909	919 929 940	952 963 974	984 1009 1032			
. P.	Н. Р.	7.58	7.90 8.28 8.79	$\begin{array}{c} 9.37 \\ 10.1 \\ 10.8 \\ 10.8 \end{array}$	11.5 12.3 13.0	13.9 14.7 15.6	16.5 17.5 18.5	19.5 21.7 24.1			
3″ S.	R.P.M.	782	789 797 804	811 820 829	837 847 857	869 880 892	903 914 926	937 963 987			
2 ½" S. P.	Н. Р.	$5.54 \\ 5.81 \\ 6.10 \\ 6.10 \\$	$6.44 \\ 6.91 \\ 7.42$	8.03 8.64 9.25	$ \begin{array}{c} 0.91 \\ 10.6 \\ 11.3 \end{array} $	12.1 12.8 13.6	14.5 15.4 16.3	$17.3 \\ 19.4 \\ 21.6$			
	R.P.M.	709 714 722	729 737 746	754 764 774	784 794 806	817 829 840	852 864 876	889 913 940			
Р.	Н. Р.	4.26 4.49 4.84	$5.24 \\ 5.70 \\ 6.19$	6.71 7.22 7.77	8.36 8.96 9.60	10.3 11.0 11.7	12.5 13.3 14.1	15.1 17.0 19.1			
2° S.	R.P.M.	642 649 657	664 673 683	693 703 714	726 736 747	759 772 784	797 810 822	834 862 889			
S. P.	Н. Р.	3.10 3.51 3.75	4.13 4.51 4.92	5.33 5.80 6.27	6.78 7.31 7.87	8.48 9.12 9.78	10.5 11.2 12.0	12.8 14.6 16.4			
1 3/3"	R.P.M.	569 576 584	594 604 614	626 637 649	660 673 684	697 710 723	736 749 763	777 804 832			
s. P.	Н. Р.	2.62 2.91 3.23	$3.55 \\ 3.90 \\ 4.26$	4.65 5.06 5.51	5.99 6.49 7.02	7.58 8.21 8.82	$ \begin{array}{c} 9.48 \\ 10.2 \\ 10.9 \end{array} $	11.7 13.2 15.1			
1 34"	R.P.M.	526 536 546	566 567 577	587 600 613	626 639 652	664 677 692	704 719 731	746 774 802			
Add for Total Press.		.090 .106 .122	.141 .160 .180	202 225 250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721			
Capacity Cu. Ft. Air per Min.		8580 9290 10000	10720 11430 12150	$12860 \\ 13570 \\ 14290$	$15000 \\ 15720 \\ 16430$	17150 17860 18580	19290 20000 20720	21430 22860 24290			
Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400			

FAN

CAPACITIES

RBO-CONOIDAL

PRESSURES	
S AND STATIC PRESSURE	LETER
NO. 71/2 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES /	AT 70° F. AND 29.92 INCHES BAROMETER
N (TYPE T)	ND 29.92 II
DAL FA	70° F. A
TURBO-CONC	TA
71/2	
No.	

F A

A N	ENC	HNEE	RING	- B U I	FAL	O FO	RGE	СОМ	PANY
	م:	H.P.	$2.12 \\ 2.23 \\ 2.50 $	2.80 3.11 3.44	$3.80 \\ 4.18 \\ 4.59 $	5.03 5.49 6.00	6.54 7.11 7.71	8.34 9.00 9.71	10.5 11.2 12.0
	1" S.	R.P.M.	435 441 451	460 469 480	491 503 513	525 536 548	561 575 587	599 612 625	639 652 665
	.d	Н.Р.	$ \begin{array}{c} 1.76 \\ 2.26 \\ 2.26 \end{array} $	$2.52 \\ 2.81 \\ 3.12 \\ 3.12$	$3.46 \\ 3.82 \\ 3.82 \\ 4.21$	4.64 5.07 5.57	$\begin{array}{c} 6.10 \\ 6.61 \\ 7.20 \end{array}$	$ \begin{array}{c} 7.81 \\ 8.42 \\ 9.10 \\ 9.10 \end{array} $	9.80 10.5 11.3
	7.8" S.	R. P.M.	411 419 428	439 448 459	469 481 493	505 517 529	543 556 568	581 593 607	620 635 649
	ď	H.P.	$1.55 \\ 1.76 \\ 1.99$	$2.24 \\ 2.50 \\ 2.80 $	$3.11 \\ 3.46 \\ 3.83 \\ 3.83$	4.23 4.67 5.11	$5.60 \\ 6.11 \\ 6.64$	$7.24 \\ 7.85 \\ 8.50 \\ 8.50 \\$	$ \begin{array}{c} 9.18 \\ 9.90 \\ 10.6 \end{array} $
ä	34" S.	R.P.M.	387 396 405	416 427 437	448 460 473	485 497 511	523 536 549	563 577 591	604 617 632
BAROMETER	ď	Н.Р.	$ \begin{array}{c} 1.33 \\ 1.53 \\ 1.73 \end{array} $	$ \begin{array}{c} 1.96 \\ 2.21 \\ 2.48 \end{array} $	$2.78 \\ 3.10 \\ 3.45$	$3.82 \\ 4.22 \\ 4.65$	5.09 5.59 6.10	$6.64 \\ 7.22 \\ 7.83 $	$ \begin{array}{c} 8.51 \\ 9.19 \\ 9.90 \end{array} $
	5,8" S.	R. P. M.	361 371 380	$392 \\ 403 \\ 415$	427 439 451	464 476 489	503 516 529	544 557 571	585 600 613
INCHES	ď	H.P.	$ \begin{array}{c} 1.11 \\ 1.28 \\ 1.47 \end{array} $	$ \begin{array}{c} 1.68 \\ 1.91 \\ 2.16 \end{array} $	$2.44 \\ 2.73 \\ 3.06 \\ 3.06$	$3.39 \\ 3.77 \\ 4.17$	4.59 5.02 5.51	$6.02 \\ 6.58 \\ 7.15$	$7.82 \\ 8.47 \\ 9.17$
0 29.92	½″ S.	R.P.M.	332 344 355	365 377 391	403 415 428	441 455 468	481 495 509	523 536 551	567 581 596
F. AND	ď	H.P.	$ \begin{array}{c} .90\\ 1.05\\ 1.22 \end{array} $	$ \begin{array}{r} 1.41 \\ 1.62 \\ 1.84 \\ 1.84 \end{array} $	$2.09 \\ 2.35 \\ 2.65$	2.96 3.31 3.66	4.05 4.49 4.95	5.46 5.97 6.55	7.20 7.87 8.57
AT 70°	3 ₈ " S.	R. P. M.	$303 \\ 315 \\ 327$	339 351 363	376 389 403	416 429 443	457 472 487	501 516 532	547 563 577
	ď	Н.Р.	.69 .82 .96	$ \begin{array}{c} 1.13 \\ 1.31 \\ 1.50 \\ 1.50 \end{array} $	$ \begin{array}{c} 1.72 \\ 1.95 \\ 2.22 \end{array} $	2.51 2.84 3.18	3.56 3.98 4.41	$ \frac{4.90}{5.43} $	6.58 7.18 7.85
	<u></u> у" S.	R.P. M.	268 280 292	$305 \\ 319 \\ 333$	$347 \\ 361 \\ 375$	388 403 419	433 449 464	480 495 511	525 543 559
		tot tot Pre	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	8200 9020 9840	$\frac{10660}{11480}$	$\frac{13120}{13940}$ 14760	$\frac{15580}{16400}\\17220$	$\frac{18050}{18860}$	20500 21320 22150	22960 23780 24600
	elocity Min.	Outlet V Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	S. P.	Н. Р.	10.5	11.0 11.4 11.8	12.5 13.2 14.1	15.0 16.0 17.0	18.0 19.1 20.2	21.3 22.5 23.7	25.0 27.7 30.7
	3 1/2"	R.P.M.	781	788 795 801	808 815 821	829 839 848	857 867 877	888 899 909	919 941 963
	d.	Н. Р.	8.70	9.07 9.51 10.1	10.8 11.6 12.4	$13.2 \\ 14.1 \\ 15.0 $	15.9 16.9 17.9	19.0 20.1 21.2	$22.3 \\ 24.9 \\ 27.7$
	3″ S.	R. P. M.	729	736 744 751	757 765 773	008 162 800	811 821 832	843 853 864	875 899 921
	S. P.	. P.	6.36 6.67 7.00	$7.40 \\ 7.93 \\ 8.52$	$\begin{array}{c} 9.22 \\ 9.91 \\ 10.6 \end{array}$	11.4 12.2 13.0	13.8 14.7 15.7	16.6 17.6 18.7	19.8 22.2 24.8
AETER	2 1/2"	R. P. M.	661 667 673	680 688 696	704 713 723	732 741 752	763 773 784	795 807 817	829 852 877
INCHES BAROMETER	4	Н. Р.	4.89 5.15 5.56	$6.02 \\ 6.54 \\ 7.11$	7.70 8.29 8.92	9.59 10.3 11.0	11.8 12.6 13.5	14.4 15.3 16.2	17.3 19.6 21.9
INCHES	2" S.	R.P.M.	599 605 613	620 628 637	647 656 667	677 687 789	- 708 720 732	744 756 767	779 804 829
29.92	S. P.	Н. Р.	$3.56 \\ 4.03 \\ 4.30$	4.74 5.18 5.64	$6.12 \\ 6.66 \\ 7.20$	7.78 8.39 9.03	$9.71 \\ 10.5 \\ 11.2$	12.0 12.9 13.8	14.7 16.7 18.9
F. AND	1 1/2"	R.P.M.	531 537 545	555 564 573	584 595 605	616 628 639	651 663 675	687 699 712	725 751 776
AT 70°	S. P.	Н. Р.	$3.01 \\ 3.34 \\ 3.70 \\ 3.70$	4.08 4.48 4.89	5.34 5.81 6.33	$6.88 \\ 7.45 \\ 8.06$		10.9 11.7 12.5	13.4 15.2 17.3
	1 1%"	R. P. M.	491 500 509	519 529 539	548 560 572	584 596 608	620 632 645	657 671 683	696 723 748
1	or Total ress.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	ity Cu. Ft. er Min.	Сарасі Аіг р	9840 10660 11480	$12300 \\ 13120 \\ 13940$	$14760 \\ 15580 \\ 16400 \\ 16400 \\ 16400 \\ 16400 \\ 16400 \\ 16400 \\ 1600 \\ 1600 \\ 1000 \\$	17220 18050 18860	19680 20500 21320	22150 22960 23780	24600 26250 27880
	Velocity er Min.	Outlet Ft. p	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 71/5 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES

	d	H.P.	2.41 2.54 2.85	3.18 3.53 3.92	4.33 4.76 5.22	5.72 6.25 6.82	$7.44 \\ 8.09 \\ 8.77$	$ \begin{array}{c} 9.49 \\ 10.3 \\ 11.1 \end{array} $	11.9 12.8 13.7
1	1″ S.	R.M.P.	408 414 423	431 440 450	460 471 481	493 503 514	526 539 550	561 574 586	599 611 624
<i>w</i>	ď	H.P.	$2.00 \\ 2.28 \\ 2.57 $	2.87 3.20 3.55	$3.94 \\ 4.35 \\ 4.79$	5.27 5.77 6.34	6.95 7.52 8.19	$ \begin{array}{c} 8.88 \\ 9.57 \\ 10.4 \end{array} $	$11.2 \\ 12.0 \\ 12.9 \\ $
STATIC PRESSURES	7.8" S.	R.P.M.	385 393 401	411 420 430	440 451 463	474 485 496	509 521 533	545 556 569	581 595 609
C PRE		H.P.	$ \begin{array}{c} 1.76 \\ 2.00 \\ 2.27 \end{array} $	2.55 2.85 3.18	$3.54 \\ 3.94 \\ 4.35$	$\frac{4.81}{5.31}$	6.37 6.95 7.55	8.24 8.94 9.67	10.4 11.3 12.1
STATI R	34" S.	R.P.M.	363 371 380	390 400 410	420 431 444	455 466 479	490 503 515	528 541 554	566 579 593
CITIES AND BAROMETER	Ъ.	H.P.	$ \begin{array}{c} 1.51 \\ 1.74 \\ 1.97 \\ \end{array} $	$2.23 \\ 2.51 \\ 2.82 \\ 2.82 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ $	$3.16 \\ 3.53 \\ 3.92 \\ 3.92$	4.35 4.80 5.29	$5.79 \\ 6.36 \\ 6.95$	7.55 8.21 8.91	9.68 10.5 11.3
-	5,8" S.	R.P.M.	$339 \\ 348 \\ 356$	368 378 389	400 411 423	435 446 459	471 484 496	510 523 535	549 563 575
r) capa inches	Р.	H.P.	$ \begin{array}{c} 1.27 \\ 1.46 \\ 1.68 \end{array} $	$ \begin{array}{c} 1.91 \\ 2.18 \\ 2.46 \end{array} $	2.77 3.11 3.48	$3.86 \\ 4.29 \\ 4.74$	$5.22 \\ 5.72 \\ 6.27$	$ \begin{array}{c} 6.85 \\ 7.49 \\ 8.14 \end{array} $	$^{8.90}_{9.63}_{10.4}$
(TYPE D 29.92	<u>}∕</u> 2" S.	R.P.M.	$\frac{311}{323}$	$343 \\ 354 \\ 366$	378 389 401	414 426 439	451 464 478	490 503 516	531 545 559
	Ρ.	H.P.	$ \begin{array}{c} 1.03 \\ 1.19 \\ 1.38 \end{array} $	$ \begin{array}{c} 1.60 \\ 1.84 \\ 2.09 \end{array} $	$2.38 \\ 2.68 \\ 3.02 \\ $	3.37 3.76 3.76 4.17	$ \begin{array}{r} 4.61 \\ 5.11 \\ 5.63 \end{array} $	$6.22 \\ 6.80 \\ 7.46$	
TURBO-CONOIDAL FAN AT 70° F. AN	3,8'' S.	R. P. M.	284 295 306	318 329 340	353 365 378	390 403 415	429 443 456	470 484 499	513 528 541
80-C01	Ъ.	H.P.	$^{.78}_{.93}$	$ \begin{array}{c} 1.28 \\ 1.49 \\ 1.71 \end{array} $	$ \begin{array}{c} 1.96 \\ 2.22 \\ 2.52 \end{array} $	2.86 3.23 3.62	4.05 4.53 5.02	$5.58 \\ 6.18 \\ 6.82$	7.49 8.17 8.93
œ	1√" S.	R.P.M.	251 263 274	286 299 313	325 339 351	364 378 393	406 421 435	450 464 479	493 509 524
NO.		tot for Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	9330 10270 11200	12130 13060 14000	14930 15870 16790	17730 18660 19600	20530 21460 22390	23330 24260 25200	26120 27060 28000
	Min.	Outlet Ver	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

FAN ENGINEERING-BUFFALO FORGE COMPANY

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4	Н. Р.	11.9	12.5 12.9 13.5	14.2 15.1 16.0	17.1 18.2 19.3	20.5 21.7 23.0	24.2 25.6 27.0	28.4 31.5 34.9
3 ½" S.	R.P.M.	733 1	739 1 745 1 751 1	758 764 770	778 795	804 812 823 823	833 843 853 853	861 883 903 332
å	Н. Р.	06.6	10.3 10.8 11.5	12.2 13.2 14.1	15.0 16.0 17.0	18.1 19.2 20.4	21.6 22.9 24.1	$25.4 \\ 28.4 \\ 31.5 \\$
3″ S.	R.P.M.	684	690 698 704	710 718 725	733 741 750	082 770 780	790 800 810	820 843 864
S. P.	Н. Р.	7.23 7.59 7.97	8.42 9.02 9.70	10.5 11.3 12.1	13.0 13.8 14.7	15.8 16.8 17.8	18.9 20.1 21.3	22.5 25.3 28.2
2 1/2" 5	R.P.M.	620 625 631	638 645 653	660 678 678	686 695 705	715 725 735	745 756 766	778 799 822
ď	н. Р.	5.57 5.86 6.32	6.85 7.44 8.08	8.76 9.43 10.2	10.9 11.7 12.6	13.4 14.3 15.3	16.3 17.4 18.5	19.7 22.3 24.9
2″ S.	R.P.M.	561 568 575	581 589 598	606 615 625	635 644 654	664 675 686	698 709 719	730 754 778
S. P.	Н. Р.	4.05 4.58 4.90	5.39 5.89 6.42	6.96 7.57 8.19	8.85 9.54 10.3	11.1 11.9 12.8	13.7 14.7 15.7	16.7 19.0 21.5
1 32"	R. P. M.	498 504 511	520 529 538	548 558 568	578 589 599	610 621 633	644 655 668	680 704 728
s. P.	н. Р.	3.43 3.80 4.21	4.64 5.10 5.57	6.07 6.61 7.20	$7.82 \\ 8.47 \\ 9.16 \\ 9.16$	9.90 10.7 11.5	12.4 13.3 14.3	15.2 17.3 19.7
1 14"	R.P.M.	460 469 478	486 496 505	514 525 536	548 559 570	581 593 605	616 629 640	653 678 701
r Total ess.	ot bbA 19	.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
y Cu. Ft. er Min.	Capacit Air po	11200 12130 13060	14000 14930 15870	16790 17730 18660	19600 20530 21460	22390 23330 24260	25200 26120 27060	28000 29860 31730
Velocity er Min.	Outlet Ft. po	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 8 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

PRESSURES	
STATIC	~
AND	IETER
CAPACITIES	BAROMETE
CAPA	AND 29.92 INCHES I
F	4
(TVPE	29.92
L FAN (AND
H	<u>u</u>
Ď	20°
TURBO-CONOIDAL	AT 70° F.
X	
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No.	

 $\mathbf{F} \mathbf{A}$

N	EN	GINEE	RING	— B U I	FFAL	O FC	RGE	COM	I P A N Y
	ď	H. P.	2.72 2.86 3.22	$3.59 \\ 3.99 \\ 4.42$	4.89 5.37 5.89	6.46 7.05 7.70	$ \begin{array}{c} 8.40 \\ 9.13 \\ 9.90 \end{array} $	10.7 11.6 12.5	13.4 14.4 15.5
	1″ S.	R. P. M.	384 390 398	406 414 424	433 444 453	464 473 484	495 507 518	5528 540 552	564 576 587
	S. P.	H.P.	2.26 2.57 2.90	3.24 3.61 4.01	4.44 4.91 5.41	5.95 6.52 7.15	$7.83 \\ 8.49 \\ 9.24$	10.0 10.8 11.7	12.6 13.5 14.6
	1 ⁸ " S	R.P.M.	$ \begin{array}{c} 362 \\ 370 \\ 378 \\ 378 \end{array} $	387 395 405	414 425 435	446 457 467	479 491 501	513 524 535	547 560 573
	ď	Н.Р.	$1.99 \\ 2.26 \\ 2.56 \\ 2.56 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ $	$2.88 \\ 3.22 \\ 3.59$	$4.00 \\ 4.44 \\ 4.91$	$5.43 \\ 6.00 \\ 6.57$	7.19 7.85 8.53	$ \begin{array}{c} 9.30 \\ 10.1 \\ 10.9 \end{array} $	11.8 12.7 13.7
¥	34" S.	R.P.M.	341 350 358	367 377 386	395 406 418	428 439 451	461 473 485	497 510 521	533 545 558
	ď.	Н.Р.	$ \begin{array}{c} 1.71 \\ 1.96 \\ 2.23 \end{array} $	2.52 2.83 3.19	3.57 3.98 4.43	$ \frac{4.91}{5.42} $	6.54 7.18 7.84	$ \begin{array}{c} 8.53 \\ 9.27 \\ 10.1 \end{array} $	10.9 11.8 12.7
29.92 INCHES BARUMETER	5.8" S.	R. P. M.	319 327 335	346 355 366	377 387 398	410 420 432	444 455 467	480 492 504	517 530 541
	S. P.	Н. Р.	$ \begin{array}{c} 1.43 \\ 1.65 \\ 1.89 \\ 1.89 \end{array} $	$2.15 \\ 2.46 \\ 2.78 \\ 2.78 \\$	$3.13 \\ 3.51 \\ 3.92 \\$	4.36 4.84 5.35	$5.90 \\ 6.45 \\ 7.08$	7.73 8.45 9.18	10.0 10.9 11.8
	1∕2″ S	R.P.M.	293 304 313	322 333 345	355 366 378	390 401 413	425 437 450	461 473 486	500 513 526
F. AND	S. P.	Н. Р.	$ \begin{array}{c} 1.16 \\ 1.34 \\ 1.56 \end{array} $	$ \begin{array}{c} 1.81 \\ 2.07 \\ 2.36 \end{array} $	2.68 3.02 3.40	$3.80 \\ 4.25 \\ 4.70 $	$5.20 \\ 5.77 \\ 6.36 \\ 0.36$	$ \begin{array}{c} 7.02 \\ 7.67 \\ 8.42 \end{array} $	9.25 10.1 11.0
-0/ 14	3%" S	R. P. M.	267 278 288	$299 \\ 310 \\ 320$	332 344 355	367 379 391	404 417 430	442 455 470	482 497 510
	- .	H.P.	.88 1.05 1 24	$ \begin{array}{c} 1.45 \\ 1.68 \\ 1.93 \\ 1.93 \end{array} $	$2.21 \\ 2.51 \\ 2.85 \\ 2.85$	$3.22 \\ 3.64 \\ 4.09$	4.57 5.11 5.67	6.29 6.97 7.70	$ \begin{array}{c} 8.45 \\ 9.22 \\ 10.1 \\ 10.1 \end{array} $
	₩. S.	R. P. M.	237 247 258	270 281 294	306 319 331	$342 \\ 355 \\ 369 \\ 369 \\$	382 397 410	424 437 451	464 479 493
	Total .25	Add for Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft.	Capacity Air per	10530 11590 12640	$\frac{13690}{14750}$ 15800	16860 17910 18960	20010 21070 22120	23180 24230 25280	$26340 \\ 27390 \\ 28450$	29490 30550 31600
	elocity Min.	Outlet V Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	S. P.	H. P.	13.4	14.1 14.6 15.2	16.0 17.0 18.1	$ \begin{array}{c} 19.3 \\ 20.5 \\ 21.8 \end{array} $	23.1 24.5 25.9	27.4 28.9 30.5	32.1 35.6 39.4
	3 1/2"	R.P.M.	069	695 701 707	713 719 725	732 740 748	757 765 774	793 793 802	811 831 850
	S. P.	Н. Р.	11.2	11.7 12.2 13.0	13.8 14.9 15.9	17.0 18.1 19.2	20.5 21.7 23.0	24.4 25.8 27.3	28.7 32.0 35.6
	3" S	R.P.M.	644	650 657 662	668 675 682	690 698 706	715 725 734	744 753 762	772 793 813
	S. P.	Н. Р.	8.57 9.00	$ \begin{array}{c} 9.50 \\ 10.2 \\ 11.0 \end{array} $	11.8 12.7 13.7	14.6 15.6 16.6	$17.8 \\ 18.9 \\ 20.1$	$21.4 \\ 22.7 \\ 24.0 \\ 24.0 \\ 24.0 \\ 21.0 \\ $	$25.4 \\ 28.5 \\ 31.8 \\$
AETER	2 1/3"	R.P.M.	584 588 594	600 607 614	621 630 638	646 654 664	673 683 692	701 712 721	732 752 774
BAROMETER	P	Н. Р.	6.29 6.62 7.14	$ \begin{array}{c} 7.73 \\ 8.40 \\ 9.13 \end{array} $	$ \begin{array}{c} 9.89 \\ 10.7 \\ 11.5 \end{array} $	12.3 13.2 14.2	15.1 16.2 17.3	$18.4 \\ 19.6 \\ 20.9$	22.3 25.1 28.1
29.92 INCHES	2" S.	R.P.M.	528 534 541	547 554 563	571 579 588	598 606 615	625 635 646	657 667 677	687 710 732
	S. P.	Н. Р.	4.57 5.17 5.53	$\begin{array}{c} 6.08 \\ 6.65 \\ 7.25 \end{array}$	7.86 8.55 9.25	$\begin{array}{c} 9.99 \\ 10.8 \\ 11.6 \end{array}$	12.5 13.5 14.4	15.4 16.6 17.7	18.9 21.5 24.2
° F. AND	1 1/2"	R. P. M.	468 474 481	490 498 506	515 525 534	544 554 564	574 585 595	606 617 628	640 662 685
AT 70°	S. P.	Н. Р.	3.87 4.29 4.76	$5.24 \\ 5.75 \\ 6.29$	6.86 7.46 8.13	$ \begin{array}{c} 8.83 \\ 9.57 \\ 10.4 \end{array} $	11.2 12.1 13.0	14.0 15.0 16.1	$17.2 \\ 19.5 \\ 22.2$
	1 1/4"	R.P.M.	433 441 449	458 467 475	484 494 505	515 526 537	547 558 570	580 592 602	614 638 660
	or Total ress.	d I PPV	.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	ty Cu. Ft. er Min.	isbagb3 d itA	$12640 \\ 13690 \\ 14750$	15800 16860 17910	18960 20010 21070	22120 23180 24230	25280 26340 27390	28450 29490 30550	31600 33710 35810
	Velocity er Min.	Outlet Ft. p	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 8½ TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES

Min.	Cu. Ft. Min.		14" S.	4	3,8" S.	ď.	1⁄2" S.	d,	5," S.	d.	34" S	S. P.	2″% S	S. P.	1″ S.	ď
Ft. per	Capacity Air per	' toî bbA Pres	R.P.M.	H.P.	R. P. M.	H.P.	R. P. M.	H.P.	R.P.M.	H.P.	R.P.M.	H.P.	R. P. M.	H.P.	R.P.M.	H.P.
000 100 200	11810 129900 14170	060 [.] 063 .068	223 233 243	$^{99}_{-1.39}$	252 262 272	1.30 1.51 1.75	277 287 296	$1.60 \\ 1.85 \\ 2.12 \\ 2.12$	301 309 317	$ \begin{array}{c} 1.91 \\ 2.20 \\ 2.50 \end{array} $	322 330 338	2.23 2.54 2.87	342 349 357	2.54 2.88 3.25	362 368 376	3.05 3.21 3.61
300 500	15350 16530 17710	.106 .122 .141	255 266 278	$ \begin{array}{c} 1.62 \\ 1.88 \\ 2.16 \end{array} $	282 292 302	2.03 2.33 2.65	305 315 326	2.41 2.76 3.11	327 336 346	$2.82 \\ 3.18 \\ 3.57 \\$	347 356 365	$3.22 \\ 3.60 \\ 4.03 $	366 373 382	3.63 4.05 4.50	383 391 400	4.03 4.47 4.96
600 700 800	18900 20080 21250	.160 .180 .202	289 301 312	2.48 2.81 3.19	313 324 336	3.01 3.39 3.82	336 346 357	$3.51 \\ 3.93 \\ 4.40$	356 366 376	$4.00 \\ 4.46 \\ 4.97$	373 383 395	$4.48 \\ 4.98 \\ 5.51$	391 401 411	4.98 5.50 6.06	409 419 428	$5.48 \\ 6.02 \\ 6.60$
1900 22000 2100	22440 23620 24800	.225 .250 .275	323 336 349	$3.61 \\ 4.08 \\ 4.59 \\ 4.59 \\ $	347 358 369	$\frac{4.26}{5.27}$	368 379 390	$ \begin{array}{c} 4.89\\ 5.43\\ 6.00 \end{array} $	387 397 408	5.50 6.08 6.70	405 415 426	$ \begin{array}{c} 6.09 \\ 6.72 \\ 7.36 \end{array} $	421 431 441	6.68 7.31 8.02	438 447 457	7.24 7.91 8.64
2200 2300 2400	$25990 \\ 27160 \\ 28350$.302 .330 .360	361 375 387	$5.12 \\ 5.73 \\ 6.35$	381 393 406	$5.83 \\ 6.47 \\ 7.13$	401 412 425	$ \begin{array}{c} 6.61 \\ 7.23 \\ 7.94 \end{array} $	419 430 441	7.33 8.04 8.79	436 447 458	8.06 8.80 9.56	452 463 475	$^{8.78}_{9.52}_{10.4}$	468 479 489	$ \begin{array}{c} 9.42 \\ 10.2 \\ 11.1 \end{array} $
2500 2600 2700	29520 30710 31890	.390 .422 .455	400 412 426	$7.06 \\ 7.82 \\ 8.63$	418 430 443	$ \begin{array}{c} 7.87 \\ 8.60 \\ 9.44 \end{array} $	436 447 459	$^{8.67}_{9.48}$	453 465 476	$ \begin{array}{c} 9.56 \\ 10.4 \\ 11.3 \end{array} $	469 481 492	10.4 11.3 12.2	485 495 506	11.3 12.1 13.1	499 510 521	12.0 13.0 14.0
2800 2900 3000	33060 34250 35430	.489 .525 560	438 452 466	9.48 10.3	456 469 481	10.4	472 485	11.3	488 500	12.3	503 515	13.2	517 529	$14.1 \\ 15.2$	532 543	15.1 16.1

	S. P.	Н. Р.	15.1	$15.8 \\ 16.4 \\ 17.0 $	$18.0 \\ 19.0 \\ 20.3 $	21.6 23.0 24.4	25.9 27.5 29.1	30.7 32.4 34.2	$35.9 \\ 39.9 \\ 44.2 $
	3 ½"	R.P.M.	651	657 662 668	673 679 685	669 699 707	715 722 731	740 749 758	766 785 802
ES	P.	Н. Р.	12.5	$13.1 \\ 13.7 \\ 14.5$	15.5 16.6 17.8	19.0 20.3 21.6	22.9 24.3 25.8	27.3 28.9 30.5	$32.2 \\ 35.9 \\ 39.9 \\ $
RESSUR	3″ S.	R.P.M.	608	613 620 626	631 638 645	651 659 667	676 685 693	702 711 720	729 749 768
CAPACITIES AND STATIC PRESSURES INCHES BAROMETER	S. P.	Н. Р.	$9.15 \\ 9.61 \\ 10.1$	10.7 11.4 12.3	$13.3 \\ 14.3 \\ 15.3$	16.4 17.5 18.7	$ \begin{array}{c} 19.9 \\ 21.2 \\ 22.5 \end{array} $	23.9 25.4 26.9	28.5 32.0 35.7
TIES AND ST BAROMETER	2 3/2"	R.P.M.	551 556 561	567 573 580	587 595 602	610 618 627	636 645 653	662 672 681	691 710 731
SITIES . S BARO	, P.	Н. Р.	7.05 7.42 8.00	$^{8.67}_{9.42}$	$11.1 \\11.9 \\112.8$	13.8 14.8 15.9	17.0 18.1 19.4	20.7 22.0 23.3	$25.0 \\ 28.2 \\ 31.6 \\$
		R. P. M.	499 505 511	517 523 531	539 547 556	565 572 581	590 600 610	620 630 639	649 670 691
FAN (TYPE T) F. AND 29.92	S. P.	н. р.	$5.12 \\ 5.80 \\ 6.20$	$6.82 \\ 7.45 \\ 8.12 \\$	$^{8.81}_{9.58}$ 10.4	11.2 12.1 13.0	$14.0 \\ 15.1 \\ 16.2 \\ 16.2$	$17.3 \\ 18.6 \\ 19.9$	$21.2 \\ 24.1 \\ 27.2$
FAN (1 32"	R.P.M.	442 448 455	462 470 478	487 496 505	513 523 532	542 552 562	572 582 593	605 626 647
NOIDAL AT 70°	1 ½" S. P.	Н. Р.	4.33 4.81 5.33	5.87 6.45 7.05	$7.69\\8.37\\9.11$	$\begin{array}{c} 9.90 \\ 10.7 \\ 11.6 \end{array}$	12.6 13.6 14.6	15.7 16.8 18.0	19.3 21.9 24.9
TURB0-CONOIDAL AT 70°	1 14"	R.P.M.	409 417 425	432 441 449	457 467 477	487 497 507	517 527 538	548 559 569	580 602 623
NO. 9 TU	or Total :ess.	a bba q	.090 .106 .122	$ \begin{array}{c} .141 \\ .160 \\ .180 \\ \end{array} $.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
~	ty Cu. Ft. er Min.	Capaci Air p	$\frac{14170}{15350}$	17710 18900 20080	$21250 \\ 22440 \\ 23620$	24800 25990 27160	28350 29520 30710	31890 33060 34250	35430 37790 40150
	Velocity st Min.	Outlet Ft. po	1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

PRESSURES	
STATIC	a sub
AND	METE
PACITIES	AT 70° F. AND 29.92 INCHES BAROMETER
() CAI	INCH
(TYPE T	D 29.92
FAN	F. AN
10 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURE	AT 70°
9	
.0N	

F A

ENG	GINEE	RING-	— B U I	FFAL	O FO	RGE	COM	I P A N Y
	Н.Р.	3.76 3.96 4.45	4.97 5.52 6.12	6.76 7.43 8.15	$ \begin{array}{c} 8.94 \\ 9.76 \\ 10.7 \end{array} $	$11.6 \\ 12.6 \\ 13.7 \\ 13.7 \\ 13.7 \\ 12.6 \\ 13.7 \\ $	14.8 16.0 17.3	$19.6 \\ 21.4 \\ 21.4 \\ 21.4 \\ 31.4 \\ $
1" S.	R. P. M.	326 331 338	$345 \\ 352 \\ 360 \\ 360 \\$	368 377 385	$394 \\ 402 \\ 411$	421 431 440	449 459 469	479 489 499
ď	Н. Р.	3.13 3.56 4.01	$ \begin{array}{c} 4.48 \\ 5.00 \\ 5.55 \end{array} $	$ \begin{array}{c} 6.15 \\ 6.79 \\ 7.48 \end{array} $	$ \begin{array}{c} 8.24 \\ 9.02 \\ 9.90 \end{array} $	$10.8 \\ 11.8 \\ 12.8 \\ $	$13.9 \\ 15.0 \\ 16.2 $	$17.4 \\ 18.7 \\ 20.2 \\ 20.2 \\ 17 \\ 20.2 \\ 17 \\ 18.7 \\ 18.7 \\ 18.7 \\ 10.1$
7." S.	R. P. M.	308 314 321	32 9 336 344	$352 \\ 361 \\ 370 \\$	379 388 397	407 417 426	436 445 455	465 476 487
ď	Н.Р.	2.75 3.13 3.54	$3.98 \\ 4.45 \\ 4.97 $	$5.53 \\ 6.15 \\ 6.80 \\ 0.80 \\ $	$7.52 \\ 8.30 \\ 9.09$	$\substack{\textbf{9.95}\\10.9\\11.8$	$12.9 \\ 14.0 \\ 15.1$	$16.3 \\ 17.6 \\ 18.9$
3." S.	R.P.M.	290 297 304	$312 \\ 320 \\ 328 \\ 328 \\$	336 345 355	364 373 383	$392 \\ 402 \\ 412$	422 . 433 443	453 463 474
ď	Н.Р.	2.36 2.71 3.08	3.48 3.92 4.41	$4.94 \\ 5.51 \\ 6.13$	$ \begin{array}{c} 6.79 \\ 7.50 \\ 8.27 \end{array} $	$ \begin{array}{c} 9.05 \\ 9.93 \\ 10.9 \end{array} $	$ \begin{array}{c} 11.8 \\ 12.8 \\ 13.9 \\ \end{array} $	$ \begin{array}{c} 15.1 \\ 16.3 \\ 17.6 \end{array} $
58" S.	R.P.M.	271 278 285	294 302 311	320 329 338	348 357 367	377 387 397	408 418 428	439 450 460
ď	. н.р.	$ \begin{array}{c} 1.98 \\ 2.28 \\ 2.62 \end{array} $	2.98 3.40 3.84	4.33 4.85 5.43	$ \begin{array}{c} 6.03 \\ 6.70 \\ 7.41 \end{array} $		10.7 11.7 12.7	$13.9 \\15.1 \\16.3$
1⁄2" S.	R.P.M.	249 258 266	274 283 293	$302 \\ 311 \\ 321 \\ 321 \\$	331 341 351	$361 \\ 371 \\ 382$	392 402 413	425 436 447
à	Н.Р.	$ \begin{array}{c} 1.60 \\ 1.86 \\ 2.16 \end{array} $	$2.50 \\ 2.87 \\ 3.27 \\ $	$3.71 \\ 4.18 \\ 4.71$	5.26 5.88 6.51	$7.20 \\ 7.98 \\ 8.80 \\ 8.80 \\$	$\begin{array}{c} 9.71 \\ 10.6 \\ 11.7 \end{array}$	$12.8 \\ 14.0 \\ 15.2 $
3,8" S.	R. P.M.	227 236 245	254 263 272	282 292 302	312 322 332	343 354 365	376 387 399	410 422 433
à	H.P.	$ \begin{array}{c} 1.22 \\ 1.45 \\ 1.71 \end{array} $	$2.00 \\ 2.32 \\ 2.67 \\ 2.67 $	3.06 3.47 3.94	$ \frac{4.46}{5.04} $	$6.32 \\ 7.07 \\ 7.84$	$ \begin{array}{c} 8.71 \\ 9.65 \\ 10.7 \end{array} $	11.7 12.8 14.0
}√" S.	R.P.M.	$201 \\ 210 \\ 219 \\ 219$	229 239 250	260 271 281	291 302 314	325 337 348	360 371 383	394 407 419
	Add for Pres	.060 .076 .090	.106 .122 .141	$ \frac{160}{180} $.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
Cu. Ft. Min.	Capacity Air per	14580 16040 17500	18950 20410 21870	$23330 \\ 24790 \\ 26240 $	$27700 \\ 29160 \\ 30620$	$32080 \\ 33530 \\ 34990$	$36450 \\ 37910 \\ 39370$	40820 42280 43740
elocity Min.	Outlet Ver	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	2" S. P.	Н. Р.	18.6	$ \begin{array}{c} 19.5 \\ 20.2 \\ 21.0 \end{array} $	22.2 23.5 25.1	26.7 28.4 30.1	32.0 33.9 35.9	37.9 40.0 42.2	44.4 49.2 54.5
AND STATIC PRESSURES METER	3 1/2" S	R.P.M.	586	591 596 601	606 611 616	622 629 636	643 650 658	666 674 682	689 706 722
	ď	Н. Р.	15.5	$16.1 \\ 16.9 \\ 17.9 \\ 17.9 \\ 17.9 \\ 10.1 \\ $	$19.1 \\ 20.5 \\ 22.0 \\ 22.0 \\ 19.1 \\ $	23.5 25.0 26.6	28.3 30.0 31.8	33.7 35.7 37.7	39.7 44.3 49.2
	3″ S.	R.P.M.	547	552 558 563	568 574 580	586 593 600	608 616 624	632 640 648	656 674 691
CATIC P	S. P.	Н. Р.	11.3 11.9 12.5	$13.2 \\ 14.1 \\ 15.2 \\ $	16.4 17.6 18.9	$20.2 \\ 21.6 \\ 23.0$	24.6 26.2 27.8	29.6 31.4 33.2	35.2 39.5 44.0
AND ST METER	2 3/3"	R.P.M.	496 500 505	$510 \\ 516 \\ 522$	528 535 542	549 556 564	$572 \\ 580 \\ 588 $	596 605 613	622 639 658
T) CAPACITIES AND S INCHES BAROMETER	2" S. P.	Н. Р.	8.70 9.16 9.88	10.7 11.6 12.6	13.7 14.7 15.9	17.1 18.3 19.6	20.9 22.4 23.9	25.5 27.1 28.9	30.8 34.8 39.0
		R.P.M.	449 454 460	465 471 478	485 492 500	508 515 523	531 540 549	558 567 575	584 603 622
YPE 7	1 ½" S. P.	Н. Р.	6.32 7.16 7.65	$^{8.42}_{9.20}$	10.9 11.8 12.8	13.8 14.9 16.1	17.3 18.6 20.0	21.4 22.9 24.5	26.2 29.7 33.5
L FAN (T		R.P.M.	398 403 409	416 423 430	438 446 454	462 471 479	488 497 506	515 524 534	544 563 582
DNOIDAL AT 70°	s. P.	Н. Р.	5.35 5.94 6.58	7.25 7.96 8.70	9.49 10.3 11.3	12.2 13.2 14.3	15.5 16.8 18.0	19.3 20.8 22.3	23.8 27.0 30.7
10 TURBO-CONOIDAL FAN AT 70° F. AN	1 14"	R.P.M.	368 375 382	389 397 404	411 420 429	438 447 456	465 474 484	493 503 512	522 542 561
NO. 10 TI	Add for Total Press.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	Cu. Ft.	Capacity Air pei	17500 18950 20410	21870 23330 24790	26240 27700 29160	30620 32080 33530	$34990 \\ 36450 \\ 37910 \\$	39370 40820 42280	43740 46650 49570
	Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

PRESSURES	
, FAN (TYPE T) CAPACITIES AND STATIC F	OMETER
CAPACITIES	AT 70° F. AND 29.92 INCHES BAROMETER
(TYPE T)	AND 29.92
NOIDAL FAN	AT 70° F.
TURB0-CONOIDAL	
Ξ	
NO.	

FAN

EN	GINEE	RING-	— B U F	FAL	O FO	RGE	COM	PANY
- d	Ч.Р.	4.55 4.79 5.39	$ \begin{array}{c} 6.01 \\ 6.68 \\ 7.41 \end{array} $	$8.18 \\ 8.99 \\ 9.86$	$10.8 \\ 11.8 \\ 12.9$	14.1 15.3 16.6	$18.0 \\ 19.4 \\ 20.9$	22.5 24.1 25.9
1″ S.	R. P. M.	296 301 307	$314 \\ 320 \\ 327$	335 343 350	358 365 374	383 392 400	408 417 426	436 445 454
S. P.	H.P.	$3.79 \\ 4.31 \\ 4.85$	$5.42 \\ 6.05 \\ 6.72$	$7.44 \\ 8.22 \\ 9.05$	$ \begin{array}{c} 9.97 \\ 10.9 \\ 12.0 \end{array} $	$13.1 \\ 14.2 \\ 15.5 \\ $	16.8 18.1 19.6	21.1 22.7 24.4
7 ₈ " S	R. P. M.	280 286 292	$299 \\ 306 \\ 313 \\ 313$	320 328 336	345 353 361	370 379 387	$396 \\ 405 \\ 414$	423 433 443
S. P.	H.P.	3.33 3.79 4.28	$\frac{4.82}{5.39}$	6.69 7.44 8.23	$ \begin{array}{c} 9.10 \\ 10.1 \\ 11.0 \end{array} $	12.1 13.1 14.3	$15.6 \\ 16.9 \\ 18.3 \\ $	$ \begin{array}{c} 19.7 \\ 21.3 \\ 22.9 \end{array} $
34" S	R.P.M. H.P.	264 270 278	284 291 298	$306 \\ 314 \\ 323 \\$	331 339 348	356 366 375	384 394 403	412 421 431
S. P.	H.P.	2.86 3.28 3.73	$4.21 \\ 4.74 \\ 5.34$	$5.98 \\ 6.67 \\ 7.42$	$^{8.22}_{9.08}_{10.0}$	$11.0 \\ 12.0 \\ 13.1 \\ 13.1 \\ 13.1 \\ 12.0 \\ 13.1 \\ $	$14.3 \\ 15.5 \\ 16.9 $	18.3 19.8 21.3
5 ⁸ " S	R.P.M.	246 253 259	267 275 283	291 299 307	$316 \\ 325 \\ 334$	343 352 361	371 380 389	399 409 418
S. P.	Н.Р.	$2.40 \\ 2.76 \\ 3.17$	$3.61 \\ 4.11 \\ 4.65$	$5.24 \\ 5.87 \\ 6.57$	7.30 8.11 8.97	$ \begin{array}{c} 9.87 \\ 10.8 \\ 11.9 \end{array} $	$ \begin{array}{c} 13.0 \\ 14.2 \\ 15.4 \end{array} $	16.8 18.2 19.7
3%" S	H.P. R.P.M. H.P. R.P.M. H.P. R.P.M.	226 235 242	249 257 266	275 283 292	301 310 319	328 337 347	356 366 376	386 396 406
S. P.	H.P.	$ \begin{array}{c} 1.94 \\ 2.25 \\ 2.61 \end{array} $	$3.03 \\ 3.47 \\ 3.96 \\ 3.96$	$ \begin{array}{r} 4.49 \\ 5.06 \\ 5.70 \\ \end{array} $	$ \begin{array}{c} 6.37 \\ 7.12 \\ 7.88 \\ 7.88 \end{array} $	$ \begin{array}{c} 8.71 \\ 9.66 \\ 10.7 \\ \end{array} $	11.8 12.9 14.1	15.5 16.9 18.5
3.8" S	R.P.M.	206 215 223	231 239 247	256 266 275	284 293 302	312 322 332	342 352 363	373 384 394
S. P.		$ \begin{array}{c} 1.48 \\ 1.76 \\ 2.07 \end{array} $	$2.42 \\ 2.81 \\ 3.23$	$3.70 \\ 4.20 \\ 4.77$	$5.40 \\ 6.10 \\ 6.85$	7.65 8.56 9.49	10.5 11.7 12.9	$14.2 \\ 15.4 \\ 16.9$
34" S	R.P.M.	183 191 199	208 217 227	236 246 256	265 275 286	296 306 316	327 337 348	358 370 381
lotal	Add for Total Press.		.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
a. Ft.	Capacity Cu. Ft. Air per Min.		$\frac{22930}{24700}\\26460$	$28230 \\ 30000 \\ 31750$	$33520 \\ 35280 \\ 37050 \\ 3700$	$38820 \\ 40570 \\ 42340$	44100 45870 47640	49390 51160 52920
Outlet Velocity Ft. per Min.		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	S. P.	н. Р.	22.5	23.6 24.5 25.5	26.8 28.4 30.3	32.3 34.3 36.5	38.7 41.0 43.4	45.8 48.4 51.0	53.7 59.5 66.0
	3 ½" S	R.P.M.	533	537 542 546	551 556 560	566 572 578	585 591 598	606 613 620	626 642 656
-	Р.	Н. Р.	18.7	19.5 20.5 21.7	$23.1 \\ 24.9 \\ 26.6$	28.4 30.3 32.2	34.3 36.3 38.5	40.8 43.2 45.6	48.0 53.6 59.5
	3″ S.	R.P.M.	497	502 507 512	516 522 527	533 539 546	553 560 567	575, 582 589	596 613 628
	S. P.	Н. Р.	13.7 14.4 15.1	$15.9 \\ 17.1 \\ 18.3$	$ \begin{array}{c} 19.8 \\ 21.3 \\ 22.9 \end{array} $	24.5 26.2 27.9	29.8 31.7 33.7	35.8 37.9 40.2	42.6 47.8 53.2
METER	2 1/2"	R.P.M.	451 455 459	464 469 475	480 486 493	499 506 513	520 527 535	542 550 557	566 581 598
29.92 INCHES BAROMETER	S. P.	н. Р.	10.5 11.1 12.0	13.0 14.1 15.3	16.6 17.8 19.2	20.6 22.1 23.7	25.3 27.1 28.9	30.9 32.8 34.9	37.3 42.1 47.1
INCHE	2" S	R.P.M.	408 413 418	423 428 435	441 447 455	462 468 476	483 491 499	507 515 523	531 548 566
AND 29.92	S. P.	н. Р.	7.65 8.66 9.26	10.2 11.1 12.1	$13.2 \\ 14.3 \\ 15.5 \\ 15.5 \\ 1$	16.7 18.1 19.4	20.9 22.5 24.1	25.9 27.7 29.7	31.7 35.9 40.5
Ľ.	1 3/2"	R.P.M.	362 366 372	$\frac{378}{385}$	398 406 413	420 428 436	444 452 460	468 476 486	495 512 529
AT 70°	S. P.	Н. Р.	6.47 7.19 7.96	$ \begin{array}{c} 8.77 \\ 9.63 \\ 10.5 \end{array} $	$ \begin{array}{c} 11.5 \\ 12.5 \\ 13.6 \end{array} $	14.8 16.0 17.3	18.7 20.3 21.8	23.4 25.2 27.0	28.8 32.7 37.2
	1 34"	R. P. M.	335 341 347	354 361 367	374 382 390	398 406 416	423 431 440	448 457 466	475 493 510
		add for Pres	.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	Capacity Cu. Ft. Air per Min.		21170 22930 24700	26640 28230 30000	$31750 \\ 33520 \\ 35280 \\ 35280 \\ \end{array}$	$37050 \\ 38820 \\ 40570$	42350 44100 45870	47640 49390 51160	52920 56460 59980
	Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 11 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES

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RESSURES	
S AND STATIC PRESSURE	'ER
ES AND	ROMET
PACITII	AT 70° F. AND 29.92 INCHES BAROMETER
T) CA	92 INCE
TYPE	ND 29.
L FAN	0° F. A
NO. 12 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES A	AT 70
12	
No.	

 $\mathbf{F}\mathbf{A}$

N	ENC	GINEE.	RING-	— B U I	FAL	O FO	RGE	COM	PANY
	ď	H.P.	$5.42 \\ 5.70 \\ 6.41$	$7.16 \\ 7.95 \\ 8.81$	$ \begin{array}{c} 9.74 \\ 10.7 \\ 11.7 \end{array} $	12.9 14.1 15.4	16.8 18.2 19.7	$21.4 \\ 23.0 \\ 24.9$	26.8 28.7 30.8
	1″ S.	R.P.M.	272 276 282	288 293 300	307 314 321	328 335 343	351 359 367	374 383 391	399 408 416
	å	H.P.	4.51 5.13 5.78	6.45 7.20 7.99	8.86 9.78 10.8	$ \begin{array}{c} 11.9 \\ 13.0 \\ 14.3 \\ \end{array} $	15.6 16.9 18.4	20.0 21.6 23.3	25.1 27.0 29.0
	7, ⁸ S.	R.P.M.	257 262 268	274 280 287	293 301 308	$316 \\ 323 \\ 331 \\ 331 \\$	339 348 355	363 371 379	388 397 406
	ď	H.P.	$3.96 \\ 4.51 \\ 5.10$	$5.73 \\ 6.41 \\ 7.16$	7.96 8.86 9.79	10.8 12.0 13.1	14.3 15.6 17.0	$ \begin{array}{c} 18.5 \\ 20.1 \\ 21.8 \\ \end{array} $	23.5 25.4 27.2
í	34" S.	R.P.M.	242 248 253	260 267 273	280 288 296	303 311 319	327 335 343	352 361 369	378 386 395
	.d	H.P.	3.40 3.90 4.44	5.01 5.65 6.35	7.11 7.94 8.83	$ \begin{array}{c} 9.78 \\ 10.8 \\ 11.9 \end{array} $	13.0 14.3 15.6	17.0 18.5 20.1	21.8 23.5 25.4
	5.8" S.	R.P.M.	226 232 238	245 252 259	267 274 282	290 298 306	314 323 331	340 348 357	366 375 383
	ď	H.P.	2.85 3.28 3.77	$4.29 \\ 4.90 \\ 5.53$	$ \begin{array}{c} 6.24 \\ 6.98 \\ 7.82 \end{array} $	$ \begin{array}{c} 8.68 \\ 9.65 \\ 9.65 \\ 10.7 \end{array} $	11.8 12.9 14.1	15.4 16.9 18.3	20.0 21.7 23.5
	1∕₂″ S.	R.P.M.	208 215 222	228 236 244	252 259 268	276 284 293	301 309 318	327 335 344	354 363 373
	ď	H.P.	2.30 2.68 3.11	$3.60 \\ 4.13 \\ 4.71$	$5.34 \\ 6.02 \\ 6.78 \\ 0.78 \\ $	7.58 8.47 9.37	10.4 11.5 12.7	$ \begin{array}{r} 14.0 \\ 15.3 \\ 16.8 \\ \end{array} $	18.4 20.2 22.0
	3,8" S.	R.P.M.	189 197 204	212 219 227	235 243 252	260 268 277	286 295 304	$313 \\ 323 \\ 333 \\ 333 \\$	342 352 361
	å	H.P.	$ \begin{array}{c} 1.76 \\ 2.09 \\ 2.45 \end{array} $	2.88 3.34 3.85	$ \frac{4.41}{5.00} $	$6.42 \\ 7.26 \\ 8.15$	$ \begin{array}{c} 9.10 \\ 10.2 \\ 11.3 \end{array} $	$12.6 \\ 13.9 \\ 15.3 \\ $	$16.9 \\ 18.4 \\ 20.1$
	₩. S.	R.P.M.	168 175 183	191 199 208	217 226 234	243 252 262	271 281 290	300 309 319	328 339 349
	Outlet Velocity Ft. per Min. Gapacity Cu. Ft. Air per Min. Press.		.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
			$21000 \\ 23100 \\ 25200 $	27290 29390 31490	33600 35700 37780	$39890 \\ 41990 \\ 44090 \\ 64000 \\ 64000 \\ 60$	$\begin{array}{c} 46190 \\ 48280 \\ 50380 \end{array}$	52480 54590 56680	58780 60880 62980
			1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

NO. 12 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

10	RBU-U	UNUI	DAL		0			
S. P.	Н. Р.	26.8	28.0 29.1 30.3	$31.9 \\ 33.9 \\ 36.1$	38.5 40.8 43.4	46.1 48.8 51.6	54.5 57.6 60.7	63.9 70.9 78.5
3 1/2" S	R. P. M.	488	493 497 501	505 509 513	518 524 530	536 542 549	555 562 568	574 588 602
ď	H. P.	22.3	23.2 24.3 25.8	27.5 29.6 31.6	33.8 36.0 38.3	40.8 43.2 45.8	$\frac{48.5}{51.4}$	57.2 63.8 70.9
3″ S.	R.P.M.	456	460 465 469	473 479 483	488 494 500	507 513 520	527 533 540	547 562 576
S. P.	H. P.	$16.3 \\ 17.1 \\ 17.9$	$ \begin{array}{c} 18.9 \\ 20.3 \\ 21.8 \end{array} $	23.6 25.4 27.2	$29.1 \\ 31.1 \\ 33.2 \\ 33.2 \\$	$35.4 \\ 37.7 \\ 40.1$	42.6 45.2 47.8	50.7 56.9 63.4
2 1/2"	R.P.M.	413 417 421	425 430 435	440 446 452	458 463 470	478 483 490	497 504 511	518 533 549
ď	Н. Р.	12.5 13.2 14.2	$15.4 \\ 16.8 \\ 18.2 \\ 18.2 \\ 18.2 \\ 18.2 \\ 10.1 \\ $	$ \begin{array}{c} 19.7 \\ 21.2 \\ 22.8 \\ \end{array} $	24.5 26.3 28.2	30.1 32.2 34.4	36.7 39.1 41.6	44.4 50.1 56.1
2" S.	R.P.M.	374 378 383	388 393 398	404 410 417	423 429 436	443 450 458	465 473 479	487 503 518
S. P.	H. P.	9.1 10.3 11.0	$12.1 \\ 13.3 \\ 14.5 \\ $	$15.7 \\ 17.0 \\ 18.4$	19.9 21.5 23.1	24.9 26.8 28.7	30.8 33.0 35.3	37.7 42.8 48.3
1 1/3"	R. P. M.	$332 \\ 336 \\ 341$	347 353 358	365 372 378	385 393 399	407 414 422	429 437 445	453 469 485
S. P.	Н. Р.	$7.71 \\ 8.55 \\ 9.48$	10.4 11.5 12.5	$13.7 \\ 14.9 \\ 16.2$	$17.6 \\ 19.1 \\ 20.6$	22.3 24.1 25.9	27.9 29.9 32.1	34.3 38.9 44.3
1 34"	R.P.M.	307 313 318	324 331 337	343 350 358	365 373 380	388 395 403	411 419 427	435 452 468
	Add for Total Press.		.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390	.455 .489 .525	.560 .638 .721
t. Ft. Min.	Capacity Cu. Ft. Air per Min.		$31490 \\ 33600 \\ 35700$	37780 39890 41990	$\begin{array}{c} 44090\\ 46190\\ 48280 \end{array}$	50380 52480 54590	56680 58780 60880	62980 67180 71380
	Outlet Velocity Ft. per Min.		1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

FAN	ENC	INEE	RING	- B U I	FFAL	O FC	RGE	COM	IPANY
	Ŀ.	н. Р.	6.36 6.69 7.52	$ \begin{array}{c} 8.40 \\ 9.33 \\ 10.4 \end{array} $	11.4 12.6 13.8	15.1 16.5 18.0	$ \begin{array}{c} 19.7 \\ 21.4 \\ 23.2 \end{array} $	$25.1 \\ 27.1 \\ 29.2 $	31.4 33.7 36.2
	1″ S.	R. P. M. H. P.	251 255 260	265 270 277	$^{+}283$ 290 296	303 309 316	324 332 339	$346 \\ 353 \\ 361$	$369 \\ 376 \\ 384$
<i>^</i>	S. P.	Н. Р.	5.29 6.02 6.78	7.57 8.45 9.38	10.4 11.5 12.7	13.9 15.3 16.7	18.3 19.9 21.6	23.5 25.3 27.4	29.4 31.7 34.1
SSUKE	7/8" S	R.P.M.	237 242 247	253 259 265	271 278 285	$292 \\ 299 \\ 305 $	313 321 328	$335 \\ 342 \\ 350 \\ 350 \\$	358 366 375
R PRE	S. P.	Н.Р.	4.65 5.29 5.98	$ \begin{array}{c} 6.73 \\ 7.52 \\ 8.40 \end{array} $	$^{0.35}_{10.4}$	$12.7 \\ 14.0 \\ 15.4$	$ \begin{array}{r} 16.8 \\ 18.4 \\ 20.0 \\ \end{array} $	21.8 23.6 25.5	27.6 29.8 31.9
AND STATIC PRESSURES BAROMETER	3₄" S.	R. P. M. H. P. R. P. M. H. P. R. P. M.	223 229 234	240 246 252	259 265 273	280 287 295	302 309 317	325 333 341	349 356 365
~ <u>~ </u>	. Р.	H.P.	$ \frac{3.99}{5.21} $	5.88 6.63 7.45	$ \begin{array}{c} 8.35 \\ 9.31 \\ 10.4 \end{array} $	$ \begin{array}{c} 11.5 \\ 12.7 \\ 14.0 \\ \end{array} $	15.3 16.8 18.3	$20.0 \\ 21.7 \\ 23.5 \\ 23.5$	25.6 27.6 29.7
29.92 INCHES	5%" S.	R. P. M.	209 214 219	226 232 239	246 253 260	268 275 282	290 298 305	$314 \\ 322 \\ 329 \\ 329$	338 346 354
<u>3</u> ⊆	S. P.	H.P.	3.35 3.85 4.43	5.04 5.75 6.49	7.32 8.20 9.18	$10.2 \\ 11.3 \\ 12.5$	$13.8 \\ 15.1 \\ 16.6 \\ 16.6 \\ 10.1 \\ $	$ \begin{array}{c} 18.1 \\ 19.8 \\ 21.5 \end{array} $	23.5 25.4 27.6
(LYPE F. AND	1⁄2″ S.	R.P.M.	$ \begin{array}{c} 192 \\ 198 \\ 205 \end{array} $	$211 \\ 218 \\ 225 \\ 225$	232 239 247	$255 \\ 262 \\ 270 \\$	278 285 294	$302 \\ 309 \\ 318 \\ 318 \\$	327 335 344
AT 70°	Р.		2.71 3.14 3.65	4.23 4.85 5.53	6.27 7.07 7.96	$ \begin{array}{c} 8.89 \\ 9.94 \\ 11.0 \end{array} $	$12.2 \\ 13.5 \\ 14.9 $	$16.4 \\ 18.0 \\ 19.7 $	21.6 23.7 25.8
	3 _{/8} " S.	H.P. R.P.M. H.P.	175 182 189	$ \begin{array}{c} 196 \\ 202 \\ 209 \\ \end{array} $	217 225 232	240 248 255	$264 \\ 272 \\ 281 $	289 298 307	$315 \\ 325 \\ 333 \\ 333 \\$
B0-CC	ч.	н. Р.	2.06 2.45 2.89	$3.38 \\ 3.92 \\ 4.51$	5.17 5.87 6.66	$7.54 \\ 8.52 \\ 9.57 \\ 9.57 \\ \end{array}$	10.7 12.0 13.3	14.7 16.3 18.0	19.8 21.6 23.6
NO. 13 IUKBU-CUNUIDAL FAN AT 70°	14" S.	R.P.M.	155 162 169	$176 \\ 184 \\ 192 \\ 192 \\$	200 209 216	224 232 242	250 259 268	$277 \\ 286 \\ 295$	303 313 322
So z	Total ss.	Add for Pre:	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	Cu. Ft. Min.	Capacity Air per	$\begin{array}{c} 24640 \\ 27110 \\ 29570 \end{array}$	$32020 \\ 34490 \\ 36960$	$\begin{array}{c} 39430 \\ 41900 \\ 44340 \end{array}$	46810 49280 51740	54220 56660 59130	$61600 \\ 64060 \\ 66530$	68980 71450 73920
	elocity Min.	Outlet V Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	S. P.	Н. Р.	31.4	32.9 34.1 35.6	37.4 39.7 42.3	45.1 47.9 50.9	54.1 57.3 60.6	64.0 67.6 71.2	75.0 83.2 92.1
	3 1/2"	R.P.M.	451	455 459 462	466 470 474	479 484 489	495 500 506	512 519 525	530 543 556
ł	S. P.	Н. Р.	26.1	27.3 28.6 30.3	32.3 34.7 37.1	39.7 42.3 45.0	47.8 50.7 53.8	57.0 60.3 63.7	67.1 74.9 83.1
	3"	R.P.M.	421	425 429 433	437 442 446	451 456 462	468 474 480	486 492 499	505 519 532
	S. P.	Н. Р.	$ \begin{array}{c} 19.1 \\ 20.1 \\ 21.1 \end{array} $	22.2 23.8 25.6	27.7 29.8 31.9	34.2 36.5 38.9	41.6 44.3 47.0	49.0 53.0 56.1	59.5 66.7 74.4
BAROMETER	2 1/2"	R.P.M.	382 385 389	392 397 402	406 412 417	422 428 434	440 446 452	459 465 472	479 492 506
S BARO	2″ S. P.	Н. Р.	14.7 15.5 16.7	18.1 19.7 21.4	$23.1 \\ 24.9 \\ 26.8 \\ $	28.8 30.9 33.1	35.4 37.8 40.4	43.1 45.8 48.8	52.1 58.7 65.8
INCHES		R.P.M.	346 349 354	358 362 368	373 379 385	391 396 402	409 415 422	429 436 442	449 464 479
AND 29.92	S. P.	Н. Р.	10.7 12.1 12.9	14.2 15.6 17.0	18.4 20.0 21.6	23.4 25.2 27.2	29.2 31.5 33.7	$36.1 \\ 38.7 \\ 41.4$	44.2 50.2 56.6
70° F. AN	1 32"	R.P.M.	306 310 315	320 325 331	337 343 349	356 362 369	375 382 389	396 403 411	419 433 448
AT 7(S. P.	Н. Р.	9.04 10.0 11.1	$12.3 \\ 13.5 \\ 14.7$	16.0 17.5 19.0	20.7 22.4 24.2	26.1 28.3 30.4	32.7 35.1 37.6	40.2 45.7 52.0
	1 14"	R.P.M.	283 289 294	299 305 311	$316 \\ 323 \\ 330 \\$	337 344 351	$358 \\ 365 \\ 372 \\ 372 \\$	379 387 394	402 417 432
	Total .s.	roî bbA Pres	.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	Capacity Cu. Ft. Air per Min.		29570 32020 34490	$36960 \\ 39430 \\ 41900$	44340 46810 49280	51740 54220 56660	$59130 \\ 61600 \\ 64060$	66530 68980 71450	73920 78830 83770
	Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 13 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES

	Р.	Н.Р.	7.37 7.76 8.72	$ \begin{array}{c} 9.74 \\ 10.8 \\ 12.0 \end{array} $	$13.3 \\ 14.6 \\ 16.0$	$17.5 \\ 19.1 \\ 20.9$	$22.8 \\ 24.8 \\ 26.9 \\ $	$29.1 \\ 31.4 \\ 33.8 \\ 33.8 \\$	$36.4 \\ 39.0 \\ 42.0 $
	1″ S.	R. P.M.	233 237 242	247 252 257	263 269 275	$282 \\ 287 \\ 294 $	$301 \\ 308 \\ 314 \\ 314$	321 328 335	342 349 357
	S. P.	H.P.	$6.14 \\ 6.98 \\ 7.86$	$^{8.78}_{9.80}$	12.1 13.3 14.7	$16.2 \\ 17.7 \\ 19.4$	$21.3 \\ 23.0 \\ 25.1$	$27.2 \\ 29.3 \\ 31.7$	$34.2 \\ 36.7 \\ 39.5$
	7/8" S.	R. P.M.	220 224 229	235 240 246	252 258 264	271 277 284	291 298 304	$312 \\ 318 \\ 325 \\ 325 \\$	332 340 348
	Р.	Н.Р.	$5.39 \\ 6.14 \\ 6.94$	$ \begin{array}{c} 7.80 \\ 8.72 \\ 9.74 \end{array} $	$10.8 \\ 12.1 \\ 13.3 \\ 13.3 \\ 13.2 \\ 12.1 \\ $	14.7 16.3 17.8	$ \begin{array}{c} 19.5 \\ 21.3 \\ 23.1 \end{array} $	$25.2 \\ 27.4 \\ 29.6$	32.0 34.5 37.0
ER	34" S.	R. P.M.	207 212 217	223 229 234	$\begin{array}{c}240\\2546\\254\end{array}$	260 267 274	280 287 294	302 309 317	324 331 339
OMET		н.Р.	4.63 5.31 6.04	$6.82 \\ 7.68 \\ 8.64 $	${}^{9.68}_{10.8}$ 12.0	$13.3 \\ 14.7 \\ 16.2$	$17.7 \\ 19.5 \\ 21.3$	$23.1 \\ 25.2 \\ 27.3 \\ 27.3 \\ 27.3 \\ 23.1 \\ 23.1 \\ 23.1 \\ 23.1 \\ 23.1 \\ 23.1 \\ 23.1 \\ 24.1 \\ 25.1 \\ 34.1 \\ 25.1 \\ 34.1 \\ 25.1 \\ 34.1 \\ 25.1 \\ 34.1 \\ 25.1 \\ 25.1 \\ 34.1 \\ 25.1 \\ $	29.7 32.0 34.5
INCHES BAROMETER	S. P. 58" S.	R. P.M.	194 199 204	$210 \\ 216 \\ 222 $	229 235 242	249 255 262	269 277 284	292 299 306	314 322 329
		H.P.	3.88 4.47 5.14	5.84 6.67 7.53	$8.49\\9.51\\10.7$	$ \begin{array}{c} 11.8 \\ 13.1 \\ 14.5 \end{array} $	$16.0 \\ 17.5 \\ 19.2 $	$21.0 \\ 22.9 \\ 24.9$	$27.2 \\ 29.5 \\ 32.0 \\$
0 29.92	P. 32"	R. P.M.	178 184 190	196 202 209	216 222 229	236 244 251	258 265 273	280 287 295	304 312 319
F. AND		H.P.	$3.14 \\ 3.65 \\ 4.23$	$ \begin{array}{r} 4.90 \\ 5.63 \\ 6.41 \\ \end{array} $	$ \begin{array}{c} 7.27 \\ 8.19 \\ 9.23 \end{array} $	$10.3 \\ 11.5 \\ 12.8 \\ $	$ \begin{array}{c} 14.1 \\ 15.7 \\ 17.3 \\ \end{array} $	$ \begin{array}{c} 19.0 \\ 20.8 \\ 22.8 \\ \end{array} $	$25.1 \\ 27.4 \\ 29.9$
AT 70°	3,8" S.	н.р. к.р.м. н.р. к.р.м. н.р. к.р.м.	$162 \\ 169 \\ 175$	182 188 194	$202 \\ 209 \\ 216$	223 230 237	$245 \\ 253 \\ 261 $	$\frac{269}{277}$	293 302 309
	. Р.		2.39 2.84 3.35	$3.92 \\ 4.55 \\ 5.23 \\ 5.23 \\$	$\begin{array}{c} 6.00 \\ 6.80 \\ 7.72 \end{array}$	$8.74\\9.88\\11.1$	$12.4 \\ 13.9 \\ 15.4$	$17.1 \\ 18.9 \\ 20.9$	22.9 25.0 27.4
	<u>}</u> 4″ S.	R. P.M.	144 150 157	164 171 179	186 194 201	208 216 224	232 241 249	257 265 274	282 291 299
	Total ss.	Add for Pre	.060 .076 .076	.106 .122 .141	$.160 \\ .180 \\ .202$.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
	, Cu. Ft.	Capacity Air per	$28580 \\ 31440 \\ 34300 \\ 34300 \\$	$37140 \\ 40000 \\ 42870$	$\begin{array}{c} 45730\\ 48590\\ 51430\end{array}$	54300 57150 60020	62870 65720 68580	71440 74300 77170	80000 82870 85730
1	elocity Min.	Outlet V Ft. per	1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

FAN ENGINEERING-BUFFALO FORGE COMPANY

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L FAN (TYPE T) CAPACITIES	AT 70° F. AND 29.92 INCHES BAROME
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1.0		CONO	10.11			1 11 0 1	TIES	
S. P.	H.P.	36.5	38.2 39.6 41.2	43.4 46.1 49.1	52.3 55.6 59.0	62.7 66.5 70.3	74.2 78.4 82.6	86.9 96.4 106.8
3 1/2"	R. P. M.	419	422 426 429	433 437 440	444 449 454	459 464 470	476 482 487	492 504 516
S. P.	Н. Р.	30.3	31.6 33.1 35.2	37.5 40.3 43.1	46.0 49.1 52.1	55.5 58.8 62.3	66.1 70.0 73.9	77.8 86.8 96.4
3" 5	R.P.M.	391	394 399 402	406 410 414	419 424 429	434 440 446	452 457 463	469 482 494
S. P.	Н. Р.	22.2 23.3 24.4	25.8 27.6 29.7	32.1 34.5 37.0	39.7 42.4 45.1	48.2 51.4 54.5	57.9 61.5 65.1	69.0 77.4 86.3
2 1/2"	R.P.M.	354 357 361	364 369 373	377 382 387	392 397 403	410 414 420	426 432 438	444 457 470
à	Н. Р.	17.1 18.0 19.4	$21.0 \\ 22.8 \\ 24.8 \\ $	26.8 28.9 31.1	33.4 35.8 38.4	41.0 43.9 46.9	50.0 53.2 56.6	60.4 68.1 76.4
2" S.	R.P.M.	321 324 329	332 337 342	347 352 357	363 368 374	379 386 392	399 405 411	417 431 444
S. P.	Н. Р.	12.4 14.0 15.0	16.5 18.0 19.7	$21.3 \\ 23.2 \\ 25.1 $	$27.1 \\ 29.2 \\ 31.5$	33.9 36.5 39.1	41.9 44.9 48.0	51.3 58.2 65.7
1 35"	R. P. M.	284 288 292	297 302 307	$313 \\ 319 \\ 324$	330 337 342	349 355 362	368 374 382	389 402 416
S. P.	Н. Р.	10.5 11.7 12.9	14.2 15.6 17.1	18.6 20.3 22.1	24.0 26.0 28.1	30.3 32.8 35.3	37.9 40.8 43.7	46.7 53.0 60.3
">1	R.P.M.	263 268 273	278 284 289	294 300 307	$313 \\ 319 \\ 326 \\ 326$	332 339 346	352 359 366	373 387 401
Add for Total Press.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
Capacity Cu. Ft. Air per Min.		34300 37140 40000	42870 45730 48590	51430 54300 57150	60020 62870 65720	68580 71440 74300	77170 80000 82870	85730 91440 97160
Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 15 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

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<u>a</u>	H.P.	$8.46 \\ 8.91 \\ 10.0 $	11.2 12.4 13.8	$15.2 \\ 16.7 \\ 18.3 \\ $	20.1 22.0 24.0	$26.2 \\ 28.4 \\ 30.8 \\ $	$33.4 \\ 36.0 \\ 38.8 \\ $	41.8 44.8 48.2
1" S.	R.P.M.	217 221 225	230 235 240	245 251 257	263 268 274	281 287 293	2 9 9 306 313	319 326 333
S. P.	Н. Р.	7.04 8.01 9.02	10.1 11.3 12.5	$13.8 \\ 15.3 \\ 16.8 \\ 16.8 \\ 16.8 \\ 10.8 \\ $	$ \begin{array}{c} 18.5 \\ 20.3 \\ 22.3 \end{array} $	24.4 26.4 28.8	$\frac{31.2}{33.7}$	39.2 42.2 45.3
1 ^{8/2}	R.P.M.	205 209 214	219 224 229	235 241 247	253 259 265	271 278 284	291 297 303	310 317 325
S. P.	Н. Р.	6.19 7.04 7.97	$^{8.96}_{10.0}$	$12.5 \\ 13.8 \\ 15.3 \\ 15.3 \\ 15.3 \\ 12.3 \\ $	$16.9 \\ 18.7 \\ 20.5$	22.4 24.4 26.6	29.0 31.4 34.0	36.7 39.6 42.5
3.4" S	R.P.M.	$ \begin{array}{c} 193 \\ 198 \\ 203 \end{array} $	$208 \\ 213 \\ 219 \\ 219 \\ 219 \\ 219 \\ 219 \\ 219 \\ 210 $	224 230 237	243 249 255	261 268 275	$281 \\ 289 \\ 295 $	$302 \\ 309 \\ 316$
S. P.	Н.Р.	$5.31 \\ 6.10 \\ 6.93 \\ 6.93$	7.83 8.82 9.92	$11.1 \\ 12.4 \\ 13.8 \\ 13.8 \\ 13.8 \\ 12.1 \\ $	15.3 16.9 18.6	20.4 22.4 24.4	26.6 28.9 31.3	34.1 36.8 39.6
5%" 5	R.P.M.	181 185 190	$ \begin{array}{c} 196 \\ 201 \\ 207 \end{array} $	213 219 225	$232 \\ 238 \\ 245 $	$251 \\ 258 \\ 265 \\ 265$	$272 \\ 279 \\ 285$	293 300 307
S. P.	Н.Р.	4.46 5.13 5.90	6.71 7.65 8.64	$\begin{array}{c} 9.74 \\ 10.9 \\ 12.2 \end{array}$	$13.6 \\ 15.1 \\ 16.7 \\ 16.7 \\ 16.7 \\ 10.7 \\ $	18.4 20.1 22.1	24.1 26.3 28.6	$31.3 \\ 33.9 \\ 36.7$
12" S	R. P. M.	166 172 177	183 189 195	201 207 214	221 227 234	241 247 255	$261 \\ 268 \\ 275$	283 291 298
S. P.	H.P.	3.60 4.19 4.86	5.63 6.46 7.36	$ \begin{array}{c} 8.35 \\ 9.41 \\ 10.6 \end{array} $	11.8 13.2 14.7	16.2 18.0 19.8	21.9 23.9 26.2	28.8 31.5 34.3
38"	R.P.M.	151 157 163	169 175 181	188 195 201	$208 \\ 215 \\ 221$	229 236 243	$\begin{array}{c} 251\\ 258\\ 266\end{array}$	273 281 289
S. P.	H.P.	2.75 3.26 3.85	4.50 5.22 6.01	6.89 7.81 8.87	10.0 11.4 12.7	$14.2 \\ 15.9 \\ 17.7 $	$ \begin{array}{c} 19.6 \\ 21.7 \\ 24.0 \end{array} $	26.3 28.7 31.4
14" S	R.P.M.	134 140 146	153 159 167	173 181 187	194 201 209	217 225 232	240 247 255	263 271 279
	Add for Total Press.		.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
Cu. Ft. Min.	Сарасіtу Аіг рег	32800 36090 39370	42650 45920 49200	52490 55780 59040	62320 65600 68900	72180 75440 78720	82000 85300 88580	$\begin{array}{c} 91840\\ 95120\\ 98410\\ 98410 \end{array}$
Outlet Velocity Ft. per Min.		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

IDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES	AT 70° F. AND 29.92 INCHES BAROMETER
. 1	70°
TURBO-CONOIDAI	AT
15	
NO.	

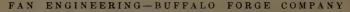
TURBO-CONOIDAL FAN CAPACITIES								
S. P.	Н. Р.	41.9	43.8 45.5 47.3	49.8 52.9 56.4	60.1 63.8 67.8	72.0 76.3 80.7	85.2 90.0 94.8	99.8 110.7 122.6
3 1/2"	R.P.M.	391	394 397 401	404 407 411	415 419 424	429 433 439	444 449 455	459 471 481
-d	Н. Р.	34.8	36.3 38.0 40.4	43.0 46.2 49.4	52.8 56.3 59.9	63.7 67.5 71.6	75.8 80.3 84.8	89.3 99.7 110.7
3″ S.	R. P. M.	365	368 372 375	379 383 387	391 395 400	405 411 416	421 427 432	437 449 461
s. p.	Н. Р.	25.4 26.7 28.0	29.6 31.7 34.1	36.9 39.7 42.5	45.5 48.7 51.8	55.4 59.0 62.6	66.5 70.5 74.7	79.2 88.8 99.0
2 1/2"	R. P. M.	331 333 337	340 344 348	352 357 361	366 371 376	381 387 391	397 403 409	415 426 439
S. P.	Н. Р.	$ \begin{array}{c} 19.6 \\ 20.6 \\ 22.2 \end{array} $	24.1 26.2 28.4	30.8 33.2 35.7	$38.4 \\ 41.1 \\ 44.1$	47.1 50.4 53.8	57.4 61.0 64.9	69.3 78.2 87.6
2″ S	R. P. M.	299 303 307	310 314 319	323 328 333	339 343 349	354 360 366	$\frac{372}{378}$	389 402 415
S. P.	Н. Р.	$14.2 \\ 16.1 \\ 17.2 $	19.0 20.7 22.6	24.5 26.6 28.8	$31.1 \\ 33.6 \\ 36.1$	38.9 41.9 44.9	48.1 51.5 55.1	58.8 66.8 75.4
1 1/3"	R.P.M.	265 269 273	277 282 287	292 297 303	308 314 319	325 331 337	343 349 356	363 375 388
S. P.	н. Р.	12.0 13.4 14.8	16.3 17.9 19.6	21.4 23.3 25.3	27.5 29.8 32.2	34.8 37.7 40.5	43.5 46.8 50.1	53.6 60.8 69.2
1 34"	R.P.M.	245 250 255	259 265 269	274 280 286	292 298 304	310 316 323	329 335 341	348 361 374
Add for Total Press.		.090 .106 .122	.141 .160 .180	.202 .225 .250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
Capacity Cu. Ft. Air per Min.		39370 42650 45920	49200 52490 55780	59040 62320 65600	68900 72180 75440	78720 82000 85300	88580 91840 95120	$\begin{array}{c} 98410 \\ 104950 \\ 111530 \end{array}$
Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

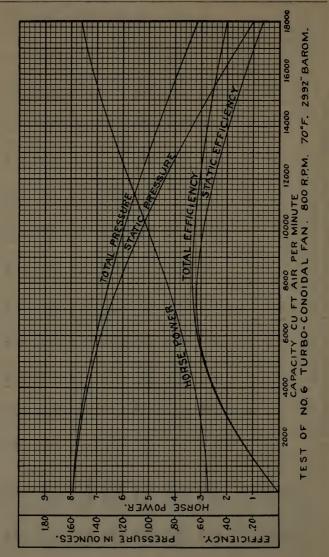
NO. 16 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES AT 70° F. AND 29.92 INCHES BAROMETER

E M	GINEE	RING.	- B U I	FFAL	0 FC	JRGE	001	IPANI
7%" S. P. 1" S. P.	H.P.	9.63 10.1 11.4	12.7 14.1 15.7	17.3 19.0 20.9	22.9 25.0 27.3	29.8 32.4 35.1	38.0 41.0 44.2	47.6 51.0 54.8
	R. P. M.	204 208 211	216 220 225	230 236 241	246 251 257	263 270 275	281 287 293	300 306 312
	Н.Р.	8.01 9.11 10.3	11.5 12.8 14.2	15.8 17.4 19.2	21.1 23.1 25.4	27.8 30.1 32.7	35.5 38.3 41.4	44.6 48.0 51.6
	R. P. M.	193 196 201	$206 \\ 210 \\ 215 \\ 215 $	$220 \\ 226 \\ 231 \\ 231$	237 243 248	$254 \\ 261 \\ 266$	$273 \\ 278 \\ 284 \\ 284$	291 298 304
S. P.	Н.Р.	7.04 8.01 9.06	$10.2 \\ 11.4 \\ 12.7$	$ \begin{array}{r} 14.2 \\ 15.8 \\ 17.4 \\ \end{array} $	19.3 21.3 23.3	25.5 27.8 30.2	33.0 35.7 38.7	41.8 45.1 48.3
34" S	R. P. M.	$181 \\ 186 \\ 190 \\ 190 \\$	$ \begin{array}{c} 195 \\ 200 \\ 205 \end{array} $	210 216 222	228 233 239	245 251 258	264 271 277	283 289 296
§″ S. P.	Н. Р.	6.04 6.94 7.89		12.7 14.1 15.7	$17.4 \\ 19.2 \\ 21.2$	23.2 25.4 27.8	30.2 32.9 35.6	38.7 41.8 45.1
	R.P.M.	170 174 178	$184 \\ 189 \\ 194 $	200 206 211	218 223 229	236 242 248	$255 \\ 261 \\ 268 $	274 281 288
S. P.	Н.Р.	5.07 5.84 6.71	$7.63 \\ 8.70 \\ 9.83 \\ 9.83 \\ 100 \\ $	11.1 12.4 13.9	15.4 17.2 19.0	20.9 22.9 25.1	27.4 30.0 32.5	35.6 38.5 41.7
1/3" 5	R.P.M.	$156 \\ 161 \\ 166 \\ 166$	171 177 183	189 195 201	207 213 219	226 232 239	245 251 258	266 273 280
S. P.	Н.Р.	4.10 4.76 5.53	6.40 7.35 8.37	$^{9.50}_{10.7}$	$13.5 \\ 15.1 \\ 16.7 \\ 16.7 \\ 16.7 \\ 10.7 \\ $	18.4 20.4 22.5	$24.9 \\ 27.2 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 29.8 \\ 20.8 \\ $	32.8 35.8 39.0
3.8" 5	R. P. M.	142 148 153	$\begin{array}{c} 159\\ 164\\ 170 \end{array}$	176 183 189	195 201 208	214 221 228	$235 \\ 242 \\ 249 $	256 264 271
S. P.	H.P.	3.12 3.71 4.38	5.12 5.94 6.84	$^{7.83}_{8.88}_{10.1}$	$11.4 \\ 12.9 \\ 14.5$	16.2 18.1 20.1	22.3 24.7 27.3	30.0 32.7 35.7
34" S	R. P. M.	126 131 137	$\begin{array}{c} 143\\149\\156\end{array}$	163 169 176	182 189 196	$203 \\ 211 \\ 218 $	225 232 239	246 254 262
	Add for Pres	.063 .076 .090	.106 .122 .141	.160 .180 .202	.225 .250 .275	.302 .330 .360	.390 .422 .455	.489 .525 .560
Capacity Cu. Ft. Air per Min.		37320 41060 44800	$\frac{48510}{52240}$	59720 63460 67170	70900 74640 78380	82120 85830 89570	93300 97040 100780	104500 108230 111970
Outlet Velocity Ft. per Min.		1000 1100 1200	1300 1400 1500	1600 1700 1800	1900 2000 2100	2200 2300 2400	2500 2600 2700	2800 2900 3000

	S. P.	Н.Р.	47.6	49.8 51.7 53.8	56.7 60.2 64.1	68.4 72.6 77.1	81.9 86.8 91.8	$ \begin{array}{c} 96.9 \\ 102.4 \\ 107.9 \end{array} $	113.5 126.0 139.5
	3 ½" S	R.P.M.	366	370 373 376	379 382 385	389 393 398	402 406 411	416 421 426	431 441 451
	S, P.	Н. Р.	39.6	41.3 43.3 45.9	49.0 52.6 56.2	60.1 64.1 68.1	72.5 76.8 81.4	86.3 91.4 96.5	101.6 113.4 126.0
	3″ S	R. P. M.	342	345 349 352	355 359 363	366 371 375	380 385 390	395 400 405	410 421 · 432
	S. P.	Н. Р.	$28.9 \\ 30.4 \\ 31.9$	33.7 36.1 38.8	41.9 45.1 48.3	51.8 55.4 59.0	63.0 67.1 71.2	75.7 80.3 85.0	90.1 101.1 112.6
METER	2 3/2"	R. P. M.	310 313 316	319 323 326	330 334 339	343 348 353	358 363 368	373 378 383	389 400 411
D 29.92 INCHES BAROMETER	S. P.	Н. Р.	22.3 23.5 25.3	27.4 29.8 32.3	35.1 37.7 40.6	43.7 46.8 50.2	53.6 57.3 61.2	65.3 69.4 73.9	78.9 89.0 99.7
	2" S	R. P. M.	281 284 288	291 294 299	$303 \\ 308 \\ 312 \\ 312$	318 322 327	332 338 343	349 354 360	365 377 389
	1 ½″ S. P.	Н. Р.	16.2 18.3 19.6	21.6 23.6 25.7	27.9 30.3 32.8	35.4 38.2 41.1	44.3 47.6 51.1	54.7 58.6 62.7	67.0 76.0 85.8
% F. AND		R. P.M.	249 252 256	260 264 269	274 279 284	.289 294 299	305 311 316	322 328 334	340 352 364
AT 70°	S. P.	Н. Р.	$13.7 \\ 15.2 \\ 16.9 \\ 16.9 \\ 16.9 \\ 10.1 \\ $	18.6 20.4 22.3	24.3 26.5 28.8	31.3 33.9 36.7	39.6 42.9 46.1	49.5 53.2 57.0	60.9 69.2 78.7
	1 34"	R. P. M.	230 234 239	243 248 253	257 263 268	274 280 285	291 296 303	308 314 320	326 339 351
	Add for Total Press.		.090 .106 .122	.141 .160 .180	-202 -225 -250	.275 .302 .330	.360 .390 .422	.455 .489 .525	.560 .638 .721
	CapacityCu.Ft. Air per Min.		44800 48510 52240	55980 59720 63460	67170 70900 74640	78380 82120 85830	89570 93300 97040	$\frac{100780}{104500}$ $\frac{108230}{108230}$	111970 119400 126900
	Outlet Velocity Ft. per Min.		1200 1300 1400	1500 1600 1700	1800 1900 2000	2100 2200 2300	2400 2500 2600	2700 2800 2900	3000 3200 3400

NO. 16 TURBO-CONOIDAL FAN (TYPE T) CAPACITIES AND STATIC PRESSURES





Induced Draft Tables

Induced draft tables are given for both Planoidal and Niagara Conoidal fans, with gases at 300° and 550° Fahr. The 300° tables are to be used in case the gases are passed through an economizer. These tables give the boiler horsepower that will be served, together with the speed, cubic feet of gases handled per minute, and the power required to drive the fan, for different sizes of fans operating at various pressures measured at the breeching of the boiler. Thus, if we operate a 100-inch Planoidal fan handling gases at 550° at 355 R. P. M., and 0.75 inch static pressure, we will be able to develop 670 boiler H. P. In case we speed up to 502 R. P. M., with a pressure of 1.5 inches, we will be able to develop 950 boiler H. P., or an increase of 41 per cent. The power required to drive the fan will increase from 7.06 H. P. to 20.0 H. P.

Special Narrow Induced Draft Fans

The tables of special steel plate fans to be direct connected to Buffalo steam engines and used for induced draft work will be found especially convenient when selecting apparatus for this purpose. The first column gives a number, which refers to that particular combination of engine and fan. It will be noticed that these are narrow, tall fans, of the special high efficiency type, operating at such a speed as to make them suitable for direct connection to steam engines.

These fans are to be operated with a static pressure of 1.69inches at the breeching of the boiler, with gases at 550° , and develop 50 per cent. overload on the boiler. These combinations are so selected that a peak load on the boiler of at least 100 per cent. may be carried for a limited time, and approximately 50 per cent. overload all of the time. The engines are to be operated at their normal rated cut-off and at the speed indicated, the steam pressure required being indicated in the third column. The above is based on the assumption that under average conditions a pressure of 0.75 in. at the up-take will be required, when operating at normal rated capacity.

300°	I ½ In. or 0.865 0z. Static Press.	Fan	Н. Р.	$4.34 \\ 6.21 \\ 6.63$	11.1 14.0 17.3	$21.0 \\ 25.0 \\ 29.2$	$33.8 \\ 38.6 \\ 44.1$	50.0 56.0 62.3	69.1 76.0 83.7	91.2 99.6 107.8
			Vol.	6660 9590 13070	17020 21550 26640	$32200 \\ 38350 \\ 44700 \\ $	52170 59860 67970	$76910 \\ 86340 \\ 95860$	$\begin{array}{c} 106600\\ 117300\\ 128600 \end{array}$	140700 153300 166100
		-	R. P. M.	871 725 622	543 483 435	396 363 334	310 290 272	256 241 228	217 207 197	189 181 174
ONOMIZEI	$1 $ $\frac{1}{\sqrt{4}}$ In. or 0.721 Oz. Static Press. 1 $\frac{1}{\sqrt{2}}$ In.	Boiler H. P. at	24.4 A.P.M.	270 395 535	700 885 1090	$1320 \\ 1570 \\ 1830$	2140 2455 2785	$3150 \\ 3540 \\ 3930 \\ $	4370 4810 5270	5765 6285 6810
INDUCED DRAFT FAN CAPACITIES BUFFALO PLANOIDAL (TYPE L) EXHAUSTERS WITH ECONOMIZER			H.P.	$3.30 \\ 4.72 \\ 6.44$	$^{8.41}_{10.7}$	$15.9 \\ 19.0 \\ 22.2$	25.7 29.4 33.6	38.0 42.6 47.3	52.5 57.8 63.6	69.4 75.7 82.0
		Fan	Vol.	$6080 \\ 8750 \\ 11940$	$\frac{15540}{19670}\\24320$	$29390 \\ 35000 \\ 40800$	$\begin{array}{c} 47630\\ 54640\\ 62050\end{array}$	70200 78810 87500	97330- 107100 117400	$\begin{array}{c} 128500 \\ 140000 \\ 151600 \end{array}$
			R.P.M.	795 662 568	495 441 397	361 331 305	283 265 248	234 220 208	198 189 180	172 166 159
CED DRA (TVPE L	1 In. or 0.577 Oz. Static Press. 1 \mathcal{H} In.	Boiler H. P. at	24.4 A.P.M.	250 360 490	635 805 995	1205 1435 1670	1950 2240 2545	2875 3230 3585	3990 4390 4810	5265 5740 6215
ANOIDAL			Н. Р.	2.36 3.38 4.61	$6.02 \\ 7.63 \\ 9.41$	11.4 13.6 15.9	18.4 21.0 24.0	27.2 30.5 33.9	37.6 41.4 45.5	49.7 54.2 58.7
FALO PL		or 0.577 Uz. Static Fan	Vol.	$5440\\7830\\10670$	$\begin{array}{c} 13900 \\ 17600 \\ 21750 \end{array}$	26290 31310 36500	42600 48880 55500	62800 70500 78270	$\begin{array}{c} 87050\\95770\\105020\end{array}$	$\frac{114900}{125160}$ $\frac{125620}{135620}$
BUFF			R.P.M.	711 592 508	443 394 355	323 296 273	253 237 222	209 197 186	177 169 161	154 148 142
		Boiler H. P. at	24.4 A.P.M.	225 320 430	570 720 890	1080 1285 1495	1745 2005 2275	2575 2890 3210	3570 3925 4300	4710 5130 5560
	Size of Fan			50 50 70	100 1000 1000	110 120 130	140 150 160	170 180 190	200 210 220	230 240 250

FAN ENGINEERING-BUFFALO FORGE COMPANY

PLA	NOI	DAI	LI	NDUC	EDI	RAF	TFA	N C	APAC	ITIE
300°	Press.		Н. Р.	9.33 13.4 18.2	23.8 30.2 37.2	45.1 53.8 62.9	72.7 83.1 95.0	107.5 120.4 133.9	148.6 163.5 180.0	196.3 214.2 231.9
	2 ½ In. or 1.442 Oz. Static Press.	Fan	Vol.	8600 12380 16870	21970 27830 34390	41560 49500 57700	67350 77280 87740	$ \begin{array}{c} 99280 \\ 111500 \\ 123800 \end{array} $	$\begin{array}{c} 137600\\ 151400\\ 166000\end{array}$	$\frac{181700}{197900}$ 214400
	or 1.442		R. P. M.	$1124 \\ 936 \\ 803$	701 623 561	511 468 432	400 375 351	331 312 294	280 267 255	244 234 225
NOMIZER	2 ½ In.	Boiler H. P. at	24.4 A.P.M.	350 505 690	900 1140 1410	1705 2030 2365	$2760 \\ 3165 \\ 3595$	4070 4570 5075	5640 6205 6805	7445 8110 8790
IES TTH ECO	Press.		Н. Р.	$6.68 \\ 9.56 \\ 13.0$	$17.0 \\ 21.6 \\ 26.6$	32.3 38.5 45.0	$52.1 \\ 59.5 \\ 68.0$	76.9 86.2 95.8	106.3 117.0 128.8	140.4 153.3 166.0
INDUCED DRAFT FAN CAPACITIES BUFFALO PLANOIDAL (TYPE L) EXHAUSTERS WITH ECONOMIZER	2 In. or 1.154 Oz. Static Press.	Fan	.Vol.	$ \begin{array}{c} 7690 \\ 11070 \\ 15090 \end{array} $	$19660 \\ 24890 \\ 30760$	$37180 \\ 44280 \\ 51620$	$60240 \\ 69120 \\ 78480$	88800 99700 110700	$\begin{array}{c} 123100 \\ 135400 \\ 148500 \end{array}$	162500 177000 191700
FT FAN EXHAU	or 1.154 (R. P. M.	1006 837 718	627 557 502	457 419 386	358 335 314	296 279 263	250 239 228	218 209 201
CED DRA (TYPE L)	2 In. e	Boiler H. P. at	A. P. M.	315 455 620	805 1020 1260	1525 1815 2115	2470 2835 3215	3640 4085 4535	5045 5550 6085	6660 7255 7855
NOIDAL	Press.		Н. Р.	5.46 7.83 10.7	13.9 17.7 21.8	26.4 31.5 36.8	42.6 48.7 55.6	63.0 70.6 78.5	87.0 95.7 105.4	115.0 125.5 135.8
ALO PLA	1 34 In. or 1.010 Oz. Static Press.	Fan	Vol.	7200 10360 14120	$ \begin{array}{c} 18390 \\ 23290 \\ 28780 \end{array} $	$34780 \\ 41420 \\ 48290$	$56620 \\ 64670 \\ 73430$	83080 93270 103500	$\frac{115200}{126700}$ $\frac{126700}{138900}$	$\frac{152000}{165600}$ $\frac{179400}{179400}$
BUFF	or 1.010		R. P. M.	941 783 672	586 521 470	427 392 361	335 314 294	277 261 246	234 224 213	204 196 188
	1 34 In.	Boiler H. P. at	24.4 A. P. M.	295 425 580	755 955 1180	$1425 \\ 1700 \\ 1980$	2315 2650 3010	3405 3825 4240	4720 5190 5690	6230 6785 7350
		of of Fan		50 50 70	80 90 100	110 120 130	140 150 160	170 180 190	200 210 220	230 240 250

				BUI	FALO P	INDUCED DRAFT FAN O BUFFALO PLANOIDAL (TYPE	AFT FAN NL (TYPI	INDUCED DRAFT FAN CAPACITIES Lo planoidal (Type L) exhaus	CAPACITIES L) EXHAUSTERS		*		550°
	1/2	In. or 0.	288 Oz. St	atic P	ress.	34 In.	or 0.433	Oz. Static	Press.	I In.	or 0.577 (Oz. Static	Press.
R.P.M. Vol. H.P. 3.2.4 R.P.M. Vol. H.P. 3.2.4 K.P.M. Vol. H.P. Yol. H.P. 580 4440 158 320 502 773 245 829 533 3943 533 3943 533 5	E d	er at	Fa	=		Boiler H. P. at		Fan		Boiler H. P. at		Fan	
580 4440 .961707115440 1.77 19582163803.77245865901.382.40503106703.473805871.23205.33302113502.464.304.44139004.534.955121.60505.33302117003.8165.4707.507.534.955121.60505.33201177003.8165.4707.5754.955.121.60505.3320214704.678103.9527537.501.9055.33203177005.5510.5537337501.6953.812045.55111252733651011.9213620381.815205347005.55111252733651011.921362138205347007.533651011.913003152038018.4207347007.533651018.0257440021.3203349107.533651018.0257440021.320451210552335510018.0254273300.940020511119402137500224274021.321.32051125128011387500224274021.321.41215128011387500224274021.3<	. P.				Н. Р.	32.4 A. P. M.	R. P. M.	Vol.	Н. Р.	32.4 A. P. M.	R.P.M.	Vol.	Н. Р.
312 11350 2.46 430 414 13900 4.53 495 512 16030 6.96 200 17760 312 545 395 17700 573 450 20330 8.81 201 1770 575 676 775 410 572 20330 8.81 201 21470 6.51 810 525 1150 8.75 410 25120 10.95 201 21470 6.51 1125 305 0.551 1125 31320 10.55 1115 3173 303100 18.7 207 39700 7.53 11255 2373 31320 18.6 1155 2033 49100 13.7 207 39700 7.53 13155 237 4500 18.8 1710 2133 30300 13.7 207 39700 7.53 13155 237 4500 13.6 296 2933 111 51280 1112 1940 210 62800 204 2240 213 111 51280 1112 2940 277 49100 213 111 51280 1112 9940 2313 5100 213 111 51280 1126 2002 204 2240 277 1111 51280 1126 2002 204 2250 3114 1111 51280 2132 2128 2129 2132 11111	13 27			90 10	.96 1.38 1.89	$\begin{array}{c} 170\\ 240\\ 330\end{array}$	711 592 508	$5440 \\ 7830 \\ 10670$	1.77 2.54 3.47	195 280 380	821 683 587	6280 9040 12320	2.72 3.91 5.33
$ \begin{array}{c cccccccccccccccccccccccc$	35 44 55			80 80 80	2.46 3.12 3.86	430 545 670	444 395 355	$\begin{array}{c} 13900 \\ 17600 \\ 21760 \end{array}$	4.53 5.73 7.06	495 630 775	512 456 410	$16050 \\ 20330 \\ 25120$	$^{6.96}_{8.81}_{10.9}$
	66 92			02 10	4.67 5.55 6.51	810 965 1125	323 296 273	$26290 \\ 31320 \\ 36510$	$ \begin{array}{c} 8.55 \\ 10.2 \\ 11.9 \\ \end{array} $	935 1115 1300	373 342 315	30360 36160 42160	$13.2 \\ 15.7 \\ 18.4 \\ $
$ \begin{bmatrix} 171 & 51280 & 11.1 & 1940 & 210 & 62800 & 20.4 & 2240 & 242 & 72520 & 31.4 \\ 152 & 53920 & 12.5 & 2175 & 198 & 70500 & 22.9 & 2352 & 51420 & 35.2 \\ 152 & 63920 & 13.8 & 2415 & 186 & 75290 & 25.4 & 2770 & 215 & 90400 & 35.1 \\ 144 & 71100 & 154 & 2685 & 177 & 87760 & 28.2 & 3105 & 204 & 100530 & 43.4 \\ 138 & 85770 & 18.6 & 3240 & 1610 & 95780 & 31.2 & 3145 & 196 & 110600 & 478 \\ 128 & 85770 & 18.6 & 3240 & 161 & 105050 & 31.2 & 3145 & 196 & 110600 & 478 \\ 128 & 93840 & 20.3 & 3550 & 154 & 114900 & 373 & 4065 & 178 & 132700 & 574 \\ 126 & 93840 & 20.3 & 3550 & 154 & 114900 & 373 & 4965 & 178 & 132700 & 574 \\ 121 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 121 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.1 & 4835 & 164 & 166820 & 678 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 126 & 100200 & 24.0 & 4185 & 142 & 135500 & 40.7 & 4460 & 171 & 144500 & 674 \\ 127 & 4205 & 4411 & 4835 & 164 & 166 & 171 & 144500 & 674 \\ 128 & 128 & 128 & 128 & 142 & 135640 & 676 & 678 \\ 128 & $	107 123 140			80 30 30	7.53 8.59 9.80	1315 1505 1700	254 237 223	42570 48800 55100	13.8 15.8 18.0	$1515 \\ 1740 \\ 1980$	293 273 257	49160 56440 64100	$21.3 \\ 24.3 \\ 27.7$
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	158 177 197			2020	$11.1 \\ 12.5 \\ 13.8 \\ 13.8 \\ 1$	1940 2175 2415	210 198 186	62800 70500 78290	20.4 22.9 25.4	2240 2525 2790	$242 \\ 228 \\ 215 $	$\begin{array}{c} 72520\\ 81420\\ 90400 \end{array}$	$\frac{31.4}{35.2}$ 39.1
126 93840 20.3 3550 154 114900 37.3 4095 178 132700 57.4 121 102200 22.1 3865 148 125500 40.7 4460 171 144560 62.6 116 110800 24.0 4185 142 135640 44.1 4835 164 156820 67.8	219 241 265			888	$15.4 \\ 16.9 \\ 18.6$	2685 2955 3240	177 169 161	87060 95780 105050	$28.2 \\ 31.0 \\ 34.2 \\ $	$3105 \\ 3415 \\ 3745$	$204 \\ 195 \\ 186 $	$\begin{array}{c} 100530\\ 110600\\ 121300\end{array}$	43.4 47.8 52.6
	$289 \\ 315 \\ 342 $			2 88	20.3 22.1 24.0	3550 3865 4185	154 148 142	$\frac{114900}{125200}$ $\frac{125200}{135640}$	37.3 40.7 44.1	4095 4460 4835	178 171 164	$\frac{132700}{144560}$ 156320	57.4 62.6 67.8

COMPANY

FAN ENGINEERING-BUFFALO FORGE

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LAN	10	ID.	A L	IN	DUCE	D D	RAFT	FAL	N CA	PACI	TIE
,ncc	Press.		Н. Р.	7.69 11.1 15.1	19.7 24.9 30.7	37.2 44.5 51.9	60.1 68.7 78.5	88.8 99.6 110.6	$122.8 \\ 135.1 \\ 148.7$	$162.2 \\ 177.0 \\ 191.7$	207.3 223.5 220.5
	2 In. or 1.154 Oz. Static Press.	Fan	Vol.	8880 12790 17430	22700 28750 35530	$\begin{array}{c} 42940\\ 51440\\ 59630\end{array}$	69530 79820 90660	$\begin{array}{c} 102600\\ 115200\\ 127900 \end{array}$	$\frac{142200}{156400}$ 171600	$\frac{187700}{204500}$ 221500	239700 258000
	or 1.154		R. P. M.	1160 966 830	724 645 580	528 484 446	415 383 364	342 323 304	289 276 263	252 242 232	222 214
	2 In.	Boiler H. P. at	32.4 A. P. M.	270 395 540	700 890 1095	1325 1590 1840	$2145 \\ 2435 \\ 2800 \\ $	3165 3555 3950	4390 4830 5300	5795 6310 6835	7400 7965
(TVPE L) EXHAUSTERS	Press.		H. P.	5.00 7.18 9.79	12.8 16.2 20.0	24.2 28.9 33.7	$39.1 \\ 44.7 \\ 51.0$	57.7 64.7 71.9	79.7 87.7 96.6	105.3 115.0 124.5	134.6
ALO PLANOIDAL (TYPE L) EXHAU	1 ½ In. or 0.865 Oz. Static Press	Fan	Vol.	7690 11070 15090	$\frac{19660}{24900}\\30760$	$37180 \\ 44290 \\ 51630$	$60200 \\ 69120 \\ 78500$	88810 99710 110800	$\frac{123100}{135500}$ 148600	$\frac{162500}{177000}$ 191800	207500 223400
L (TYPE	or 0.865		R. P. M.	1006 837 719	627 559 502	457 419 386	359 334 315	296 279 263	250 239 228	218 210 201	192
LANOIDA	1 ½ In.	Boiler H. P. at	32.4 A. P. M.	235 340 465	605 770 950	1150 1365 1595	1860 2135 2425	$2740 \\ 3075 \\ 3420 \\$	3800 4180 4585	5015 5465 5920	6405 6895
BUFFALO PLANOIDAL	Press.		Н. Р.	3.80 5.46 7.45	9.72 12.3 15.2	18.4 22.0 25.6	29.7 34.0 38.8	$43.9 \\49.2 \\54.6$	60.6 66.7 73.5	80.1 87.4 94.7	102.4
BU	1 1/4 In. or 0.721 Oz. Static Press.	Fan	Vol.	7020 10110 13770	$\frac{17940}{22730}\\22080$	$33940 \\ 40420 \\ 47130$	$54960 \\ 63110 \\ 71660$	001101 000101	$\frac{112400}{123600}$ $\frac{1123600}{135600}$	$\frac{148300}{161600}$ $\frac{175100}{175100}$	189500 204000
	or 0.721		R. P. M.	918 764 656	572 510 458	417 382 352	328 305 287	271 255 240	228 218 208	199 191 183	176 170 163
	1 ½ In.	Boiler H. P. at	A. P. M.	215 310 425	555 700 865	1050 1250 1455	1695 1950 2210	$2500 \\ 2810 \\ 3120 \\ $	3470 3815 4185	4580 4990 5400	5850 6295 6750
	Class	of Fan		50 60 70	80 90 100	110 120 130	140 150 160	170 180 190	200 210 220	230 240 250	260 270 280

P 0000

FAN	ΕN	GIN	EE	RING-	-BUF	FALO) FO	RGE	СОМ	PANY
550°	Press.		Н. Р.	$1.28 \\ 1.67 $	$2.12 \\ 2.61 \\ 3.16$	$3.76 \\ 5.12 \\ 6.69$	8.47 10.5 12.7	$15.1 \\ 17.7 \\ 20.5$	23.5 26.8 30.2	33.9 37.7 41.8
LU)	1 In. or 0.577 Oz. Static Press.	Fan	Vol.	$3240 \\ 4410 \\ 5760$	$\begin{array}{c} 7290 \\ 9000 \\ 10890 \end{array}$	$\frac{12960}{17640}$ 23040	$29160 \\ 36000 \\ 43560$	$51840 \\ 60840 \\ 70560$	$81000 \\ 92150 \\ 104000$	$\frac{116600}{130000}$ $\frac{144000}{144000}$
	or 0.577		R.P.M.	$ \begin{array}{c} 1080 \\ 926 \\ 810 \end{array} $	720 648 589	540 463 405	360 324 295	270 249 232	$216 \\ 203 \\ 191$	180 171 162
	1 In.	Boiler H. P. at	A. P. M.	100 135 180	225 275 335	400 545 710	$ \begin{array}{c} 900 \\ 1110 \\ 1345 \end{array} $	1600 1880 2180	2500 2845 3210	3600 4010 4445
ies n) fans	Press.		Н. Р.	.61 .83 1.09	$1.38 \\ 1.70 \\ 2.06$	2.45 3.33 4.35	$ \begin{array}{c} 5.51 \\ 6.79 \\ 8.22 \end{array} $	$ \begin{array}{c} 9.78 \\ 11.5 \\ 13.3 \end{array} $	$15.3 \\ 17.4 \\ 19.6$	22.0 24.5 27.2
INDUCED DRAFT FAN CAPACITIES NLO NIAGARA CONOIDAL (TVPE N)	34 In. or 0.433 Oz. Static Press.	Fan	Vol.	2810 3820 4990	$6310 \\ 7800 \\ 9430$	$11220 \\ 15280 \\ 19950 \\ 19950 \\ 19950 \\ 1000 \\ 10$	25250 31180 37730	44900 52690 61100	70150 79800 90100	$\begin{array}{c} 101000\\ 112600\\ 124700\end{array}$
FT FAN CONOIDA	or 0.433 (R. P. M.	935 802 702	624 561 510	468 401 351	$ \begin{array}{c} 312 \\ 281 \\ 255 \end{array} $	234 216 201	187 176 166	156 148 140
ED DRA	34 In.	Boiler H. P. at	^{32.4} A. P. M.	$^{85}_{155}$	$ \begin{array}{c} 195 \\ 240 \\ 290 \\ \end{array} $	$345 \\ 470 \\ 615$	$ \begin{array}{c} 780 \\ 960 \\ 1165 \end{array} $	1385 1625 1885	$2165 \\ 2465 \\ 2780 \\ 2780 \\ 2780 \\ 310 \\$	3120 3480 3850
INDUCED DRAFT FAN CAPACITIES BUFFALO NIAGARA CONOIDAL (TYPE N) FANS	Press.		Н. Р.	.33 .45 .59	.75 .92 1.12	$ \begin{array}{c} 1.33 \\ 1.81 \\ 2.37 \end{array} $	$3.00 \\ 3.70 \\ 4.47$	$5.32 \\ 6.25 \\ 7.24$	$ \begin{array}{c} 8.31 \\ 9.46 \\ 10.7 \end{array} $	12.0 13.4 14.8
BU	1/2 In. or 0.288 Oz. Static Press.	Fan	Vol.	2290 3120 4070	5160 6360 7700	$ \begin{array}{c} 9160 \\ 12470 \\ 16290 \\ \end{array} $	20620 25450 30800	$36650 \\ 43020 \\ 49890$	$57270 \\ 65160 \\ 73540$	$\begin{array}{c} 82450\\91920\\101800\end{array}$
	or 0.288		R.P.M.	764 655 573	509 458 417	382 327 286	255 229 209	191 176 164	153 144 135	127 121 115
	<u>1/2</u> In.	Boiler H. P. at	32.4 A. P. M.	70 95 125	160 195 240	285 385 505	635 785 950	$1130 \\ 1330 \\ 1540$	1770 2010 2270	2545 2835 3140
		Size of Fan		3 3 ^{1/2} 4	5 1/2 5 1/2	\$10	°011	13 13 14	1165	19 20

550°	Press.		Н. Р.	2.66 3.62 4.72	6.00 8.94	10.6 14.5 18.9	24.0 29.6 35.8	42.6 50.0 57.9	66.5 75.7 85.4	95.8 106.7 118.2
	2 In. or 1.154 Oz. Static Press.	Fan	Vol.	4580 6240 8150	$\begin{array}{c} 10310 \\ 12730 \\ 15400 \end{array}$	$\frac{18330}{24950}\\32580$	$\begin{array}{c} 41240\\ 50900\\ 61600\end{array}$	73300 86040 99800	$\frac{114600}{130000}$ $\frac{130000}{147100}$	$\frac{164900}{183900}$ $\frac{203700}{203}$
	or 1.154		R. P.M.	1527 1310 1146	1018 916 833	764 655 573	509 458 417	382 352 328	306 287 270	255 242 229
	2 In.	Boiler H. P. at	32.4 A. P. M.	140 195 250	320 395 475	565 770 1005	$1275 \\ 1570 \\ 1900 \\ 1000 \\ $	2260 2655 3080	3535 4015 4540	5090 5680 6285
TIES E N) FANS	c Press.		H. P.	1.73 2.35 3.07	$3.90 \\ 4.80 \\ 5.81$	$ \begin{array}{c} 6.91 \\ 9.41 \\ 12.3 \end{array} $	$15.6 \\ 19.2 \\ 23.3 \\ 23.3 \\ 15.6 \\ 19.2 \\ 10.2 \\ $	27.7 32.5 37.6	43.2 49.2 55.5	62.2 69.3 76.8
INDUCED DRAFT FAN CAPACITIES VLO NIAGARA CONOIDAL (TYPE N)	1 ½ In. or 0.865 Oz. Static Press.	Fan	Vol.	3970 5400 7050		$15860 \\ 21600 \\ 28200$	$35700 \\ 44100 \\ 53300$	63450 74460 86400	$ \begin{array}{c} 99200 \\ 113100 \\ 127300 \end{array} $	$\begin{array}{c} 142700 \\ 159100 \\ 176200 \end{array}$
FT FAN CONOID	or 0.865		R. P. M.	1322 1133 992	881 793 721	661 567 496	$\frac{441}{397}$	331 305 284	264 249 234	220 209 198
CED DRA	1 ½ In.	Boiler H. P. at	A P. M.	123 165 220	$275 \\ 340 \\ 410$	490 665 870	$1100 \\ 1360 \\ 1645$	1960 2300 2665	3060 3490 3930	4405 4910 5440
INDUCED DRAFT FAN CAPACITIES BUFFALO NIAGARA CONOIDAL (TYPE N)	c Press.		Н. Р.	$ \begin{array}{c} 1.31 \\ 1.79 \\ 2.33 \end{array} $	$2.96 \\ 3.65 \\ 4.42$	5.25 7.15 9.35	$11.8 \\ 14.6 \\ 17.7 $	21.0 24.7 28.6	32.9 37.4 42.2	47.3 52.7 58.4
BL	1114 In. or 0.721 Oz. Static Press.	Fan	Vol.	3620 4930 6440	8150 10060 12180	$14490 \\ 19720 \\ 25760$	$32600 \\ 40250 \\ 48700$	57960 68000 78900	90560 103000 116300	130300 145300 161000
	or 0.72		R. P. M.	1208 1035 906	805 725 659	604 518 453	403 362 330	302 279 259	242 227 214	201 191 181
	1 ½ In.	Boller H. P. at	A. P. M.	110 150 200	250 310 375	445 610 795	1000 1245 1505	1790 2100 2435	2795 3180 3590	4020 4485 4970
		of Fan	-	3 3 ½ 4	5 ½ 5 ½	\$0 M @	°01	132	15 16 17	18 19 20

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NIAGARA CONOIDAL INDUCED DRAFT FAN CAPACITIES

	ENGINES
FANS	CLASS "A" I
DRAFT FANS	SPEED CL
INDUCED	HIGH SP
PLATE	UFFALO
STEEL	TO E
SPECIAL	CONNECTEI
	DIRECT

											_		_			
Normal	Boiler Rating	150 200 300	400	560	650	750 900	1000	1000	1280	1280	1200	1200	1200	1600	1770	1770
Boller H. P.	Developed 50% Overload	225 300 450	675 675	750 840	900 975	1120	1500	1200	1920	1920	1800	1800	1800 2250	2400	2660 2400	2660
Cu. Ft. Gas per Min. at	sauce F. and 1.69" Static Press.	7260 9700 14400	19400	24200 27100	29100 31450	36100 43600	48400	048400 48400	62000 54800	62000	58200	58200	58200	77450	86000	86000
Rev.	per Min.	500 500 416	385 385	355	300	290 290	290	273	273 290	273	238	258	244 244	244	232 244	232
l. H. P.	Required	° 4.2 5.7 8.6	11.7	14.7	17.7	22.2 27.6	31.3	30.6	41.6 36.8	41.6	35.8 8	36.8	35.8	52.0	52.0	57.7
Max. I. H. P.	of Engine Frame	996	15 20 20	88	45	45	45	45	45	45	45	65	65	65	65	65
Fan Outlet	Width of Fan	11 14 1/2 17 3/2	$21\frac{34}{22}$	25 X	26 <u>7</u> 26 7	$\frac{30}{37}$	41	38 1/2	49 ½ 46	49 14	41 122	43 1/2	41 ½ 51 %	55	57 34	5734
Fan (Height of Outlet	32 32 32	42 <i>3</i> /4	46 1/4 53 1/4	53 X 56 3 X	56 34 56 34	56 34	89 472	60 ½ 56 %	60 1/2	64 % 67 %	64 14	222 62 62	67 1/2	71 K4 67 K	71 14
Diam. of	Fan Inlet	27 3% 30 1% 36 5%	41 88	45 34	50 ³⁴ 53 ³⁴	55 ^{7/8} 59 ^{5/8}	61 58	62 7/8	68 % 64 1/	683%	69 %	68 14	69 % 74 %	763%	×0 × 26 3%	80 %
Size	of Fan	90 90	120	130	150 160	160 160	160	170	170	170	190	180	190	190	200 1 80	200
Steam	Press. Gauge	55 76 70	102	81 66	73 95	111 78	83	104 92	125 67	81	22	94	96 127	80	104 62	73
Engine Cylinder	Diam. and Stroke	4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	999 8 X X 999 999	40 2 × 20 2 × 20 2 × 20	: × ×	2000 2000 2000	×	××	××	×	××	×	××	×	××	×
	nidmoð mu ^N	- 90	0 4 M	00		2=	22	24	29	<u>_</u>	22	8	52	53	25	26

	Normal	Rating	1950 2150 2150	2340 2540	2150 2340 2540	2760 3000	3280 3470	3470 3730 4000	4000	4260 4530	4800 5130	5400 5750	6050 6050 6400	6750 7100
	Boiler H. P.	Ueveloped 50% Overload	2920 3220 3220	$3510 \\ 3820$	3220 3510 3090	4150 4500	4925 5200	5200 5600 6000	6000 6400	6400	7220 7700	8120 8620	9075 9075 0600	10100
ENGINES	Cu. Ft. Gas per Min. at	and 1.69" Static Press.	$94500 \\ 103800 \\ 103800 \\ 103800 \\ 103800 \\ 103800 \\ 103800 \\ 103800 \\ 10080$	113300 123500	103800	134000	159000	168000	193500	206500	233500 248000	262000 278000	293500 293500 210000	327000 344000
"A" ENG	Rev.	Min.	220 212 212	202	212 202	186 186 179	$172 \\ 166$	166 160	155	150	141 137	133 129	125 125	119
CLASS	I. H. P.	Required	63.5 69.5 69.5	76.0 82.8	69.5 76.0	89.8 89.8 97.4	106.5	113.0 122.0	130.0	139.0	157.0 167.0	176.0 186.0	197.0 197.0	219.0 231.0 231.0
DH SPEED	Max. I. H. P.	or Engine Frame	95 95 95	95 95	95 95 95	35 135 135	135	200 200	285 285	285	285 350	350 350	350 350 350	350 350
BUFFALO HIGH	Fan Outlet	Width of Fan	60 % 63 ½ 63 ½	69 77 77 77	63 X 66 X X	08 % 72 75	77 3% 80 1/3	888 8772 8772	86 8 86 8 872 7	80% %	95 98	101 103 1/2	106%	115 %
TO BUF	Fan (Height of Outlet	74 58 78 78	81 % 85 ½3	78 81 34 85 34	89 89 92 1/	96 99 ½	$ \frac{99 }{103} $	106%	110	117 14	$124 \frac{1}{128}$	131 %	138 14 138 14 142 1/2
CONNECTED	Diam.	Fan Inlet	84 34 88 1/4 88 1/4	92 26 272	88 92 74 88 72 74	90 %3 100 %3 104 %	112 1/2	112% 116%	120 %3	124 1/2	132 22	$140\frac{15}{145}$	148 ½ 148 ½	157 157 161
RECT CO	Size	Fan	210 220 220	230	530 530	250 250	270	0000	300 300 310	310	330 340	350 360	370 370 320	390 400
IQ	Steam	Press. Gauge	100 115 80	92 104	988 188	101	95	91 98	211 98 108	95 95	114	95 104	113 92	106
	Engine Cylinder	Diam. and Stroke	10 x 12 10 x 12 10 x 12	< × ×	××	×××	××	XX	×××	< x >	××	××	××	20 x 18 20 x 18 20 x 18 20 x 18
	noitai Der	nidmoJ muN	27 28 28	30	333	32	37	6 9: 9 9:	-44	344	44	49	210	53

SPECIAL STEEL PLATE INDUCED DRAFT FANS

						ALO	FOI			
	Normal	Boiler Rating		100 150 200	250 300 350	500 600 750	900 1000		300 300 400	400 600 1200
	Boiler H. P.	Developed 50% Overload		150 225 300	375 450 525	750 900 1120	1350 1500		450 450 600	600 900 1800
	Cu. Ft. Gas per Min. at	2	•	4800 7260 9700	$12100 \\ 14400 \\ 17000$	$24200 \\ 29100 \\ 36100 \\$	43600 48400	-	$14400 \\ 14400 \\ 19400 \\ 19400 \\ 19400 \\ 100 \\ $	$19400 \\ 29100 \\ 58200$
SUGINES	Rev.	per Min.		580 580 580	415 415 415	325 290 290	260 260		580 580 500	500 415 290
SPECIAL STEEL PLATE INDUCED DRAFT FANS ST CONNECTED TO BUFFALO HIGH SPEED ENGINES	L H. P.	Required	ow Shaft	2.8 6.4 6.4	$^{7.2}_{8.8}_{10.6}$	14.9 17.8 22.9	27.2 30.0	ing	9.6 9.6 12.9	$12.9 \\ 19.5 \\ 38.7 \\ $
IDUCED I	Rated L. H. P.	of Engine	Vertical-Class "I"-Cylinder Below Shaft	5.0 7.5	0.11 0.11 0.11	$ \begin{array}{c} 18.5 \\ 25.0 \\ 25.0 \\ \end{array} $	30.0 30.0	Double Vertical—Double Acting	20.0 20.0 20.0	20.0 35.0 60.0
PLATE IN O BUFFA	utlet	Width of Fan	s "I"—Cy	8 12 16 15 16 12	$15 \\ 17 \\ 21 \\ 21$	$\begin{array}{c} 23 y_2 \\ 24 34 \\ 30 y_2 \\ \end{array}$	$32\frac{3}{14}$ $36\frac{1}{14}$	Vertical—I	$\begin{array}{c} 24 \ 1\% \\ 24 \ 1\% \\ 29 \end{array}$	$29 \\ 35 \\ 34 \\ 48 \\ 14 \\ 48 \\ 14 \\ 48 \\ 14 \\ 14 \\ 1$
VECTED 1	Fan Outlet	Height of Outlet	tical-Clas	28 14 28 14 28 14	39 39	$\frac{4934}{5634}$	64 64	Double	$^{28}_{22}_{22}_{22}_{24}_{22}_{22}_{22}_{22$	$32 \\ 39 \\ 56 \frac{3}{4}$
SPECIAL STEEL DIRECT CONNECTED	Diam. of	Fan Inlet	Ver	$22 \frac{1}{26}$ $28 \frac{1}{12}$	34 ½ 36 ½2 38 ½2	47 ¼ 52 56	61 34 63		$32 \frac{1}{12}$ $32 \frac{1}{12}$ 38	38 46 14 65 1/2
DIR	Size	Fan		8088	110 110 110	140 160 160	180 180		80 80 80	90 110 160
	Steam	Press. Gauge		65 100 85	75 90 105	90 80 100	85 95		110 65 85	55 55 60
	Engine Cylinder	Diam. and Stroke		3 x 31/2 3 x 31/2 4 x 31/2 2 x 31/2	4 1/2 x 5 4 1/2 x 5 4 1/2 x 5 7 2 5 2 5	5 ½ x 7 6 ½ x 8 6 ½ x 8 6 ½ x 8	7 1/2 x 9 7 1/2 x 9		3 x 3 ½ 4 x 3 ½ 4 x 4	5 x 4 6 x 5 8 x 8 8 x 8
	noitsi Der	nidmoJ muN		55 56 57	58 59 60	62 63 63	64 65		66 67 68	710

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Planoidal Type "L" Fan Direct Connected to Double-Vertical, Double-Acting Engine



Double Turbo-Conoidal Type "T" Fan

BUFFALO CONE WHEELS



The cone wheel is a style of fan frequently used where the resistance to be overcome is moderate, or where it is merely required to exhaust the air from a chamber or to exhaust from a series of ducts into an attic or out of doors. It may be used in many cases where a disk fan is ordinarily installed, and will give better efficiency than the latter. The efficiency is, however, lower than that obtainable with a wheel enclosed in a housing, so that it is generally advisable to use a standard steel plate or multivane fan. This is especially true if it is necessary to operate against any considerable resistance.

The table on page 333 gives the cubic feet of air per revolution at free delivery, as well as the performance under various pressures. The air H. P. under free delivery may be calculated by H. P. = $0.00026 \times \text{cap.} \times \text{press.}$ corresponding to the peripheral velocity expressed in inches. This should be increased to cover belt and bearing losses. CAPACITIES OF BUFFALO CONE WHEELS UNDER AVERAGE WORKING CONDITIONS AT 70° F. AND 29.92 INCHES BAROMETER

SS.	H. P.	3.43 4.95 6.75	8.80 11.1 13.7	16.7 19.8 27.0	35.2 44.6 54.9	79.2 108. 124.
1" Static Press.	Vol.	4600 6650 9050	$11800 \\ 14950 \\ 18400 \\ 18400 \\ 18400 \\ 18400 \\ 18400 \\ 1800 \\ $	22300 26600 36200	47200 59900 73600	$\frac{106000}{144800}$ $\frac{144800}{166500}$
1, S	R. P. M.	785 655 560	491 436 393	357 328 282	246 218 196	164 141 131
ress.	H. P.	2.23 3.22 4.39	$5.72 \\ 7.22 \\ 8.90$	10.9 12.9 17.6	22.9 29.0 35.6	51.5 70.2 80.6
Static Press.	Vol.	$3990 \\ 5760 \\ 7840$	$10220 \\ 12950 \\ 15950$	$ \begin{array}{c} 19300 \\ 23050 \\ 31350 \end{array} $	$\begin{array}{c} 40900\\ 51900\\ 63800\end{array}$	$ \begin{array}{c} 91850 \\ 125200 \\ 144200 \end{array} $
34"	R. P. M.	680 568 486	425 378 340	309 284 244	213 189 170	$142 \\ 122 \\ 114$
ress.	Н. Р.	$ \begin{array}{c} 1.21 \\ 1.75 \\ 2.39 \end{array} $	$3.11 \\ 3.92 \\ 4.84$	5.90 7.00 9.55	12.4 15.8 19.4	28.0 38.2 43.9
Static Press.	Vol.	3250 4700 6390	8350 10550 13000	$\frac{15750}{18800}$ $\frac{25500}{25500}$	$33350 \\ 42250 \\ 52000$	$\begin{array}{c} 75000\\ 102000\\ 117500\end{array}$
1/2"	R. P. M.	555 463 396	347 308 278	252 232 199	174 154 138	116 100 93
ress.	Н. Р.	$^{.79}_{1.13}$	$2.02 \\ 2.54 \\ 3.14$	$3.83 \\ 4.54 \\ 6.19$		$ \begin{array}{c} 18.1 \\ 24.8 \\ 28.4 \\ \end{array} $
Static Press.	Vol.	2810 4060 5530	$\begin{array}{c} 7210\\ 9150\\ 11250\end{array}$	$13600 \\ 16250 \\ 22100$	28800 36600 45000	${}^{64850}_{88450}_{101800}$
3%"	R. P.M.	480 400 343	300 266 240	218 200 172	150 133 120	001 88 80 80
ress.	Н. Р.	.43 .62 .85	1.10 1.39 1.71	$2.10 \\ 2.48 \\ 3.38 \\ 3.38 \\ 3.10 \\ $	4.40 5.58 6.85	$\begin{array}{c} 9.90 \\ 13.5 \\ 15.5 \end{array}$
Static Press.	Vol.	2300 3330 4530	$5900 \\ 7480 \\ 9200$	$11150 \\ 13300 \\ 1810$	$23600 \\ 29950 \\ 36800 \\ 36800 \\$	53000 72400 83250
M"	R. P.M.	393 328 282	246 219 197	178 164 141	123 109 98	82 71 66
Air ev. at livery		10 17 27	40 57 78	105 136 214	322 • 459 • 631	$ \begin{array}{c} 1085 \\ 1730 \\ 2110 \end{array} $
92	ZIS.	30 36	48 54 60	66 72 84	96 108 120	144 168 180

BUFFALO "B" VOLUME BLOWERS AND EXHAUSTERS (TYPES BB AND BE)



"B" Volume Blower

"B" Volume Exhauster

The table on page 335 shows the range of pressures and capacities for which these blowers and exhausters are designed, either for producing blast for forges and furnaces, for removing smoke and fumes in small ventilating installations, or for conveying dust and refuse from emery and polishing wheels. Data on application is given in another section. For forge blast a pressure of 3 to 5 ounces at the fan is sufficient, and for removing smoke a suction of 2 ounces at the fan is usually employed. For exhaust conveying systems either "B" volume exhausters or planing-mill exhaust fans may be used according to the nature of the material handled. With either type extra heavy blast wheel construction neutralizes the effect of abrasive material, while acid gases may be handled by blast wheels of cast iron, lead, copper, monel metal, or other suitable acid resisting material.

BE)	
AND I	
BB	
(TYPES	
EXHAUSTERS	
EXH	
AND	in Oz.
UME BLOWERS	al Pressure
VOLUME	Tot
"B"	
OF	
CAPACITIES	
RATED	
CZ.	

½ 0z.				1 0z.			1 ½ 0z.			2 0z.	
Cap.		Н. Р.	R. P. M.	Cap.	Н. Р.	R. P. M.	Cap.	Н. Р.	R. P. M.	Cap.	Н. Р.
104 264 438		.10	2396 1976 1387	148 374 621	.07 .19 .31	2935 2420 1695	181 458 760	14 34 57	3393 2800 1965	210 534 888	.23 .59 .99
585 837 837 1185	101-10	.13 .19 .26	1216 1098 898	828 1185 1677	.41 .59 .84	1490 1345 1100	1015 1450 2055	$\begin{array}{c} .76\\ 1.09\\ 1.54\end{array}$	1724 1556 1274	$1174 \\ 1688 \\ 2382 \\ 2382 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ $	1.30 1.87 2.65
$1372 \\ 1986 \\ 3299$	0010	.31 .44 .73	823 706 581	$\frac{1941}{2810} \\ \frac{2810}{4668} \\$.97 1.41 2.33	1010 865 710	2380 3440 5710	$1.78 \\ 2.58 \\ 4.28 \\ $	1168 1000 824	2752 3983 6641	3.06 4.43 7.30
4488	ø	1.00	494	6350	3.18	605	7780	5.82	702	9003	9.90
2 1/2	2 ½ 0z.			3 Oz.			4 Oz.			6 Oz.	
$234 \\ 592 \\ 983 \\ 983$	400	.29.75 1.23	4169 3437 2414	258 651 1090	.38 .96 1.62	3977 2794	753 1261	1.37 2.29	3436	1551	3.86
$1310 \\ 1875 \\ 2650 \\ 2650 \\ 1310 \\ 2650 \\ 2050 \\ $	000	1.65 2.36 3.34	$2119 \\ 1912 \\ 1563$	1441 2071 2923	2.14 3.08 4.33	2452 2212 1809	1667 2397 3382.	3.03 • 4.36 6.15	3015 2721 2225	$2051 \\ 2948 \\ 4160$	5.13 7.37 10.40
$3080 \\ 4450 \\ 7400$	800	$3.86 \\ 5.60 \\ 9.28$	1434 1229 1012	3377 4888 8150	5.00 7.24 12.10	1660 1422 1171	3908 5656 9431	7.10 10.20 17.10	2041 1748 1440	4806 6957 11599	12.00 17.40 28.90
10050	0	12.60	861	11050	15.00	966	12786	21.90	1225	15726	37.00

"B" VOLUME BLOWERS AND EXHAUSTERS

BUFFALO STEEL PRESSURE BLOWERS (TYPE P)



Steel Pressure Blowers are designed for relatively higher pressures and smaller capacities than "B" Volume Blowers and while they may be used for the same purposes, are intended especially for supplying blast to cupolas, furnaces, and forges requiring air pressure of from 6 to 14 ounces per square inch.

Steel Pressure Blowers for pressures as high as 16 ounces are also built in two stages.

The table on page 337 gives capacities and horsepower required for these blowers at various speeds and pressures. Table on page 110 gives special information regarding requirements for foundry service, and table on page 338 describes method of choosing blower and laying out piping in forge shops.

KING CONDITIONS	-00
DER ORDINARY WORI BAROMETER	7.02
CAPACITIES OF BUFFALO STEEL PRESSURE BLOWERS (TYPE P) UNDER ORDINARY WORKING CONDITION: TEMPERATURE 70° F. AND 29.92 INCHES BAROMETER Static Pressure in Ounces	6 Oz.
STEEL PRESSURE B TEMPERATURE 70° Stati	5 Oz.
ACITIES OF BUFFALO	4 0Z.
CAP	er DI

	Н. Р.	4.14	$5.42 \\ 6.40 \\ 9.66$	13.7 20.0 24.7	28.5 32.0		Н. Р.		27.1 38.3 56.7	69.1 80.5 90.5
8 Oz.	Cap.	950	$\begin{array}{c} 1240 \\ 1470 \\ 2220 \end{array}$	$3135 \\ 4590 \\ 5660 $	6350 7350	16 Oz.	Cap.		$ \begin{array}{c} 3115 \\ 4400 \\ 6510 \end{array} $	7940 8960 10395
	R.P.M.	4130	$3585 \\ 3180 \\ 2890 \\ 2890 \\ \end{array}$	2585 1935 1615	$1280 \\ 1310$		R.P.M.		4060 3635 2720	2265 1795 1840
	H. P.	3.05 3.38	4.42 5.25 7.93	$11.2 \\ 16.4 \\ 20.3 \\ $	23.4 26.3		Н. Р.	14.7	$22.3 \\ 31.4 \\ 46.1$	56.7 65.5 73.5
7 0z.	Cap.	785 890	$1160 \\ 1375 \\ 2080$	2940 4305 5300	$5940 \\ 6880$	14 Oz.	Cap.	1930	$2920 \\ 4125 \\ 6040$	7455 8340 9660
	R.P.M.	4395 3870	$3360 \\ 2985 \\ 2710$	$2425 \\ 1815 \\ 1510 \\ 1510 \\ 1$	1200 1230	ļ Į	R.P.M.	4195	$3810 \\ 3410 \\ 2545 \\ 2545 \\ $	$2120 \\ 1680 \\ 1720$
	Н. Р.	2.40 2.70	$3.52 \\ 4.15 \\ 6.28 $		$ \frac{18.5}{20.8} $		Н. Р.	9.90 11.7	$17.6 \\ 25.0 \\ 36.5$	45.0 52.0 58.4
6 Oz.	Cap.	730 825	$1076 \\ 1275 \\ 1925 \\ 1925 \\ 1925 \\ 1000 \\ $	2720 3090 4915	5500 6380	12 Oz.	Cap.	1510 1790	$2705 \\ 3825 \\ 5595 \\ 5595 \\ \end{array}$	6900 7720 8955
6 Oz.	R.P.M.	4065 3585 1	$3115 \\ 2765 \\ 2510 \\ 2510 \\ $	$2245 \\ 1680 \\ 1400 $	1110		R.P.M.	4380 3880	$3525 \\ 3155 \\ 2360 \\ 2360 \\$	1970 1555 1595
	Н. Р.	$ \begin{array}{c} 1.75 \\ 1.85 \\ 2.06 \end{array} $	2.70 3.32 4.80	$ \begin{array}{c} 0.80 \\ 9.93 \\ 12.3 \end{array} $	$14.1 \\ 15.9$		Н. Р.	7.55 8.90	$13.6 \\ 19.0 \\ 27.9$	34.4 40.2 44.6
5 Oz.	Cap.	635 670 755	$ \begin{array}{c} 985 \\ 1170 \\ 1765 \\ \end{array} $	2500 ° 3655 4515	5040 5840	19 Oz.	Cap.	$1385 \\ 1640$	$2480 \\ 3500 \\ 5135$	6320 7150 8200
	R. P. M.	4435 3730 3290	2860 2535 2300	$\begin{array}{c} 2060 \\ 1540 \\ 1285 \end{array}$	$1020 \\ 1045$		R.P.M.	4000 3560	$3225 \\ 2890 \\ 2160$	1800 1425 1460
	Н. Р.	$1.25 \\ 1.32 \\ 1.47 \\ $	1.94 2.27 3.43	4.84 7.09 8.74	$10.1 \\ 11.3$		Н. Р.	$4.95 \\ 6.45 \\ 7.61$	$11.6 \\ 16.3 \\ 23.8 \\ $	$29.4 \\ 33.8 \\ 38.1 \\ $
4 Oz.	Cap.	565 600 670	880 1045 1570	$2225 \\ 3255 \\ 4010 \\$	$\frac{4500}{5210}$	9 Oz.	Cap.	$ \begin{array}{c} 960 \\ 1310 \\ 1555 \end{array} $	$2350 \\ 3320 \\ 4870 \\ 4870 \\ \end{array}$	5995 6700 7780
	R.P.M.	3950 3330 2930	2550 2255 2050	1840 1375 1145	930 930		R. P. M.	4375 3810 3375	3065 2740 2050	1710 1355 1390
10 . Tew		₩ 4 10	879	° 9 I	11 ½	of Wer	BIO	10.01	80.0	11 32

STEEL PRESSURE BLOWERS

BUFFALO STEEL PRESSURE BLOWERS (TYPE P) APPLICATION TO FORGE FIRES

Many rges		m. of Blast- ipe	4 oz. P	ressure	5 oz. P	ressure	6 oz. P	ressure	8 oz. Pressure		
How	For Blowe Main		Speed H. P.		Speed	Н. Р.	Speed	Н. Р.	Speed	н. р.	
2 4 6	$2 \\ 3 \\ 4$	$4\frac{1}{2}$ 5 5 $\frac{1}{2}$	4986 3993 3363	.79 1.47 1.56	$5596 \\ 4473 \\ 3754$	$1.01 \\ 1.63 \\ 1.80$	$\begin{array}{c} 4811\\ 4051 \end{array}$	$2.45 \\ 2.60$			
8 10 13	5 6 7	6 7 8	2952 2573 2275	$1.78 \\ 1.95 \\ 2.23$	$3308 \\ 2883 \\ 2549$	$1.96 \\ 2.53 \\ 3.02$	$3564 \\ 3104 \\ 2749$	$2.95 \\ 3.31 \\ 4.28$	4107 3577 3168	$4.39 \\ 4.93 \\ 6.60$	
18 26 38 50	8 9 10 11	$9\frac{1}{2}$ $10\frac{1}{2}$ $12\frac{1}{2}$ 15	$2067 \\1851 \\1384 \\1154$	$3.25 \\ 4.75 \\ 6.75 \\ 8.50$	2316 2074 1550 1293	$\begin{array}{r} 4.53 \\ 6.45 \\ 9.41 \\ 11.60 \end{array}$	$2499 \\ 2238 \\ 1673 \\ 1394$	$\begin{array}{r} 6.46 \\ 9.03 \\ 12.91 \\ 15.77 \end{array}$	2880 2579 1928 1608	9.76 13.66 19.65 24.11	

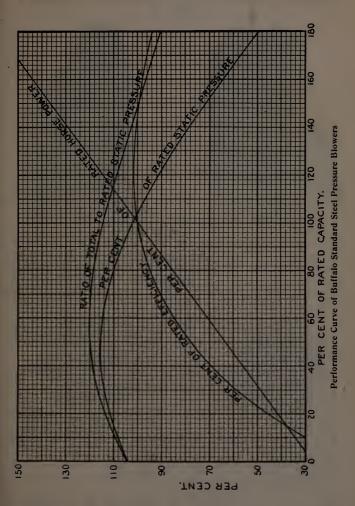
Static Pressure in Ounces

For a number of average fires not exceeding a total of ten, four ounces pressure at the blower is sufficient. If length of main blast-pipe is over 100 feet use next larger size pipe than shown in above table for the blower chosen. If length of main blast-pipe is over 150 feet increase pipe two sizes. Branch pipes to each forge should be three inches in diameter. Increasing size of pipes reduces friction, increases pressures at the fires, allows speed of blower to be reduced and saves power. If fires are extra heavy run the blower at a higher speed than shown in above table, if necessary, to get satisfactory results.

For 12 or more average fires five ounces pressure at the blower is necessary. If main blast-pipe is over 100 feet long, increase size as described above.

In railroad, implement and similar shops where some or all of the fires are large and deep it is necessary to maintain six or eight ounces pressure at the blower, depending on the number of fires.

As the outlet of the blower is smaller than the pipe recommended use an increaser to connect them.



BUFFALO STEEL PLATE PRESSURE BLOWERS (TYPE R)



Pulley Driven

Motor Driven

These are high efficiency fans, and are usually designed for pressures up to 14 or 16 ounces for cupola or furnace service, but may be built for pressures up to two or three pounds per square inch. The speeds for cupola work are suitable for direct connected motors, which are usually mounted on a sub-base built as a part of the fan. In large units the bearings are frequently mounted on independent pedestals, and the fans driven through flexible couplings, while for smaller sizes the fan wheel is overhung on the extended motor shaft.

It is possible to obtain, with a fan of this type, higher efficiencies than with standard radial blade steel plate fans, or with any form of multiblade fan.

Blower	Static Pressure in Oz. per Sq. In.													
of Blo		10 Oz.			12 Oz.			14 Oz.		16 Oz.				
No.	R.P.M.	Vol.	Н. Р.	R.P.M.	Vol.	Н. Р.	R.P.M.	Vol.	Н. Р.	R.P.M.	Vol.	H.P.		
5 6 7 8	1700 1700 1700 1700	$2700 \\ 3600 \\ 4800 \\ 6400$	$ \begin{array}{r} 13 \\ 18 \\ 24 \\ 32 \end{array} $	1700 1700 1700 1700 1700	$2700 \\ 3600 \\ 4800 \\ 6400$	16 21 29 38	1700 1700 1700 1700 1700	2700 3600 4800 6400						
9 10 11 12				$1120 \\ 1120 \\ 860 \\ 860 \\ 860$	8000 10000 12000 15000	48 58 71 89	$1120 \\ 1120 \\ 860 \\ 860 \\ 860$	8000 10000 12000 15000	$55 \\ 69 \\ 83 \\ 104$	$1120 \\ 1120 \\ 860 \\ 860 \\ 860$	8000 10000 12000 15000	63 79 95 119		

CAPACITIES OF BUFFALO STEEL PLATE PRESSURE BLOWERS

BUFFALO STANDARD REVERSIBLE PLANING-MILL EXHAUSTERS (TYPE M)



Pulley Driven



Motor Driven



Standard Blast-Wheel for Buffalo Steel Plate Mill Exhauster



Blast-Wheel for Stringy Material

BUFFALO STANDARD PLANING-MILL EXHAUSTERS (TYPE M)

These fans are ordinarily used for conveying materials and for removing shavings and factory refuse in general. Instructions for application are given in another section. The construction is similar to steel plate ventilating fans, but with special proportions and of considerably heavier material to stand wear. The fan wheels are always overhung, and the bearings of extra size. These fans are made single and double. The table below gives speed, capacity and horsepower for various pressures for single fans.

CAPACITIES UNDER NORMAL WORKING CONDITIONS Total Pressure in Ounces

		· · · · · · · · · · · · · · · · · · ·								
Size		1 Oz.			2 Oz.			3 Oz.		
Si	R. P. M.	Cap.	H. P.	R.P.M.	Cap.	Н. Р.	R.P.M.	Cap.	Н. Р.	
30 35 40	1025 890 770	$1650 \\ 2300 \\ 3000$	$.90 \\ 1.25 \\ 1.63$	$1450 \\ 1260 \\ 1090$	$2340 \\ 3250 \\ 4250$	2.55 3.53 4.60	$1775 \\ 1540 \\ 1334$	2850 3975 5190	$4.65 \\ 6.48 \\ 8.40$	
45 50 55	690 622 570	3825 4750 5750	$2.08 \\ 2.58 \\ 3.12$	976 880 806	5410 6720 8120	5.95 7.28 8.83	1195 1078 987	6620 8220 9950	$10.78 \\ 13.38 \\ 16.25$	
60 70 80	520 450 390	6900 9400 12200	$3.75 \\ 5.10 \\ 6.63$	735 637 552	9750 13300 17280	$10.60 \\ 14.50 \\ 18.75$	900 780 676	11950 16 30 0 21200	$19.50 \\ 26.60 \\ 34.50$	
Size		4 Oz.			5 Oz.		6 Oz.			
Si	R. P. M.	Cap.	Н. Р.	R. P. M.	Cap.	Н. Р.	R. P. M.	Cap.	Н. Р.	
30 35 40	$2050 \\ 1780 \\ 1540$	$3300 \\ 4600 \\ 6000$	$7.20 \\ 10.00 \\ 13.00$	2290 1990 1722	3680 5140 6700	$10.05 \\ 13.92 \\ 18.15$	$2510 \\ 2180 \\ 1888$	4040 5630 7350	$13.32 \\ 18.35 \\ 23.85$	
45 50 55	$1380 \\ 1245 \\ 1140$	7650 9500 11500	$16.60 \\ 20.60 \\ 25.00$	$1542 \\ 1391 \\ 1275$	$\begin{array}{r} 8550 \\ 10600 \\ 12850 \end{array}$	23.20 28.80 34.90		9350 11620 14080	30.40 37.90 45.80	
60 70 80	1040 900 780	$\frac{13800}{18800}\\24400$	30.00 40.90 53.00	1162 1005 872	$15400 \\ 21000 \\ 27300$	$\begin{array}{c} 41.90 \\ 56.90 \\ 74.00 \end{array}$	1100	16900 23000 29850	55.00 75.00 97.20	

NOTE-To make connections for special operating conditions use table on page 343.

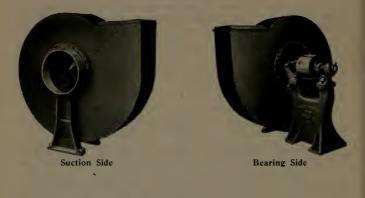
BUFFALO SINGLE STANDARD PLANING-MILL EXHAUSTERS (TYPE M) WITH DIFFERENT AREA SUCTION PIPES AND VARYING VELOCITIES

Speed and Power Requirements

Ext	hauster 52 Velocity Through Branch Suction Pipes In Feet per Minute															
	Ini ar Out	nd	Suction	Branc	3	000		3	500			4000			4500	
Size	Diameter	Area Sq. In.	-	Equivalent	Cubic Feet per Minute	R. P. M.	Brake H. P.	Cubic Feet per Minute	R. P. M.	Brake H. P.	Cubic Feet per Minute	R. P. M.	Brake H. P.	Cubic Feet per Minute	R. P. M.	Brake H. P.
30	12	113	79 113 154	10 12 14	1635 2360 3190	1620	2.0 3.2 5.6	1910 2750 3720	1890	3.3 5.1 9.2	2180 3150 4250	1925 2170 2552	4.72 7.60 13.50	2450 3540	2140 1485	6.6 10.8
35	14	154	113	12 14	2360 3190 4200	1185 1350	$2.52 \\ 3.90 \\ 6.35$	2750 3720 4890	1570	4.02 6.25 10.00	3150 4250 5540	1780	6.00 9.35 14.60		1990 1470	
40	16	201	154	14 16	3190 4200 5310	1018 1120	3.12 4.70 7.58	3720 4890 6200	1320	5.0 7.7 12.4	5540	1350 1495 1730	7.4 11.3 18.1	6280 7980	1520 1755 1970	$ \begin{array}{c} 16.2 \\ 25.8 \end{array} $
45	18	254	201	16 18	4200 5310 6550	908 973	3.90 5.65	6200	1030 1140 1370	6.25 9.10 13.40	7080	1170 1295 1450	9.25 13.30 19.20	7980 9820	$1320 \\ 1458 \\ 1640$	$19.2 \\ 28.2$
50	20	314	254	18 1 20	5310 6550 7920	770	4.7	6200 7650 9250	001	10 70		1028 1130 1260	15.7	9820 11890	1270	$15.85 \\ 22.30 \\ 31.80$
58	5 22	2 38	314	4 20 0 22	6550 7920 9450	690 748	5.50	9250	810	8.8	8730	908	$12.6 \\ 17.6$	9820 11890 14150	1265	25.4 35. 5
6	2	4 45	38	0 22 2 24	7920 9450	630 684	1 8.60	2 9250 0 11000 0 12900	808	13.8	5 1057 0 1255 0 1470	0 911	$15.3 \\ 20.4 \\ 24.6$	11890 14150 16500	1043	38.0
7	0 2	8 61	53	1 26 6 28	1110	0 530 0 57	8.3	1290 1495 1710	0 62 0 67	2 13.4 0 18.3 0 22.6	1470 1710 1960	0 744	19.4 25.8 33.2	1650 1920 2210	0 858 0 920	27.8 36.6 47.4
8	0 3	2 80	70	07 30 04 32	1470 1670	0 46 0 48	0 10.5 5 13.2 1 16.8	1710 1950 2210	0 56	5 16.8 9 22.6 1 26.7	2220	0 645	24.9 5 31.2 5 40.0	2210 2500 2830	0 73	0 35.6 0 48.0 9 57.5

Nore—Tables are computed on the basis that the system will have 275 feet of piping including equivalent of one collector. The diameter of main discharge pipe is in each instance assumed of same area as the fan outlet. For each additional 10 feet of suction or discharge piping, the speed should be increased approximately one per cent. and the power will be increased approxi-mately three per cent. If a collector and elbows are included in the system, the length of pipe to which they are equivalent must be added to the sectual length, in order to determine the total equivalent operating length from which speed and power may be figured. If the total operating length is less than 275 feet, the speed should be decreased approximately one per cent. For double fans, power and air handled will be doubled.

BUFFALO SLOW SPEED REVERSIBLE PLANING-MILL EXHAUSTERS (TYPE E)





Standard Slow Speed, High Efficiency Slow Speed Blast-Wheel for Stringy Blast=Wheel



Material

BUFFALO SLOW SPEED PLANING-MILL EXHAUSTERS (TYPE E)

These fans are of the high efficiency type explained elsewhere, and while intended for the same purposes as the standard mill exhausters, require from 15 to 50 per cent. less power. The speed is also reduced one-third, and the size of the fan is increased nearly 50 per cent. For cases where refuse fuel is not available for furnishing power, it is advisable to use this fan, on account of the decrease in power cost.

0		1 Oz.			2 Oz.		3 Oz.			
Size	R. P. M .	Cap.	н. р.	R. P. M.	Cap.	Н. Р.	R. P. M.	Cap.	Н. Р.	
30 35 40	640 552 482	$1650 \\ 2300 \\ 3000$.75 1.04 1.36	906 781 682	$2340 \\ 3250 \\ 4250$	2.12 2.94 3.83	1110 958 837	2850 3975 5190	$3.87 \\ 5.40 \\ 7.00$	
45 50 55	428 385 350	3825 4750 5750	$1.73 \\ 2.15 \\ 2.60$	$ \begin{array}{r} 605 \\ 544 \\ 494 \end{array} $	5410 6720 8120	$4.96 \\ 6.06 \\ 7.35$	742 667 606	6620 8220 9950	8.97 11.10 13.50	
60 70 80	321 • 275 • 241	$\begin{array}{r} 6900 \\ 9400 \\ 12200 \end{array}$	$3.12 \\ 4.25 \\ 5.52$	453 387 341	9750 13300 17280	$8.83 \\ 12.10 \\ 15.60$	556 477 418	$ \begin{array}{r} 11950 \\ 16300 \\ 21200 \end{array} $	$16.20 \\ 22.10 \\ 28.70$	
e		4 Oz.			5 Oz.		6 Oz.			
Size	R. P. M.	Cap.	Н. Р.	R. P. M.	Cap.	Н. Р.	R . P. M.	Cap.	Н. Р.	
30 35 40	$1280 \\ 1100 \\ 965$	$3300 \\ 4600 \\ 6000$	$6.00 \\ 8.32 \\ 10.80$	1428 1230 1075	3680 5140 6700	8.37 11.59 15.10	1570 1350 1180	4040 5630 7350	$11.10 \\ 15.25 \\ 19.84$	
45 50 55	855 769 698	7650 9500 11500	$13.80 \\ 17.12 \\ 20.80$	955 860 782	$\begin{array}{r} 8550 \\ 10600 \\ 12850 \end{array}$	$19.3 \\ 24.0 \\ 29.1$	$1050 \\ 942 \\ 856$	9350 11620 14080	$25.30 \\ 31.50 \\ 38.10$	
60 70 80	641 550 482	$\frac{13800}{18800}\\24400$	$25.00 \\ 34.10 \\ 44.20$	718 613 570	15400 21000 27300	34.7 47.3 61.7	786 674 590	16900 23000 29850	45.80 62.40 81.00	

CAPACITIES UNDER NORMAL WORKING CONDITIONS

Total Pressure in Ounces

NOTE-To make connections for special operating conditions use table on page 346.

BUFFALO SINGLE SLOW SPEED HIGH EFFICIENCY MILL EXHAUSTERS (TYPE E) WITH DIFFERENT AREA SUCTION PIPES AND VARYING VELOCITIES

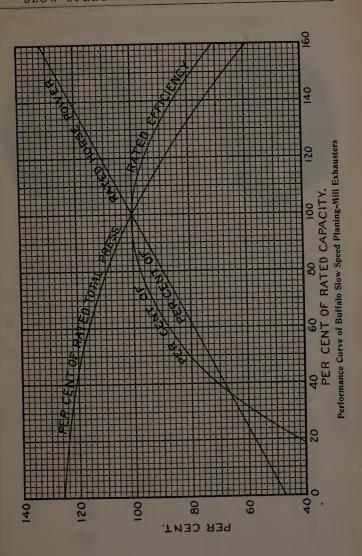
	Speed ar	id Power	Requi	rements		
nes	Veloci	ty Through	Branch	Suction	Pipes In	Feet

Exhauster

		irements

	<u> </u>					che	Velocity Through Branch Suction Pipes in Feet per Min.											
	Inlet Outlet		Outlet	Suction	Branche		3000			8500			4000			4500		
Size	Diameter	Area Sq. In.	Size	Area Sq. In.	Area Sq. in.	Equivalent Diameter	Cubic Feet per Minute	R. P. M.	Brake H. P.	Cubic Feet per Minute	R. P. M.	Brake H. P.	Cubic Feet per Minute	R. P. M.	Brake H. P.	Cubic Feet per Minute	R. P. M.	Brake H. P.
30	121	123	112x94	116	79 113 154	10 12 14	1635 2360 3190	989	1.6 2.6 4.6	2750	1022 1155 1365	4.2	3150	1175 1319 1552	6.3		1300 1485	
35	14§	168	13#x11	157	113 154 201	$ \begin{array}{r} 12 \\ 14 \\ 16 \end{array} $	2360 3190 4200	724 822 935	2.1 3.2 5.3	2750 3720 4890	850 955 1082	3.3 5.2 8.3	3150 4250 5540	1083	5.0 7.8 12.2		1081 1215 1470	
40	16	217	158x134	206	154 201 254	14 16 18	3190 4200 5310	620 683 790	$2.6 \\ 3.9 \\ 6.3$	3720 4890 6200	721 806 936	4.1 6.4 10.3	4250 5540 7080	824 911 1055	6.1 9.4 15.1		927 1070 1200	
45	18§	272	178×148	258	201 254 314	16 18 20	4200 5310 6550	553 593 664	3.2 4.7 7.0	4890 6200 7650	629 695 777	$5.2 \\ 7.6 \\ 11.1$	5540 7080 8730	714 790 888	7.7 11.1 16.0	6280 7980 9820		10.9 16.0 23.5
50	20§	334	194x163		254 314 380	18 20 22	5310 6550 7920	470 526 575	3.9 5.5 7.9	6200 7650 9250	551 606 678	6.2 8.9 12.6	7080 8730 10570		9.2 13.1 18.5	7980 9820 11890	775	$13.2 \\ 18.6 \\ 26.5$
55	223	406	8		314 380 452	20 22 24	6550 7920 9450	422 456 512	4.6 6.3 8.8	7650 9250 11000	494 534 606	7.3 10.2 14.2	8730 10570 12550	606	$10.5 \\ 14.7 \\ 20.5$	9820 11890 14150	634 674 772	21.2
60	243	481	234x197	460	380 452 531	22 24 26	7920 9450 11100	384 417 450		9250 11000 12900	437 491 526	11.5	10570 12550 14700	556	16.9	11890 14150 16500	573 637 678	23.4
70	283	649	3	621	531 616 707	28	11100 12800 14700	323 351 378	9.2	12900 14950 17100	408	15.3	14700 17100 19600	454	21.5	16500 19200 22100	484 522 561	30.5
80	321	842	304x264	804	707 804 908	32	14700 16700 18900	280 296 319	11.0	17100 19500 22100	347	18.8	19600 22200 25200	394	26.0	22100 25000 28300	421 446 481	40.0

NOTE—Tables are computed on the basis that the system will have 275 feet of piping including equivalent of one collector. The diameter of main discharge pipe is in each instance assumed of same area as the fan outlet. For each additional 10 feet of suction or discharge piping, the speed should be increased approximately one per cent. and the power will be increased approxi-mately three per cent. If a collector and elbows are included in the system, the length of pipe to which they are equivalent must be added to the actual length, in order to determine the total equivalent operating length irom which speed and power may be figured. If the total operating length is less than 275 feet, the speed should be decreased approximately one per cent. For double fans, power and air handled will be doubled.



BUFFALO DISK FANS (TYPE D)





Pulley Driven

Motor Driven

The ordinary disk or propeller fans should not be used in connection with a system of piping, but should discharge directly into a room, or exhaust from it without obstruction. Although not as efficient as a centrifugal cased fan, the lower first cost, large air capacity and simplicity of installation account for the wide use of fans of this type for ventilating engine and boiler rooms, kitchens, restaurants, small theatres, brass foundries, etc. A conservative table for the air capacities of actual disk fan installations is given below for normal speeds, and table on page 349 gives capacities and horsepowers for various speeds.

These disk fans are probably more often installed with direct connected motors than for belt drive, and such outfits have become standardized for both direct and alternating current.

Normal Speed	Cu. Ft. Air per Min.				
1060	2050				
	3725				
660	5950				
530	8240				
	11150				
400	14600				
350	18450				
320	22900				
265	32850				
230	44800				
200	58700				
175	74300				
	$ \begin{array}{c} 1060\\ 800\\ 660\\ 530\\ 450\\ 400\\ 350\\ 320\\ 265\\ 230\\ 200\\ \end{array} $				

		Н. Р.		247.795 .795 1.410	$ \begin{array}{c} 1.780 \\ 2.410 \\ 3.150 \end{array} $	$3.980 \\ 4.940 \\ 7.120$	$ \begin{array}{c} 9.660 \\ 12.660 \\ 16.620 \end{array} $
	7000	Vol.		2880 5210 8360	$11520 \\ 15660 \\ 20520$	25920 32040 46260	62800 82300 103500
		R.P.M.		$1486 \\1115 \\929$	743 637 557	495 446 372	318 279 248
		Н. Р.		.155 .498 .876	$ \begin{array}{c} 1.100 \\ 1.520 \\ 2.000 \end{array} $	2.570 3.220 4.490	$\begin{bmatrix} 6.060 \\ 7.740 \\ 10.000 \end{bmatrix}$
S 30°	6000	Vol.		2480 4470 7160	$ \begin{array}{c} 9900 \\ 13410 \\ 17550 \end{array} $	22230 27450 39600	53900 66600 89000
BLADE		R.P.M.		$1274 \\ 956 \\ 796$	637 546 478	425 382 319	273 226 212
LE OF		Н. Р.		.089 .286 .526	.630 .870 1.150	$ \begin{array}{c} 1.450\\ 1.890\\ 2.580 \end{array} $	$3.550 \\ 4.600 \\ 5.830$
NA-NG	5000	Vol.		2050 3720 5970	8240 11160 14580	18450 22860 32850	44800 58700 74300
TIVER		R.P.M.	1	1060 796 663	530 454 308	353 318 318	227 199 177
REE DE		Н. Р.		.046 .148 .259	.328 .484	.744 .972 .972	1.350 2.350 3.020
DERFORMANCE OF DOLLARD ANGLE OF BLADES 30° OPERATING AT FREE DELIVERY-ANGLE OF BLADES 30°	4000	Vol.	Í	1650 2990 4780	6590 8970	11/00 14850 18360 18360	203300 35900 46900 59600
RATING		R.P.M.		850 638 531	425 364	283 255	213 182 159 142
PE OPE		H. P.		.019	.137	.249 .307 .388	.550 .750 .978 1.250
	3000	Vol.		1230 2230	4940 6730	8790 11070 13680	$ \begin{array}{r} 19700 \\ 26800 \\ 35000 \\ 44500 \\ \end{array} $
		R.P.M.		636 477	398 318 273	239 212 191	159 136 119 106
	Peri. Velocity	Size		18 24	30 36 42	48 54 60	72 84 108

PERFORMANCE OF BUFFALO DISK WHEELS (TYPE D)

NorE-Air Velocity = 16.2% of Peripheral Velocity

349

DISK FANS

BUFFALO MULTIBLADE DISK FANS (TYPE CM)



Disk fans with many overlapping blades are better suited than standard disk fans for maintaining sufficient pressure to overcome a moderate piping resistance or other friction, and are usually employed for boosters, in mine ventilation, or for producing air flow in cooling towers for condensing plants. The casing and bearings are self-contained to facilitate installation. The normal speeds, air capacities and horsepowers are given in the following table:

Size	Normal Speed	Cu. Ft. Air per Min.	Horsepower
18	900	3200	.25
24	800	6300	.50
30	650	10000	.75
36	525	14000	1.00
42	450	19300	1.50
48	400	25200	2.00
54	350	32000	2.50
60	320	36000	3.00
72	265	56000	5.00
84	226	77000	7.50

BUFFALO PROPELLER FANS (TYPE F)



Pulley Driven

Motor Driven

The propeller fan has a capacity 25 to 30 per cent. greater than a disk fan of the same size, is used for the same general purposes, and may be furnished either pulley driven or with direct connected motor. 48-inch and smaller disk and propeller fans are made with overhung wheels, so that it is unnecessary to reach between the blades for oiling the outer bearing.

Table of capacities and horsepowers at normal speed is given below.

Size	Normal Speed Cu. Ft. Air per Min.		Horsepower	Pulley Size
18	1050	2600	.14	$\begin{array}{cccccccccccccccccccccccccccccccccccc$
24	800	4750	.37	
30	650	7600	.79	
36 42 48	525 450 400	$10500 \\ 14250 \\ 18650$.95 1.30 1.75	$ \begin{array}{ccccccccccccccccccccccccccccccccccc$
54	350	23550	2.20	$\begin{array}{cccc} 4 & x & 9 \\ 5 & x & 10 \\ 5 & 2 & x & 12 \\ 6 & x & 14 \end{array}$
60	320	29200	2.85	
72	265	42000	3.90	
84	225	57000	5.30	

FAN

PERFORMANCE OF BUFFALO PROPELLER WHEELS (TYPE F) OPERATING AT FREE DELIVERY—ANGLE OF BLADES 30°

	Н. Р.	$371 \\ 1.19 \\ 2.12 $	2.67 3.62 4.73	$ \begin{array}{c} 5.97 \\ 7.41 \\ 7.41 \\ 10.68 \\ \end{array} $	$ \begin{array}{r} 14.49 \\ 18.99 \\ 24.93 \\ \end{array} $
7000	Vol.	3680 6660 10690	$14720\\20000\\26220$	$33130 \\ 40950 \\ 59100$	80300 105000 132300
	R.P.M.	1486 1115 929	743 637 557	495 446 372	318 279 248
	Н. Р.	233 .747 1.31	1.65 2.28 3.00	3.86 4.83 6.74	$ \begin{array}{c} 9.09 \\ 11.61 \\ 15.00 \end{array} $
6000	Vol.	$3160 \\ 5720 \\ 9160$	$12650 \\ 17140 \\ 22430$	$\begin{array}{c} 28410\\ 35080\\ 50610 \end{array}$	68900 86000 113800
	R.P.M.	1274 956 796	637 546 478	425 382 319	273 226 212
	Н. Р.	.134 .369 .789	$ \begin{array}{c} .945 \\ 1.31 \\ 1.73 \end{array} $	$2.18 \\ 2.84 \\ 3.87 \\ 3.87 \\$	5.33 6.90 8.75
5000	Vol.	2620 4750 7630	$10520 \\ 14260 \\ 18630$	$23580 \\ 29210 \\ 41980$	57300 75000 94900
	R.P.M.	1060 796 663	530 454 398	$353 \\ 318 \\ 265 $	227 199 177
	Н. Р.	.069 .232 .389	.492 .726 .888	$1.12 \\ 1.46 \\ 2.01$	2.70 3.53 4.53
. 4000	Vol.	$2110 \\ 3820 \\ 6110 \\ 6110 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 $	8420 11470 14950	$18980 \\ 23460 \\ 33930 \\$	$\frac{45900}{59900}$ 76100
	R. P.M.	850 638 531	425 364 319	283 255 213	182 159 142
	Н. Р.	.029 .093 .164	.206 .284 .374	.461 .582 .834	$1.13 \\ 1.47 \\ 1.88 \\ 1.88 \\$
3000	Vol.	1580 2850 4580	$\begin{array}{c} 6310 \\ 8600 \\ 10100 \end{array}$	$\frac{14150}{17480}\\25200$	34280 44740 56800
	R.P.M.	636 477 398	318 273 239	$212 \\ 191 \\ 159$	136 119 106
Peri. Velocity	Size	18 24 30	36 42 48	54 60 72	84 96 108

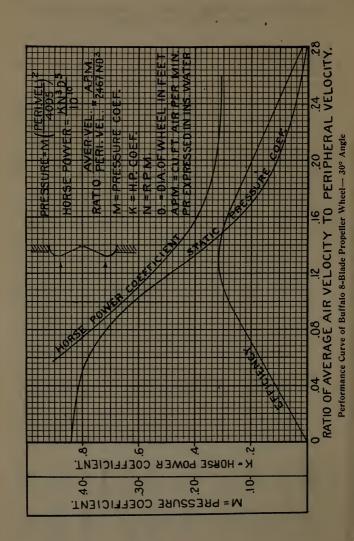
Nore-Air Velocity = 20.7% of Peripheral Velocity

>

PROPELLER FANS

PERFORMANCE OF 8-BLADE PROPELLER WHEELS—30° ANGLE OPERATING AGAINST RESISTANCE

Vol. 2070	Н. Р.
2070	
2920 3570 4130	.52 1.46 2.70 4.13
3760 5190 6350 7340	.92 2.59 4.76 7.34
$5730 \\ 8100 \\ 9930 \\ 11450$	$1.43 \\ 4.04 \\ 7.43 \\ 11.4$
8260 11680 14290 16520	2.07 5.83 10.7 16.5
11240 15890 19450 22480	$2.81 \\ 7.93 \\ 14.6 \\ 22.5$
$14680 \\ 20760 \\ 25400 \\ 29360$	3.68 10.4 19.0 29.4
19050 26300 32200 37200	4.66 13.1 24.1 37.2
22940 32440 39690 45880	5.7516.229.845.9
33040 46720 57160 66080	$\begin{array}{r} 8.28 \\ 23.3 \\ 42.8 \\ 66.0 \end{array}$
44960 63560 77800 89920	11.2 31.7 58.4 90.0
	4130 3760 5190 6350 7340 9930 11450 8100 9930 11450 11680 14290 16520 11240 15890 19450 22480 2480 2480 2480 20760 25400 29360 19050 26300 32200 37200 32240 32400 32240 32400 32240 32400 32200 32240 32600 32200 32600 32000 32600 37600 37600 37600 377000 37700 37700 37700 37700 37700 37700 37700



BUFFALO ELECTRIC BLOWERS (TYPE FB)



Constant Speed

Variable Speed

This type of blower has been developed for furnishing small volumes of air at pressures from one to three ounces for forge fires and furnaces, for blowing church organs, and in fact any purpose for which the various sizes may be applicable, handling from 60 to 250 cu. ft. per minute.

These fans may be used for exhausting at the same pressures, and are furnished with motors for 110 or 220 volts, either alternating or direct current. The design of the blast-wheel and casing is special, similar to the high efficiency steel plate fans, so as to make the power consumption remarkably low.

No. of Blower	R. P. M.	Cu. Ft. Air per Min.	Pressure Oz. per Sq. 1n.	Diam. of Outlet	Total Height
1E 2E 2EH 3E 4E	3800 1800 3000 3000 3200	60 75 150 200 250	1 1 ½ 2 ½ 2 2 ½ 2 ½	3" 3" 3" 4" 5"	10" 15" 15" 15" 20"

BABY CONOIDAL FANS (TYPE IC)



Small motor driven fans for exhaust ventilation are preferable to the use of desk fans, since they provide means for introducing fresh air, or for positively removing fumes and odors. They are also used for small drying outfits in connection with steam or electrical heaters. Standard sizes are arranged for direct or alternating current motors; fans are of Conoidal type with housings which are reversible. The following table shows capacities of some of the smaller stock sizes.

Size	Cu. Ft. Air per Min.	Horsepower	Speed R. P. M.	Height, Inches	
No. 1	90	1/30	1800		
No. 2	250	1/8	1800		
No. 3	500	1/4	1800		



Planoidal Type "L" Fan Wheel

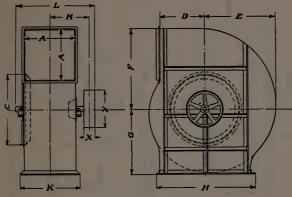


Cowl Ventilator

SECTION IV FAN DIMENSIONS

Included in this section will be found dimensions of various fans and blowers. Dimensions of Planoidal, Niagara Conoidal and Turbo-Conoidal fans are given for both full and threequarter housing, for top horizontal, bottom horizontal, up and down discharge. Dimensions are given on pages 382 to 385 for double width Niagara Conoidal and Turbo-Conoidal fans. Dimensions of slow speed and standard planing-mill exhausters, single and double width, will be found on pages 394 to 397, and on page 398 are given dimensions of steel pressure blowers.

PLANOIDAL (TYPE L) FANS

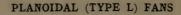


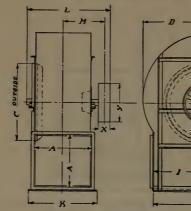
OVERHUNG PULLEY FULL HOUSING—TOP HORIZONTAL DISCHARGE

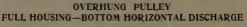
Dimensions in Inches

Size	A	Exh.	C Blow.	D	E	F	G	н	к	L	M	x	Y
30 35 40	$10\frac{34}{12\frac{1}{2}}$ $12\frac{1}{2}$ $14\frac{1}{4}$	$ \begin{array}{r} 13 \frac{1}{4} \\ 15 \frac{3}{8} \\ 17 \frac{1}{2} \end{array} $	$11\frac{5}{13}\frac{1}{12}$ $13\frac{1}{2}$ $15\frac{1}{2}$	$10\frac{1}{2}$ 12 $13\frac{1}{2}$	$14\frac{7}{8}\\17\frac{1}{4}\\19\frac{5}{8}$	$16\frac{5}{8}$ 19 ¹ / ₄ 21 ⁷ / ₈	$14\frac{1}{8}\\16\frac{1}{4}\\18\frac{3}{8}$	25 28 31	15163/4181/2	$25\frac{1}{4}\\27\frac{1}{8}\\28\frac{3}{4}$	$13\frac{1}{4}$ $14\frac{1}{4}$ 15	333	8 9 10
45 50 55	17 %	19 5/8 23 25 1/2	$17\frac{3}{8}\\19\frac{1}{4}\\21\frac{1}{4}$	$15\\16\frac{1}{2}\\18$	$22\frac{3}{8}$ $24\frac{3}{4}$ 27	$25 \\ 27\frac{5}{8} \\ 30\frac{1}{8}$	$20\frac{3}{4}\\22\frac{7}{8}\\24\frac{7}{8}$	34 37 40	$20\frac{3}{8}$ $22\frac{1}{8}$ $23\frac{7}{8}$	3011 335 3578 3578	$16 \\ 17\frac{1}{4} \\ 18\frac{1}{4}$	3 4 4	$ \begin{array}{c} 11 \\ 12 \\ 14 \end{array} $
60 70 80	$21\frac{1}{25}$ $28\frac{1}{2}$	$28\frac{1}{2}$ 35 40	23 ½ 27 30 %	19 ½ 23 26	$\begin{array}{r} 29\frac{3}{8}\\ 34\frac{1}{2}\\ 39\frac{5}{8} \end{array}$	$32\frac{3}{4}$ $38\frac{1}{2}$ $44\frac{1}{4}$	$27 \\ 31 \frac{1}{2} \\ 36$	43 50 56	$25\frac{3}{4}\\29\frac{1}{4}\\32\frac{3}{4}$	39 ¹ / ₈ 45 ³ / ₈ 49 ³ / ₈	$20 \\ 21 \frac{3}{4} \\ 25$	5 5 6	$\begin{array}{c}16\\18\\20\end{array}$
90 100 110	$32\frac{1}{4}$ $35\frac{3}{4}$ $39\frac{1}{4}$	45 50 55	$\begin{array}{r} 34 {}^3\!\!\!/_4 \\ 38 {}^5\!\!\!/_8 \\ 42 {}^1\!\!\!/_2 \end{array}$	32	$\begin{array}{r} 44\frac{3}{8}\\ 49\frac{3}{8}\\ 54\frac{1}{8}\end{array}$	$\begin{array}{r} 49\frac{1}{2} \\ 55\frac{1}{8} \\ 60\frac{3}{8} \end{array}$	$\begin{array}{r} 40\frac{1}{4} \\ 44\frac{5}{8} \\ 48\frac{7}{8} \end{array}$	62 68 75	$36\frac{1}{2}$ 40 44 $\frac{1}{2}$	$53\frac{1}{4}$ $58\frac{1}{2}$ 63	$27 \\ 29 \frac{1}{2} \\ 31 \frac{3}{4}$	6 7 8	24 26 28
120 130 140	$43 \\ 46 \frac{1}{2} \\ 50$	60 65 70	$\begin{array}{r} 46 \frac{1}{4} \\ 50 \frac{1}{8} \\ 54 \end{array}$		$59\frac{1}{4}\\63\frac{7}{8}\\69$	$\begin{array}{c} 66\frac{1}{8} \\ 71\frac{1}{4} \\ 77 \end{array}$	$53\frac{3}{8}$ 57 $\frac{1}{2}$ 62	81 88 94	$\begin{array}{r} 48\frac{1}{4} \\ 52\frac{3}{4} \\ 56\frac{1}{4} \end{array}$	66 ⁵ /8 73 ⁵ /8 77 ⁷ /8	33 ½ 37 39	8 9 10	30 34 36
150 160 170	$53 \frac{1}{2}$ 57 60 $\frac{3}{4}$	75 80 85	$57\frac{7}{8}$ $61\frac{3}{4}$ $65\frac{5}{8}$	47 50 54	$73\frac{3}{4}\\78\frac{7}{8}\\83\frac{7}{8}$	82 ¹ / ₄ 88 93 ⁵ / ₈	$\begin{array}{r} 66 \frac{1}{4} \\ 70 \frac{3}{4} \\ 75 \frac{1}{8} \end{array}$	100 107 116	$59\frac{3}{4}$ $64\frac{1}{4}$ 69	$\begin{array}{c} 85 \frac{7}{8} \\ 90 \frac{1}{8} \\ 95 \end{array}$	43 45 47 ½	$ \begin{array}{c} 11 \\ 12 \\ 13 \end{array} $	$38 \\ 40 \\ 44$
180 190 200	$\begin{array}{c} 64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2} \end{array}$	95	69 ½ 73 ¼ 77 ¼	60	88 ⁵ / ₈ 93 ³ / ₄ 98 ³ / ₄	$98\frac{7}{8}\\104\frac{5}{8}\\110\frac{1}{4}$	83 1/8	128	72 ½ 76 79 ¾	$103 \\ 107 \frac{1}{2} \\ 115 \frac{7}{8}$	$51\frac{1}{2}$ $53\frac{3}{4}$ 58	$ \begin{array}{r} 14 \\ 15 \\ 16 \end{array} $	46 48 50

NOTE-Blowers have two Inlets but no Inlet Cone.







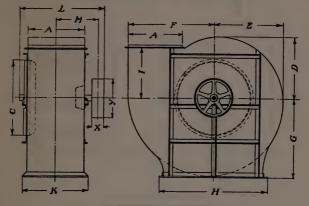
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Dimensions in Inches

Size	A	Exb.	C Blow.	D	E	F	G	н	I	к	L	M	x	Y
	121/2	15 3/8	$11 \frac{5}{13} \frac{1}{12} \frac{1}{15} \frac{1}{12}$	13 1/4	17 14	1514	$175 \\ 2014 \\ 227 \\ 8$	23 26 29	$ \begin{array}{r} 10 \frac{1}{2} \\ 12 \\ 13 \frac{1}{2} \end{array} $	15 $16\frac{3}{4}$ $18\frac{1}{2}$	27 1/8	$13\frac{1}{14}\frac{1}{14}\frac{1}{14}\frac{1}{14}$	333	8 9 10
50	17 %	23	$17\frac{3}{19}\frac{1}{14}$ $21\frac{1}{14}$	19	24 34	$19\frac{3}{21}\frac{7}{78}$ $23\frac{7}{8}$	$26 \\ 28 \frac{5}{8} \\ 31 \frac{1}{8}$	32 35 38	$15 \\ 16 \frac{1}{2} \\ 18$	20 % 22 ½ 23 ½		16 17 ¼ 18 ¼	3 4 4	11 12 14
60 70 80	25	35	23 ½ 27 30 ½	26 1/2	34 1/2	30 1/2	$33\frac{3}{40}$ $40\frac{45\frac{3}{4}}{45\frac{3}{4}}$	41 48 54	$ \begin{array}{r} 19 \frac{1}{22} \\ 23 \\ 26 \end{array} $	$\begin{array}{r} 25 {}^3_{4} \\ 29 {}^1_{4} \\ 32 {}^3_{4} \end{array}$	39 ¹ / ₈ 45 ³ / ₈ 49 ³ / ₈	21 3/4	5 5 6	16 18 20
90 100 110	$32\frac{1}{4}$ $35\frac{3}{4}$ $39\frac{1}{4}$	50	$34\frac{3}{4}$ $38\frac{5}{8}$ $42\frac{1}{2}$		49 3/8	43 5 8	$\begin{array}{c} 51 \\ 56 \frac{5}{8} \\ 61 \frac{7}{8} \end{array}$		29 32 35	$36\frac{1}{2}$ 40 44 $\frac{1}{2}$	58 1/2	27 $29\frac{1}{2}$ $31\frac{3}{4}$	6 7 8	24 26 28
120 130 140	46 1/2	60 65 70	50 ½	49 1/8	63 %	$52\frac{8}{8}$ $56\frac{1}{2}$ 61	$ \begin{array}{r} 67 \frac{5}{8} \\ 72 \frac{3}{4} \\ 78 \frac{1}{2} \end{array} $		$38 \\ 41 \\ 44$	$\begin{array}{r} 48 \frac{1}{4} \\ 52 \frac{3}{4} \\ 56 \frac{1}{4} \end{array}$	66 ⁵ / ₅ 73 ⁵ 77 ⁷ ₅		8 9 10	30 34 36
150 160 170	$53\frac{1}{2}$ 57 60 $\frac{3}{4}$	80	61 34	60 5/8	7878	$ \begin{array}{r} 65 \frac{1}{4} \\ 69 \frac{3}{4} \\ 74 \frac{1}{8} \end{array} $	89 1/2	103 1/2	47 50 54	$59\frac{3}{4}$ 64 $\frac{1}{4}$ 69	90 1/8		$\begin{array}{c}11\\12\\13\end{array}$	38 40 44
180 190 200	$\begin{array}{r} 64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2} \end{array}$	95	73 1/4	72	93 34	8278	100 ^{\$} / ₈ 106 ¹ / ₈ 111 ³ / ₄	124	57 60 63	76	103 107 ½ 115 7,8	53 34	14 15 16	46 48 50

NOTE-Blowers have two Inlets but no Inlet Cone.

PLANOIDAL (TYPE L) FANS

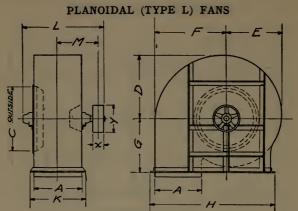


OVERHUNG PULLEY FULL HOUSING—UP DISCHARGE

Dimensions in Inches

			С											
Size	A	Exh.	Blow.	D	E	F	G	Н	I	К	L	M	X	Y
30 35 40	$12\frac{1}{2}$	$15\frac{3}{8}$	${}^{11\frac{5}{8}}_{13\frac{1}{2}}_{15\frac{1}{2}}$	13 1/4	15 1/4	$19\frac{1}{4}$	$15\frac{7}{8}\\18\frac{1}{4}\\20\frac{5}{8}$	28	$10\frac{1}{2}$ 12 $13\frac{1}{2}$	15 $16\frac{3}{4}$ $18\frac{1}{2}$	27 1/8	$13\frac{1}{4}\\14\frac{1}{4}\\15$	333	8 9 10
45 50 55	$17\frac{7}{8}$	23	$17\frac{3}{8}\\19\frac{1}{4}\\21\frac{1}{4}$	19	21 1/8	27 5/8	$23\frac{3}{8}$ $25\frac{3}{4}$ 28	37	$ \begin{array}{c} 15 \\ 16 \frac{1}{2} \\ 18 \end{array} $	$20\frac{3}{8}\\22\frac{1}{8}\\23\frac{7}{8}$	3316	$16 \\ 17 \frac{1}{4} \\ 18 \frac{1}{4}$	3 4 4	$ \begin{array}{c} 11 \\ 12 \\ 14 \end{array} $
60 70 80		$28 \frac{1}{2}$ 35 40		26 1/2	$30\frac{1}{2}$	38 1/2	30 ³ /8 35 ¹ /2 40 ⁵ /8	50	$19\frac{1}{22}$ 23 26	$25\frac{3}{4}$ $29\frac{1}{4}$ $32\frac{3}{4}$		$21\frac{3}{4}$	5 5 6	16 18 20
90 100 110	$32\frac{1}{4}$ $35\frac{3}{4}$ $39\frac{1}{4}$	45 50 55	${ 34 \frac{3}{4} \\ 38 \frac{5}{8} \\ 42 \frac{1}{2} } $	37 1/8	43 5/8	55 1/8	45 ³ /8 50 ³ /8 55 ¹ /8	68	29 32 35	36 ½ 40 44 ½	58 1/2	$27 \\ 29 \frac{1}{2} \\ 31 \frac{3}{4}$	6 7 8	24 26 28
120 130 140	46 1/2	60 65 70	$\begin{array}{r} 46 \frac{1}{4} \\ 50 \frac{1}{8} \\ 54 \end{array}$	49 1/8	$52\frac{3}{8}50\frac{1}{2}61$		60 ¼ 64 ¾ 70		41	$\begin{array}{r} 48 \frac{1}{4} \\ 52 \frac{3}{4} \\ 56 \frac{1}{4} \end{array}$	66 ⁵ / ₈ 73 ⁵ / ₈ 77 ⁷ / ₈	33 ½ 37 39	8 9 10	$30 \\ 34 \\ 36$
150 160 170	53 ½ 57 60 ¾	80	$57 \frac{7}{8} \\ 61 \frac{3}{4} \\ 65 \frac{5}{8}$	60 3/8	69 34	88	74 ¾ 79 ⅔ 84 ⅔	107	50	$59\frac{3}{4}\64\frac{1}{4}\69$	85 ⁷ / ₈ 90 ¹ / ₈ 95	43 45 47 ½	$ \begin{array}{c} 11 \\ 12 \\ 13 \end{array} $	38 40 44
180 190 200	$\begin{array}{r} 64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2} \end{array}$	95	73 1/4	72	82 1/8	98 7/8 104 5/8 110 1/4	94 3/4	128	60	72 ½ 76 79 ¾	103 107 ½ 115 78	$51\frac{1}{2}$ $53\frac{3}{4}$ 58	$ \begin{array}{r} 14 \\ 15 \\ 16 \end{array} $	46 48 50

NOTE-Blowers have two Inlets but no Inlet Cone.

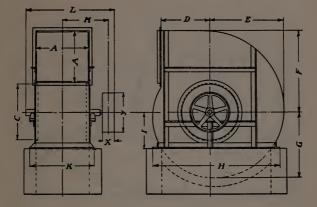


OVERHUNG PULLEY FULL HOUSING—DOWN DISCHARGE

Dimensions in Inches

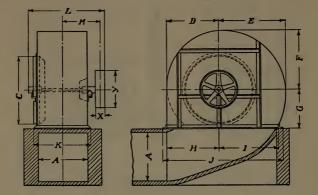
Size	A		2	D	E	F	G	н	к	L	м	x	Y
		Exh.	Blow.			•	G			-			
30 35 40	$12\frac{1}{2}$	$13\frac{14}{15\frac{3}{8}}$ $17\frac{1}{2}$	${}^{115_8}_{131_2}_{151_2}$	17 1/4	$13\frac{1}{8}\\15\frac{1}{4}\\17\frac{3}{8}$	$16\frac{5}{8}$ $19\frac{14}{2178}$	$12\frac{3}{8}$ $14\frac{1}{4}$ $16\frac{1}{8}$	$31\frac{1}{8}$ $35\frac{1}{4}$ $39\frac{3}{8}$	15 $16\frac{3}{4}$ $18\frac{1}{2}$	$\begin{array}{r} 25 \frac{1}{4} \\ 27 \frac{1}{8} \\ 28 \frac{3}{4} \end{array}$	$13 \frac{1}{4} \\ 14 \frac{1}{4} \\ 15$	3 3 3	8 9 10
45 50 55	$16\frac{1}{8}\\17\frac{7}{8}\\19\frac{5}{8}$	23	$17\frac{3}{8}\\19\frac{1}{4}\\21\frac{1}{4}$		$19\frac{3}{4}\\21\frac{7}{8}\\23\frac{7}{8}$	$25 \\ 27 \frac{5}{8} \\ 30 \frac{1}{8}$	$18\frac{1}{8}{20}{21\frac{3}{4}}$	$\begin{array}{c} 44 \\ 48 \frac{1}{8} \\ 52 \frac{1}{8} \end{array}$	$20\frac{3}{8}$ $22\frac{1}{8}$ $23\frac{7}{8}$	$\begin{array}{r} 30\frac{11}{16} \\ 33\frac{6}{16} \\ 35\frac{7}{16} \end{array}$	$16 \\ 17\frac{1}{4} \\ 18\frac{1}{4}$	3 4 4	$\begin{array}{c}11\\12\\14\end{array}$
60 70 80	$21 \frac{1}{2}$ $25 \\ 28 \frac{1}{2}$	$28 \frac{1}{2}$ 35 40	$23 \frac{1}{8} \\ 27 \\ 30 \frac{7}{8}$	34 1/2	$26 \\ 30 \frac{1}{2} \\ 35$	$\begin{array}{r} 32\frac{3}{4} \\ 38\frac{1}{2} \\ 44\frac{1}{4} \end{array}$	$23\frac{5}{8}$ $27\frac{1}{2}$ $31\frac{8}{8}$	$56\frac{1}{4}\\65\frac{1}{2}\\74\frac{1}{4}$	$25\frac{3}{4}$ $29\frac{1}{4}$ $32\frac{3}{4}$	$39\frac{1}{8}$ $45\frac{3}{8}$ $49\frac{3}{8}$	$20 \\ 21 \frac{3}{4} \\ 25$	5 5 6	$ \begin{array}{c} 16 \\ 18 \\ 20 \end{array} $
90 100 110	$32\frac{1}{4}$ $35\frac{3}{4}$ $39\frac{1}{4}$	$45 \\ 50 \\ 55$	$34\frac{3}{4}$ $38\frac{5}{8}$ $42\frac{1}{2}$	49 3/8	$\begin{array}{r} 39 \frac{1}{4} \\ 43 \frac{5}{8} \\ 47 \frac{7}{8} \end{array}$	$55\frac{1}{8}$	$35\frac{1}{8}$ $38\frac{7}{8}$ $42\frac{5}{8}$	$\begin{array}{r} 82\frac{1}{2}\\ 91\frac{1}{8}\\ 100\frac{3}{8}\end{array}$	$36\frac{1}{2}$ 40 $44\frac{1}{2}$	$53\frac{1}{4}$ $58\frac{1}{2}$ 63	$27 \\ 29 \frac{1}{2} \\ 31 \frac{3}{4}$	6 7 8	24 26 28
120 130 140	$43 \\ 46 \frac{1}{2} \\ 50$	60 65 70	$46\frac{1}{4}$ 50 $\frac{1}{8}$ 54	59 ¼ 63 ½ 69	$52\frac{3}{8}$ 56 $\frac{1}{2}$ 61	$66\frac{1}{8}$ 71 $\frac{1}{4}$ 77	$46\frac{1}{2}$ 50 $\frac{1}{8}$ 54	${}^{109{}^{1}\!/_{8}}_{118{}^{1}\!/_{4}}_{127}$	$\begin{array}{r} 48{}^{1}\!$	66 ⁵ / ₈ 73 ⁵ / ₈ 77 ⁷ / ₈	37	8 9 10	$30 \\ 34 \\ 36$
150 160 170	$53\frac{1}{2}$ 57 $60\frac{3}{4}$	75 80 85	61 34	73 34 78 7/8 83 7/8	$\begin{array}{r} 65 \frac{1}{4} \\ 69 \frac{3}{4} \\ 74 \frac{1}{8} \end{array}$	88	$57\frac{3}{4}\ 61\frac{5}{8}\ 65\frac{3}{8}$	$135\frac{1}{4}$ 145 $155\frac{5}{8}$	$59\frac{3}{4}\ 64\frac{1}{4}\ 69$	85 ⁷ / ₈ 90 ¹ / ₈ 95	43 45 47 ½	$ \begin{array}{c} 11 \\ 12 \\ 13 \end{array} $	$\begin{array}{c} 38\\ 40\\ 44 \end{array}$
180 190 200	$64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2}$		$\begin{array}{r} 69 \frac{1}{2} \\ 73 \frac{1}{4} \\ 77 \frac{1}{4} \end{array}$	88 ⁵ /8 93 ³ /4 98 ³ /4	78 3/8 82 7/8 87 1/4	104 %	69 ½ 73 76 ¾	$163\frac{7}{8}$ $172\frac{5}{8}$ $181\frac{1}{4}$	72 ½ 76 79 ¾	$103 \\ 107 \frac{1}{2} \\ 115 \frac{7}{8}$	$51\frac{1}{2}$ 53 $\frac{3}{4}$ 58	$\begin{array}{c} 14\\15\\16\end{array}$	46 48 50
NOTE	-Blo	wers	have	two I	nlets l	but no	Inlet	Cone					

NOTE—Blowers have two Inlets but no Inlet Cone.



OVERHUNG PULLEY THREE-QUARTER HOUSING—TOP HORIZONTAL DISCHARGE

Size	A	с	D	E	F	G	н	I	к	L	M	x	Y
60 70 80	$21\frac{1}{25}$ $28\frac{1}{2}$	$28\frac{1}{2}$ 35 40	23	29 ³ / ₈ 34 ¹ / ₂ 39 ⁵ / ₈	38 1/2	$30\frac{1}{2}$	$\begin{array}{c} 45 \frac{7}{8} \\ 53 \frac{1}{4} \\ 60 \frac{5}{8} \end{array}$	20 1/2	$25\frac{3}{4}$ $29\frac{1}{4}$ $32\frac{3}{4}$	39 ¹ / ₈ 45 ³ / ₈ 49 ³ / ₈	$21\frac{3}{4}$	5 5 6	16 18 20
90 100 110	$32\frac{1}{4}\\35\frac{3}{4}\\39\frac{1}{4}$	$45 \\ 50 \\ 55$	29 32 35	44 ³ / ₈ 49 ³ / ₈ 54 ¹ / ₈	$55\frac{1}{8}$	43 5/8	74 1/2	$28\frac{1}{2}$	$36\frac{1}{2}$ 40 44 $\frac{1}{2}$	58 1/2	$27 \\ 29 \frac{1}{2} \\ 31 \frac{3}{4}$	6 7 8	$24 \\ 26 \\ 28$
120 130 140	43 46 ½ 50	60 65 70	$\begin{array}{c} 38\\ 41\\ 44 \end{array}$	59 ¼ 63 7 69	71 1/4	$52\frac{3}{8}$ $56\frac{1}{2}$ 61	$ 89\frac{3}{4} \\ 97\frac{3}{4} \\ 105\frac{1}{4} $	37	$\begin{array}{r} 48{}^{1}\!$	66 ⁵ /s 73 ⁵ /s 77 ⁷ /s		8 9 10	30 34 36
150 160 170	$53\frac{1}{2}$ 57 60 $\frac{3}{4}$	75 80 85	47 50 54	73 34 78 7/8 83 7/8	88	69 34	111 3/8 120 127 7/8	46	$64\frac{1}{4}$	85 7/8 90 1/8 95		$ \begin{array}{c} 11 \\ 12 \\ 13 \end{array} $	38 40 44
180 190 200	$\begin{array}{c} 64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2} \end{array}$	90 95 100	$57 \\ 60 \\ 63$		104 5/8	82 1/8	$134\frac{7}{8}\\141\frac{5}{8}\\148\frac{3}{4}$	54		107 1/2		$14 \\ 15 \\ 16$	46 48 50



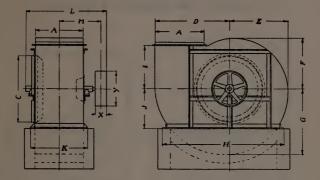
OVERHUNG PULLEY

THREE-QUARTER HOUSING-BOTTOM HORIZONTAL DISCHARGE

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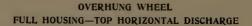
Size

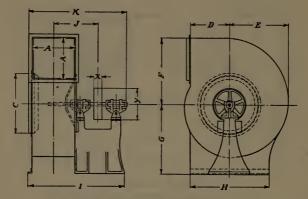
SILC	1 1	· ·		1 -	1 .			•		IX.	-	118	1 1	
60 70 80			$26\frac{1}{2}$		30 1/2	$18 \\ 20 \frac{1}{22} \\ 23 \frac{1}{22} \\ 23 \frac{1}{2} \\ 23 \frac{1}{2$	$26\frac{1}{2}$		61 1/4	25 ³ ⁄4 29 32 ³ ⁄4	$39\frac{1}{8}$ $45\frac{3}{8}$ $49\frac{3}{8}$	$21\frac{3}{4}$	5 5 6	16 18 20
90 100 110	$32\frac{1}{4}\\35\frac{3}{4}\\39\frac{1}{4}$	50	37 1/8	$49\frac{3}{8}$	43 5/8	$26 \\ 28 \frac{1}{2} \\ 31 \frac{1}{2}$	37 1/8	44 1/4	86 1/8	$36\frac{1}{2}$ 40 44 $\frac{1}{2}$		$29\frac{1}{2}$		$24 \\ 26 \\ 28$
120 130 140	$46\frac{1}{2}$		$49\frac{1}{8}$	63 1/8	56 1/2	37	49 1/8	$57\frac{1}{8}$	$103 \frac{1}{2} \\ 112 \frac{1}{4} \\ 120 \frac{3}{4} \\ 100 \frac{3}{4} \\ $	$52\frac{3}{4}$	66 ⁵ / ₈ 73 ⁵ / ₈ 77 ⁷ / ₈	37	8 9 10	30 34 36
150 160 170	$53\frac{1}{2}$ 57 60 $\frac{3}{4}$	80	60 5/8	78 1/8	$69\frac{3}{4}$	46	60 5%	70 1/2	$128\frac{5}{8}$ $138\frac{1}{8}$ $147\frac{1}{2}$	64 1/4	$85\frac{7}{8}$ 90 $\frac{1}{8}$ 95	45	$ \begin{array}{c} 11 \\ 12 \\ 13 \end{array} $	38 40 44
	$\begin{array}{r} 64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2} \end{array}$	95	72	88 5/8 93 3/4 98 3/4	82 1/8	54	72	83 5/8	$155\frac{1}{2}$ $163\frac{5}{8}$ 172	76	$ \begin{array}{r} 103 \\ 107 \frac{1}{2} \\ 115 \frac{7}{8} \end{array} $	$51\frac{1}{2}$ $53\frac{3}{4}$ 58	$\begin{array}{c} 14\\15\\16\end{array}$	46 48 50



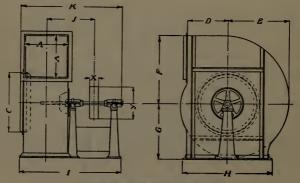
OVERHUNG PULLEY THREE-QUARTER HOUSING—UP DISCHARGE

Size	A	c	D	E	F	G	н	ľ	J	к	L	M	x	Y
60 70 80	$21 \frac{1}{25} \\ 28 \frac{1}{2}$	$28 \frac{1}{2}$ 35 40	$32\frac{3}{4}$ $38\frac{1}{2}$ $44\frac{1}{4}$	30 1/2	22 5/8 26 1/2 30 3/8	34 1/2	62 3/4	$19\frac{1}{22}$ 23 26	20 1/2	$25\frac{3}{4}$ $29\frac{1}{4}$ $32\frac{3}{4}$	$39\frac{1}{8}$ $45\frac{3}{8}$ $49\frac{3}{8}$	$21\frac{3}{4}$	5 5 6	16 18 20
90 100 110	$32\frac{1}{4}$ $35\frac{3}{4}$ $39\frac{1}{4}$	50	$49\frac{1}{2} \\ 55\frac{1}{8} \\ 60\frac{3}{8}$	43 5%	$34\frac{1}{8}$ 37 $\frac{7}{8}$ 41 $\frac{5}{8}$	$49\frac{3}{8}$	88 1/4	32	28 1/2	$36\frac{1}{2}\ 40\ 44\frac{1}{2}$		27 29 ½ 31 ¾	6 7 8	$24 \\ 26 \\ 28$
120 130 140	$43 \\ 46 \frac{1}{2} \\ 50$	60 65 70	71 1/4	56 1/2	$49\frac{1}{8}$	63 7/8	$106\frac{5}{8}\\115\frac{3}{8}\\124\frac{3}{8}$	41	34 37 39 ½	$\begin{array}{r} 48 \ \frac{1}{4} \\ 52 \ \frac{3}{4} \\ 56 \ \frac{1}{4} \end{array}$	66 5/8 73 5/8 77 7/8		8 9 10	30 34 36
150 160 170	$53\frac{1}{2}$ 57 60 $\frac{3}{4}$	80	88	$69\frac{3}{4}$	56 ³ / ₄ 60 ⁵ / ₈ 64 ³ / ₈	$78\frac{7}{8}$	$132 \\ 141 \frac{8}{4} \\ 151 \frac{1}{2}$	50		$59\frac{3}{4}\64\frac{1}{4}\69$	85 ⁷ / ₈ 90 ¹ / ₈ 95		$11 \\ 12 \\ 13$	38 40 44
180 190 200	$\begin{array}{r} 64 \frac{1}{4} \\ 67 \frac{3}{4} \\ 71 \frac{1}{2} \end{array}$	95	104 %	82 %	72	93 3/1	$159\frac{1}{2}\\167\frac{7}{8}\\176\frac{1}{2}$	60	54	72 ½ 76 79 ¾	$ 103 107 \frac{1}{2} 115 \frac{7}{8} $	$51\frac{1}{2}$ $53\frac{3}{4}$ 58	$\begin{array}{c}14\\15\\16\end{array}$	46 48 50





This Style for 30 to 60-Inch Fans



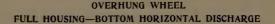
This Style for 70 to 140-Inch Fans

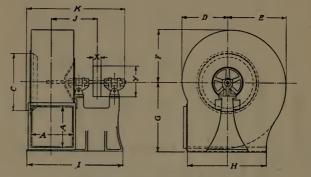
OVERHUNG WHEEL FULL HOUSING-TOP HORIZONTAL DISCHARGE

Dimensions in Inches

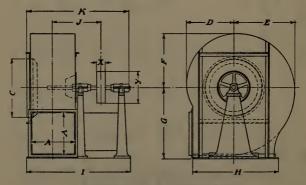
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I	×	31 J 34 J 37 J	42 44 34 49	51 56 61 9	65 78 81	84 89 92 92
-	1	14/20/40	000000	100/00/00	Jaks /4	100/00/00 100/00/00
	7	141	19 % 2018 2218	24 27 28	30 38 40	42 43 45
-		- 10 × 1	100 00 00	14/4/4	Ka/u/u	74/4/4
	-	31 351 38	41 7/8 45 7/8 48 7/8	51 57 60	64 81 85	89 93 96
-			30 33 36	609	010010	1004
	I	ลลัง		ດີເດີເດ	000	0000
-		14	18.14	Z	4/8/8	100/00
	Ð	24 24 20 20	$26\% \\ 29\% \\ 32\%$	35 31 36	40 44 48	53 57 62
		100/40/00	100/00	1/2/10/4	7/1/20/20	7874
	Ľ.	16 19 21	25 27 30 1%	32 38 44	49 55 60	66 71 77
		12/4/0	100 /4×	20/20/20 20/20/20	8 8 1 8 8 1 8 1 8 1 8 1 8 1 8 1 8 1 8 1	14/20
	ш	114	22 % 24 %	29 34 39	44 49 54	63 59
		X X	2	72		
	Q	1220	15 16 ½	19 23 26	32 35 35	38 41 44
		74/80/2	· /8 /5	1 20		
	C	15	19 % 23 25 ½	28 35 40	45 55 55	60 65 70
		14/2/2	16 1% 17 7% 19 5%	X X X	74/4/2	X :
	×	10	16 117 119	552 I	352	5440
	Size	30 35	45 45 550	928	001	140
	s					

PLANOIDAL FAN DIMENSIONS





This Style for 30 to 60-Inch Fans

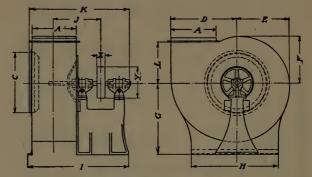


This Style for 70 to 140-Inch Fans

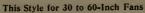
OVERHUNG WHEEL FULL HOUSING—BOTTOM HORIZONTAL DISCHARGE

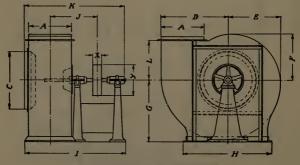
>	10 .	11 12 14	16 18 20	26 26 28	36 34 36
×	ကကက	€0 4 4	ອຍຄ	918	8 9 10
K	$\begin{array}{c} 31 \ M_{2} \\ 34 \ M_{8} \\ 37 \ M_{2} \end{array}$	42 44 34 49	$\frac{51}{56} \frac{7}{8} \\ 61 \frac{38}{38} \\ 61$	65 ½8 78 ½8 81 ½8	$\begin{array}{c} 84 \ 7_8 \\ 89 \ 3_8 \\ 92 \ 7_8 \\ 7_8 \end{array}$
ſ	$14 \frac{14}{15} \frac{14}{58}$ 17 $\frac{12}{12}$	$19\frac{5}{8}$ $20\frac{5}{16}$ $22\frac{16}{16}$	24 3% 27 1/8 28 7/8	$30\frac{3}{24}$ $38\frac{1}{25}$ $40\frac{1}{24}$	42 1/8 43 7/8 45 5/8
	$\frac{31}{38 \mathrm{M}^4}$	$\frac{417_8}{4518}$	51 34 57 34 60 34	64 12 81 12 85 12 85 12 22	89 93 <u>%</u> 96 %
н	21 24 27	30 33 36	39 48 54	60 66 72 ½	78 ½ 85 91
Ð	$ \frac{18}{24} $	$26\frac{56}{32}$	35 40 45 ¾	$51 \\ 56 \\ 56 \\ 58 \\ 61 \\ 78 \\ 61 \\ 78 \\ 78 \\ 61 \\ 78 \\ 78 \\ 78 \\ 78 \\ 78 \\ 78 \\ 78 \\ 7$	67 5% 72 3% 78 ½
Ľ.	$\frac{13}{15}\frac{18}{14}$	$\frac{19\%}{21\%}$	26 30 ½ 35	$39 \frac{1}{28} \frac{39 \frac{1}{28}}{128}$	$52\% 56 \frac{52\%}{22} 61$
Щ	${ \begin{smallmatrix} 14 & 3_4 \\ 17 & 3_4 \\ 19 & 5_8 \\ 19 & 5_8 \\ \end{smallmatrix} }$	22 3% 24 3 <u>%</u> 27	29 % 34 ½ 39 ½2 8	$\frac{44}{49}\frac{3}{88}$ $54\frac{1}{88}$	$59 \frac{1}{26}$
Q	$11\frac{36}{15\frac{14}{88}}$	17 ½8 19 20 ¾	225% 261% 30%	34 1% 37 7% 41 5%	45 ½ 49 ½ 53
υ	13 % 15 % 17 %	19 % 23 25 ½	28 ½ 2 35 40	45 55 55	60 65 70
V	$10\frac{3}{4}$ 12 $\frac{1}{2}\frac{1}{4}$ 14 $\frac{1}{4}$	16 1/8 17 7/8 19 5/8	$21 \frac{1}{25}$ $28 \frac{1}{23}$	32 ½ 35 % 39 ½	43 46 ½ 50
Size	30 35 40	45 50 55	60 80 80	90 1100	120 130 140

PLANOIDAL FAN DIMENSIONS



OVERHUNG WHEEL FULL HOUSING—UP DISCHARGE





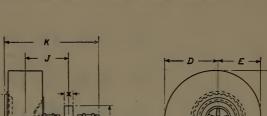
This Style for 70 to 140-Inch Fans

OVERHUNG WHEEL FULL HOUSING-UP DISCHARGE

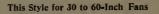
Dimensions in Inches

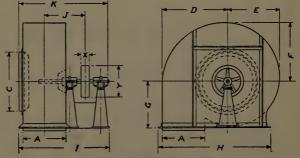
*	8 9 10	11 12 14	16 18 20	26 28 28	30 34 36
×	ကကက	€0 4 4	ບດາດ	∞~a©	8 9 10
¥	$\begin{array}{c} 31\%\\ 34\%\\ 37\%\\ 37\%\\ \end{array}$	42 44 34 49	$\frac{51}{56}\frac{7}{88}$	65 ½ 78 ½% 81 %	84 7, 89 3, 92 7,8 8
~	$\frac{14}{15} \frac{14}{58} \frac{14}{17} \frac{17}{12}$	$19\frac{5_8}{2018}$ $22\frac{15}{16}$	24 3% 27 1/8 28 7/8	$\begin{array}{c} 30 & 3.0 \\ 38 & 1.5 \\ 38 & 1.5 \\ 40 & 1.4 \\ 1.4 \end{array}$	42 43 78 8 78 8 8
-	$\frac{31}{38 J_4^6}$	$\frac{41}{45}\frac{7_{\%}}{18}$	$\frac{51}{57} \frac{3}{14} \\ 60 \frac{3}{4}$	$\begin{array}{c} 64 \\ 81 \\ 85 \\ 1/2 \\ 85 \\ 1/2$	89 14 93 14 96 34
E	21 24 27	30 33 36	39 48 54	$60 \\ 66 \\ 72 \\ 12 \\ 12 \\ 12 \\ 12 \\ 12 \\ 12 \\ 12$	78 ½ 85 91
IJ	$ \begin{array}{c} 18 \\ 20 34 \\ 24 \end{array} $	$\begin{array}{c} 26 \frac{58}{88} \\ 29 \frac{14}{44} \\ 32 \end{array}$	$35 \\ 35 \\ 10 \\ 58 \\ 40 \\ 58 \\ 8 \\ 8 \\ 8 \\ 8 \\ 9 \\ 58 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ $	$45 \frac{45}{50} \frac{3}{8}$	60 <u>14</u> 64 7% 70
Ľ.	$11 \frac{36}{15}$	$^{17}_{19}^{18}_{20\%}$	$22 \frac{58}{26}$ $30 \frac{32}{8}$	$34 \frac{1}{28}$ $37 \frac{1}{88}$ $41 \frac{5}{88}$	45 <u>12</u> 49 <u>18</u> 53
ш	$\frac{13}{15}\frac{18}{14}$	$\frac{19}{21}^{34}_{78}$	$ \begin{array}{c} 26 \\ 30 \\ 35 \\ 35 \end{array} $	$39 \frac{14}{28}$ $43 \frac{54}{88}$ $47 \frac{78}{78}$	52 % 56 ½ 61
Q	$16 \frac{5}{8}$ $18 \frac{14}{24}$ $21 \frac{7}{8}$	$25 \\ 27 \\ 58 \\ 30 \\ 78 \\ 30 \\ 98 \\ 8 \\ 90 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10$	32 34 38 ½ 44 ½	$\begin{array}{c} \textbf{49} \\ \textbf{55} \\ \textbf{55} \\ \textbf{128} \\ \textbf{60} \\ \textbf{38} \\ \textbf{88} $	66 % 71 ½
U	$\frac{13}{15}\frac{14}{3\%}$	19 5% 23 25 ½	28 ½ 35 40	45 50 55	60 65 70
A	10 % 12 % 14 %	16 1/8 17 7/8 19 5/8	21 ½ 25 28 ½	32 <u>14</u> 35 <u>34</u> 39 <u>14</u>	43 46 ½ 50
Size	30 35 40	45 50 55	80 80 80	90 110 110	120 130 140

PLANOIDAL FAN DIMENSIONS



OVERHUNG WHEEL FULL HOUSING—DOWN DISCHARGE





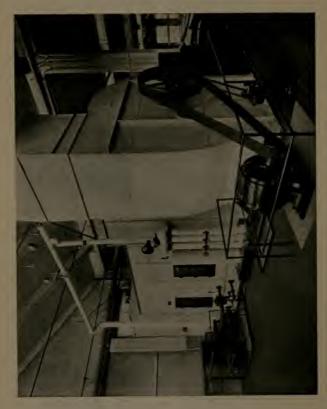
This Style for 70 to 140-Inch Fans

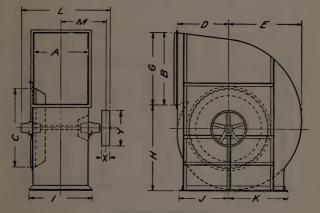
PLANOIDAL FAN DIMENSIONS

PLANOIDAL (TYPE L) EXHAUSTERS

OVERHUNG WHEEL FULL HOUSING-DOWN DISCHARGE

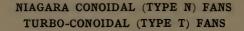
>	8 10 10 8	11 12 14	$16 \\ 18 \\ 20 \\ 20 \\ 16 \\ 18 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10 \\ 10$	24 28 28	30 34 36
×	ကကက	c0 4 4	လက္က	∞~∞	8 10 10
L	$10\frac{1}{12}$ $13\frac{1}{23}$	$15 \\ 16 \\ 18 \\ 18$	19 ½		
×	31 ½ 34 ½ 37 ½	$42 \\ 44 \\ 49 \\ 49$	51 7. 56 58 61 38	65 1/8 78 1/8 81 1/8	84 7/ 89 3/8 92 7/8
-	$\frac{14}{15} \frac{14}{58} \frac{1}{28}$	19_{16}^{10} 20_{16}^{10} 22_{16}^{10}	$\begin{array}{c} 24 \ \frac{3}{8} \\ 27 \ \frac{1}{8} \\ 28 \ \frac{7}{8} \\ \frac{3}{8} \end{array}$	30 % 38 % 40 %	42 1/8 43 7/8 45 5/8
-	$\frac{31}{35}$	$\frac{41}{45}\frac{7_8}{16}$ $\frac{45}{18}\frac{3}{76}$	51 % 57 % 60 %	64 ½ 81 ½ 85 ½	89 X 93 X 96 %
H	$14 \frac{14}{26}$ $16 \frac{32}{4}$ $19 \frac{14}{4}$	22 24 ½ 26 ½	28 % 65 ½ 74 ¾	$\begin{array}{c} 82 \frac{1}{22}\\ 91 \frac{1}{88}\\ 100 \frac{3}{88} \end{array}$	$\frac{109\%}{118\%}$
ŋ	$\frac{18}{24}$	$26 \frac{56}{8}$ 29 $\frac{14}{14}$ 32	35 27 1 <u>2</u> 31 38	35 1% 38 7% 42 5%	46 ½ 50 ½ 54
۳.	$14 \frac{7}{14} \\ 17 \frac{1}{14} \\ 19 \frac{5}{8} \\ 8$	22 3% 24 3% 27	29% 34% 39% 39% 39%	44 3% 49 3% 54 1%	59 14 63 7% 69
<u>ت</u>	13 1/8 15 1/4 17 3/4	$\frac{19\%}{217/8}$	$ \begin{array}{c} 26 \\ 30 \\ 35 \\ 35 \end{array} $	39 <u>14</u> 43 5% 47 7%	52% 56% 61
Q	$\frac{16}{19} \frac{5_8}{14} \\ 21 \frac{7_8}{28}$	25 27 58 30 18	32 34 38 1/2 44 1/4	49 ½ 55 ½ 60 % 8	66 ½8 71 ½4 77
c	13 14 15 38 17 1/2	$ \begin{array}{c} 19 \\ 23 \\ 25 \\ 94 \\ \end{array} $	28 ½ 35 40	45 50 55	60 65 70
A	10^{84}_{12} 12 15_{14}_{14}	16 1% 17 7% 19 58	21 ½ 25 28 ½	$32 \frac{1}{24}$ $35 \frac{1}{24}$ $39 \frac{1}{24}$	43 46 ½ 50
Size	30 35 40	45 50 55	80 20 80	90 1100	120 130 140

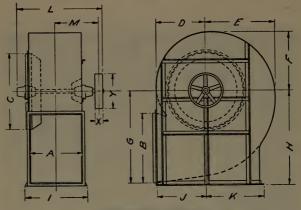




OVERHUNG PULLEY FULL HOUSING—TOP HORIZONTAL DISCHARGE

Size	A	В	С	D	Е	G	Н	1	J	к	L	M	x	Y
3 3½ 4	$12 \\ 14 \\ 16$	$15\frac{3}{4}$ 18 $\frac{3}{8}$ 21	20	$11 \frac{3}{16}$ 13 14 $\frac{7}{8}$	$15\frac{7}{8}$ $18\frac{9}{16}$ $21\frac{3}{16}$	20 18 24 1/4 27 3/4	$14 \\ 16 \frac{1}{2} \\ 18 \frac{1}{2}$	18 1/4	$13 \frac{1}{14} \\ 15 \\ 16 \frac{7}{8}$	16	27 29 31	$14\frac{1}{2}$ $15\frac{1}{2}$ $16\frac{1}{2}$	3	8 9 10
4 ¹ ⁄ ₂ 5 5 ¹ ⁄ ₂	$18 \\ 20 \\ 22$	$\begin{array}{r} 23 {}^{5}\!$	28 1/2	16 ³ / ₄ 18 ⁵ / ₈ 20 ⁷ / ₁₆	$\begin{array}{c} 23 \ \frac{7}{8} \\ 26 \ \frac{1}{2} \\ 29 \ \frac{1}{8} \end{array}$	$\begin{array}{c} 31 \frac{1}{4} \\ 34 \frac{11}{16} \\ 38 \frac{3}{16} \end{array}$	23	24 1/4	$18\frac{3}{4}\\19\frac{1}{2}\\21\frac{1}{4}$	22	$33 \\ 35 \\ 36 \frac{1}{2}$	$17\frac{1}{2}$ $18\frac{1}{2}$ $18\frac{1}{2}$	3	$ \begin{array}{c} 11 \\ 12 \\ 14 \end{array} $
6 7 8	24 28 32	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	$34\frac{1}{4}\\39\frac{3}{4}\\45\frac{1}{2}$	26	$31\frac{13}{18}$ $37\frac{1}{8}$ $42\frac{3}{8}$	48 18	$27 \frac{1}{2}$ 32 $36 \frac{1}{2}$	32 1/4	26 1/2	26 30 34	40 47 53	$20\frac{1}{2}$ 24 27	3 4 5	16 18 20
9 10 11	36 40 44	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	$56\frac{3}{4}$	33 ½ 37 📲 40 18	47 11 53 58 15	62 78 69 3/8 76 58	45	44 1/4	$31\frac{3}{4}$ $34\frac{3}{4}$ $38\frac{3}{8}$		61 65 73 ½	31 33 37	6 6 8	$24 \\ 26 \\ 28$
12 13 14	48 52 56	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	73 1/2	44 ⁵ / ₈ 48 ³ / ₈ 52 ¹ π	$\begin{array}{c} 63 \frac{5}{8} \\ 68 \frac{7}{8} \\ 74 \frac{3}{18} \end{array}$	83 ¼ 90 ਜੈ 97 ½	58 1/2	58 14			79 ½ 83 92	$39\frac{1}{2}$ $41\frac{1}{2}$ 46		$30 \\ 34 \\ 36$
15 16 17	$\begin{array}{c} 60\\ 64\\ 68\end{array}$	78 ³ 4 84 89 ¹ 4		$55\frac{3}{4}$ 59 $\frac{1}{2}$ 63 $\frac{1}{4}$	84 34	104 18 111 117 18	72	71 1/4	51 ³ / ₈ 54 ⁷ / ₈ 58 ³ / ₈	$67\frac{1}{2}$	99 107 112	$49\frac{1}{2}\ 53\frac{1}{2}\ 56$	14	38 40 44
18 19 20	72 76 80	99 34	$ \begin{array}{r} 101 \frac{1}{2} \\ 107 \\ 112 \frac{3}{4} \end{array} $	70 1	95 ³ / ₈ 100 11 106	$124\frac{7}{8}$ $131\frac{13}{138}$ $138\frac{3}{4}$	85	84 1/4	64 3/8	80	$120 \\ 125 \\ 128$	$ \begin{array}{c} 60 \\ 62 \frac{1}{2} \\ 64 \end{array} $		46 48 50

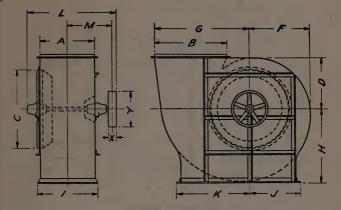




OVERHUNG PULLEY FULL HOUSING—BOTTOM HORIZONTAL DISCHARGE

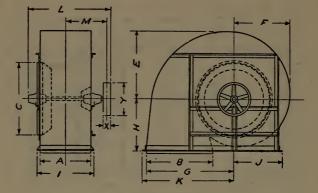
Dimensions in Inches

Size	A	B	С	D	E	F	G	Н	I	J	к	L	M	x	Y
31/2		$15\frac{3}{4}$ $18\frac{3}{8}$ 21		$ \begin{array}{c} 11 \\ 12 \\ $	$15\frac{7}{8}$ $18\frac{9}{16}$ $21\frac{3}{16}$	$13\frac{1}{15}\frac{1}{16}$ $17\frac{5}{8}$	$\begin{array}{c} 20\frac{13}{16}\\ 24\frac{1}{4}\\ 27\frac{3}{4} \end{array}$	$22 \\ 25 \frac{1}{29}$	18 1/4	$ \begin{array}{c} 11 \\ 13 \\ 14 \\ 7_{\%} \end{array} $	16	27 29 31	$14\frac{1}{12}$ $15\frac{1}{2}$ $16\frac{1}{2}$	3	8 9 10
5	20	$23 \frac{5}{8}$ $26 \frac{1}{4}$ $28 \frac{7}{8}$	28 1/2	16 ³ / ₄ 18 ⁵ / ₈ 20 ⁷ / ₁₆	$26\frac{1}{2}$	$19\frac{7}{8}$ $22\frac{1}{18}$ $24\frac{1}{4}$	$\begin{array}{c} 31 \frac{1}{4} \\ 34 \frac{11}{16} \\ 38 \frac{3}{16} \end{array}$	36	24 1/4	16 ³ / ₄ 18 ⁵ / ₂ 20 ⁷ / ₁₆	22	$33 \\ 35 \\ 36 \frac{1}{2}$	$ \begin{array}{c} 17 \frac{1}{2} \\ 18 \frac{1}{2} \\ 18 \frac{1}{2} \end{array} $	3	$ \begin{array}{c} 11 \\ 12 \\ 14 \end{array} $
6 7 8	28	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	39 3/4	2215 26 29 3⁄4	$37\frac{1}{8}$	$26\frac{1}{2}$ $30\frac{7}{8}$ $35\frac{5}{16}$	$\begin{array}{r} 41 {}^{5}\!$	43 50 57	32 1/4	22 5 26 29 3⁄4	26 30 34	40 47 53	$20\frac{1}{2}$ 24 27	4	$ \begin{array}{r} 16 \\ 18 \\ 20 \end{array} $
9 10 11	40	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	$51\frac{1}{4}$ $56\frac{3}{4}$ $62\frac{1}{2}$	33 ½ 37 ¾ 40 ⅔	$47\frac{11}{16}$ 53 58 $\frac{5}{16}$	39 ³ ⁄ ₄ 44 ¹ ⁄ ₈ 48 ¹ ⁄ ₂	$62\frac{7}{16}$ 69 $\frac{3}{8}$ 76 $\frac{5}{16}$	64 71 78	44 1/4	$\begin{array}{r} 33\frac{1}{2}\\ 37\frac{3}{16}\\ 40\frac{15}{16}\end{array}$	$38 \\ 42 \\ 46 \frac{1}{2}$	$61 \\ 65 \\ 73\frac{1}{2}$	31 33 37	6	24 26 28
12 13 14	52	${}^{63}_{68\frac{1}{4}}_{73\frac{1}{2}}$	$ \begin{array}{c} 68 \\ 73 \frac{1}{2} \\ 79 \end{array} $	44 ⁵ / ₈ 48 ³ / ₈ 52 ¹ / ₁₆	68 1/8	$52\frac{15}{57}\frac{5}{3}\frac{5}{8}}{61}\frac{3}{4}$	$\begin{array}{c} 83 \frac{1}{4} \\ 90 \frac{3}{16} \\ 97 \frac{1}{8} \end{array}$	85 92 99	58 14	44 5/8 48 3/8 52 16	50 ½ 55 59	79 ½ 83 92	$39\frac{1}{2}$ $41\frac{1}{2}$ 46	10	30 34 36
15 16 17	64	78 ³ ⁄4 84 89 ¹ ⁄4	90 1/4	$55\frac{3}{4}$ 59 $\frac{1}{2}$ 63 $\frac{1}{4}$	84 3/4	70 3/8	104 1 111 117 1 5	112 1/2	71 14		$67\frac{1}{2}$	$99 \\ 107 \\ 112$	$\begin{array}{r} 49 \frac{1}{2} \\ 53 \frac{1}{2} \\ 56 \end{array}$		38 40 44
18 19 20	76	$94\frac{1}{2}$ 99 ³ / ₄ 105	$101\frac{1}{2}$ 107 112 ³ / ₄	6615 7011 743/8	95 ³ / ₈ 100 18 106	7978 8313 8318 8814	$124\frac{7}{8}$ $131\frac{13}{138}$ $138\frac{3}{4}$	$126 \frac{1}{2}$ $133 \frac{1}{2}$ $140 \frac{1}{2}$	80 ¼ 84 ¼ 88 ¼	6615 7011 74 3/8	76 80 84	$120 \\ 125 \\ 128$	$ \begin{array}{c} 60 \\ 62 \frac{1}{2} \\ 64 \end{array} $		46 48 50



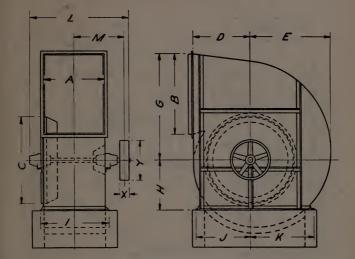
OVERHUNG PULLEY FULL HOUSING—UP DISCHARGE

Size	A	В	С	D	F	G	Н	1	J	к	L	M	x	Y
3 3½ 4	12 14 16	$ \begin{array}{r} 15 {}^{3}_{4} \\ 18 {}^{3}_{8} \\ 21 \\ \end{array} $	20	$11 \frac{3}{16}$ 13 14 $\frac{7}{8}$	$15\frac{7}{16}$	24 1/4	19 1/2	$16\frac{1}{4}$ $18\frac{1}{4}$ $20\frac{1}{4}$	15	$17 \\ 19 \frac{1}{2} \\ 22$	27 29 31	$14\frac{1}{2}\\15\frac{1}{2}\\16\frac{1}{2}$	3	8 9 10
$ \begin{array}{r} 4 \frac{1}{2} \\ 5 \\ 5 \frac{1}{2} \end{array} $	18 20 22	$\begin{array}{r} 23 {}^{5}\!$	28 1/2	${\begin{array}{*{20}c} 16\frac{3}{4} \\ 18\frac{5}{8} \\ 20\frac{7}{16} \\ 16 \end{array}}$	22 16	34 11	27 1/2	$\begin{array}{c} 22 \frac{1}{4} \\ 24 \frac{1}{4} \\ 26 \frac{1}{4} \end{array}$	19 1/2	27	$33 \\ 35 \\ 36 \frac{1}{2}$	$17\frac{1}{2}$ $18\frac{1}{2}$ $18\frac{1}{2}$ $18\frac{1}{2}$		$ \begin{array}{c} 11 \\ 12 \\ 14 \end{array} $
6 7 8	24 28 32	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	$\begin{array}{r} 34 \frac{1}{4} \\ 39 \frac{3}{4} \\ 45 \frac{1}{2} \end{array}$		$30^{7}\frac{1}{8}$	$\begin{array}{r} 41 \frac{5}{8} \\ 48 \frac{9}{16} \\ 55 \frac{1}{2} \end{array}$	38	$\begin{array}{c} 28 \ \frac{1}{4} \\ 32 \ \frac{1}{4} \\ 36 \ \frac{1}{4} \end{array}$	26 1/2	32 37 42	40 47 53	$20\frac{1}{2}$ 24 27	3 4 5	16 18 20
9 10 11	36 40 44	$47\frac{1}{4}$ $52\frac{1}{2}$ $57\frac{3}{4}$	$51\frac{1}{4}$ $56\frac{3}{4}$ $62\frac{1}{2}$	$ \begin{array}{c} 33 \frac{1}{2} \\ 37 \frac{3}{16} \\ 40 \frac{15}{16} \end{array} $	44 1/8	$\begin{array}{c} 62 rac{7}{18} \\ 69 rac{3}{8} \\ 76 rac{5}{16} \end{array}$	54	$\begin{array}{r} 40 \frac{1}{4} \\ 44 \frac{1}{4} \\ 49 \frac{1}{4} \end{array}$	34 %	52	$ \begin{array}{c} 61 \\ 65 \\ 73 \frac{1}{2} \end{array} $	31 33 37	6 6 8	24 26 28
12 13 14	$48 \\ 52 \\ 56$	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	73 1/2	44 5/8 48 3/8 52 18	57 3/8	83 ¼ 90 诸 97 ⅛	70	$53 \frac{1}{4}$ $58 \frac{1}{4}$ $62 \frac{1}{4}$	45 %	68	79 ½ 83 92	$39\frac{1}{2}$ $41\frac{1}{2}$ 46		30 34 36
15 16 17		78 3⁄4 84 89 1⁄4	90 1/4	$55\frac{8}{4}$ 59 $\frac{1}{2}$ 63 $\frac{1}{4}$	$70\frac{5}{8}$	104 18 111 117 18	86	$\begin{array}{c} 66 \frac{1}{4} \\ 71 \frac{1}{4} \\ 76 \frac{1}{4} \end{array}$	54 %	83 1/2	99 107 112	$49\frac{1}{2}$ $53\frac{1}{2}$ 56	14	38 40 44
18 19 20	76	99 ³ 4	107	70 11	83 18	124 7 4 131 13 138 34	102	80 ¼ 84 ¼ 88 ¼	$64\frac{8}{8}$	99	120 125 128	$ \begin{array}{c} 60 \\ 62 \frac{1}{2} \\ 64 \end{array} $		46 48 50



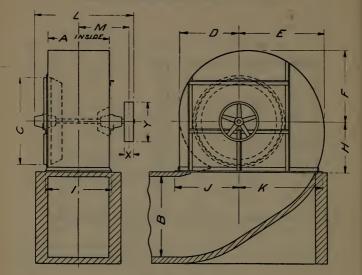
OVERHUNG PULLEY FULL HOUSING-DOWN DISCHARGE

Size	A	В	c	E	F	G	н	I	J	к	L	м	x	Y
3 3½ 4	12 14 16	$ 15\frac{3}{4} 18\frac{3}{8} 21 $	$17\frac{1}{4}\\20\\22\frac{3}{4}$		$13\frac{1}{4}$ $15\frac{7}{18}$ $17\frac{5}{8}$	$20\frac{13}{18}\\24\frac{1}{4}\\27\frac{3}{4}$	14	$16\frac{1}{4}$ $18\frac{1}{4}$ $20\frac{1}{4}$		$\begin{array}{c} 22\frac{13}{16} \\ 26\frac{1}{4} \\ 29\frac{3}{4} \end{array}$	27 29 31	$14\frac{1}{15}\frac{1}{12}$ $16\frac{1}{2}$	333	8 9 10
$4\frac{1}{2}$ 5 5 $\frac{1}{2}$	$ \begin{array}{r} 18 \\ 20 \\ 22 \end{array} $	$23\frac{5}{8}$ $26\frac{1}{4}$ $28\frac{7}{8}$	$25\frac{3}{4}$ $28\frac{1}{2}$ $31\frac{1}{2}$	$\begin{array}{c} 23 \frac{7}{8} \\ 26 \frac{1}{2} \\ 29 \frac{1}{8} \end{array}$	$\begin{array}{r} 19 \frac{7}{8} \\ 22 \frac{1}{16} \\ 24 \frac{1}{4} \end{array}$	3411	20		$18\frac{3}{4}\\19\frac{1}{2}\\21\frac{1}{4}$	$\begin{array}{r} 33 \frac{1}{4} \\ 36 \frac{11}{16} \\ 40 \frac{3}{16} \end{array}$	33 35 36 ½	17 ½ 18 ½ 18 ½	3	$11 \\ 12 \\ 14$
6 7 8	24 28 32	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	$34\frac{1}{4}$ $39\frac{3}{4}$ $45\frac{1}{2}$	$31\frac{13}{18}\ 37\frac{1}{8}\ 42\frac{3}{8}$	$26\frac{1}{2}$ $30\frac{7}{8}$ $35\frac{5}{18}$	$\begin{array}{r} 41 \frac{5}{8} \\ 48 \frac{9}{16} \\ 55 \frac{1}{2} \end{array}$	27	$\begin{array}{c} 28 \ \frac{1}{4} \\ 32 \ \frac{1}{4} \\ 36 \ \frac{1}{4} \end{array}$	$23 \\ 26 \frac{1}{2} \\ 28 \frac{3}{4}$	43 5/8 50 8 57 1/2	40 47 53	$20\frac{1}{2}$ 24 27	3 4 5	16 18 20
9 10 11	36 40 44	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	$51\frac{1}{4}\\56\frac{3}{4}\\62\frac{1}{2}$	4711 53 5816	$39\frac{3}{4}\\44\frac{1}{8}\\48\frac{1}{2}$	$\begin{array}{c} 62 \frac{7}{16} \\ 69 \frac{3}{8} \\ 76 \frac{6}{16} \end{array}$	$38\frac{1}{2}$	40 ¼ 44 ¼ 49 ¼	$31\frac{3}{4}$ $34\frac{3}{4}$ $38\frac{3}{8}$	64 7 71 3/8 78 13 78 13	$ \begin{array}{c} 61 \\ 65 \\ 73 \frac{1}{2} \end{array} $	31 33 37	6 6 8	24 26 28
12 13 14	$48 \\ 52 \\ 56$	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	$68 \\ 73 \frac{1}{2} \\ 79$	$63\frac{5}{8}$ $68\frac{7}{8}$ $74\frac{3}{18}$	52_{16}^{15} $57_{3/8}^{3/8}$ $61_{3/4}^{3/4}$	83 1/4 90 3 97 1/8	49 1/2	58 14	$\begin{array}{r} 41 \ \frac{7}{8} \\ 45 \ \frac{3}{8} \\ 47 \ \frac{3}{8} \end{array}$	85 ³ / ₄ 93 ³ / ₁₈ 100 ¹ / ₈	79 ½ 83 92	$ \begin{array}{r} 39 \frac{1}{2} \\ 41 \frac{1}{2} \\ 46 \end{array} $		30 34 36
15 16 17	$\begin{array}{c} 60\\64\\68\end{array}$	78 ³ ⁄4 84 89 ¹ ⁄4	$\begin{array}{r} 84\frac{3}{4} \\ 90\frac{1}{4} \\ 96 \end{array}$	79 1/2 84 3/4 90 18	70 5/8	10418 111 11718	$5760 \frac{1}{2}64 \frac{1}{2}$	$\begin{array}{c} 66 \frac{1}{4} \\ 71 \frac{1}{4} \\ 76 \frac{1}{4} \end{array}$	$51\frac{3}{8}$ $54\frac{7}{8}$ $58\frac{3}{8}$	$107\frac{1}{16}$ $114\frac{1}{16}$ $121\frac{15}{16}$	99 107 112	$49\frac{1}{2}$ 53 $\frac{1}{2}$ 56		38 40 44
18 19 20	72 76 80	99 34		95 3/8 10011 106	797 831 831 8814	$124\frac{7}{8}$ $131\frac{13}{138}$ $138\frac{3}{4}$	68 72 75 ½	84 1/4	$64\frac{3}{8}$	$\frac{128\frac{7}{8}}{135\frac{13}{16}}$	125	$60 \\ 62 \frac{1}{2} \\ 64$		46 48 50



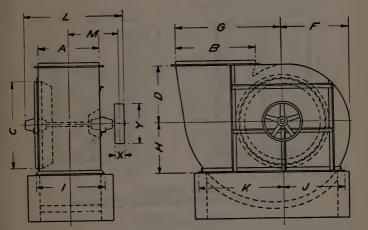
OVERHUNG PULLEY THREE-QUARTER HOUSING—TOP HORIZONTAL DISCHARGE

Size	A	В	С	D	E	G	н	1	J	к	L	M	x	Y
6 7 8		$31\frac{1}{2}$ $36\frac{3}{4}$ 42	$34\frac{1}{4}$ $39\frac{3}{4}$ $45\frac{1}{2}$	26	$31\frac{13}{18}\\37\frac{1}{8}\\42\frac{3}{8}$	$\begin{array}{r} 41 \frac{5}{8} \\ 48 \frac{9}{16} \\ 55 \frac{1}{2} \end{array}$	23 3/4		$23 \\ 26 \frac{1}{2} \\ 28 \frac{3}{4}$		40 47 53	$20\frac{1}{2}$ 24 27	3 4 5	16 18 20
9 10 11	36 40 44	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	56 3/4	$\begin{array}{c} 33 \frac{1}{2} \\ 37 \frac{3}{18} \\ 40 \frac{1}{18} \end{array}$	$\begin{array}{r} 47 \frac{11}{18} \\ 53 \\ 58 \frac{5}{18} \end{array}$	62 7 69 3/8 76 5 6	3234	44 1/4		36 11 40 ⁷ / ₈ 45 ¹ / ₂	$ \begin{array}{c} 61 \\ 65 \\ 73 \frac{1}{2} \end{array} $	31 33 37	6 6 8	24 26 28
12 13 14	$ \begin{array}{r} 48 \\ 52 \\ 56 \end{array} $	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	73 1/2	44 5/8 48 3/8 52 18	68 7%	$90\frac{3}{16}$	42	58 1/4	45 3/8	54 18	79 ½ 83 92	$39\frac{1}{2}$ $41\frac{1}{2}$ 46	9 10 11	30 34 36
15 16 17	60 64 68	78 ³ ⁄ ₄ 84 89 ¹ ⁄ ₄		$55\frac{3}{4}\\59\frac{1}{2}\\63\frac{1}{4}$	84 34	104 급 111 117 급통	51 1/2	71 1/4	54 %	66 3/4	107	$\begin{array}{r} 49 \frac{1}{2} \\ 53 \frac{1}{2} \\ 56 \end{array}$		38 40 44
18 19 20	72 76 80	9934	107	70 1	95 % 100 11 106	131 18	59 %	84 14	64 3/8	79 1/2	125	$ \begin{array}{c} 60 \\ 62 \frac{1}{2} \\ 64 \end{array} $		46 48 50



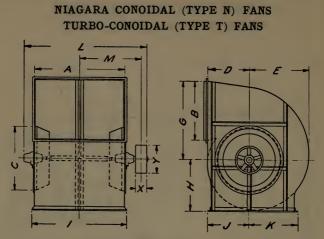
OVERHUNG PULLEY THREE-QUARTER HOUSING—BOTTOM HORIZONTAL DISCHARGE

Size	A	B	C	D	Е	F	Н	1	J	K	L	M	x	Y
6 7 8	$24 \\ 28 \\ 32$	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	39 3/4	$23\frac{3}{8}$ $27\frac{5}{16}$ $31\frac{3}{16}$	39 1/4	27 ⁷ / ₈ 32 7 / ₈ 37 ¹ / ₈	23 3/4	32 1/4	25 ³ / ₈ 29 ¹ / ₆ 33 ³ / ₁₈	32 7/8 38 1/8 43 3/8		$20\frac{1}{2}$ 24 27	3 4 5	16 18 20
9 10 11	$36 \\ 40 \\ 44$	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	56 3/1			$41\frac{3}{4}$ $46\frac{3}{8}$ 51	3234	40 ¼ 44 ¼ 49 ¼	$37 \frac{1}{16} \\ 41 \\ 45 \frac{3}{8}$	48 16 53 ⁷ ₈ 59 ⁵ /8	$61 \\ 65 \\ 73 \frac{1}{2}$	31 33 37	6 6 8	$24 \\ 26 \\ 28$
12 13 14	$48 \\ 52 \\ 56$	${}^{63}_{68\frac{1}{4}}_{73\frac{1}{2}}$	73 1/2	$\begin{array}{r} 46 \frac{3}{4} \\ 50 \frac{11}{16} \\ 54 \frac{9}{16} \end{array}$	72 1/8	60 16	42	$53 \frac{1}{4}$ 58 $\frac{1}{4}$ 62 $\frac{1}{4}$	53 16	$\begin{array}{r} 64 \frac{7}{8} \\ 70 \frac{3}{4} \\ 75 \frac{15}{16} \end{array}$	79 ½ 83 92	$39\frac{1}{2}$ $41\frac{1}{2}$ 46	9 10 11	$30 \\ 34 \\ 36$
15 16 17	$\begin{array}{c} 60\\ 64\\ 68\end{array}$	78 ¾ 84 89 ¼		$58\frac{7}{16}62\frac{3}{8}66\frac{1}{4}$	$\begin{array}{r} 84 \\ 16 \\ 89 \\ 11 \\ 95 \\ 16 \\ 95 \\ 16 \\ 16 \end{array}$	74 1/4	51 1/2	71 1/4	65 7.8	81 ¹ / ₈ 86 ⁷ / ₈ 92 ¹ / ₁₆	107	$49\frac{1}{2}$ $53\frac{1}{2}$ 56	14	$\begin{array}{c} 38\\ 40\\ 44 \end{array}$
18 19 20	72 76 80	99 3/4	107	$74\frac{1}{16}$	100 15 106 1/2 112 1/8	88 1/8	59 3/4	84 1/4	78 1	$97\frac{15}{16}\\103\frac{1}{4}\\108\frac{3}{8}$	125	$ \begin{array}{c} 60 \\ 62 \frac{1}{2} \\ 64 \end{array} $		46 48 50



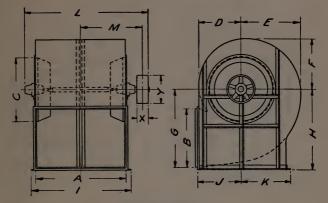
OVERHUNG PULLEY THREE-QUARTER HOUSING-UP DISCHARGE

Size	A	В	с	D	F	G	н	1	J	к	L	M	x	Y
6 7 8	24 28 32	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	$34\frac{1}{4}$ $39\frac{3}{4}$ $45\frac{1}{2}$	26	26 1⁄2 30 7/8 35 18	41 ⁵ / ₈ 48 ³ / ₁₈ 55 ¹ / ₂	23 3/4	$28 \frac{1}{4} \\ 32 \frac{1}{4} \\ 36 $	$23\frac{3}{4}\\27\frac{5}{8}\\31\frac{1}{2}$	$33\frac{1}{4}\\38\frac{5}{8}\\44\frac{1}{8}$	40 47 53	$20\frac{1}{2}$ 24 27	3 4 5	16 18 20
9 10 11	$36 \\ 40 \\ 44$	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	56 34	37 4	$39\frac{3}{4}$ $44\frac{1}{8}$ $48\frac{1}{2}$		32 3/4	44 1/4	35 ½ 39 43 5 18	49 3/8 54 7/x 60 3/4	$ \begin{array}{c} 61 \\ 65 \\ 73 \frac{1}{2} \end{array} $	1	6 6 8	24 26 28
12 13 14	48 52 56	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	$73\frac{1}{2}$	48 3/8	52 15 57 3/8 61 3/4	90 -	42	58 1/4	$\begin{array}{r} 47 \frac{1}{8} \\ 51 \frac{1}{2} \\ 55 \frac{1}{4} \end{array}$	$72\frac{1}{4}$	83	$ \begin{array}{r} 39 \frac{1}{2} \\ 41 \frac{1}{2} \\ 46 \end{array} $	9 10 11	30 34 36
15 16 17	60 64 68	78 ⁸ ⁄4 84 89 ¹ ⁄4	90 1/4	$55\frac{3}{4}$ 59 $\frac{1}{2}$ 63 $\frac{1}{4}$	70 %	104 🛧 111 117 👬	51 1/2	71 1/4	63 18	82 7/8 88 7/8 94 16	107	$ \begin{array}{r} 49 \frac{1}{2} \\ 53 \frac{1}{2} \\ 56 \end{array} $		38 40 44
18 19 20	72 76 80	00 3/	$101\frac{1}{2}$ 107 112 ³ / ₄	70 +	83 13	1314	59 %	84 1/4	10 14	$ \begin{array}{r} 100 \frac{1}{4} \\ 105 \frac{3}{4} \\ 111 \end{array} $	$120 \\ 125 \\ 128$	$ \begin{array}{c} 60 \\ 62 \\ 64 \end{array} $		46 48 50



DOUBLE WIDTH FULL HOUSING—TOP HORIZONTAL DISCHARGE

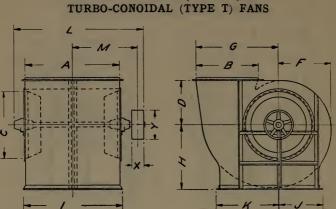
Size	A	В	c	D	E	G	н	I	J	к	L	M	x	Y
3 3½ 4		$15\frac{3}{4}$ $18\frac{3}{8}$ 21	20	11 18 13 14 7/8	$15\frac{7}{8}\\18\frac{9}{16}\\21\frac{3}{16}$	$\begin{array}{r} 20 \ \frac{13}{16} \\ 24 \ \frac{1}{4} \\ 27 \ \frac{3}{4} \end{array}$	$ \begin{array}{r} 14 \\ 16 \frac{1}{2} \\ 18 \frac{1}{2} \end{array} $	32 1/4	$ \begin{array}{r} 13 \frac{1}{4} \\ 15 \\ 16 \frac{7}{8} \end{array} $	16	38 44 48	$ \begin{array}{r} 19 \frac{1}{22} \\ 22 \frac{1}{2} \\ 24 \frac{1}{2} \end{array} $		8 9 10
4 ¹ ⁄ ₂ 5 5 ¹ ⁄ ₂	40	$23\frac{5}{8}$ $26\frac{1}{4}$ $28\frac{7}{8}$	28 1/2	$18\frac{5}{8}$	$\begin{array}{c} 23 \frac{7}{8} \\ 26 \frac{1}{2} \\ 29 \frac{1}{8} \end{array}$	$31 \frac{1}{4} \\ 34 \frac{11}{16} \\ 38 \frac{3}{16} \\ 38 \frac{3}{16} \\ \end{array}$	23	44 1/4	$18\frac{3}{4}\\19\frac{1}{2}\\21\frac{1}{4}$	22	$55 \\ 59 \\ 65$	28 30 33	4 4 5	$11 \\ 12 \\ 14$
6 7 8	56	$31\frac{1}{2}$ $36\frac{3}{4}$ 42		26	$\begin{array}{r} 31 \frac{13}{18} \\ 37 \frac{1}{8} \\ 42 \frac{3}{8} \end{array}$	$\begin{array}{c} 41 \ \frac{5}{8} \\ 48 \ \frac{16}{16} \\ 55 \ \frac{1}{2} \end{array}$	32	$52\frac{1}{4}$ $60\frac{1}{4}$ $68\frac{1}{4}$	$23 \\ 26 \frac{1}{2} \\ 28 \frac{3}{4}$	26 30 34	$69\frac{1}{2}$ 77 $\frac{1}{2}$ 87	35 39 43 ½	6 6 8	16 18 20
9 10 11	80	47 ¼ 52 ½ 57 ¾	56 34	$\begin{array}{c} 33 \frac{1}{2} \\ 37 \frac{3}{16} \\ 40 \frac{15}{16} \end{array}$	53	$\begin{array}{c} 62 & \frac{7}{16} \\ 69 & \frac{3}{8} \\ 76 & \frac{5}{16} \end{array}$	45	84 1/4	$31\frac{3}{4}$ $34\frac{3}{4}$ $38\frac{3}{8}$	42	100 110 124	$50 \\ 55 \\ 62$	10 12 15	24 26 28
12 13 14	96 104 112	63 68 ¼ 73 ½	73 1/2	$\begin{array}{r} 44 \frac{5}{8} \\ 48 \frac{3}{8} \\ 52 \frac{1}{16} \end{array}$	$\begin{array}{c} 63 \frac{5}{8} \\ 68 \frac{7}{8} \\ 74 \frac{3}{16} \end{array}$	83 ¼ 90 ⅓ 97 ⅛ 97 ⅛	$58\frac{1}{2}$	$ \begin{array}{r} 101 \frac{1}{4} \\ 110 \frac{1}{4} \\ 118 \frac{1}{4} \\ 118 \frac{1}{4} \end{array} $	$45\frac{3}{8}$	55	146	69 73 79		$30 \\ 34 \\ 36$
15 16 17	128	78 ¾ 84 89 ¼	90 1/4	$55\frac{3}{4}\\59\frac{1}{2}\\63\frac{1}{4}$	84 3/4	104 👍 111 117 👬	72	$126\frac{1}{4}\\135\frac{1}{4}\\144\frac{1}{4}$	$54\frac{7}{8}$	$67\frac{1}{2}$		83 ½ 89 ½ 94		38 40 44
18 19 20	152	99 34	107	70 11	95 3⁄8 100 18 106	131 13	85	160 1/4	$64\frac{3}{8}$	80	202	97 101 106		46 48 50



DOUBLE WIDTH FULL HOUSING—BOTTOM HORIZONTAL DISCHARGE

Dimensions in Inches

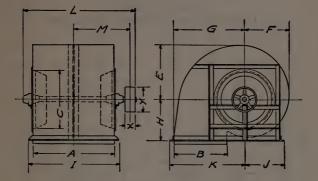
Size	A	В	с	D	E	F	G	н	I	J	к	L	M	x	Y
3 31/2 4	24 28 32	153 183 21	20	$ \begin{array}{c} 11 & 3 \\ 13 \\ 14 & 14 \\ 14 & 8 \end{array} $	$15\frac{7}{8}$ $18\frac{9}{18}$ $21\frac{3}{16}$	131 15 ₁ 7 175 175	20 18 24 1 27 1 27 1	$22 \\ 25\frac{1}{2} \\ 29$	284 324 364		$14 \\ 16 \\ 18$	38 44 48	$19\frac{1}{2}$ $22\frac{1}{2}$ $24\frac{1}{2}$	3333	8 9 10
$4\frac{1}{2}$ 5 $5\frac{1}{2}$	36 40 44	23 5 26 1 28 5		163 188 207 16	23 3 26 1 29 1	$19\frac{7}{8}$ 22 $\frac{1}{18}$ 24 $\frac{1}{4}$	$31\frac{1}{4}$ $34\frac{11}{16}$ $38\frac{3}{16}$	$32\frac{1}{2}$ 36 39 $\frac{1}{2}$	401 441 481	163 185 20 7 16	$20 \\ 22 \\ 24$	55 59 65	28 30 33	4	11 12 14
6 7 8	48 56 64	$ \begin{array}{r} 31 \frac{1}{3} \\ 36 \frac{3}{4} \\ 42 \end{array} $		22 18 26 29 3	31 13 371 423	26½ 30% 35%	$41\frac{5}{8}$ $48\frac{9}{16}$ $55\frac{1}{2}$	43 50 57	521 601 681	22 5 26 29 1 29 1	26 30 34	69 <u>1</u> 77 <u>1</u> 87	$35 \\ 39 \\ 43\frac{1}{2}$	6	16 18 20
9 10 11	72 80 88	471 521 571	511 563 621	331 3778 4018	47 16 53 58 16	393 445 481	$\begin{array}{r} 62 \frac{7}{18} \\ 69 \frac{3}{8} \\ 76 \frac{5}{16} \end{array}$	64 71 78		331 37 18 40 18	$38 \\ 42 \\ 46 \frac{1}{2}$	$100 \\ 110 \\ 124$	50 55 62	$ \begin{array}{r} 10 \\ 12 \\ 15 \end{array} $	
12 13 14	96 104 112	$ \begin{array}{c} 63 \\ 681 \\ 731 \\ 731 \\ 7 \end{array} $	68 73 1 79	445 485 52 16	635 685 74 18	5215 573 611	831 9018 971	85 92 99	101 1 110 1 118 1		$50\frac{1}{2}$ 55 59	$137\frac{1}{2}$ 146 158	69 73 79		30 34 36
15 16 17	120 128 136	783 84 891	843 901 96	553 591 631	791 841 901	66 38 708 75	104 18 111 117 1 8	$112\frac{1}{2}$	$1261 \\ 1351 \\ 1441 \\ $		$63 \\ 67\frac{1}{2} \\ 72$	$ \begin{array}{r} 166rac{1}{2} \\ 179 \\ 187rac{1}{2} \end{array} $	83½ 89½ 94		38 40 44
19	144 152 160	993	$101\frac{1}{2}$ 107 112 $\frac{3}{4}$	70 14	95 3 100 11 106	83 18	131	$133\frac{1}{2}$	$152\frac{1}{160\frac{1}{4}}$ $168\frac{1}{4}$	66 18 70 18 74 8	76 80 84	194 202 212	97 101 106		46 48 50



DOUBLE WIDTH FULL HOUSING-UP DISCHARGE

Dimensions in Inches

Size	A	В	с	D	F	G	н	I	J	к	L	м	XY	7
$ 3 \frac{3}{3} \frac{1}{2} \frac{1}{2} 4 $	24 28 32	$15\frac{3}{4}$ $18\frac{3}{8}$ 21	20	11_{16}^{3} 13 14 $\frac{7}{8}$	$15\frac{7}{16}$	$20{}^{13}_{16}\\24{}^{14}_{14}\\27{}^{34}_{4}$	$17 \\ 19 \frac{1}{2} \\ 22 \frac{1}{2}$	$\begin{array}{r} 28 \frac{1}{4} \\ 32 \frac{1}{4} \\ 36 \frac{1}{4} \end{array}$		$17 \\ 19 \frac{1}{2} \\ 22$	38 44 48	$ \begin{array}{r} 19\frac{1}{22} \\ 22\frac{1}{2} \\ 24\frac{1}{2} \end{array} $	3 3 3 1	8 9 0
$ \begin{array}{r} 4 \frac{1}{2} \\ 5 \\ 5 \frac{1}{2} \end{array} $	$36 \\ 40 \\ 44$	$23\frac{5}{8}$ $26\frac{1}{4}$ $28\frac{7}{8}$	$28\frac{1}{2}$	16 ³ ⁄4 18 ⁵ ⁄8 20 ⁷ /18	$\begin{array}{c} 19 \frac{7}{8} \\ 22 \frac{1}{16} \\ 24 \frac{1}{4} \end{array}$	$\begin{array}{c} 31 \frac{1}{4} \\ 34 \frac{11}{16} \\ 38 \frac{3}{16} \end{array}$	$25 \\ 27 \frac{1}{2} \\ 30$	44 1/4	$18\frac{3}{4}\\19\frac{1}{2}\\21\frac{1}{4}$	27	55 59 65	28 30 33	$ \begin{array}{c} 4 & 1 \\ 4 & 1 \\ 5 & 1 \end{array} $	2
6 7 8	$48 \\ 56 \\ 64$	${31}\frac{1}{2}$ ${36}\frac{3}{4}$ ${42}$	39 34	22 1 8 26 29 ¾	30 1/8	$\begin{array}{r} 41 \frac{5}{8} \\ 48 \frac{9}{16} \\ 55 \frac{1}{2} \end{array}$	$33 \\ 38 \\ 43 \frac{1}{2}$		$23 \\ 26 \frac{1}{2} \\ 28 \frac{3}{4}$		$\begin{array}{c} 69\frac{1}{2} \\ 77\frac{1}{2} \\ 87 \end{array}$	$35 \\ 39 \\ 43 \frac{1}{2}$		8
9 10 11	72 80 88	$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	56 34	$\begin{array}{c} 33 \frac{1}{2} \\ 37 \frac{3}{16} \\ 40 \frac{15}{16} \end{array}$	44 1/8	$\begin{array}{c} 62 \ rac{7}{16} \\ 69 \ rac{3}{8} \\ 76 \ rac{5}{16} \end{array}$	$49 \\ 54 \\ 59 \frac{1}{2}$	84 1/4	$31\frac{3}{4}$ $34\frac{3}{4}$ $38\frac{3}{8}$	52	100 110 124	50 55 62	$\begin{array}{c} 10 & 24 \\ 12 & 20 \\ 15 & 28 \end{array}$	6
12 13 14	96 104 112	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	$73\frac{1}{2}$	$\begin{array}{r} 44 \ \frac{5}{8} \\ 48 \ \frac{3}{8} \\ 52 \ \frac{1}{16} \end{array}$	$57\frac{3}{8}$	$\begin{array}{c} 83 \frac{1}{4} \\ 90 \frac{3}{18} \\ 97 \frac{1}{8} \end{array}$	$ \begin{array}{c} 65 \\ 70 \\ 75 \frac{1}{2} \end{array} $	$101\frac{1}{4}$ $110\frac{1}{4}$ $118\frac{1}{4}$	$45\frac{3}{8}$	68	$137\frac{1}{2}$ 146 158	69 73 79	3) 3. 3)	4
15 16 17	$120 \\ 128 \\ 136$	78 ¾ 84 89 ¼	90 1/4	$55\frac{3}{4}$ $59\frac{1}{2}$ $63\frac{1}{4}$	$70\frac{5}{8}$	$104 \frac{1}{16}$ 111 117 $\frac{1}{16}$	$ \begin{array}{r} 80 \frac{1}{2} \\ 86 \\ 91 \end{array} $	$126\frac{1}{4}$ $135\frac{1}{4}$ $144\frac{1}{4}$	54 1/8	$83\frac{1}{2}$	$166\frac{1}{2}$ 179 187 $\frac{1}{2}$	83 ½ 89 ½ 94	38 40 4-	0
18 19 20	$144 \\ 152 \\ 160$	$94\frac{1}{2}$ 99 ³ / ₄ 105	$ \begin{array}{r} 101 \frac{1}{2} \\ 107 \\ 112 \frac{3}{4} \end{array} $	66 15 70 11 74 3/8	79 78 83 13 88 14	$124 \frac{7}{8} \\ 131 \frac{13}{138} \\ 138 \frac{3}{4}	$96\frac{1}{2}\\102\\107$	$152\frac{1}{4}\\160\frac{1}{4}\\168\frac{1}{4}$	64 3/8	99	194 202 212	97 101 106	40 48 50	8

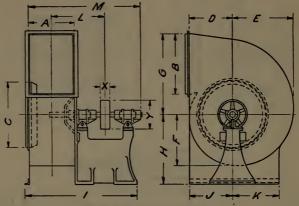


DOUBLE WIDTH FULL HOUSING—DOWN DISCHARGE

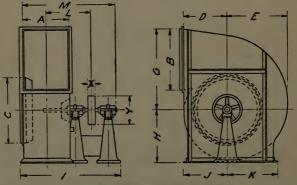
Dimensions in Inches

Size	A	В	c	E	F	G	н	I	J	к	L	M	x	Y
3 3 ½ 4		$15\frac{3}{4}$ $18\frac{3}{8}$ 21	$17\frac{1}{4}$ 20 22 $\frac{3}{4}$	15 % 18 % 21 %	15 76	24 1/4	14	$ \begin{array}{r} 28 \frac{1}{4} \\ 32 \frac{1}{4} \\ 36 \frac{1}{4} \end{array} $	13 ¼ 15 17	$\begin{array}{r} 22 \\ 13 \\ 26 \\ 14 \\ 29 \\ 34 \end{array}$	38 44 48	$ \begin{array}{r} 19 \frac{1}{2} \\ 22 \frac{1}{2} \\ 24 \frac{1}{2} \\ \end{array} $	333	8 9 10
$ \begin{array}{r} 4 & \frac{1}{2} \\ 5 \\ 5 & \frac{1}{2} \end{array} $	40	$\begin{array}{r} 23 \frac{5}{8} \\ 26 \frac{1}{4} \\ 28 \frac{7}{8} \end{array}$	$25\frac{3}{4}\\28\frac{1}{2}\\31\frac{1}{2}$	26 1/2	22 16	$31\frac{1}{4}$ $34\frac{1}{16}$ $38\frac{1}{16}$	$18 \\ 20 \\ 21 \frac{1}{2}$	44 1/4	$18\frac{3}{4}\\19\frac{1}{2}\\21\frac{1}{4}$	33 1/4 36 11 40 15	55 59 65	28 30 33	4 4 5	12
6 7 8	56	$31\frac{1}{2}$ $36\frac{3}{4}$ 42	39 3/4	$31\frac{13}{18}$ $37\frac{1}{8}$ $42\frac{3}{8}$	30 1/8	48 16			$23 \\ 26 \frac{1}{2} \\ 28 \frac{3}{4}$	$\begin{array}{r} 43 \frac{5}{8} \\ 50 \frac{9}{16} \\ 57 \frac{1}{2} \end{array}$	77 1/2		6 6 8	$ \begin{array}{r} 16 \\ 18 \\ 20 \end{array} $
9 10 11		$\begin{array}{r} 47 \frac{1}{4} \\ 52 \frac{1}{2} \\ 57 \frac{3}{4} \end{array}$	$51\frac{1}{4}$ $56\frac{3}{4}$ $62\frac{1}{2}$	53	44 1/8	69 3/8	$34\frac{1}{2}$ $38\frac{1}{2}$ 42	84 14	$31\frac{3}{4}$ $31\frac{3}{4}$ $38\frac{3}{8}$	71 3/8	110	50 55 62	10 12 15	$24 \\ 26 \\ 28$
12 13 14	104	$\begin{array}{c} 63 \\ 68 \frac{1}{4} \\ 73 \frac{1}{2} \end{array}$	$ \begin{array}{c} 68 \\ 73 \frac{1}{2} \\ 79 \end{array} $	68 1/8	$52\frac{15}{57\frac{3}{8}}$ $57\frac{3}{8}$ $61\frac{3}{4}$		49 1/2	101 1/4 110 1/4 118 1/4	45 3/8	93 18		69 73 79		30 34 36
15 16 17	128	78 ³ ⁄4 84 89 ¹ ⁄4	$ 84\frac{3}{4} 90\frac{1}{4} 96 $	79 ½ 84 ½ 90 18	70 5/8	104 16 111 117 18	60 1/2	$126 \frac{1}{4} \\ 135 \frac{1}{4} \\ 144 \frac{1}{4}$	54 %	114 1/2	179	89 1/2		38 40 44
18 19 20	152	99 34	$ \begin{array}{r} 101 \frac{1}{2} \\ 107 \\ 112 \frac{3}{4} \\ \end{array} $	10011	83 18	$124 \frac{74}{131} \frac{13}{138} \frac{13}{4}$	72	$152\frac{1}{4}$ $160\frac{1}{4}$ $168\frac{1}{4}$	64 3/8	135 18	202	97 101 106		46 48 50

OVERHUNG WHEEL FULL HOUSING—TOP HORIZONTAL DISCHARGE



This Style for No. 3 to No. 6 Fans



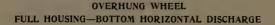
This Style for No. 7 to No. 13 Fans

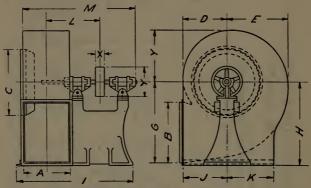
	0.000	-07	980	4000	30 34
				~~~~~	~~~~
×	ကကက	ကကက	co.4∙Ω	မမ	9 10
W	$31\frac{3}{8}$ $34\frac{1}{2}$ $38\frac{3}{4}$	43 <u>4</u> 3 <u>4</u> 5 46 <u>45</u> 50 <u>34</u>	$53\frac{3}{4}$ $53\frac{3}{4}$ $63\frac{3}{4}$	$\begin{array}{c} 67 \\ 81 \\ 81 \\ 85 \\ 38 \\ 85 \\ 88 \\ 85 \\ 86 \\ 86 \\ 81 \\ 81 \\ 81 \\ 81 \\ 81 \\ 81$	91 95
	$\frac{14\ 7_8}{16\ 3_8}$	$20 \frac{y_2}{22}$ 24 $y_8$	25 58 28 58 30 58 858 30 58	$\begin{array}{c} 32.5\% \\ 40.5\% \\ 42.5\% \\ 8 \end{array}$	44 58 46 58
М	12 14 16	18 20 22	24 30 34	38 42 46 ½	50 ½ 55
~	$11 \frac{11}{13}$ $13 \frac{14}{8}$	$16\frac{34}{12}$ 17 $\frac{12}{22}$ 19 $\frac{14}{2}$	$21 \\ 26 y_3 \\ 28 \frac{3}{2}$	$31\frac{3}{34}$ $34\frac{34}{34}$ $38\frac{34}{38}$	41 7% 45 3%
	32 ½ 36 18 40	$\begin{array}{c} 43 \\ 47 \\ 51 \\ 51 \\ 47 \\ 51 \\ 47 \\ 51 \\ 47 \\ 51 \\ 44 \\ 51 \\ 51 \\ 51 \\ 51 \\ 51 \\ 51$	54 60 74 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	68 <u>7</u> 85 <u>34</u> 90 <u>74</u>	94 14 98 34 98 34
Ŧ	$     \begin{array}{c}       18 \\       20  rac{34}{4}     \end{array}     $	$26\% \\ 29\% \\ 32\%$	$\frac{35}{32}$ $36 \frac{1}{23}$	$\frac{41}{45}$ $\frac{45}{19}$	54 58 ½
Ū	20 H3 24 ½ 27 ¾	31 ½ 34 14 38 16	$\frac{415_8}{4816}$	$\begin{array}{c} 62 \ {}^{7}_{18} \\ 69 \ {}^{8}_{8} \\ 76 \ {}^{6}_{18} \end{array}$	83 14 90 18
<u></u>	13 14 15 74 17 5/3	$\begin{array}{c} 19 \ \% \\ 22 \ \% \\ 24 \ \% \end{array}$	26 ½		
ш	${{157_8}\atop{1818}\atop{2118}}$	23 78 26 178 29 188	31 13 37 18 32 88	47 H 53 58 fa	63 5% 68 7% 8 7%
٩	11 18 13 14 78	$\frac{16\ {}^{8}}{18\ {}^{5}}_{8}$	22 fa 26 29 ¾	33 ½ 37 16 40 18	44 5% 48 3%
C	17 ¾ 20 22 ¾	25 % 28 ½ 31 ½	34 <u>14</u> 39 <u>34</u> 45 <u>1</u> 2	$51 \frac{34}{56} \\ 56 \frac{34}{5} \\ 62 \frac{3}{22} \\ 52 \frac{3}{22} \\$	68 73 ½
Ē	$15\frac{34}{18}$ $18\frac{36}{21}$	$\begin{array}{c} 23 \ 5 \\ 26 \ 1 \\ 28 \ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 8 \\ 7 \\ 7$	$31 \frac{15}{36} \frac{31}{34}$	47 ¼ 52 ½ 57 ¾	$63 \\ 68 \\ 1/4$
×	12 14 16	18 22 22	24 32 32 84	36 44	48 52
	B. C D E F G H . I J K L W	B         C         D         E         F         G         H         I         J         K         L         M         X           15%         17%         11%         16%         13%         20%         32%         11%         12         14%         31%         3         3           15%         17%         11%         16%         13%         20%         32%         11%         12         14%         31%         3         3         3         1         14%         31%         3         3         3         3         3         1         14%         31%         3         3         1         1         14%         31%         3         3         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1	B         C         D         E         F         G         H         I         J         K         L         M         X           155%         17 ¼         11 Å         15 Å         20 Å         13 Å         20 Å         14 Å         1         M         X           155%         13 Å         20 Å         13 Å         20 Å         13 Å         1         1         1         M         X           21         22 Å         20 Å         28 Å         20 Å         13 Å         1         1         1         M         X           21         22 Å         20 Å         20 Å         20 Å         38 Å         33 Å<	B         C         D         E         A           15%         17 W         11 %         15 %         20 %         11 %         15 %         21 %         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M         M <td>B         C         D         E         F         G         H         -         J         K         L         M         X           115%         117 M         115 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %</td>	B         C         D         E         F         G         H         -         J         K         L         M         X           115%         117 M         115 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         113 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %         114 %

### CONOIDAL FAN DIMENSIONS

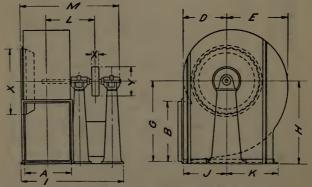
387

Size





This Style for No. 3 to No. 6 Fans



This Style for No. 7 to No. 13 Fans

FANS	FANS
N	Ĥ
(TYPE	TYPE
CONOIDAL	TURBO-CONOIDAL (
IIAGARA	TURB0-C

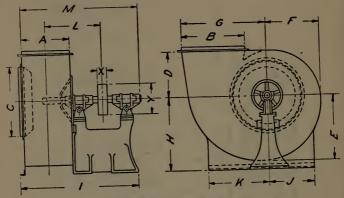
# OVERHUNG WHEEL FULL HOUSING-BOTTOM HORIZONTAL DISCHARGE

### Dimensions in Inches

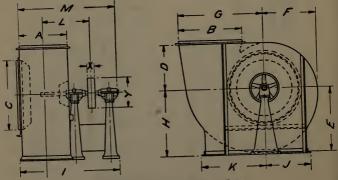
>	8 8 10 10	1121	16 18 20	24 26
×	~~~~		co.4∗ro	99
E	$     31 \frac{3}{8}     38 \frac{3}{4}     38 \frac{3}{4}     3     $	43 1/2 46 1/2 50 3/2	53 ³ / 64 ¹ / ₄ 68 ¹ / ₄	74 ³⁴ 83 ³⁴
	14 78 16 38 18 38	$22 \frac{20}{8} \frac{7}{8}$	25 ⁵ / ₈ 31 ¹ / ₈ 33 ¹ / ₈	36 5 5 40 5 5
K	12 14 16	18 20 22	24 30 34	38 42
-	$11_{13}^{3}$ $13_{13}^{13}$ $14_{78}^{\circ}$	$\frac{16^{3}}{18}^{6}_{54}$	$\frac{22}{28}\frac{f_8}{14}$	35 ½ 39 38
-	30 34 30 34 39 34	43 ^{3,4} 48 51	54 66 34 70 34	77 34
Ξ	23 38 27 14 30 58	34 1/3 38 1/3 41 7/8	45 ³ 4 50 57	64 71
IJ	20 18 24 14 27 34	31 1/4 34 1/4 38 1/8	$\frac{41}{55} \frac{5}{12} \frac{9}{12}$	$62 \frac{7}{38}$
Ľ.	$13 \frac{14}{15}$ $15 \frac{7}{18}$ $17 \frac{58}{58}$	19 7% 22 18 24 14	$\frac{26}{30}\frac{1/5}{7\frac{6}{8}}$	39 ³ 4 44 ¹ 8
ш	$\frac{15}{18} \frac{7_{\%}}{18} \\ 21 \frac{3}{36}$	23 7 _x 26 1 ₂ 29 1 ₈	31 18 37 18 42 38	47 H
Q	$\frac{11}{13}\frac{7_8}{7_8}$	$16\frac{34}{18}$ $18\frac{54}{8}$ $20\frac{7}{18}$	22 % 26 %	33 ½ 37 18
v	17 ½ 20 22 ¾	25 ³ ( 28 1/2 31 1/2 28 1/2	34 14 39 34 45 1/2	51 14 56 34
2	15 34 18 34 21	23 % 26 ½ 28 7 %	31 <u>15</u> 36 34 42	47 14 52 ½
×	12 14 16	18 22 23	24 32 32	36 40
Size	3 3 3 3 23	5 ½ 5 ½	010	10

### CONOIDAL FAN DIMENSIONS

OVERHUNG WHEEL FULL HOUSING—UP DISCHARGE



This Style for No. 3 to No. 6 Fans

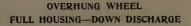


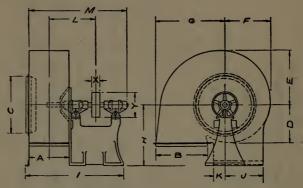
This Style for No. 7 to No. 13 Fans

### CONOIDAL FAN DIMENSIONS

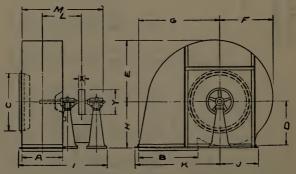
	×	
	W	31 3/8 34 1/2
		14 7/8 16 8/8
	K	15 17 ½
FANS	7	32 ½ 11 ½ 15 36 18 13 17 ½
E N) T) F HARGE	-	32 ½ 36 18
(TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (TYPE) (T	I	18 20 %
ARA CONOIDAL (TYPE N) BO-CONOIDAL (TYPE T) F OVERHUNG WHEEL FULL HOUSINGUP DISCHARGE Dimensions in Inches	ŋ	20 H3
A CON -CONO OVER L HOUS Dime	щ	13 14 20 43 15 1a 24 14
NIAGARA CONOIDAL (TYPE N) FANS TURBO-CONOIDAL (TYPE T) FANS OVERHUNG WHEEL FULL HOUSINGUP DISCHARGE Dimensions in Inches	ш	15 % 18 %
IN	٩	17 1/4 11 1/8 20 0.33
	v	20 20

~	8 10 10	11 12	16 20 20	26 26 28	30 34
×		ကကက	co <b>4 ro</b>	898	9 10
W	31 3/8 34 1/8 38 3/2 38 3/2	43 15 46 15 50 3/5	$53^{34}_{34}$ $59^{34}_{34}$ $63^{34}_{34}$	$\begin{array}{c} 67 \\ 81 \\ 81 \\ 85 \\ 38 \\ 85 \\ 38 \\ 85 \\ 86 \\ 81 \\ 81 \\ 81 \\ 81 \\ 81 \\ 81 \\ 81$	91 95
-	$\frac{14\ 7_8}{16\ 3_8}$	$^{20}_{24}^{12}_{\%}$	25 5 8 28 5 8 30 5 8 8	${}^{32}_{42}^{5}_{8}^{6}_{8}_{8}_{8}$	44 5/8 46 5/8
×	15 17 ½ 20	$22 \frac{32}{25}$ $27 \frac{3}{32}$	30 37 42	47 52 57 ½	$62 \frac{1}{2}$
7	11 1/4 13 15	16 % 17 1/2 19 1/4	$26 \frac{1}{12}$	$31_{34}^{34}$ $34_{34}^{34}$ $38_{84}^{34}$	41 7% 45 3%
-	32 ½ 36 18 40	43 34 47 16 51 14	54 ½ 60 ½ 64 ½	68 14 85 34 90 14	$\begin{array}{c} 94 & 14 \\ 98 & 34 \\ 98 & 34 \end{array}$
I	18 20 ¾ 24	26 % 29 ¼ 32 ¼	35 38 43 ½	$     \frac{49}{54} $	65 70
IJ	20 H8 24 14 27 34	31 ½ 34 ∰ 38 18	41 % 48 % 55 ½	$\begin{array}{c} 62 & 7_8 \\ 69 & 3_8 \\ 76 & 1_8 \end{array}$	83 14 90 34 38
ц,	13 14 15 74 17 58	19 7% 22 14 24 14	26 ½ 30 ½ 35 ½	$\frac{39}{44}^{34}_{12}$	52 18 57 38
ш	15 7% 18 76 21 76	23 78 26 7/8 29 /28	$\begin{array}{c} 31 \\ 37 \\ 42 \\ 38 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ 8 \\ $	47 <del>] }</del> 53 58 _{Åa}	63 54 68 78 68 78
Q	11 18 13 14 7/8	${ 16 \ _{18}^{34} \atop 20 \ _{78}^{26} }$	$\begin{array}{c} 22 & 48 \\ 26 & 34 \end{array}$	33 ½ 37 18 40 18	44 5% 48 8%
υ	$17 \frac{17}{20}$	25 ³⁴ 28 ^{1/2} 31 ^{1/2}	$34 \frac{14}{39}$ $39 \frac{34}{34}$ $45 \frac{15}{12}$	51 14 56 % 62 1/2	68 73 ½
æ	$     \begin{array}{c}       15 & \frac{3}{4} \\       18 & \frac{3}{8} \\       21 \\       21     \end{array} $	23 % 26 1% 28 7%	$31 \frac{1}{26} \frac{1}{36} \frac{31}{34} \frac{1}{42}$	52 14 52 14 57 % 57 % 57	63 68 ½
¥	12 14 16	18 20 23	24 28 32	36 40 44	48 52
Size	3 3 3 22	5 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	910	• 9 = 1	13





This Style for No. 3 to No. 6 Fans



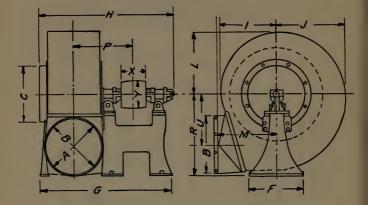
This Style for No. 7 to No. 13 Fans

### OVERHUNG WHEEL FULL HOUSING—DOWN DISCHARGE Dimensions in Inches

Y	8 9 10	11 12 14	16 20 20	24 26 28	30 34
×	ოოო	იიი	co.4∙ro	စစစ	9 10
W	$31\frac{3}{28}$ $34\frac{1/2}{38}$ $38\frac{3}{4}$	$\begin{array}{c} 43 \\ 46 \\ 50 \\ 34 \\ 46 \\ 34 \end{array}$	$\frac{53}{59}\frac{3}{34}$ $63\frac{3}{4}$	$\begin{array}{c} 67 \\ 81 \\ 81 \\ 34 \\ 85 \\ 38 \\ 85 \\ 38 \\ \end{array}$	91 95
L	$\frac{14\ 7_8}{16\ 3_8}$	$20 \frac{1}{22}$ $24 \frac{1}{28}$	25 5% 28 5% 30 5%	$\frac{32}{40} \frac{5}{28}$	44 5/8 46 5/8
×	60.00 4 24 24 24 24	6197 72/27 72/27		64 1 <u>7</u> 71 3 <u>8</u> 78 3 <u>4</u>	85 ¾ 93 ¼
~	11 14 13 15	$16\frac{3}{17}$ $17\frac{13}{12}$ $19\frac{14}{14}$	$21 \\ 26 \\ \frac{22}{28} \\ \frac{34}{4}$	$\begin{array}{c} 31 \begin{array}{c} 31 \\ 34 \\ 34 \\ 38 \\ 38 \\ 38 \\ 38 \end{array}$	41 7/8 45 3/8
-	32 ½ 36 ¹ 8 40	$\begin{array}{c} 43\frac{3}{4}\\ 47\frac{5}{16}\\ 51\frac{1}{14}\end{array}$	54 14 60 14 64 14	68 <u>14</u> 85 <u>34</u> 90 <u>14</u>	$\begin{array}{c} 94 \ 14 \\ 98 \ 34 \\ 98 \ 34 \end{array}$
I	$     \frac{18}{24} $	$26\frac{56}{29}$	35 27 31	$34 \frac{1}{22}$ $38 \frac{1}{22}$ 42	$\frac{46}{49}\frac{1}{2}$
Ð	20 13 24 14 27 34	31 <u>14</u> 34 <u>14</u> 38 <u>1</u> 8	$\frac{41}{55} \frac{58}{12}$	$\begin{array}{c} 62 & 16 \\ 69 & 38 \\ 76 & 16 \end{array}$	$^{83}_{ m Me}$
Ľ.	13 14 15 14 17 58	$\frac{19\%}{22\frac{18}{14}}$	26 ½ 30 ½ 35 ft	$ \frac{39}{44} $ $ \frac{44}{2} $ $ \frac{1}{2} $	52 15 57 38
ш	15 7% 18 7% 21 73	23 78 26 7% 29 78	31 13 37 16 37 18 42 3%	47 18 53 58 58	63 5/8 68 7/8
Q	11 1 ³ 13 14 78	$\frac{16\frac{3}{4}}{18\frac{5}{4}}$	22 fa 26 29 ¾	33 ½2 37 32 40 15	44 5% 48 3%
υ	17 ½ 20 22 ¾	25% 28% 31% 31%	$34 \frac{14}{24}$ $39 \frac{34}{24}$ $45 \frac{13}{22}$	${\begin{array}{c} 51 \\ 56 \\ 56 \\ 4 \\ 62 \\ \% \\ 2 \\ \% \end{array}}$	68 73 ½
8	$\frac{15^{84}}{18^{36}}$	23 5% 26 % 28 7/8	$31 \frac{1}{22}$ $36 \frac{3}{24}$ 42	47 14 52 14 57 34	63 68 ¼
¥	12 14 16	18 20 22	24 32 32	36 44	48 52
Size	3 3 ½ 4	5 72	% <b>7</b> ¢	° 011	13

### CONOIDAL FAN DIMENSIONS

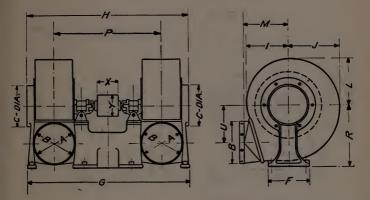
### STANDARD REVERSIBLE PLANING-MILL EXHAUST FANS (TYPE M)



### BOTTOM HORIZONTAL DISCHARGE

Size	A	в	с	F	G	н	I	J	L	M	P	R	U	x	Y
30 35 40	$   \begin{array}{r}     11 \frac{1}{2} \\     13 \frac{1}{2} \\     15 \frac{3}{8}   \end{array} $	14	14	13 3/4	35 18		13 1/8	17 3/8	15 5/8	15 1/8	15 5/8	20 3/4	$     \begin{array}{c}       11 \\       12 \frac{7}{8} \\       15     \end{array} $	4 1/2 5 1/2 6 1/2	7
45 50 55	$17\frac{3}{8}$ $19\frac{3}{8}$ $21\frac{1}{4}$	20	20	19 34	46 16	47 1/2	1934	24 34	22 1/4	21 1/4	21	$29\frac{1}{4}$	$16\frac{5}{8}$ $18\frac{1}{4}$ $20\frac{1}{8}$	81/2	10
60 70 80	$23 \frac{1}{4} \\ 27 \frac{1}{4} \\ 31 \frac{1}{4}$	28	28	24		60 1/2		34 1/2	31	28 3/4	27 1/4	39 1/4	$\begin{array}{c} 22 \frac{1}{4} \\ 25 \frac{1}{2} \\ 29 \frac{1}{2} \end{array}$	11 1/2	14

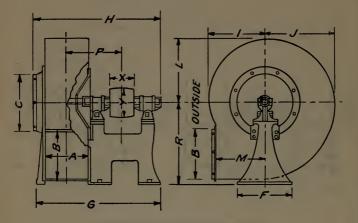
# STANDARD REVERSIBLE DOUBLE PLANING-MILL EXHAUST FANS (TYPE M)



### BOTTOM HORIZONTAL DISCHARGE

Size	A	B	c	F	G	н	1	J	L	M	Р	R	U	x	Y
35 -		14	14	12133⁄4153⁄4	53 1/4			17 3/8		$15\frac{1}{8}$	$31\frac{1}{8}$ $34\frac{1}{2}$ $38\frac{1}{4}$	20 3/4	$     \begin{array}{c}       11 \\       12 \frac{7}{8} \\       15     \end{array}   $	$6\frac{1}{2}$ $7\frac{1}{2}$ $8\frac{1}{2}$	6 7 8
50	193/8	20	20	$17\frac{1}{2}$ $19\frac{3}{4}$ $21\frac{1}{4}$	71 34	70 1/2	19 34	24 3/4	22 1/4	21 1/4	$\begin{array}{r} 42 \frac{1}{4} \\ 46 \frac{1}{2} \\ 49 \frac{7}{8} \end{array}$	29 1/4	$18\frac{1}{4}$	9½ 10½ 11½	10 12 13
60 70 80	23 ¼ 27 ¼ 37 ¼	28	28	24	$83\frac{1}{4}\\93\frac{3}{4}\\101\frac{3}{4}$	91 1/2	27 1/2	34 1/2	31	28 3/4	$54\frac{1}{2}\\60\frac{1}{2}\\65\frac{1}{2}$	39 1/4		14	$14 \\ 16 \\ 20$

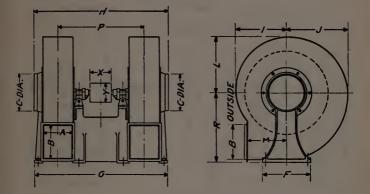
# SLOW SPEED REVERSIBLE PLANING-MILL EXHAUST FANS (TYPE E)



### BOTTOM HORIZONTAL DISCHARGE

Size	A	B	c	F	G	н	I	J	L	M	Р	R	x	Y
30 35 40	111/2	13 5/8	$     \begin{array}{r} 12 \frac{1}{2} \\     14 \frac{5}{8} \\     16 \frac{5}{8}   \end{array} $	1334	$31\frac{1}{4}$ $35\frac{1}{4}$ $38\frac{3}{4}$	40 3/1	19 1/8	23 %	21 1/2	$     \begin{array}{r} 12 \frac{1}{2} \\     14 \frac{1}{4} \\     16 \frac{1}{4}     \end{array} $	15 1/8	23 ³ / ₈ 27 ¹ / ₄ 30 ⁵ / ₈	6	8 9 10
45 50 55	16 5/8	19 1/4	20 5%	$   \begin{array}{r} 17 \frac{1}{2} \\     19 \frac{3}{4} \\     21 \frac{1}{4} \\   \end{array} $	45 1/2	58 14	27 3/8	34 1/8	$   \begin{array}{r}     27 \frac{1}{2} \\     30 \frac{3}{4} \\     33 \frac{5}{8}   \end{array} $	19 1/2	20 3/8	$     \begin{array}{r}       34 \frac{1}{2} \\       38 \frac{1}{2} \\       41 \frac{7}{8}     \end{array} $		$     \begin{array}{c}       11 \\       12 \\       13     \end{array}   $
60 70 80	23	27	$24\frac{3}{4}$ $28\frac{3}{4}$ $32\frac{3}{4}$	24	51 ⁷ / ₈ 60 ³ / ₈ 66 ⁵ / ₈		38 1/8	42 34	$36\frac{3}{4}$ $42\frac{3}{4}$ 49	27 34	26 1/4	$\begin{array}{r} 45\frac{3}{4} \\ 53\frac{1}{2} \\ 61\frac{1}{4} \end{array}$	$\begin{array}{c}11\\12\\14\end{array}$	14 16 20

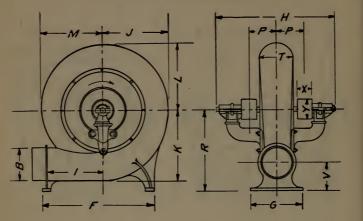
# DOUBLE SLOW SPEED REVERSIBLE PLANING-MILL EXHAUST FANS (TYPE E)



## BOTTOM HORIZONTAL DISCHARGE

Size	A	В	c	F	G	н	1	J	L	M	Р	R	x	Y
30 35 40		13 5/8	$12\frac{1}{2}$ $14\frac{5}{8}$ $16\frac{5}{8}$	13 3/4	$46\frac{3}{4}$ 50 $\frac{1}{2}$ 58	52 1/2		23 7/8	18 ³ / ₈ 21 ¹ / ₂ 24 ³ / ₈	14 1/4	$32\frac{3}{4}$	27 14	81/2	9
45 50 55	14 5/8 16 5/8 18 1/8	1914		19 34	69 1/4	71 34	27 3/8	34 1/8	$27\frac{1}{2}$ $30\frac{3}{4}$ $33\frac{5}{8}$	19 1/2		$38\frac{1}{2}$		13
60 70 80	23	27	$24\frac{3}{4}$ $28\frac{3}{4}$ $32\frac{3}{4}$	24	$81\frac{3}{4}\\93\frac{1}{4}\\107$	98 14		47 3/8	$36\frac{3}{4}$ $42\frac{3}{4}$ 49	27 34		53 1/2	18	$16 \\ 20 \\ 24$

# STEEL PRESSURE BLOWERS (TYPE P)



### BOTTOM HORIZONTAL DISCHARGE

No.	В	F	G	Н	I	J	К	L	M	Р	R	Т	v	x	Y
1 2 3	4	$8\frac{3}{4}$ 10 15	71/4	$     \begin{array}{r}       14 \frac{1}{4} \\       19 \frac{1}{2} \\       23     \end{array}   $		6 3/8		5 16	6	334	67.8 916 10,4	3 16	3 18		23/8 27 3 1/4
4 5 6	5 %	18%	1334	24 1/2	11	11 2	12 3	11 1/2	911 1011 1116	41/2	$   \begin{array}{r} 13 \frac{1}{2} \\     14 \frac{1}{4} \\     16 \frac{5}{8} \\   \end{array} $	4%	434	31/4	$3\frac{3}{4}$ 4 4 $1\frac{1}{2}$
7 8 9	8 16	29 5/8	17 1/2	40	15 1/4	173/8	18 14	16 %	$13\frac{5}{8}$ $15\frac{1}{8}$ $17\frac{1}{2}$	85%	19 21 ⁷ / ₈ 24 ³ / ₄	5 % 7 ½ 9	814	4 3/4	5 6¼ 7¼
11	14 3/8		23 1/4	50	23 1/2	30 %	32 1/4	29 1/8	$\begin{array}{c} 22 \frac{1}{2} \\ 27 \frac{3}{8} \\ 32 \frac{1}{5} \end{array}$	11 1/8	36	11 1/4	11	6 3/8	81/2
12	18	57 34	26 ½	53 ¼	28 ¼	35 1/8	37 3⁄8	34	32 <del>}⁄</del> 8	12 1/4	41 ¼	13 ½	121/4	9 1/8	10

# SECTION V

### HEATERS

The heaters used in connection with fan systems of heating are usually some form of pipe coil heater like the Buffalo heater or of cast iron like the Vento heater. Either style is made up in sections or units in the direction of the air flow, which makes it possible to assemble a heater of any desired depth. The general arrangement would be the same for either kind of heater, each being enclosed in a sheet-iron case or jacket.

### **Buffalo Heaters**

The Buffalo Standard Pipe Coil Heater is usually one of two styles, the regular open area pattern (usually written R. O. A. pattern) or the return bend pattern (R. B. pattern). The cuts on page 400 show clearly the difference. Both are made of oneinch full weight steel pipe screwed into a cast-iron base, the pipes being spaced on 25%-inch centers. These sections are ordinarily made four rows deep, and are called four-row sections. Detailed dimensions of these heaters will be found on page 451, of the piping connections on pages 452 to 455, and of the sheet-iron casing on page 456. Other special forms of pipe coil heater are also made, such as the mitre coil shown on page 400, or the indirect heater shown on page 459.

These heaters are usually connected up to steam and drip headers, with separate connections running to each section. In case it may be required to shut off part of the sections during mild weather, both the steam and drip connections to each section are fitted with a valve. Each section should always be fitted with an air vent which should always be thoroughly blown out on turning steam into a section.

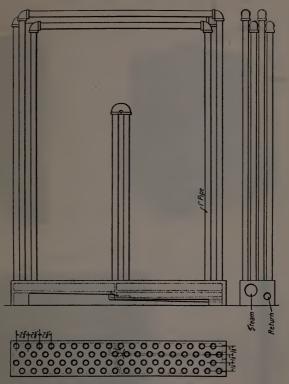
### FAN ENGINEERING-BUFFALO FORGE COMPANY



Buffalo Regular Open Area Pattern Heater Buffalo Return Bend Heater

0000

Buffalo Four-Row Open Area Pattern Section Buffalo Miter Coil Heater Without Casing or Connections

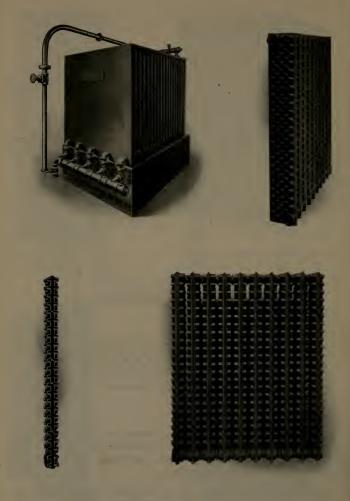


**Detail of Buffalo Heater Construction** 

### Vento Heaters

The Vento cast iron heater, an illustration of which is shown on page 402, is designed specially for use in fan and blower work. The tables and data herein given concerning this heater are taken from the catalog of the makers.

These heaters are made in two standard sizes, called the Regular and the Narrow section, and ordinarily either 40, 50 or 60 inches high. The sections may be so mounted as to make a heater of any desired size.



Vento Heaters

Heat Transfer through Metal Surfaces with Forced Circulation

The transfer of heat through metallic tubes, such as a pipe coil heater, from gases and liquids to gases and liquids may be considered of the same nature as already explained for building material in Part II, Section I. That is, there exist three separate operations—the transfer from the warmer fluid to the initial surface of the tube; the heat passage through the tube wall, and the transfer from the secondary tube wall to the cooler fluid. The amount of heat transmitted will depend on the existing conditions such as the nature of the gas or liquid, the arrangement of the surface, the velocity over the heating surface, or to some special conditions.

The total amount of heat transfer per square foot of surface in a given time will depend on the rate of transmission, upon the temperature difference between the two sides of the surface, and to a certain degree upon the absolute temperatures considered. That is, the total heat transmitted per square foot of surface per hour will be

$$\mathbf{H} = \mathbf{K}(\mathbf{t}_{\mathrm{s}} - \mathbf{t})_{\mathrm{m}} \tag{95}$$

where

- H = total heat transfer in B. t. u. per hour.
- K=B. t. u. transmitted per sq. ft. per hour per deg. temp. diff.
- $(t_s-t)_m$  = mean temp. diff. between the two sides of the surface.

As may be shown the rate of heat conduction between steam and water is approximately, as indicated by the diagram on page 404, based on data obtained from condenser tests. This gives the rate of conductivity from steam to water as

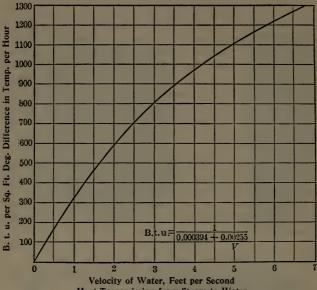
$$\mathbf{K} = \frac{1}{0.000394 + \frac{0.00255}{V}} \tag{96}$$

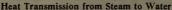
where

K = B. t. u. per hour per sq. ft. per deg. temp. diff. V = velocity in ft. per second.

Condensing coils give a much more rapid rate of conductivity per degree difference in temperature than steam coils, owing to the additional effect of condensation.

The rate of transmission from steam to air under conditions of longitudinal flow, based on a scries of tests made by the engineering department of the Buffalo Forge Company, is indicated





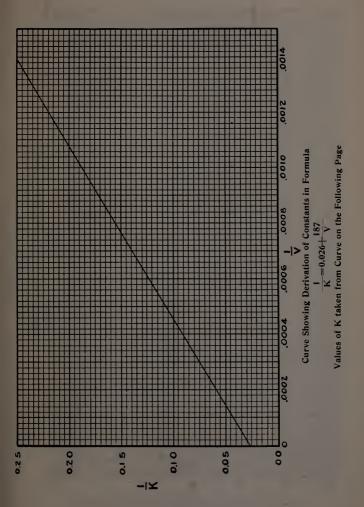
by the diagram on page 406. These tests were conducted on a boiler tube surrounded by steam, and with the air blown through the tube at different velocities. The coefficient of transmission for this condition may be determined from the formula

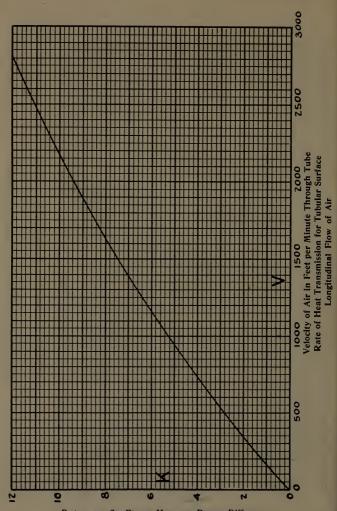
$$K = \frac{1}{0.026 + \frac{187}{V}}$$
(97)

The method of deriving this formula, as well as the one given on page 407 for transverse flow, may be explained by a reference to the diagram on page 405, where the values of  $\frac{1}{K}$  and  $\frac{1}{V}$  as obtained from the curve drawn through the plotted test points (page 406) are plotted and a straight line drawn through them. The equation of this line is found to be

$$\frac{1}{K} = 0.026 + \frac{187}{V} \tag{98}$$

from which we obtain the above equation for K.



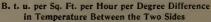


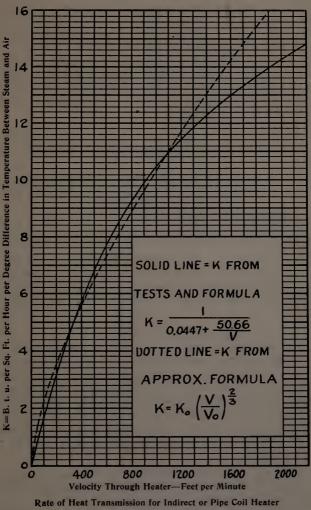
ENGINEERING --- BUFFALO

FAN

FORGE

COMPANY





Transverse Flow of Air

The theory of heat transfer with forced circulation under conditions of transverse flow has been fully discussed in the paper 'Air Conditioning Apparatus''* already referred to, in which the coefficient of heat transmission from steam to air with indirect or fan system pipe coil heaters is shown to be as indicated by the solid line of the diagram on page 407. This curve is based on tests made with a Buffalo Forge Company standard pipe coil heater composed of one-inch pipes placed on  $2\frac{5}{6}$ -inch centers. The coefficient K for transverse flow as determined from the data obtained may be expressed as

$$K = \frac{1}{0.0447 + \frac{50.66}{V}}$$
(99)

where

K=B. t. u. per hour per sq. ft. per deg. temp. diff.V=the velocity of the air through the clear area of the heater in ft. per minute.

This formula was derived by plotting  $\frac{1}{K}$  to  $\frac{1}{V}$  in a similar manner to that already explained in the case of longitudinal flow.

As already shown, the total heat transmission is dependent on the rate of transmission K, and upon the difference in temperature between the two sides of the conducting wall or surface. That is

$$\mathbf{H} = \mathbf{K} \ (\mathbf{t}_{\mathbf{s}} - \mathbf{t})_{\mathbf{m}} \tag{100}$$

It is frequently stated that the rate of transmission under the above conditions varies as the square root of the velocity, but as a matter of fact, over the range of velocities ordinarily used in fan system heaters, the transmission varies approximately as the two-thirds power of the velocity. This is shown by the dotted curve in the diagram on page 407, which is plotted from the formula as given. Thus we see that up to a velocity of 1200 feet per minute there is but slight error in assuming the above relations.

The mean temperature difference between the two sides of the surface of a heater as expressed in this formula may be determined from the formula

^{*&}quot;Air Conditioning Apparatus," by Willis H. Carrier and Frank L. Busey, Am. Soc. Mech. Engrs., 1911.

$$(t_{s}-t)_{m} = \frac{(t_{s}-t_{1}) - (t_{s}-t_{2})}{\log_{e}\left(\frac{t_{s}-t_{1}}{t_{s}-t_{2}}\right)}$$
(101)

where

 $t_s = temperature of the steam.$ 

 $t_1 = temperature of the entering air.$ 

- $t_2 = temperature of the leaving air.$
- $t_s t_1 =$ entering temp. diff. between the steam and the air.
- $t_{s}-t_{2}=leaving$  temp. diff. between the steam and the air.

Coefficient of transmission may be found approximately from the formula

$$K = \frac{C_p G}{S} \log_e \left( \frac{t_s - t_1}{t_s - t_2} \right)$$
(102)

### where

 ${\rm K}\,{=}\,{\rm B.}$  t. u. per sq. ft. per hour per deg. temp. diff.  ${\rm C}_{\rm p}\,{=}\,{\rm specific}$  heat of air.

- G = weight of air in lbs. per hour passed through the heater.
- S = total sq. ft. of heating surface.

The amount of heating surface in square feet required may be calculated approximately from the formula

$$S = (0.1119 \text{ Q} + 127 \text{ A}) \log_{10} \left( \frac{t_s - t_1}{t_s - t_2} \right)$$
(103)

and the temperature rise from

$$\log_{10}\left(\frac{t_{s}-t_{1}}{t_{s}-t_{2}}\right) = \frac{f}{0.1119 \,V + 127} \tag{104}$$

where

S = sq. ft. of heating surface.

A = clear area of heater.

f = ratio total surface to clear area.

Q = cu. ft. of air at 70° F.

- V = velocity of the air through the clear area (at 70° F.) in ft. per min.
  - $t_s = steam$  temperature.

 $t_1 = entering air temperature.$ 

 $t_2 = final air temperature.$ 

The derivation of the above formulae may be found in the papers on "Air Conditioning Apparatus" referred to on page 408, and the results obtained, while only approximate, will be found sufficiently accurate for calculations based on the temperatures obtained in heating work with exhaust or low pressure steam. Since the transmission varies slightly with different steam temperatures, for accurate work or for higher steam temperatures it will be found necessary to use the following formula. This is the formula used in the calculation of the heater tables and curves included on pages 418 to 438.

$$f = \left[ (0.0001791 \text{ V T}_{s} + 126.8) \log_{10} \left( \frac{t_{s} - t_{1}}{t_{s} - t_{2}} \right) - \frac{0.000003474 \text{ V}^{2} (t_{s} - t_{1})}{0.0447 \text{ V} + 50.66} \right]$$
(105)

where  $T_s$  = the absolute temperature of the steam.

This same theory of heat transmission has been applied to the Vento Cast Iron Heaters * and the following formula derived as an expression of the coefficient of transmission.

$$K = \frac{1}{0.47 + \frac{61.00}{V}}$$
(106)

While this investigation shows that at the same velocity the heat transmission from pipe coil heaters is greater than from Vento heaters, the frictional resistance is correspondingly greater. But it was also shown that with the same effective velocity, or with the same frictional loss, the rate of transmission was practically the same for the two types of heater.

A further study has been made between pipe coil heaters having one inch pipes on  $2\frac{34}{4}$ -inch centers and the Vento Cast Iron Heaters by L. C. Soule.[†] In discussing the results of his tests the author states: "These results show that former temperature charts published for pipe coils having  $2\frac{34}{4}$ -inch centers of pipes read much too high and are, therefore, unsafe to use. These results agree with both the Vento tests and the Buffalo Forge Company tests and by their consistency show their entire reliability." These tests further show that for the same friction the Vento requires 35 per cent. greater velocity than the pipe coil heater on  $2\frac{34}{4}$ -inch center, but with the same friction loss the heat transmission was practically the same.

^{* &}quot;Heat Transmission with Indirect Radiation," by Frank L. Busey, Am. Soc. H. and V. Engrs., 1912.

^{†&}quot;Heat Transmission with Pipe Coils and Cast Iron Heaters under Fan Blast Conditions," Am. Soc. H. and V. Engrs., July, 1913.

### **Temperatures Attained with Indirect Heaters**

While it is true that the total rise in temperature will be greater with a greater depth of heater it is also evident that after air has passed over the first few rows of coils it approaches more nearly the temperature of the steam in the coils, hence the rate of transmission is very much less, and added surface is not of proportionate value. For this reason it is seldom advisable, in heating work, to attempt to raise the temperature of the air above 135° or 140°. For special work such as drying, where higher temperatures are required, it is customary to use high pressure steam in the coils.

In case the system is used for ventilation only, and the heat loss is cared for by direct radiation, the temperature of the air leaving the heater should be from  $10^{\circ}$  to  $15^{\circ}$  above that of the room, depending on the drop of temperature in the ducts between the heater and outlets. The temperature of the air leaving the outlet should be within a few degrees of that of the room.

The ratio of the temperature difference between the steam and leaving air to the temperature difference between the steam and entering air is approximately constant for a given depth of heater and a given air velocity through the clear area. That is

$$\frac{t_s - t_2}{t_s - t_1} =$$
approximately a constant.

### **Condensation** in Coils

The weight of steam condensed in the heating coils may be determined either from the B. t. u. as given in the heater tables, or from the cubic feet of air handled and the temperature rise. The heater tables give the B. t. u. per hour per lineal foot of pipe for any given conditions. This, multiplied by the total number of lineal feet in the heater and divided by the latent heat of the steam at the pressure used will give the condensation in pounds per hour.

The weight of steam condensed per hour may also be found by means of the formula

 $C = \frac{Cu. \text{ ft. air per min.} \times \text{temp. rise} \times 60}{Cu. \text{ ft. air per deg. per B. t. u.} \times \text{ latent heat of steam}}$ 

For ordinary conditions with dry air at  $70^{\circ}$  F., it has been shown on page 56 that one B. t. u. will raise the temperature of 55.2 cu. ft. of air one degree, hence we have

$$C = \frac{Q \times (t_2 - t_1) \times 60}{55.2 L} = 1.087 \frac{Q (t_2 - t_1)}{L}$$
(107)

where

C=lbs. of steam per hour.

Q = cu. ft. air per min.

 $t_1 = temperature air entering heater.$ 

 $t_2 = temperature air leaving heater.$ 

L=latent heat of steam (=960.6 at 5 lbs. press.)

### Velocity of Air Through Heaters

The proper velocity for the air through the clear area of the heater will vary with the different conditions such as pressure carried and character of the installation. The following table of velocities is based on the assumption that the pressure loss through the heater should not exceed 50 per cent. of the total pressure on the fan.

MAXIMUM ALLOWABLE VELOCITIES OF AIR THROUGH CLEAR AREA OF HEATER FOR VARIOUS FAN PRESSURES AND FOR VARIOUS DEPTHS OF HEATER

			Jai Fair Fi	cssure m i	nenes		
No. of Sect. Deep	3⁄4	1	11/4	1 1/2	134	2	21/2
4 5 6 7 8	990 885 810 745 700	1140 1020 930 860 810	1280 1140 1040 960 910	1400 1250 1140 1055 995	1510 1350 1230 1140 1070	$     \begin{array}{r}       1610 \\       1440 \\       1320 \\       1220 \\       1150     \end{array} $	1800 1610 1470 1360 1280

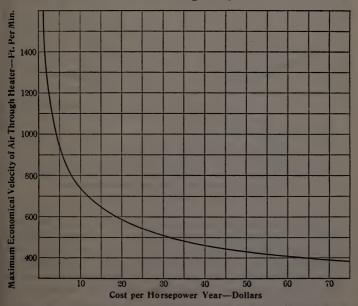
**Total Fan Pressure in Inches** 

The velocities here given are intended merely to indicate the practical limit, and except where the ducts are very short it will be found advisable to keep below this. This is especially true in the case of public buildings, where the limit should not exceed 90 per cent. of the above. The table on page 413 gives the maximum velocities advisable both for public buildings and for industrial plants for the different depths of heater indicated. These are based on the average pressures usually carried in such installations.

### MAXIMUM VELOCITY ADVISABLE THROUGH HEATER FOR DIFFERENT INSTALLATIONS

Depth of Heater in Sections	In Public Buildings	In Industrial Plants
4	1140	1500
5	1020	1350
6	930	1230
7	860	1140
8	810	1070

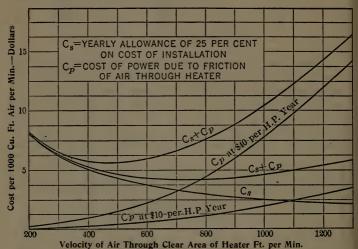
The subject of velocity of air through the heater with reference to the cost of power has been discussed in a paper* presented before the A. S. H. & V. Engineers, two of the curves and



Maximum Economical Velocity for Different Costs of Power Allowing 25 Per Cent. on Cost of Heater for Interest and Depreciation, Space, Rental, Etc.

^{*&}quot;The design of Indirect Heating Systems with Respect to Maximum Economy of Maintenance and Operation." Am. Soc. H. & V. Engrs., Jan., 1913, by F. L. Busey and W. H. Carrier.

some of the more important deductions being here reproduced. These diagrams are drawn on the assumption that an allowance of 25 per cent. on the cost of the heater be made to cover interest, depreciation, space, rental, etc. The curve shown on page 413 indicates the maximum velocity allowable under the above assumption for various costs of power.



Relative Yearly Interest and Depreciation Cost of Surface and Power Cost Due to Friction of Air Through Heater at Various Velocities Through the Clear Area, Allowing 25 Per Cent. on Cost of Heater for Interest and Depreciation

The above diagram shows the cost for power and the cost allowance for interest and depreciation at different velocities through the heaters. Two power cost curves are shown, one at \$10.00 and one at \$40.00 per H. P. year. The combined curves show the total cost, and the low points on these curves indicate the maximum economical velocity for the respective costs of power.

It was shown that the cost of surface varies as the two-thirds power and the cost of power as the seven-thirds power of the velocity. Also that the maximum economical velocity is equal to 0.66 times the assumed velocity multiplied by the ratio of the yearly cost allowed for interest and depreciation to the yearly cost of power, to the one-third power. The following deduction was then made regarding the velocity through the heater.

"As regards the heater, the most economical point will be reached when the installation is so proportioned that the yearly cost of power due to the frictional resistance of the heater amounts to 28.6 per cent. of the annual interest and depreciation allowance on the first cost of the heater. This is true regardless of variations in the depth of heater, temperature rise or steam pressure."

## Application of the Heater Tables and Curves

Two sets of heater tables will be found on the following pages, one to be used in connection with Buffalo Standard Heaters and the other with Vento Cast Iron Heaters. The methods here described for the use of the Buffalo heater tables are equally applicable to the Vento tables. The values given for the Buffalo heaters are based on data obtained by W. H. Carrier from an extensive series of tests made for the Buffalo Forge Company. The method of making these tests and of working up the data therefrom has been fully described in the paper* "Air Conditioning Apparatus" already referred to. Large diagrams similar to the charts on pages 432 to 438 were drawn and the values for the heater tables determined.

The heater tables on pages 418 to 431 are computed for various steam pressures and give the final temperature of the air and the B. t. u. transmitted per lineal foot of pipe per hour for different entering temperatures and velocities of the entering air. These results are given for different depths of heater, varying from one to eight four-row sections.

The curves showing the relation between the heater surface and air temperature are useful for obtaining the final temperatures when the entering temperature or velocity is different from that given in the tables. As an example, we will assume a steam pressure of five pounds, an entering temperature of plus  $20^{\circ}$ , a velocity of 1000 feet per minute through the clear area of the heater which is five sections deep. Starting from the left side of the diagram at  $20^{\circ}$ , follow to the right to the intersection of the 1000 velocity curve, and then downward to the base line at 2.05 sections: adding to this the five sections which we have

^{*&}quot;Air Conditioning Apparatus," by W. H. Carrier and F. L. Busey, Am. Soc. Mech. Engrs., Dec., 1911.

assumed for the depth of the heater gives 2.05+5.00=7.05 sections. Passing upward from the point 7.05 to the 1000 velocity curve and then to the left side of the chart again gives a final or leaving temperature of 113°.

In case the entering and leaving temperatures are assumed to be 0° and 140° respectively, the steam pressure five pounds, and the velocity 800 feet per minute determine how many sections of heater will be required. Passing from the left side of the diagram at 0° to the intersection of the 800 velocity curve and then downward to the base line we find a point of 1.2 sections. In the same way from the 140° point we intersect the base line at 8.6 sections. Then the difference, or 8.6 - 1.2 = 7.4sections, will be the number of 4 row sections or seven 4 row and one 2 row sections, making 30 rows of pipe deep.

The lower graduations on the base line are for use with other than the Buffalo Standard Heaters, where the value of the ratio f is known. In the case of the Buffalo Standard Heater, the value of f for a single four-row section is 12.335. That is, there are 12.335 sq. ft. of heating surface in each section to each square foot of clear area. But in the case of other than the standard heater where the pipes are on different centers the value of **f** will be different. As an example we will assume that on measuring up the surface in a pipe coil heater it is found that the total square feet of surface is 1000 and the clear area for the passage of air is 25 sq. ft. This gives a ratio of surface to clear area of f = 40. Assuming the air enters the heater at 15° above zero with a velocity of 900 ft. per minute find from the diagram on page 433 for five pound pressure what will be the final temperature of this air. Passing from 15° on the left edge of the chart to half way between the 800 and 1000 velocity curves and then to the bottom line, we find a value of f = 20. Adding to this the value of **f** as found from the heater measurements, gives a total of f = 20 + 40 = 60. Passing vertically from f = 60 on the bottom scale to a point corresponding to 900 velocity and thence to the left edge of the diagram gives a final air temperature of 83°.

These curves may be used in connection with any heater when the ratio of surface to clear area is known. In the case of pipe coil heaters composed of one inch pipes the value of f per row of pipes deep is a fixed quantity for each distance between centers of the pipes in the heater. The values of f for different spacings are given in the following table for heaters one row deep. From this we may see that with the standard Buffalo heater having centers of  $2\frac{5}{3}$  inches the value of f per single row of pipes is 3.084 and for a four-row section f is 12.335.

VALUES	OF	f	PER	SING	LE	ROW	0F	PIPE
	ON	DI	FFER	RENT	CE	NTER	S	

C=Pipe Centers in Inches Spacing of 1" Steel Pipe	$f = \frac{S_1}{A}$ Per Row of 1" Pipe
2 14 2 14 2 14 2 14 2 14 2 14 2 14	$\begin{array}{c} 6.164 \\ 5.041 \\ 4.214 \\ 3.581 \\ 3.084 \\ 2.688 \end{array}$

The scale at the top of the diagrams applies to Vento regular sections on five-inch centers, and is used in the same manner as explained for the standard Buffalo pipe coil heaters.



Planoidal (Type L) Fan Drawing Through Heater

Ibs.		0	B. t. u. per Lin. Ft. per Hour	1015 955 895 852 852 807 767 731 697	959 902 856 811 772 697 665	913 860 815 774 776 699 656 635
•		1400	Final Temp.	$\begin{array}{c} 3.9\\ 25.0\\ 43.5\\ 60.3\\ 75.0\\ 88.4\\ 110.5\\ 111.3\end{array}$	$12.6 \\ 52.5 \\ 50.5 \\ 66.4 \\ 80.9 \\ 93.8 \\ 105.0 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 115.4 \\ 11$	21.5 40.5 57.6 72.9 86.7 98.8 109.8 119.6
	-	1200	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 925\\ 870\\ 819\\ 771\\ 731\\ 692\\ 657\\ 625\end{array}$	874 826 776 733 698 661 627 596	835 788 742 700 667 597 597 568
TERS	saromete	12	Final Temp.	$\begin{array}{c} 5.5\\ 27.8\\ 47.5\\ 64.8\\ 80.4\\ 94.1\\ 106.4\\ 117.4\end{array}$	$\begin{array}{c} 14.1\\ 35.4\\ 54.0\\ 70.6\\ 85.9\\ 99.0\\ 110.6\\ 121.0\end{array}$	$\begin{array}{c} 23.0\\ 43.3\\ 61.2\\ 77.0\\ 91.6\\ 104.0\\ 114.9\\ 124.9\end{array}$
STANDARD HEATERS EMP. 212° F.	29.92 Inches Barometer	000	B. t. u. per Lin. Ft. Per Hour	834 778 727 683 645 609 577 546	797 738 652 617 552 522	755 700 661 681 586 554 498
D STANDARI TEMP. 212°	1d 29.92	10	Final Temp.	$\begin{array}{c} 7.5\\ 31.3\\ 51.9\\ 70.1\\ 86.3\\ 100.5\\ 113.1\\ 124.1\end{array}$	$\begin{array}{c} 16.3\\ 38.7\\ 58.7\\ 58.7\\ 76.0\\ 91.7\\ 105.1\\ 116.9\\ 127.8 \end{array}$	$\begin{array}{c} 24.9\\ 46.2\\ 65.4\\ 82.0\\ 96.7\\ 109.7\\ 131.5\\ 131.5\end{array}$
BUFFALO STEAM TE	at 70° F. and	800	B. t. u. per Lin. Ft. Per Hour	720 670 625 584 584 517 487 460	682 636 594 557 557 554 494 466 440	655 607 567 567 567 561 471 471 471 471 420
WITH BUI 0 LBS., ST		80	Final Temp.	$\begin{array}{c} 9.7\\ 35.2\\ 57.3\\ 76.3\\ 76.3\\ 93.2\\ 108.0\\ 120.6\\ 131.8\end{array}$	$\begin{array}{c} 18.1 \\ 42.4 \\ 63.5 \\ 81.9 \\ 98.0 \\ 112.1 \\ 124.4 \\ 135.0 \end{array}$	$\begin{array}{c} 27.0\\ 50.0\\ 70.1\\ 87.6\\ 103.2\\ 116.5\\ 138.4\\ 138.4\end{array}$
	in., Mea	0	B. t. u. per Lin. Ft. Per Hour	590 544 504 471 441 413 388 385 365	$\begin{array}{c} 559 \\ 556 \\ 556 \\ 450 \\ 450 \\ 395 \\ 371 \\ 349 \\ 349 \end{array}$	535 491 460 429 403 377 354 333
DBTAINED PRESSURE	Ft. per Min., Measured	600	Final Temp.	$\begin{array}{c} 12.4\\ 12.4\\ 39.8\\ 63.1\\ 83.6\\ 101.1\\ 116.3\\ 129.3\\ 129.3\\ 140.4\end{array}$	$\begin{array}{c} 20.7\\ 46.7\\ 69.5\\ 69.5\\ 88.9\\ 105.7\\ 120.1\\ 132.8\\ 143.4\end{array}$	29.4 54.0 754.0 94.3 110.6 124.3 136.3 146.2
remperature gauge	f Air in l	400	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 436\\ 399\\ 368\\ 342\\ 318\\ 295\\ 275\\ 228\\ 258\\ 258\\ 258\\ 258\\ 258\\ 258\\ 25$	418 352 352 326 326 282 282 282 263 247	400 364 336 336 230 252 252 252 252 236
TEMPEI	Velocity of Air in	4(	Final Temp.	$16.0 \\ 45.8 \\ 71.1 \\ 92.6 \\ 110.9 \\ 138.9 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ 150.2 \\ $	24.5 52.9 77.0 97.6 115.0 129.6 142.0 152.8	33.0 60.0 83.0 1192.8 1192.8 1133.2 155.5
	>	200	B. t. u. Per Lin. Ft. Per Hour	246 222 204 187 172 159 148 137	233 212 194 179 165 165 141 131	224 203 171 171 146 135 135 126
			Final Temp.	20.6 53.3 53.3 80.9 103.4 137.7 150.7 161.3	28.4 59.8 86.1 108.0 140.6 153.2 163.3	36.9 66.8 91.8 112.8 112.8 112.9 1440.0 155.5
		ater S	No. of He Section	-00450000	-01004001-00	-004506-00
		f Air	Temp. o Entering	-20°	01-	00

FAN ENGINEERING-BUFFALO FORGE COMPANY

0 lbs.

TEMPERATURE OBTAINED WITH BUFFALO STANDARD HEATERS **DAUGE PRESSURE 0 LBS., STEAM TEMP, 212° F.** 

1400	B. t. u. per Lin. Ft. Per Hour	853 809 771 734 697 662 662 662 662 602	807 768 732 696 661 629 600 571	637 637 572 543 543 543 543 468 468 4492 4492
	Final Temp.	30.1 48.1 64.5 79.2 92.1 103.6 114.2 123.5	$\begin{array}{c} 39.0\\ 56.2\\ 71.7\\ 71.7\\ 85.6\\ 97.8\\ 108.9\\ 118.9\\ 118.9\end{array}$	$\begin{array}{c} 75.0\\ 88.5\\ 100.4\\ 111.2\\ 121.0\\ 129.6\\ 137.2\\ 144.4\end{array}$
Barometer	B. t. u. Ber Lin. Ft. Per Hour	787 746 704 665 632 539 568 568 568 540	740 704 665 632 598 539 512 512	581 555 555 555 522 493 467 445 404 404
nches Ba	Final Temp.	$\begin{array}{c} 31.7\\ 51.0\\ 51.0\\ 68.0\\ 83.1\\ 96.9\\ 108.7\\ 119.2\\ 128.8\end{array}$	$\begin{array}{c} 40.4\\ 58.7\\ 74.8\\ 89.5\\ 89.5\\ 102.1\\ 113.4\\ 123.7\\ 132.6\end{array}$	$\begin{array}{c} 76.0\\ 76.0\\ 103.0\\ 114.2\\ 124.2\\ 133.3\\ 141.3\\ 148.8\\ 148.8\end{array}$
and 29.92 Inches Barometer	B. t. u. Per Lin. Ft. Per Hour	709 661 591 558 558 558 498 473	667 667 592 559 559 528 528 528 528 528 528 528 528 528 528	522 496 438 415 415 373 373 373
70° F. and	Final Temp.	$\begin{array}{c} 33.4\\ 53.6\\ 71.8\\ 87.9\\ 102.0\\ 114.0\\ 125.0\\ 134.9\end{array}$	$\begin{array}{c} 42.0\\ 61.4\\ 78.6\\ 93.8\\ 107.0\\ 118.8\\ 129.4\\ 138.7\end{array}$	$\begin{array}{c} 77.2\\92.7\\106.0\\117.8\\128.5\\138.5\\138.5\\138.6\\146.1\\153.4\end{array}$
at	B. t. u. Per Lin. Ft. Per Hour	616 575 539 539 506 476 448 448 423 399	582 546 510 480 451 451 401 379	458 428 403 377 356 3356 317 300 317 300
Ft. per Min., Measured	Final Temp.	$\begin{array}{c} 35.4\\ 57.4\\ 56.7\\ 76.7\\ 93.4\\ 108.1\\ 120.9\\ 132.0\\ 141.7\end{array}$	$\begin{array}{c} 44.0\\ 65.0\\ 83.1\\ 99.1\\ 113.0\\ 125.2\\ 135.8\\ 135.8\\ 144.9\end{array}$	$\begin{array}{c} 78.9\\ 95.3\\ 95.3\\ 1095.3\\ 1222.1\\ 133.4\\ 153.4\\ 158.8\\ 158.8\end{array}$
t. per Min	B. t. u. per Lin. Ft. Per Hour	504 504 437 437 437 409 332 337 337 317	$\begin{array}{c} 473 \\ 446 \\ 414 \\ 388 \\ 364 \\ 364 \\ 341 \\ 320 \\ 301 \end{array}$	378 352 329 329 329 252 252 252 252 252 252
	Final Temp.	$\begin{array}{c} 37.7\\ 61.5\\ 82.0\\ 99.9\\ 115.1\\ 128.4\\ 139.8\\ 149.3\end{array}$	$\begin{array}{c} 46.0\\ 69.0\\ 88.3\\ 105.3\\ 1195.3\\ 132.5\\ 143.1\\ 152.2\\ 152.2\end{array}$	$\begin{array}{c} 80.8\\ 98.7\\ 98.7\\ 114.2\\ 127.5\\ 1397.5\\ 1397.1\\ 148.8\\ 157.1\\ 164.7\\ 164.7\end{array}$
Velocity of Air in 400	B. t. u. per Lin. Ft. Per Hour	376 347 320 297 257 257 257 257 257 257	351 328 328 328 303 281 281 281 281 281 228 213	279 261 221 221 221 201 194 168 168
Velo 40	Final Temp.	$\begin{array}{c} 41.0\\ 67.2\\ 89.2\\ 107.9\\ 123.6\\ 136.9\\ 148.4\\ 158.1\end{array}$	$\begin{array}{c} 49.0\\74.0\\95.0\\112.8\\127.6\\140.4\\151.5\\160.7\end{array}$	83.0 103.0 119.3 133.0 145.3 155.7 164.0 171.1
200	B. t. u. per Lin. Ft. Per Hour	210 177 177 177 150 150 150 1139 119	199 183 168 155 142 132 132 114 114	158 146 133 122 113 97 89
20	Final Temp.	44.6 73.5 97.5 117.3 133.5 147.1 158.6 167.5	$\begin{array}{c} 52.8\\ 80.2\\ 80.2\\ 103.1\\ 137.3\\ 150.4\\ 161.2\\ 169.8\end{array}$	$\begin{array}{c} 86.1\\ 108.0\\ 126.0\\ 140.7\\ 153.3\\ 163.5\\ 171.4\\ 177.8\end{array}$
	No. of Hea Sections	-004001-00	-00400000	-00400000
lir Air	o. Temp. o Entering	10°	20°	¢0°

	iA 2	I emp. Entering	-20°	-100	0°
	su	No. of H Sectio	-000400000	-01004100-0	-0044000
	30	Final Temp.	$\begin{array}{c} 23.0\\ 58.0\\ 87.1\\ 1111.0\\ 131.2\\ 147.9\\ 161.5\\ 172.7\end{array}$	$\begin{array}{c} 31.1\\ 64.6\\ 64.6\\ 92.6\\ 115.4\\ 135.0\\ 151.0\\ 164.0\\ 174.7\end{array}$	39.5 71.5 98.2 120.2 138.9 154.1
	200	B. t. u. per Lin. Ft. Per Hour	261 236 236 236 236 198 183 183 169 157 146	249 226 207 190 176 163 151	239 217 198 182 168 156
Velo	4	Final Temp.	$\begin{array}{c} 17.9\\ 49.5\\ 76.5\\ 99.3\\ 118.4\\ 135.2\\ 149.0\\ 160.7\end{array}$	$\begin{array}{c} 26.0\\ 56.3\\ 56.3\\ 82.4\\ 1082.4\\ 122.7\\ 132.9\\ 152.0\\ 163.2\\ 163.2\end{array}$	34.5 63.5 88.4 109.2 127.3 142.4
/ 0f	400	B. t. u. per Lin. Ft. Per Hour	459 459 390 336 336 336 274	436 402 374 374 322 322 301 281 262	418 385 385 331 331 288 288
Air in Ft.	0	Final Temp.	$\begin{array}{c} 14.1\\ 43.1\\ 68.4\\ 90.0\\ 108.5\\ 124.6\\ 138.5\\ 150.3\end{array}$	$\begin{array}{c} 22.5\\ 50.3\\ 74.8\\ 95.4\\ 113.0\\ 128.6\\ 141.9\\ 153.3\end{array}$	31.1 58.0 81.0 81.0 117.9 132.7
in Ft. per Min., Measured	600	B. t. u. per Lin. Ft. Per Hour	620 574 575 576 500 467 412 387 387	591 553 514 479 447 420 395 371	565 527 491 428 402 402
., Measu	80	Final Temp.	$\begin{array}{c} 11.1\\ 38.0\\ 61.5\\ 61.5\\ 82.1\\ 100.0\\ 115.6\\ 129.3\\ 141.0\end{array}$	20.0 45.5 68.1 87.8 105.0 120.1 133.0 144.4	28.5 53.0 74.6 93.5 110.0
red at 70°	800	B. t. u. per Lin. Ft. Hour	754 754 659 619 582 548 517 517	728 673 631 593 558 526 495 468	691 643 603 567 534 502
Ľ.	-	Final Temp.	8.9 34.1 56.1 75.5 92.7 108.0 121.3 133.0	$\begin{array}{c} 17.7\\ 41.5\\ 62.8\\ 81.4\\ 97.9\\ 112.4\\ 125.2\\ 136.4\end{array}$	26.4 49.3 69.5 87.2 103.0
and 29.92 Inches Barometer	000	B. t. u. per Lin. Ft. Per Hour	876 820 724 683 647 612 612 580	839 839 736 653 654 618 555 555	800 747 702 661 624 591
iches Ba		Final Temp.	$6.9\\51.1\\51.1\\69.8\\66.1\\100.8\\114.0\\125.7$	$15.3 \\ 37.8 \\ 57.8 \\ 75.5 \\ 91.4 \\ 105.7 \\ 118.3 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 129.5 \\ 1$	$\begin{array}{c} 24.2\\ 45.6\\ 65.0\\ 81.8\\ 97.0\\ 110.6\end{array}$
rometer	1200	B. t. u. per Lin. Ft. Hour	976 913 862 817 772 732 696 662	918 869 822 778 778 701 667 634	878 829 744 706 670
	4	Final Temp.	$\begin{array}{c} 5.1\\ 27.2\\ 46.9\\ 64.6\\ 80.6\\ 94.9\\ 107.8\\ 119.1\end{array}$	$13.8 \\ 34.9 \\ 53.9 \\ 70.9 \\ 86.1 \\ 99.9 \\ 112.3 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 123.0 \\ 12$	22.6 42.9 61.0 77.2 91.9
	1400	B. t. u. per Lin. Ft Per Hour	1065 1001 946 898 854 813 775 738	1010 953 964 858 816 777 741 741 705	959 910 863 819 7480 7480

FAN ENGINEERING-BUFFALO FORGE COMPANY

I

B. t. u. Lin. Ft. Per Hour 913 868 821 782 7745 7745 674 643 400 Final Temp. 31.5 50.9 68.0 83.7 97.7 97.7 110.1 110.1 131.1 Lin. Ft. B. t. 1 Per 838 791 7710 7710 574 540 508 508 578 1200 and 29.92 Inches Barometer Final Temp. 33.1 53.5 71.9 88.0 88.0 102.6 1115.6 1115.6 1127.0 137.0 WITH BUFFALO STANDARD HEATERS Lin. Ft. Per B. t. 758710596534534507Ľ 000 5 LBS., STEAM TEMP. 227° Final Temp. 35.0 56.8 76.2 93.1 108.3 121.6 133.2 143.8 B. t. u. per in. Ft. per at 70° F. 800 Final Temp. 45.8 68.3 68.3 88.0 104.9 120.0 133.0 133.0 144.4 154.5 37.1 60.8 81.2 99.2 99.2 115.0 128.8 140.5 151.0 per Min., Measured per Lin. Ft. B. t. u. Hour 337 503 169 1469 384 384 384 384 384 515479 449 4417 3391 3366 3344 324 *TEMPERATURE OBTAINED* **GAUGE PRESSURE** 600 Final Temp. 39.5 65.3 87.4 106.3 1222.7 136.7 136.7 136.7 159.3  $\begin{array}{c} 48.3\\72.7\\94.0\\1111.6\\1127.4\\152.4\\152.4\\162.3\end{array}$ Velocity of Air in Ft. B. t. u. Lin. Ft. Per 100 Final Temp. 43.0 71.0 94.5 114.4 131.7 131.7 136.1 158.8 158.8 51.5 78.0 78.0 1100.5 119.6 135.6 135.6 149.8 161.2 161.2 per in. Ft. B. t. u. Hour 228 207 207 207 207 207 208 174 174 174 174 128 28 28 28 28 28 003 Final Cemp. 55.685.185.1109.4129.6146.7160.3171.8181.247.6 78.3 78.3 103.7 124.8 124.8 157.3 157.3 157.3 159.1

No. of Heater Sections

Temp. of Entering Air

### BUFFALO HEATER TABLES

866 823 783 7743 674 674 512

40.4 58.8 755.3 90.0 115.2 115.2 115.2 135.4

795755 716 674 674 610 579 550

41.9 61.5 79.0 94.1 108.1 120.5 131.4

716 673 635 635 635 600 500 500 536 536 536 536 536 538 508

43.6 64.4 82.8 99.1 113.4 113.4 126.0 137.3

-01004-000-00

692 658 658 564 513 513 513

76.3 91.0 91.0 104.2 116.0 126.4 135.9 135.9 144.6

639600570512540546344634463

77.6 93.0 93.0 107.0 119.4 130.4 130.4 149.0 157.2

576 538 538 509 509 181 154 181 154 180 887 887

 $\begin{array}{c} 79.0\\95.5\\95.5\\110.4\\123.4\\134.8\\145.2\\154.2\\154.2\\162.2\\162.2\end{array}$ 

 $\begin{array}{c} 80.5\\98.7\\98.7\\114.4\\1128.2\\140.1\\150.6\\1160.0\\168.0\end{array}$ 

82.9 102.3 119.0 133.7 133.7 157.0 166.5 166.5

308 284 284 284 226 226 226 211 198 198 198

85.4 106.8 1250.8 140.5 153.2 164.4 174.0 182.0

 $\begin{array}{c} 73\\ 58\\ 58\\ 146\\ 124\\ 124\\ 106\\ 99\\ 99\\ \end{array}$ 

88.6 112.2 132.2 148.6 162.0 173.1 190.0

-004505-00

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101041001-00

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20 lbs.		400	B. t. u. per Lin. Ft. Per Hour	1172 1105 1053 998 949 902 861 821	1112 1061 1012 958 912 867 827 750	1070 971 922 875 834 795 759
20		- 14	Final Temp.	$\begin{array}{c} 7.6\\ 32.1\\ 54.4\\ 74.0\\ 91.8\\ 107.5\\ 121.9\\ 134.7\end{array}$	$16.2 \\ 40.0 \\ 61.5 \\ 80.3 \\ 97.4 \\ 112.5 \\ 126.4 \\ 138.8 \\ 138.8 \\ 138.8 \\ 126.4 \\ 138.8 \\ 126.4 \\ 138.8 \\ 126.4 \\ 138.8 \\ 138.8 \\ 126.4 \\ 138.8 \\ 126.4 \\ 138.8 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 126.4 \\ 1$	25.2 48.3 68.6 86.9 103.0 117.9 131.0 143.0
	meter	200	B. t. u. per Lin. Ft. Per Hour	1070 1017 958 958 958 860 815 775 737	$1016 \\ 973 \\ 922 \\ 872 \\ 826 \\ 784 \\ 745 \\ 709 \\ 709 \\$	983 937 885 837 793 717 682 682
ERS	ies Baro	12(	Final Temp.	$\begin{array}{c} 9.5\\ 35.9\\ 59.0\\ 79.7\\ 98.1\\ 114.4\\ 129.1\\ 142.0\end{array}$	$\begin{array}{c} 18.0\\ 43.5\\ 66.0\\ 85.8\\ 103.5\\ 119.3\\ 133.4\\ 145.9\end{array}$	$\begin{array}{c} 27.1 \\ 51.5 \\ 73.0 \\ 92.0 \\ 108.9 \\ 124.2 \\ 138.0 \\ 149.9 \end{array}$
) HEAT 3° F.	and 29.92 Inches Barometer	0	B. t. u. per Lin. Ft. Per Hour	964 910 854 854 806 761 719 681 681 646	931 873 875 775 731 692 656 623	904 841 792 746 704 666 631 599
ANDARD IP. 258.8°	F. and 29	1000	Final Temp.	$11.8 \\ 40.0 \\ 64.5 \\ 64.5 \\ 86.3 \\ 105.5 \\ 122.3 \\ 137.3 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 150.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 100.5 \\ 1$	$\begin{array}{c} 20.7\\ 47.6\\ 711.5\\ 92.2\\ 110.6\\ 126.9\\ 141.4\\ 154.4\end{array}$	$\begin{array}{c} 29.8\\ 55.5\\ 78.4\\ 98.4\\ 116.0\\ 131.7\\ 145.6\\ 158.1\\ 158.1\end{array}$
WITH BUFFALO STANDARD HEATERS 20 LBS., STEAM TEMP. 258.8° F.	70°	0	B. t. u. per Lin. Ft. Per Hour	837 782 782 782 688 688 648 612 612 578 578 546	800 752 662 662 557 557 525	774 724 678 637 601 535 505
H BUFFAL S., STEAM	per Min., Measured at	800	Final Temp.	$14.5 \\ 44.5 \\ 70.6 \\ 93.5 \\ 113.5 \\ 131.4 \\ 146.8 \\ 160.0 \\ 160.0 \\ 160.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ 100.0 \\ $	$\begin{array}{c} 23.0\\ 52.0\\ 77.3\\ 99.1\\ 118.6\\ 135.8\\ 150.6\\ 163.3\end{array}$	$\begin{array}{c} 31.9\\ 59.7\\ 59.7\\ 83.8\\ 105.0\\ 123.8\\ 140.3\\ 154.5\\ 166.7\\ 166.7\end{array}$
ED WITH I	r Min., I	0	B. t. u. per Lin. Ft. per Hour	$\begin{array}{c} 682\\ 638\\ 5597\\ 558\\ 521\\ 489\\ 433\\ 433\end{array}$	650 614 673 573 537 537 537 537 537 537 537 537 5	630 554 554 454 427 402
BTAINE	표	600	Final Temp.	$\begin{array}{c} 17.5 \\ 50.1 \\ 78.4 \\ 102.6 \\ 123.2 \\ 141.4 \\ 157.0 \\ 170.4 \end{array}$	$\begin{array}{c} 25.7\\ 57.5\\ 57.5\\ 84.4\\ 108.0\\ 128.0\\ 145.2\\ 160.5\\ 160.5\end{array}$	$\begin{array}{c} 34.6\\ 65.1\\ 91.3\\ 91.3\\ 113.4\\ 132.6\\ 149.6\\ 164.3\\ 176.6\end{array}$
TEMPERATURE OBTAINED GAUGE PRESSURE 2	Velocity of Air in	0	B. t. u. per Lin. Ft. Per Hour	510 473 437 437 405 377 351 351 307	489 455 421 390 363 363 338 338 338 338 338 338 338 338	474 438 404 376 349 326 304
MPERA GA	Velocit	400	Final Temp.	$\begin{array}{c} 222.1\\ 572.9\\ 88.0\\ 1113.4\\ 135.3\\ 153.7\\ 169.4\\ 182.5\end{array}$	$\begin{array}{c} 30.4\\ 85.0\\ 94.0\\ 118.5\\ 139.5\\ 157.2\\ 172.2\\ 172.2\\ 185.0\end{array}$	$\begin{array}{c} 39.1\\ 72.2\\ 100.0\\ 123.9\\ 143.9\\ 161.0\\ 175.5\\ 187.8\end{array}$
TE		0	B. t. u. per Lin. Ft. Per Hour	289 264 243 223 206 190 164	$\begin{array}{c} 276\\ 255\\ 255\\ 234\\ 198\\ 184\\ 170\\ 158\end{array}$	267 245 225 207 191 177 164
		200	Final Temp.	$\begin{array}{c} 27.6\\ 67.2\\ 67.2\\ 100.0\\ 127.1\\ 149.7\\ 168.3\\ 183.7\\ 196.5\end{array}$	$\begin{array}{c} 35.5\\74.0\\105.4\\131.8\\153.5\\171.5\\186.3\\198.7\end{array}$	$\begin{array}{c} 44.0\\ 44.0\\ 111.2\\ 136.5\\ 157.4\\ 174.8\\ 189.1\\ 200.5\end{array}$
			No. of Her Sections	-00400-00	-00400000	-000400000
	Temp. of Entering Air			-20°	-100	00

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# TEMPERATURE OBTAINED WITH BUFFALO STANDARD HEATERS GAUGE PRESSURE 20 LBS., STEAM TEMP. 258.8° F.

Octocity of Afrian Liner, Measured at 70° F. and 29.03 Incress Barometer         Termp. of Healter         Descriptions         Liner         Healter         Final         Liner         Liner <thliner< th="">         Liner         <thliner< th=""><th></th><th>0</th><th>B. t. u. per Lin. Ft. Per Hour</th><th>1027 985 931 884 884 841 841 800 764 729</th><th>989 944 892 847 847 806 766 731 698</th><th>811 764 723 694 662 630 602 602 575</th></thliner<></thliner<>		0	B. t. u. per Lin. Ft. Per Hour	1027 985 931 884 884 841 841 800 764 729	989 944 892 847 847 806 766 731 698	811 764 723 694 662 630 602 602 575
Of.Li         Colify of Air in Ft. per Min., Messured at JO° F. and 29.02 Inches Barometer         Of.Lim Ft.         Termping Air         Velocity of Air in Ft. per Min., Messured at JO° F. and 29.02 Inches Barometer         200         200         200         100         120           7         7         7         7         7         7         7         3         8         100         120           7         7         7         7         7         7         3         8         8         8         8         100         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120         120		14	Final Temp.	$\begin{array}{c} 34.2\\ 56.4\\ 75.8\\ 93.3\\ 109.0\\ 123.1\\ 136.0\\ 147.3\end{array}$	43.3 64.5 63.6 83.0 99.8 114.9 128.3 140.6 151.6	$\begin{array}{c} 79.1\\ 96.0\\ 1111.1\\ 125.4\\ 138.0\\ 149.1\\ 159.3\\ 168.4\end{array}$
Of.Fi         Perofity of Afr in Ft. per Min., Messured at 70° F. and 20.92 Increas Barometer           Of.Fi         Proprint Heart         B. t. u.         Mot         600         S00         S00         Do         Do <th< th=""><th></th><th>000</th><th>B. t. u. per Lin. Ft. Per Hour</th><th>$\begin{array}{c} 954\\ 954\\ 901\\ 849\\ 804\\ 761\\ 724\\ 688\\ 654\end{array}$</th><th>911 864 813 769 729 693 658 658 628</th><th>740 706 667 633 600 545 519</th></th<>		000	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 954\\ 954\\ 901\\ 849\\ 804\\ 761\\ 724\\ 688\\ 654\end{array}$	911 864 813 769 729 693 658 658 628	740 706 667 633 600 545 519
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	ometer	12	Final Temp.	$\begin{array}{c} 36.3\\ 59.5\\ 59.5\\ 80.0\\ 98.4\\ 114.6\\ 129.3\\ 142.3\\ 153.9\end{array}$	$\begin{array}{c} 45.1\\ 67.5\\ 87.0\\ 104.5\\ 120.2\\ 134.2\\ 134.2\\ 146.6\\ 158.0\end{array}$	80.4 98.8 98.8 115.0 125.0 142.5 154.0 164.1 174.1
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	ches Bar	00	B. t. u. per Lin. Ft. per Hour	858 805 758 713 674 674 638 606 576	831 773 727 685 685 647 612 581 552	679 635 596 534 534 534 481 456
$ \begin{array}{ c c c c c c c c c c c c c c c c c c c$	29.92 Inc	10	Final Temp.	$\begin{array}{c} 38.3\\ 63.1\\ 63.1\\ 85.0\\ 104.1\\ 121.1\\ 121.1\\ 136.2\\ 149.9\\ 161.9\end{array}$	$\begin{array}{c} 47.4\\71.0\\91.9\\110.3\\126.7\\141.0\\154.1\\165.7\end{array}$	82.4 101.9 1190.0 134.4 148.0 160.4 171.1 180.4
Oricity of Air in Ft. per Min., Measured at 7 Electritors         Velocity of Air in Ft. per Min., Measured at 7 200         A00         000           10°         200         400         00         401         00           10°         33         257         47.5         493         00           10°         411.1         10°         400         00         40.7           10°         411.1         10°         10°         40.7         10°         40.7           10°         411.1         109         109.6         333         90.4         40.7           110°         116.9         116.9         116.9         118.1         119.7         10°         40.7           110°         116.9         118.1         119.9         1139.0         40.7         40.7           110°         116.9         118.1         119.7         119.9         119.9         119.9           110°         116.1         118.1         119.7         118.1         119.7         110.1           110°         118.1         118.1         119.9         118.1         119.9         110.1           110°         118.1         118.1         119.7         119.9         119.9	F. and	0	B. t. u. per Lin. Ft. Per Hour	745 695 650 611 577 514 514 514	716 667 586 555 555 522 466 466	585 547 518 458 459 432 409 386
Of ht         Temp. of ht         Alt in Fi.           Intertiene And         200         Alt in Fi.           Intertiene And         B. t. u.         Alt in Fi.           Intertiene And         Alt in Fi.         Alt in Fi.           Intertiene And         B. t. u.         Alt in Fi.           Intertiene And         Alt in Fi.         Alt in Fi.           Intertiene And <th>at</th> <th>8(</th> <th>Final Temp.</th> <th>$\begin{array}{c} 40.7\\ 67.3\\ 67.3\\ 90.4\\ 110.8\\ 129.0\\ 144.6\\ 158.3\\ 170.1\end{array}$</th> <th>$\begin{array}{c} 49.5\\75.0\\97.0\\116.7\\134.3\\149.1\\173.8\end{array}$</th> <th>84.1 105.1 124.0 140.4 154.6 166.9 177.9 187.3</th>	at	8(	Final Temp.	$\begin{array}{c} 40.7\\ 67.3\\ 67.3\\ 90.4\\ 110.8\\ 129.0\\ 144.6\\ 158.3\\ 170.1\end{array}$	$\begin{array}{c} 49.5\\75.0\\97.0\\116.7\\134.3\\149.1\\173.8\end{array}$	84.1 105.1 124.0 140.4 154.6 166.9 177.9 187.3
Of ht         Temp. of ht         Alt in Fi.           Intertiene And         200         Alt in Fi.           Intertiene And         B. t. u.         Alt in Fi.           Intertiene And         Alt in Fi.         Alt in Fi.           Intertiene And         B. t. u.         Alt in Fi.           Intertiene And         Alt in Fi.         Alt in Fi.           Intertiene And <th>Measur</th> <th>0</th> <th>B. t. u. per Lin. Ft. Per Hour</th> <th>$\begin{array}{c} 610\\ 571\\ 532\\ 496\\ 4465\\ 436\\ 436\\ 386\\ 386\end{array}$</th> <th>$\begin{array}{c} 590 \\ 549 \\ 576 \\ 475 \\ 446 \\ 418 \\ 393 \\ 370 \\ 370 \end{array}$</th> <th>488 453 421 395 370 326 326 326</th>	Measur	0	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 610\\ 571\\ 532\\ 496\\ 4465\\ 436\\ 436\\ 386\\ 386\end{array}$	$\begin{array}{c} 590 \\ 549 \\ 576 \\ 475 \\ 446 \\ 418 \\ 393 \\ 370 \\ 370 \end{array}$	488 453 421 395 370 326 326 326
Of ht         Temp. of ht         Alt in Fi.           Intertiene And         200         Alt in Fi.           Intertiene And         B. t. u.         Alt in Fi.           Intertiene And         Alt in Fi.         Alt in Fi.           Intertiene And         B. t. u.         Alt in Fi.           Intertiene And         Alt in Fi.         Alt in Fi.           Intertiene And <th>per Min.</th> <th>9(</th> <th>Final Temp.</th> <th>$\begin{array}{c} 43.5\\722.8\\97.7\\119.0\\137.7\\153.9\\167.6\\179.7\end{array}$</th> <th>$\begin{array}{c} 52.4\\ 80.4\\ 104.0\\ 124.5\\ 142.5\\ 158.0\\ 171.3\\ 182.9\end{array}$</th> <th>86.8 109.8 129.4 146.8 161.7 1741.7 185.5 195.0</th>	per Min.	9(	Final Temp.	$\begin{array}{c} 43.5\\722.8\\97.7\\119.0\\137.7\\153.9\\167.6\\179.7\end{array}$	$\begin{array}{c} 52.4\\ 80.4\\ 104.0\\ 124.5\\ 142.5\\ 158.0\\ 171.3\\ 182.9\end{array}$	86.8 109.8 129.4 146.8 161.7 1741.7 185.5 195.0
Of         Temp. of It         Velocity of           Temp. of It         No. of Heater         Velocity of           Do         Final         B. t. u.         Plent           No. of Heater         200         10         10           Sections         20         110.9         141.1         199           No. of Heater         200         116.9         216         100.0           Sections         203.1         141.1         199         128.2         176           R         203.1         160.9         247.4         136.9         138.4         138.4           R         203.1         141.1         199         128.2         139.6         138.6           R         203.1         141.3         189         138.6         138.6           R         203.1         146.1         199.5         138.6         138.6           R         203.1         146.3         189.1         138.6         138.6         138.6           R         165.3         170         199.5         138.6         138.6         138.6         138.6         138.6         138.6         138.6         138.6         138.6         138.6         138.6         1	Ft.	00	B. t. u. per Lin. Ft. Per Hour	454 419 388 361 335 335 335 335 313 292 274	439 401 372 322 322 322 322 322 322 322 322 322	359 333 333 333 333 333 333 287 287 287 287 287 287 287 287 287 287
Solution	ity of Ai	4(	Final Temp.	$\begin{array}{c} 47.5\\79.1\\106.0\\128.9\\148.1\\164.7\\164.7\\178.6\\190.4\end{array}$	56.2 86.1 112.0 134.1 152.7 168.5 181.8 193.1	89.6 114.9 136.4 154.6 170.1 183.1 194.5 204.0
00         00         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1         1 <th1< th="">         1         1         1</th1<>	Veloc	0	B. t. u. per Lin. Ft. Per Hour	257 236 216 199 184 170 158 146	248 227 208 191 176 156 151 140	206 188 159 147 135 126 117
Sector     Sector     Temp. of Entering Air       Ano. of Heater     No. of Heater		20	Final Temp.	$\begin{array}{c} 52.3\\ 87.8\\ 116.9\\ 141.1\\ 161.3\\ 178.0\\ 191.9\\ 203.1\end{array}$	$\begin{array}{c} 60.9\\94.7\\94.7\\122.8\\146.0\\165.3\\181.1\\194.5\\205.0\end{array}$	$\begin{array}{c} 94.0\\ 122.0\\ 145.5\\ 164.9\\ 181.0\\ 1941.0\\ 205.1\\ 214.0\end{array}$
Ç Ö Ö Ö				-00400000		-00450020
		10 Air		<u>°</u> 423	200	000

BUFFALO HEATER TABLES

Ibs.	1400	B. t. u. per Lin. Ft. Per Hour	1286 1206 1146 1086 1035 983 983 894	1223 1165 1101 1049 996 904 862	1167 1119 1063 960 913 870 830	
40	14	Final Temp.	$\begin{array}{c} 10.3\\ 36.8\\ 61.0\\ 82.3\\ 101.9\\ 118.9\\ 134.4\\ 148.4\end{array}$	$\begin{array}{c} 18.8\\ 44.9\\ 67.8\\ 88.8\\ 107.3\\ 123.8\\ 139.1\\ 152.5\end{array}$	27.5 52.7 75.1 95.2 113.0 129.0 143.4 156.5	
meter	1200	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 1179\\ 11044\\ 1044\\ 985\\ 934\\ 887\\ 887\\ 803\\ 803\end{array}$	$\begin{array}{c} 1128\\ 1061\\ 1007\\ 955\\ 955\\ 901\\ 856\\ 814\\ 775\end{array}$	1084 1024 9167 916 869 826 785 749	
cko hes Baro	12	Final Temp.	$\begin{array}{c} 12.4\\ 40.7\\ 66.1\\ 88.4\\ 108.4\\ 126.2\\ 142.3\\ 156.6\end{array}$	$\begin{array}{c} 21.0\\ 48.3\\ 73.0\\ 95.0\\ 113.8\\ 131.2\\ 146.6\\ 160.5\end{array}$	$\begin{array}{c} 29.8\\ 56.3\\ 79.7\\ 100.8\\ 119.4\\ 136.2\\ 151.0\\ 164.6\end{array}$	
WITH DUFFALU STANDARD THEATERS 0 LBS., STEAM TEMP. 286.7° F. Min., Measured at 70° F. and 29.92 Inches Barometer	000	B. t. u. per Lin. Ft. Per Hour	$1055 \\ 930 \\ 930 \\ 877 \\ 825 \\ 782 \\ 741 \\ 704$	$1001 \\ 952 \\ 952 \\ 894 \\ 848 \\ 798 \\ 717 \\ 717 \\ 680 \\ 680 \\$	970 917 917 861 770 777 7728 691 657	
IP. 286.7° F. and 29	10	Final Temp.	$\begin{array}{c} 14.8\\ 45.0\\ 72.0\\ 95.7\\ 116.6\\ 134.8\\ 151.0\\ 155.8\end{array}$	$\begin{array}{c} 23.0\\ 52.8\\ 78.5\\ 101.8\\ 121.6\\ 139.6\\ 155.4\\ 169.5\end{array}$	$\begin{array}{c} 32.0\\ 60.5\\ 85.2\\ 107.7\\ 127.0\\ 144.0\\ 159.4\\ 173.3\end{array}$	
AM TEMP.	800	B. t. u. per Lin. Ft. Per Hour	910 854 796 752 752 706 666 629 594	883 825 775 725 682 644 608 608	842 795 795 657 657 657 657 651 558 554	
S., STEAM Measured a	8	Final Temp.	$\begin{array}{c} 17.5\\ 50.4\\ 78.4\\ 104.0\\ 125.6\\ 144.8\\ 161.4\\ 166.0\end{array}$	$\begin{array}{c} 26.4\\ 58.0\\ 85.8\\ 109.5\\ 130.6\\ 149.2\\ 165.3\\ 179.5\end{array}$	$\begin{array}{c} 34.7\\ 65.5\\ 92.0\\ 115.2\\ 135.4\\ 153.5\\ 169.1\\ 182.7\end{array}$	
	00	600	B. t. u. per Lin. Ft. Per Hour	746 700 653 608 568 534 502 473	728 671 628 588 550 515 486 457	$\begin{array}{c} 701 \\ 652 \\ 607 \\ 667 \\ 567 \\ 667 \\ 667 \\ 668 \\ 468 \\ 442 \end{array}$
	9(	Final Temp.	$\begin{array}{c} 21.0\\ 57.0\\ 87.7\\ 113.6\\ 136.2\\ 156.0\\ 173.1\\ 173.1\\ 188.0\end{array}$	$\begin{array}{c} 30.0\\ 63.8\\ 93.6\\ 119.2\\ 141.0\\ 159.9\\ 176.8\\ 191.1\end{array}$	$\begin{array}{c} 38.5\\ 38.5\\ 71.7\\ 100.0\\ 124.6\\ 145.8\\ 164.1\\ 180.4\\ 194.4\end{array}$	
GAUGE PRESS	0	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 558\\ 516\\ 516\\ 476\\ 442\\ 442\\ 384\\ 336\\ 336\\ 336\end{array}$	536 499 461 428 398 371 347 325	513 443 412 384 358 334 314	
GAUGE I Velocity of	400	Final Temp.	$\begin{array}{c} 26.0\\ 65.0\\ 97.6\\ 125.8\\ 149.8\\ 170.0\\ 187.0\\ 201.7\end{array}$	$\begin{array}{c} 34.2\\ 72.2\\ 72.2\\ 104.1\\ 131.0\\ 154.0\\ 173.5\\ 190.0\\ 204.1\end{array}$	$\begin{array}{c} 42.3\\ 79.0\\ 109.6\\ 136.0\\ 158.2\\ 177.2\\ 193.0\\ 206.8 \end{array}$	
	200	B. t. u. per Lin. Ft. Per Hour	318 290 265 244 226 226 209 194 180	303 256 256 236 236 218 202 187 174	291 271 248 228 228 210 195 181 168	
	2(	Final Temp.	$\begin{array}{c} 32.5\\75.6\\111.3\\141.0\\166.0\\186.3\\203.3\\217.9\end{array}$	$\begin{array}{c} 40.0\\ 82.0\\ 116.5\\ 145.3\\ 169.6\\ 189.4\\ 205.9\\ 219.4\end{array}$	$\begin{array}{c} 48.0\\ 89.5\\ 122.6\\ 150.5\\ 173.5\\ 192.8\\ 208.6\\ 221.8\end{array}$	
	ater	No. of He Section	-00400-00	-004506	-004500-00	
	Temp. of Entering Air		-20°	°0 1	00	

40 lbs.		1400	B. t. u. per Lin. Ft. per Hour	1146 1076 1020 970 879 838 801	1091 1034 982 982 981 887 845 845 845 866 769	914 870 821 782 745 710 679 643	
40		14	Final Temp.	$\begin{array}{c} 37.0\\ 60.7\\ 82.1\\ 101.7\\ 118.6\\ 134.2\\ 148.2\\ 148.2\\ 160.9\end{array}$	$\begin{array}{c} 45.7\\ 68.7\\ 68.7\\ 89.4\\ 107.7\\ 129.5\\ 139.4\\ 152.9\\ 165.0\end{array}$	81.4 101.0 118.0 133.7 147.7 160.4 172.0 181.2	
		200	B. t. u. per Lin. Ft. Per Hour	$1041 \\ 929 \\ 929 \\ 882 \\ 837 \\ 795 \\ 756 \\ 720 \\ 720 \\$	990 940 893 845 804 764 728 693	842 797 752 7152 615 615 586 586	
TERS	arometer	12	Final Temp.	$38.5\\64.3\\64.3\\86.6\\107.0\\125.0\\141.0\\155.5\\168.4$	$\begin{array}{c} 47.2\\72.0\\93.6\\113.0\\136.5\\146.0\\160.0\\160.0\end{array}$	$\begin{array}{c} 83.0\\ 103.8\\ 122.0\\ 153.2\\ 153.2\\ 166.3\\ 178.2\\ 188.9\\ 188.9\end{array}$	
STANDARD HEATERS EMP. 286.7° F.	29.92 Inches Barometer	000	B. t. u. per Lin. Ft. Per Hour	940 884 831 770 667 633	895 849 757 757 713 675 642 610	767 722 674 637 603 544 516	
STANDARD TEMP. 286.7°	1 29.92	9	Final Temp.	$\begin{array}{c} 41.0\\ 68.3\\ 92.2\\ 113.7\\ 132.5\\ 148.9\\ 164.0\\ 167.1\end{array}$	49.5 76.0 99.1 119.8 137.5 153.6 168.1 181.0	$\begin{array}{c} 85.1\\ 107.6\\ 126.7\\ 144.0\\ 159.4\\ 173.2\\ 185.6\\ 196.2\end{array}$	
BUFFALO SI STEAM TE	70° F. and	800	B. t. u. per Lin. Ft. Per Hour	813 759 759 673 673 634 535 565 535	784 737 692 648 611 576 544 515	670 622 583 583 583 583 583 583 583 587 487 487 481 436	
	at	8	Final Temp.	$\begin{array}{c} 43.5\\72.6\\98.8\\98.8\\121.0\\140.6\\157.9\\172.9\\186.3\end{array}$	$\begin{array}{c} 52.3\\ 52.3\\ 105.6\\ 126.9\\ 145.9\\ 162.5\\ 176.9\\ 189.8 \end{array}$	$\begin{array}{c} 87.6\\111.3\\132.1\\150.4\\166.5\\180.4\\193.0\\204.0\end{array}$	
40 40	1., Measured	600	B. t. u. per Lin. Ft. Per Hour	677 629 585 585 547 511 452 452 425	644 605 563 526 492 482 410	548 509 474 443 416 392 369 348	
OBTAINED PRESSURE	per Min.,	9	Final Temp.	$\begin{array}{c} 47.2\\79.1\\106.4\\130.2\\150.4\\168.4\\184.0\\197.0\end{array}$	$\begin{array}{c} 55.4\\ 86.5\\ 112.8\\ 135.7\\ 155.1\\ 172.5\\ 187.6\\ 200.4\end{array}$	90.1 116.0 138.2 157.3 174.5 189.3 201.9 201.9	
	of Air in Ft.	400	B. t. u. per Lin. Ft. Per Hour	499 462 429 398 370 323 323 323	479 445 413 383 383 383 383 383 383 383 383 383 3	411 379 350 325 303 281 281 281 281 248	
remperature gauge i	Velocity of	4	Final Tcmp.	$\begin{array}{c} 51.1\\ 56.2\\ 86.2\\ 116.0\\ 141.1\\ 162.5\\ 180.9\\ 196.2\\ 209.4\end{array}$	$\begin{array}{c} 59.5\\ 53.4\\ 122.1\\ 146.4\\ 167.0\\ 184.6\\ 199.4\\ 212.2\\ 212.2\end{array}$	$\begin{array}{c} 93.9\\ 122.5\\ 146.6\\ 167.2\\ 185.0\\ 185.0\\ 199.6\\ 212.3\\ 223.4\\ \end{array}$	
TE	Velo	200	B. t. u. per Lin. Ft. Per Hour	282 260 239 239 239 239 203 174 174 162	272 251 251 212 196 181 168 156	234 214 196 180 166 154 143 133	
		20	Final Temp.	$\begin{array}{c} 56.5\\ 95.8\\ 95.8\\ 128.2\\ 154.9\\ 177.5\\ 196.0\\ 211.0\\ 223.9\end{array}$	$\begin{array}{c} 64.8\\ 102.9\\ 133.9\\ 159.5\\ 181.3\\ 199.0\\ 213.8\\ 226.2\end{array}$	98.6 130.6 156.7 179.0 197.1 212.2 224.9 235.3	
		ster sate:	No. of He	-004-00-0	-010041001-00	-00400-0	
	Temp. of Entering Air			°01	300	60°	

BUFFALO HEATER TABLES

60 lbs.		400	B. t. u. per Lin. Ft. Per Hour	1371 1278 1278 1213 1155 1096 1043 995 950	$\begin{array}{c} 1316\\ 1244\\ 1175\\ 11175\\ 1114\\ 1059\\ 1007\\ 963\\ 918\end{array}$	$\begin{array}{c} 1265\\ 1197\\ 1197\\ 1076\\ 974\\ 974\\ 929\\ 886\end{array}$
60		14	Final Temp.	$\begin{array}{c} 12.3\\ 40.2\\ 65.7\\ 88.8\\ 109.1\\ 127.4\\ 144.1\\ 159.0\end{array}$	$\begin{array}{c} 21.0\\ 248.5\\ 73.0\\ 95.0\\ 114.7\\ 132.3\\ 148.8\\ 148.8\\ 163.0\end{array}$	$\begin{array}{c} 29.8\\ 56.4\\ 79.9\\ 101.4\\ 120.5\\ 137.7\\ 153.1\\ 167.0\end{array}$
	rometer	1200	B. t. u. Per Lin. Ft. Per Hour	$\begin{array}{c} 1245\\ 1174\\ 11174\\ 1106\\ 1046\\ 991\\ 943\\ 896\\ 852\\ 852\end{array}$	$\begin{array}{c} 1197\\ 1134\\ 1067\\ 1010\\ 959\\ 912\\ 866\\ 825\\ 825 \end{array}$	$\begin{array}{c} 1161\\ 1004\\ 10031\\ 975\\ 926\\ 879\\ 837\\ 797\end{array}$
	ches Bai	12	Final Temp.	$\begin{array}{c} 14.3\\ 44.5\\ 71.2\\ 95.0\\ 116.1\\ 135.5\\ 152.4\\ 167.3\end{array}$	$\begin{array}{c} 23.0\\ 52.3\\ 78.0\\ 101.0\\ 121.8\\ 140.3\\ 156.6\\ 171.3\end{array}$	$\begin{array}{c} 32.0\\ 60.1\\ 85.0\\ 107.2\\ 127.2\\ 145.0\\ 161.0\\ 161.0\\ 175.2\end{array}$
HEATERS F.	and 29.92 Inches Barometer	000	B. t. u. Per Lin. Ft. Per Hour	$\begin{array}{c} 1122\\ 1048\\ 987\\ 930\\ 878\\ 831\\ 788\\ 788\\ 748\end{array}$	$\begin{array}{c} 1079\\ 1013\\ 951\\ 961\\ 804\\ 724\\ 724\end{array}$	1046 975 922 869 821 778 737 700
	Ľ.	10	Final Temp.	$\begin{array}{c} 17.0 \\ 49.1 \\ 77.6 \\ 102.7 \\ 124.8 \\ 144.5 \\ 162.0 \\ 162.0 \\ 177.4 \end{array}$	$\begin{array}{c} 25.6\\ 56.8\\ 56.8\\ 84.1\\ 108.8\\ 130.0\\ 149.1\\ 166.1\\ 166.1\\ 181.0\end{array}$	$\begin{array}{c} 34.5\\ 64.3\\ 91.2\\ 91.2\\ 114.6\\ 135.4\\ 154.0\\ 170.2\\ 184.6\end{array}$
TEMP. 307.3°	ed at 70°	800	B. t. u. per Lin. Ft. Per Hour	978 978 905 849 797 750 708 669 632	944 944 876 820 770 725 685 685 648 612	905 847 793 7144 701 663 663 663 653 626
BUFFALO S STEAM TE	, Measured	æ	Final Temp.	20.3 54.6 85.0 111.4 134.5 155.0 173.0 173.0	$\begin{array}{c} 28.9\\ 62.2\\ 61.4\\ 117.0\\ 139.5\\ 159.4\\ 176.9\\ 191.8\\ 191.8\end{array}$	$\begin{array}{c} 37.3\\ 69.8\\ 98.0\\ 122.7\\ 144.5\\ 164.0\\ 180.7\\ 195.2\end{array}$
WITH BUF 0 LBS., STI	per Min.,	600	B. t. u. per Lin. Ft. Hour	804 742 692 646 605 534 503 503	775 719 669 625 586 550 517 488	746 695 647 605 568 532 501 472
% (	in Ft.	Air In Ft	Final Temp.	$\begin{array}{c} 24.2\\ 61.6\\ 94.1\\ 122.0\\ 146.2\\ 167.5\\ 185.5\\ 201.2\\ 201.2\end{array}$	$\begin{array}{c} 32.6\\ 69.0\\ 100.3\\ 127.5\\ 151.0\\ 171.3\\ 171.3\\ 189.0\\ 204.4\end{array}$	$\begin{array}{c} 41.0\\ 76.4\\ 106.7\\ 1330.0\\ 155.5\\ 192.8\\ 207.5\end{array}$
OBTAINED	Velocity of A		B. t. u. per Lin. Ft. Per Hour	594 546 505 470 470 438 408 382 382 358	578 530 491 456 425 395 395 395 347	550 511 411 411 335 335 335
ATURE	Veloe	40	Final Temp.	$\begin{array}{c} 29.0\\ 70.0\\ 105.0\\ 134.9\\ 160.4\\ 182.0\\ 200.2\\ 215.9\end{array}$	$\begin{array}{c} 37.7\\77.4\\1111.4\\140.2\\165.0\\185.6\\203.5\\218.6\end{array}$	$\begin{array}{c} 45.4\\ 85.4\\ 845.3\\ 1172.0\\ 1452.3\\ 169.0\\ 189.2\\ 206.5\\ 221.0\end{array}$
remperature gauge i		200	B. t. u. per Lin. Ft. Hour	340 340 283 283 283 283 283 283 283 283 293 206 193	$\begin{array}{c} 329\\ 329\\ 374\\ 252\\ 252\\ 232\\ 215\\ 200\\ 187\\ 187\end{array}$	317 290 244 225 208 194 181
-		2(	Final Temp.	$\begin{array}{c} 36.0\\ 82.0\\ 151.8\\ 177.8\\ 177.8\\ 218.2\\ 218.2\\ 234.0 \end{array}$	$\begin{array}{c} 44.2\\ 84.2\\ 88.9\\ 156.4\\ 156.4\\ 181.6\\ 203.0\\ 221.0\\ 236.3\end{array}$	$\begin{array}{c} 52.3\\ 95.5\\ 131.2\\ 161.0\\ 185.4\\ 226.2\\ 224.0\\ 239.0\end{array}$
		iste: 21	No. of He Section	H016641067-80	-01004-1001-00	-00400000
	Temp. of Entering Air			-20°	-100	°O
				426		

60	
TEMPERATIOF ORTAINED WITH BUFFALO STANDARD HEATERS	CALLERATION DESSURE 60 LBS., STEAM TEMP. 307.3° F.
BUFFALO	, STEAM
WITH	60 LBS.
OBTAINED	DEFSSURE
TENDEDATIDE	I ENFERANCE

Ibs.

1	0	1	B. t. u. per Lin. Ft. Per Hour	$1210 \\ 1146 \\ 1090$	1035 985	940 807	856	1167	1051	951	865		981 936				1
neter	1400		Final Temp.	$38.5 \\ 64.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ 87.0 \\ $	107.5 126.0	142.9	171.3	47.5	94.3	132.0	162.7	175.7	83.1	123.0	155.4	169.1	193.0
	-		B. t. u. per Lin. Ft. Per Hour	1121 1055 999	942 895	850	170	1078	958	908 862	780	743	907 859	815	735	669 999	636
es Barof	0061		Final Temp.	40.9 68.0	113.5	150.2	179.4	49.7	75.7 99.0	119.9	155.0	183.4	85.0	127.2	145.0	175.2	199.9
. 30/.3 F.			B. t. u. per Lin. Ft. per Hour	1004 946	838 838 703	752	676	020	910 857	810 764	725 688	653	819	728	655	620	559
TP. 50/.4		1001	Final I Temp.	43.1	120.6	140.8	174.5 188.5	52.0	80.0 104.8	126.8 146.0	163.5	192.2	87.0	111.0	151.0	182.7	207.5
TEA	2		B. t. u. per in. Ft. Per Hour	873 814	767	678 640	605 572	220	737	694	618	552	720	631	594	529 529	501 474
s., STEAM	Measured at	800	Final I Temp.	46.0	104.8 128.7	149.8 168.4	184.6 198.8	64.0	85.0 85.0	134.4	172.9	202.2	89.7	115.3	158.0	175.8	204.5 216.4
60 LI	Min.,		B. t. u. per Lin. Ft. Per Hour	719	624 584	548	484	000	646 646	565	497	408 440	591	551	484	454 426	401 378
PRESSURE	n Ft. per	600	Final I Temp.	49.5	112.9	160.5	196.2		58.1 91.0	144.1	165.5	200.0 213.6	92.5	120.8	166.4	184.8 200.5	214.3
GAUGE PR	y of Air in	-	B. t. u. per Lin. Ft. Hour	533	457	396	346	-	516 479	443 412	408 358	334	6VV	411	354	329	289
<b>GA</b>	Velocity of	400	Final I Temp.	54.0	91.0 123.1	173.3	193.0 209.6 224 0	D. E ===	62.6 99.0	129.5	178.0 197.0	213.0	200	127.7	154.0	195.6	226.7
		-	B. t. u. Per Lin. Ft. Hour	309	250 257	218	202 188	110	295 270	248 227	210 195	181	GOI	232	213	181	156
		200	Final I	61.0	102.3	165.9 189.4	209.7 226.5	0.012	68.7 109.0	142.8	193.1	229.3	242.7	101.7	165.3	209.4	226.3 240.5 969 1
	-	er	No. of Heato Sections	-	c1 m	4 50	91	x	10	100 4	• <b>1</b> 0 4	-10	œ	-0	~~~	4 10	610
	Temp. of Entering Air				10°				200	2				001	00		

BUFFALO HEATER TABLES

	400	B. t. u. per Lin. Ft Per Hour	$\begin{array}{c} 1431\\ 1350\\ 1274\\ 1208\\ 11208\\ 1146\\ 1092\\ 1040\\ 991 \end{array}$	$\begin{array}{c} 1384\\ 1305\\ 1234\\ 1167\\ 11167\\ 1116\\ 1058\\ 1007\\ 960\end{array}$	1354 1265 1193 1129 1074 1022 975 975	
	4	Final Temp.	$13.7 \\ 13.7 \\ 70.0 \\ 93.8 \\ 115.0 \\ 134.3 \\ 151.5 \\ 166.8 \\ 166.8 \\ 166.8 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1000 \\ 1$	$\begin{array}{c} 22.6\\51.5\\77.2\\120.7\\120.7\\139.5\\156.0\\171.0\end{array}$	$\begin{array}{c} 31.9\\ 59.6\\ 59.6\\ 84.3\\ 106.4\\ 126.5\\ 144.4\\ 160.8\\ 175.9\end{array}$	
meter	1200	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 1310\\ 1234\\ 1158\\ 1095\\ 1095\\ 985\\ 985\\ 937\\ 891 \end{array}$	$\begin{array}{c} 1274\\ 1126\\ 1120\\ 1059\\ 1004\\ 954\\ 908\\ 864\end{array}$	1233 1146 1086 972 923 880 880 880	
hes Baro	12	Final Temp.	$16.0 \\ 75.5 \\ 75.5 \\ 122.6 \\ 142.4 \\ 160.3 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 176.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\ 186.0 \\$	$\begin{array}{c} 25.0\\ 55.2\\ 82.3\\ 106.4\\ 128.0\\ 147.3\\ 164.7\\ 180.0\end{array}$	33.9 63.0 89.5 112.8 133.6 152.2 169.2	
and 29.92 Inches Barometer	1000	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 1182\\ 1095\\ 1033\\ 972\\ 919\\ 869\\ 825\\ 783\\ 783\end{array}$	$1137 \\1061 \\1000 \\941 \\842 \\842 \\799 \\758 \\758 \\$	1098 1028 969 911- 861 816 775	
F. and 2	10	Final Temp.	$\begin{array}{c} 19.0\\ 52.2\\ 82.2\\ 82.2\\ 108.2\\ 131.5\\ 152.0\\ 170.5\\ 186.6\end{array}$	$\begin{array}{c} 27.5\\ 60.0\\ 88.9\\ 114.1\\ 136.8\\ 156.6\\ 174.5\\ 190.1\end{array}$	36.2 67.8 95.9 120.2 142.0 161.5 178.9	
d at 70°	800	B. t. u. per Lin. Ft. per Hour	1024 950 890 835 786 740 700 662	985 921 861 861 808 761 718 679 642	961 885 834 782 737 695 657 695	
Measured	8(	Final Temp.	22.2 58.3 90.0 117.6 142.0 163.1 182.0 198.3	$\begin{array}{c} 30.6\\ 65.9\\ 96.5\\ 123.2\\ 146.9\\ 167.5\\ 185.8\\ 201.6\end{array}$	39.6 73.0 103.1 129.0 151.9 172.0 189.5	
er Min.,	600	Ft. per 600	B. t. u. per Lin. Ft. Per Hour	846 780 726 676 633 596 533 560 527	812 755 755 755 653 653 615 515 543 512	782 731 679 595 595 526 526
Ft.			Final Temp.	$\begin{array}{c} 26.5\\ 65.7\\ 65.7\\ 99.7\\ 128.5\\ 154.0\\ 176.4\\ 195.3\\ 211.7\end{array}$	$\begin{array}{c} 34.6\\73.0\\105.8\\133.5\\158.9\\158.9\\198.8\\215.0\\215.0\end{array}$	$\begin{array}{c} 43.0\\ 80.3\\ 80.3\\ 1112.0\\ 139.4\\ 163.6\\ 184.5\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.4\\ 202.$
ity of Air in	400	B. t. u. per Lin. Ft. Per Hour	625 574 531 492 459 428 428 428 375	607 559 576 477 445 388 364	587 541 499 462 432 432 376	
Velocity	4(	Final Temp.	$\begin{array}{c} 31.5\\74.5\\111.3\\142.3\\169.0\\191.7\\2210.8\\227.2\end{array}$	$\begin{array}{c} 40.0\\82.0\\117.5\\147.3\\173.2\\195.4\\214.1\\230.0\end{array}$	$\begin{array}{c} 48.4\\ 89.0\\ 123.3\\ 152.5\\ 178.0\\ 199.0\\ 217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ 2217.1\\ $	
	200	B. t. u. per Lin. Ft. Per Hour	255 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 273 271 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201 201	346 315 288 288 265 244 210 195	334 335 257 257 257 257 257 257 257 257 257	
	3(	Final Temp.	$\begin{array}{c} 38.5\\ 38.5\\ 86.6\\ 126.5\\ 160.0\\ 187.5\\ 229.8\\ 225.8\\ 245.4\end{array}$	$\begin{array}{c} 47.0\\ 93.8\\ 132.5\\ 165.0\\ 191.5\\ 232.6\\ 232.6\\ 247.8\end{array}$	$\begin{array}{c} 55.0\\ 100.6\\ 138.0\\ 169.5\\ 195.5\\ 235.1\\ 235.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255.1\\ 255$	
	ister sr	No. of Ho Section	-004-00-00	-0041001-00	-004506-0	
Temp. of Entering Air		Temp. Entering	-20°	-100	0	

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TEMPERATURE OBTAINED WITH BUFFALO STANDARD HEATERS GAUGE PRESSURE 80 LBS., STEAM TEMP. 323.7° F.

1	0	B. t. u. per .in. Ft. Per Hour	1295 11295 1149 1090 1038 943 899	1235 1167 1104 1051 1051 1051 952 910 873	1057 998 947 902 858 817 782 747
	1400	Final Temp.	$\begin{array}{c} 40.5\\ 67.3\\ 67.3\\ 91.2\\ 112.7\\ 132.2\\ 149.5\\ 165.4\\ 179.5\end{array}$	49.1 75.0 98.0 119.0 137.8 154.5 170.0 184.5	$\begin{array}{c} 84.9\\ 107.0\\ 126.9\\ 145.0\\ 161.0\\ 175.5\\ 189.0\\ 2200.8\end{array}$
ometer	1200	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 1179\\ 11110\\ 1047\\ 991\\ 991\\ 892\\ 892\\ 849\\ 810\\ 810\end{array}$	1146 1072 1007 955 907 861 821 782	972 919 866 819 782 707 707 675
ches Bar	12(	Final Temp.	$\begin{array}{c} 42.4\\71.0\\96.3\\118.9\\1339.0\\157.0\\157.0\\158.0\end{array}$	$\begin{array}{c} 51.5\\ 78.9\\ 78.9\\ 103.0\\ 125.0\\ 144.6\\ 162.0\\ 178.0\\ 192.0\end{array}$	$\begin{array}{c} 86.7\\ 110.5\\ 131.6\\ 150.0\\ 167.4\\ 182.4\\ 196.0\\ 208.3\end{array}$
and 29.92 Inches Barometer	000	B. t. u. per Lin. Ft. per Hour	1058 993 934 879 834 738 738 711	1031 957 957 957 957 901 850 805 763 763 723 688	879 820 776 736 694 658 658 658 594
a.	10	Final Temp.	$\begin{array}{c} 44.9\\75.5\\102.4\\126.0\\147.5\\166.0\\182.9\\197.6\end{array}$	$\begin{array}{c} 54.0\\ 54.0\\ 83.1\\ 109.1\\ 132.1\\ 152.8\\ 171.0\\ 187.0\\ 201.4\end{array}$	89.0 114.1 136.8 156.5 174.4 190.1 204.0 216.6
ed at 70°	800	B. t. u. per Lin. Ft. Per Hour	927 861 861 758 773 673 637 602	885 828 778 731 651 651 615 582	759 716 671 631 596 562 562 503
, Measured	8(	Final Temp.	$\begin{array}{c} 48.2\\81.0\\110.0\\157.0\\157.0\\176.5\\193.7\\208.5\end{array}$	$\begin{array}{c} 56.5\\ 88.3\\ 116.2\\ 140.5\\ 162.1\\ 181.0\\ 197.5\\ 211.9\end{array}$	$\begin{array}{c} 91.3\\ 119.0\\ 143.0\\ 164.1\\ 182.8\\ 199.0\\ 213.4\\ 226.0\end{array}$
Ft. per Min.,	0	B. t. u. per Lin. Ft. per Hour	768 710 658 658 615 577 510 510 480	728 632 633 594 558 558 558 558 558 558 558 558 558 55	637 586 547 514 453 426 426 403
Air in Ft.	600	Final Temp.	$\begin{array}{c} 52.2\\ 88.0\\ 118.5\\ 145.1\\ 168.5\\ 168.5\\ 188.7\\ 2206.0\\ 221.0\end{array}$	$\begin{array}{c} 60.0\\ 95.0\\ 124.3\\ 150.5\\ 173.2\\ 192.5\\ 209.5\\ 224.0\end{array}$	$\begin{array}{c} 95.0\\ 124.4\\ 150.2\\ 173.0\\ 192.4\\ 209.3\\ 224.0\\ 236.9\\ 236.9\end{array}$
of	400	B. t. u. per Lin. Ft. Per Hour	568 525 484 449 418 365 365 341	546 566 467 434 435 377 352 331	477 437 404 376 327 327 327 327 287
Velocity	40	Final Temp.	$\begin{array}{c} 56.8\\ 96.4\\ 129.6\\ 158.0\\ 182.4\\ 2202.8\\ 220.5\\ 235.0\end{array}$	$\begin{array}{c} 65.0\\ 1035.4\\ 1355.4\\ 163.0\\ 186.8\\ 206.5\\ 223.4\\ 238.0\end{array}$	$\begin{array}{c} 99.3\\ 132.0\\ 160.0\\ 184.0\\ 204.3\\ 221.5\\ 236.5\\ 249.0\\ 249.0\end{array}$
	200	B. t. u. per Lin. Ft. Per Hour	323 296 271 249 249 230 213 198 183	311 287 262 241 223 223 206 191 178	270 248 226 209 193 179 166 154
	2(	Final Temp.	$\begin{array}{c} 63.2\\ 107.5\\ 143.8\\ 174.3\\ 174.3\\ 199.5\\ 238.0\\ 252.0\\ \end{array}$	$\begin{array}{c} 71.2\\ 1149.4\\ 178.8\\ 203.4\\ 223.4\\ 2240.5\\ 254.3\end{array}$	$\begin{array}{c} 104.5\\ 141.6\\ 172.0\\ 198.0\\ 219.0\\ 237.0\\ 251.2\\ 263.3\\ 263.3\end{array}$
L	eatei sn	No. of H Sectio	-004500-0	10045028	-0040000
	Temp. of Entering Air		100	20°	60°

BUFFALO HEATER TABLES

100 1he	CUL UU
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HEATERS	Ľ
D WITH BUFFALO STANDARD HEATER	GAUGE PRESSURE 100 LBS., STEAM TEMP, 337.6° F.
BUFFALO	. STEAM TI
WITH	00 LBS.
<b>OBTAINED</b>	RESSURE 1
TEMPERATURE OBTAINED	GAUGE PI

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400	B. t. u. Per Lin. Ft. Per Hour	$\begin{array}{c} 1465\\ 1465\\ 1388\\ 1313\\ 1242\\ 1128\\ 1128\\ 1075\\ 1026 \end{array}$	$\begin{array}{c} 1414\\ 1341\\ 1271\\ 1271\\ 1205\\ 1148\\ 1092\\ 1042\\ 995\end{array}$	1358 1295 1295 1167 11167 1112 1010 965
	Final Temp.	$\begin{array}{c} 14.5\\ 45.4\\ 72.8\\ 97.0\\ 119.6\\ 139.5\\ 157.2\\ 173.3\end{array}$	$\begin{array}{c} 23.3\\ 53.2\\ 53.2\\ 79.8\\ 103.5\\ 125.2\\ 144.4\\ 161.8\\ 177.6\end{array}$	$\begin{array}{c} 32.0\\ 61.0\\ 86.7\\ 110.0\\ 131.0\\ 149.8\\ 166.5\\ 181.8\end{array}$
ometer	B. t. u. Per Lin. Ft. Per Hour	$\begin{array}{c} 1344\\ 1266\\ 1194\\ 1132\\ 1073\\ 1073\\ 1018\\ 971\\ 925\end{array}$	$\begin{array}{c} 1306\\ 1226\\ 1155\\ 1097\\ 1097\\ 987\\ 941\\ 898\end{array}$	1252 1186 1122 1063 1008 957 913 870
es Baror	Final Temp.	$\begin{array}{c} 17.0\\ 19.6\\ 78.4\\ 104.4\\ 127.4\\ 147.9\\ 166.7\\ 183.3\end{array}$	$\begin{array}{c} 26.0\\ 57.4\\ 85.2\\ 110.6\\ 133.0\\ 152.8\\ 171.0\\ 187.4 \end{array}$	$\begin{array}{c} 34.5\\ 65.2\\ 92.5\\ 116.8\\ 138.5\\ 157.8\\ 157.6\\ 191.4\end{array}$
and 29.92 Inches Barometer	B. t. u. Per Lin. Ft. Per Hour	$\begin{array}{c} 1219\\ 1137\\ 1065\\ 1007\\ 952\\ 952\\ 952\\ 854\\ 811 \end{array}$	$\begin{array}{c} 1182\\ 1098\\ 1031\\ 975\\ 975\\ 873\\ 827\\ 786\end{array}$	1137 1064 1001 945 893 846 893 846 804 763
F. and 29	Final Temp.	20.2 55.0 85.4 112.8 137.0 158.0 177.2 194.0	$\begin{array}{c} 29.0\\ 62.4\\ 92.0\\ 118.6\\ 142.0\\ 162.8\\ 181.0\\ 197.5 \end{array}$	$\begin{array}{c} 37.5\\ 70.2\\ 99.0\\ 124.6\\ 147.2\\ 167.4\\ 185.5\\ 201.3\end{array}$
70°	B. t. u. Per Lin. Ft. Hour	1050 982 9864 864 812 725 685	$1019 \\ 952 \\ 952 \\ 837 \\ 788 \\ 778 \\ 773 \\ 665 \\ 665$	980 919 862 811 763 722 683 645
leasured	Final Temp.	$\begin{array}{c} 23.3\\ 61.0\\ 93.8\\ 122.5\\ 147.4\\ 169.5\\ 189.2\\ 206.0\end{array}$	$\begin{array}{c} 32.0\\ 68.5\\ 68.5\\ 68.5\\ 100.1\\ 128.0\\ 152.5\\ 174.0\\ 193.0\\ 209.5\end{array}$	$\begin{array}{c} 40.4\\ 75.8\\ 106.6\\ 133.7\\ 157.2\\ 178.5\\ 197.0\\ 212.9\end{array}$
Ft. per Min., Measured at	B. t. u. Per Lin. Ft. Per Hour	873 804 749 749 656 617 580 545	839 779 679 6679 6679 563 563 563 563	811 755 704 658 618 581 546 515
in Ft. per	Final Temp.	$\begin{array}{c} 28.0\\ 68.4\\ 68.4\\ 103.5\\ 134.0\\ 160.3\\ 160.3\\ 183.4\\ 203.1\\ 219.7\end{array}$	$\begin{array}{c} 36.1\\ 75.6\\ 110.0\\ 139.3\\ 165.0\\ 187.3\\ 206.7\\ 223.3\end{array}$	$\begin{array}{c} 44.6\\ 83.0\\ 116.0\\ 144.7\\ 169.9\\ 191.5\\ 226.4\\ \end{array}$
Air	B. t. u. Per Lin. Ft. Per Hour	646 595 550 550 550 550 444 444 415 389	625 576 533 494 462 482 431 378	606 561 518 448 448 392 367
Velocity of	Final Temp.	$\begin{array}{c} 33.3\\ 78.1\\ 116.0\\ 148.0\\ 176.0\\ 199.6\\ 219.7\\ 236.5\end{array}$	$41.5\\85.0\\121.8\\153.0\\180.3\\203.0\\222.7\\239.2$	$\begin{array}{c} 50.0\\ 92.5\\ 128.0\\ 158.3\\ 184.8\\ 206.9\\ 226.0\\ 226.0\\ 242.0\\ \end{array}$
200	B. t. u. Per Lin. Ft. Per Hour	368 337 283 283 283 283 283 283 283 283 283 283	355 326 326 229 275 275 275 275 275 275 275 275 275 203	343 317 289 267 246 228 212 212 198
36	Final Temp.	$\begin{array}{c} 40.7\\91.0\\132.1\\166.7\\195.6\\239.0\\256.0\end{array}$	$\begin{array}{c} 48.5\\97.5\\97.5\\137.8\\171.3\\199.5\\241.8\\258.2\\258.2\end{array}$	$\begin{array}{c} 56.6\\ 104.4\\ 104.4\\ 176.0\\ 203.1\\ 225.5\\ 244.5\\ 260.7\\ 260.7\end{array}$
ter	No. of Heat Sections	-01004-000-00	-0104-00-0	
Temp. of Entering Air		-200	-100	°0

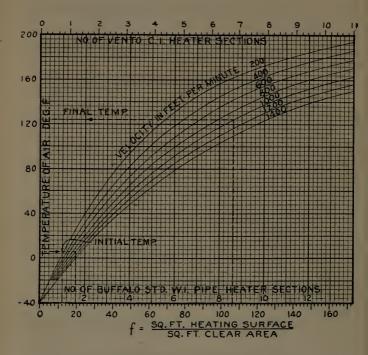
FAN ENGINEERING-BUFFALO FORGE COMPANY

1DS.		1400	B. t. u. per Lin. Ft. per Hour	1337 1254 1189 1130 1076 1076 978 934	1278 1210 1146 1093 1041 991 9946 904	$\begin{array}{c} 1112\\ 1040\\ 991\\ 944\\ 899\\ 856\\ 819\\ 819\\ 784\end{array}$
		14(	Final Temp.	$\begin{array}{c} 41.5\\ 69.1\\ 69.1\\ 94.0\\ 116.5\\ 136.7\\ 154.8\\ 171.2\\ 171.2\\ 186.0\end{array}$	$\begin{array}{c} 50.1 \\ 77.0 \\ 101.0 \\ 123.0 \\ 142.5 \\ 166.0 \\ 176.0 \\ 190.3 \end{array}$	$\begin{array}{c} 86.2\\ 1090.0\\ 1300.0\\ 148.9\\ 165.9\\ 181.0\\ 195.0\\ 195.0\\ 207.7\end{array}$
		200	B. t. u. per Lin. Ft. Per Hour	$\begin{array}{c} 1216\\1154\\1083\\1028\\975\\927\\884\\844\end{array}$	1161 1106 1047 992 943 898 898 856 816	1016 955 909 859 819 781 743 709
	rometer	12	Final Temp.	$\begin{array}{c} 43.5\\ 73.4\\ 99.3\\ 123.0\\ 144.0\\ 162.8\\ 180.1\\ 195.5\end{array}$	$\begin{array}{c} 52.0\\ 80.8\\ 106.3\\ 129.0\\ 149.6\\ 168.0\\ 184.7\\ 199.4\end{array}$	$\begin{array}{c} 88.0\\ 112.5\\ 134.9\\ 154.4\\ 172.6\\ 188.8\\ 203.0\\ 215.8\end{array}$
337.6° F.	29.92 Inches Barometer	000	B. t. u. per Lin. Ft. per Hour	$1107 \\ 1036 \\ 967 \\ 916 \\ 867 \\ 821 \\ 778 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 739 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 730 \\ 73$	$\begin{array}{c} 1055\\ 993\\ 993\\ 934\\ 884\\ 884\\ 837\\ 793\\ 753\\ 776\\ 716\\ 716\end{array}$	910 858 810 766 688 688 654 623
TEMP. 33		10	Final Temp.	$\begin{array}{c} 46.5\\ 78.3\\ 78.3\\ 105.7\\ 130.8\\ 153.0\\ 172.4\\ 189.7\\ 205.1\end{array}$	$\begin{array}{c} 54.8\\ 85.5\\ 112.4\\ 136.6\\ 158.0\\ 177.0\\ 194.0\\ 209.0\end{array}$	$\begin{array}{c} 90.0\\ 116.6\\ 140.1\\ 161.0\\ 180.0\\ 196.2\\ 211.0\\ 224.4\end{array}$
STEAM TE	70° F. and	800	B. t. u. per Lin. Ft. per Hour	953 892 835 785 740 699 661 626	922 864 864 759 717 640 606	796 746 661 588 558 528 528
LBS., ST	at	8(	Final Temp.	$49.3\\83.5\\113.3\\139.5\\162.5\\183.0\\200.8\\216.5$	$\begin{array}{c} 58.0\\ 91.2\\ 91.2\\ 145.1\\ 167.8\\ 187.5\\ 204.8\\ 220.0\end{array}$	$\begin{array}{c} 92.8\\121.5\\146.8\\169.0\\188.6\\205.5\\234.3\\234.3\end{array}$
100	., Measured	600	B. t. u. per Lin. Ft. per Hour	784 731 682 639 569 563 563 563	$\begin{array}{c} 755\\ 755\\ 658\\ 658\\ 618\\ 545\\ 545\\ 513\\ 513\\ 484 \end{array}$	664 615 575 539 539 506 447 447 422
PRESSURE	per Min.,	66	Final Temp.	$\begin{array}{c} 53.1 \\ 90.4 \\ 122.5 \\ 174.6 \\ 195.5 \\ 214.0 \\ 229.8 \end{array}$	$\begin{array}{c} 61.6\\97.9\\128.5\\155.8\\179.4\\199.7\\232.8\\232.8\end{array}$	$\begin{array}{c} 96.5\\ 127.6\\ 154.8\\ 178.5\\ 199.0\\ 216.7\\ 232.0\\ 245.7\end{array}$
JAUGE P	Vir In Ft. 1	400	B. t. u. per Lin. Ft. Per Hour	585 543 566 486 435 435 435 378 378 356	$\begin{array}{c} 568 \\ 525 \\ 485 \\ 485 \\ 452 \\ 421 \\ 393 \\ 368 \\ 345 \\ 345 \end{array}$	501 456 395 395 368 368 368 368 368 368 368 368 368 368
ġ	Velocity of Air	4(	Final Temp.	$\begin{array}{c} 58.2\\ 99.5\\ 133.7\\ 163.5\\ 163.5\\ 209.5\\ 228.3\\ 244.9\end{array}$	$\begin{array}{c} 66.8\\ 106.6\\ 140.0\\ 169.0\\ 193.6\\ 214.3\\ 232.3\\ 247.5\end{array}$	$\begin{array}{c} 101.3\\ 135.2\\ 164.4\\ 211.6\\ 229.9\\ 245.5\\ 258.8\\ \end{array}$
	Velo	200	B. t. u. per Lin. Ft. Per Hour	$334 \\ 334 \\ 239 \\ 259 \\ 221 \\ 221 \\ 221 \\ 221 \\ 221 \\ 222 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 \\ 192 $	$\begin{array}{c} 324\\ 298\\ 251\\ 251\\ 251\\ 232\\ 214\\ 199\\ 186\end{array}$	285 260 239 239 239 239 239 239 175 175 162
		2(	Final Temp.	$\begin{array}{c} 65.0\\ 1111.1\\ 149.0\\ 181.0\\ 207.3\\ 228.8\\ 247.3\\ 262.8\\ \end{array}$	$\begin{array}{c} 73.4\\ 118.3\\ 154.9\\ 185.7\\ 211.1\\ 232.0\\ 2550.0\\ 265.0\end{array}$	$\begin{array}{c} 107.0\\ 145.6\\ 178.0\\ 205.0\\ 227.0\\ 245.5\\ 261.6\\ 274.3\\ \end{array}$
	L	iatei eatei	No. of He	-004500-0	-01004-000-00	-00400200
		lo Air	Temp. Entering	00	20°	60°

# BUFFALO HEATER TABLES

10016

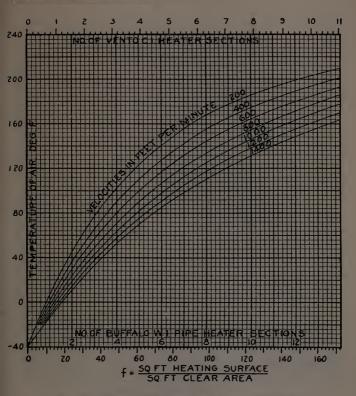
TEMPERATURE OBTAINED WITH BUFFALO STANDARD HEATERS

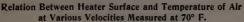


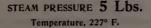
> STEAM PRESSURE 0 Lbs. Temperature, 212° F.

Application of Heater Curves. For example, the air enters the heating coils at 5 deg. above zero, with a velocity through the clear area of 1000 ft. per min. What will be the final air temperature with a Buffalo standard pipe coil heater, seven sections deep? Follow dotted line from + 5 deg. to 1.6 sections on bottom edge. Adding 7 sections gives 8.6 sections. Following

#### HEATER CURVES

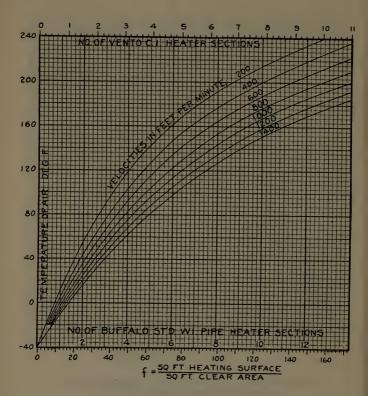




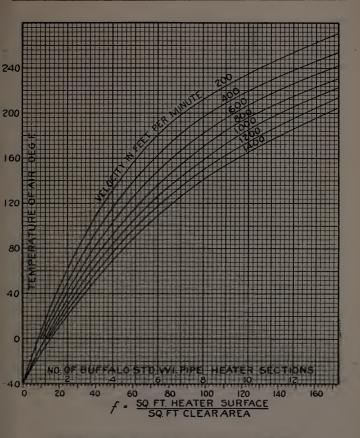


dotted line upward to 1000 velocity curve and to left edge gives final temperature of 124 deg. Reverse this process where the depth of heater is required for a given temperature rise.

For more complete directions see "Application of Heater Tables and Curves" on page 415.

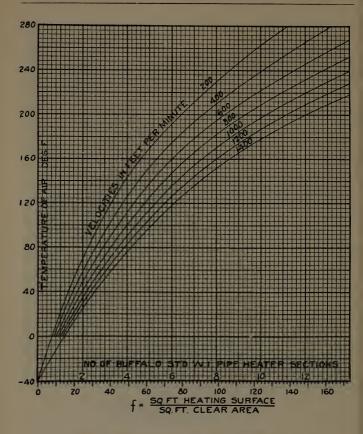


# STEAM PRESSURE 20 Lbs. Temperature, 258.8° F.



STEAM PRESSURE 40 Lbs.

Temperature, 286.7° F.

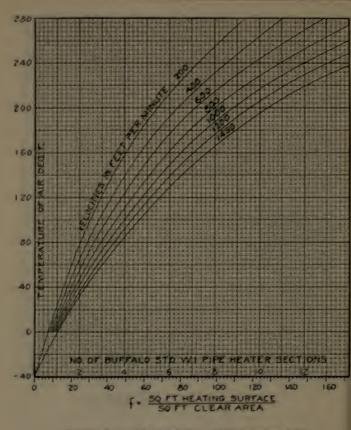


# STEAM PRESSURE 60 Lbs.

#### Temperature, 307.3° F.



> STEAM PRESSURE 80 Lbs. Temperature, 323.7° F.



STEAM PRESSURE 100 Lbs.

Temperature, 337.6* F.

#### FINAL TEMPERATURES WITH VENTO CAST IRON HEATERS REGULAR SECTION-45%-INCH CENTERS OF LOOPS STEAM 227°, 5 LBS. GAUGE

3	1	Ve	elocity	Throu	gh Hea	ter in	Ft. per	Min.	Measu	red at 1	70°
Stack	re of Air	60		80	00	10	00	120	00	14	00
Number of Stacks Deep	Temperature of Entering Air	Final Temp. Air Leaving Heater	Cond. Lbs. per Sq. Ft. per Hour	F. T.	C.	F. T.	с.	F. T.	с.	F. T.	c.
1	$-20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70$	$\begin{array}{c} 31 \\ 46 \\ 62 \\ 77 \\ 93 \\ 100 \end{array}$	$1.66 \\ 1.50 \\ 1.37 \\ 1.21 \\ 1.07 \\ .98$	42 57 73 89 97	$1.82 \\ 1.61 \\ 1.43 \\ 1.26 \\ 1.17$	38 54 70 87 95	2.06 1.85 1.63 1.47 1.36	35 52 68 85 93	2.28 2.08 1.82 1.63 1.50	$33 \\ 50 \\ 66 \\ 83 \\ 91$	$2.51 \\ 2.28 \\ 1.98 \\ 1.75 \\ 1.60$
2	-20 0 +20 +40 +60 +70	$70 \\ 82 \\ 94 \\ 106 \\ 118 \\ 124$	1.47 1.34 1.21 1.07 .94 .88	63 75 87 100 112 119	$     1.80 \\     1.63 \\     1.46 \\     1.30 \\     1.13 \\     1.06   $	57 69 82 95 108 115	$\begin{array}{r} 2.09 \\ 1.87 \\ 1.68 \\ 1.49 \\ 1.30 \\ 1.22 \end{array}$	$51 \\ 65 \\ 78 \\ 91 \\ 105 \\ 112$	$2.31 \\ 2.11 \\ 1.89 \\ 1.66 \\ 1.46 \\ 1.37$	47 61 75 88 102 109	$\begin{array}{r} 2.55 \\ 2.32 \\ 2.09 \\ 1.82 \\ 1.60 \\ 1.48 \end{array}$
3	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \\ \end{array} $	100 110 119 128 137 141	1.30 1.20 1.07 .96 .84 .77	$91 \\ 101 \\ 110 \\ 120 \\ 130 \\ 135$	1.61 1.46 1.30 1.16 1.01 .94	84 94 104 115 125 131	$     1.88 \\     1.70 \\     1.52 \\     1.36 \\     1.18 \\     1.10   $	78 89 98 110 121 127	$\begin{array}{r} 2.13 \\ 1.93 \\ 1.69 \\ 1.52 \\ 1.33 \\ 1.24 \end{array}$	72 84 94 106 118 124	2.33 2.13 1.87 1.67 1.47 1.37
4	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60 \\       +70     \end{array} $	$123 \\ 131 \\ 138 \\ 145 \\ 152 \\ 156$	$     \begin{array}{r}       1.16 \\       1.07 \\       .96 \\       .86 \\       .75 \\       .70 \\       \end{array} $	$     \begin{array}{r}       114 \\       122 \\       130 \\       138 \\       146 \\       150     \end{array} $	$\begin{array}{r} 1.46 \\ 1.32 \\ 1.20 \\ 1.06 \\ .93 \\ .87 \end{array}$	$     \begin{array}{r}       105 \\       114 \\       123 \\       132 \\       140 \\       145     \end{array} $	$     1.70 \\     1.55 \\     1.41 \\     1.25 \\     1.09 \\     1.02   $	99 108 117 126 135 140	$     1.94 \\     1.76 \\     1.58 \\     1.40 \\     1.22 \\     1.14   $	$93 \\103 \\112 \\122 \\131 \\136$	$\begin{array}{r} 2.15 \\ 1.96 \\ 1.75 \\ 1.56 \\ 1.35 \\ 1.25 \end{array}$
5	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60     \end{array} $	$     \begin{array}{r}       142 \\       147 \\       152 \\       158 \\       164 \\     \end{array} $	1.05 .96 .86 .77 .68	$     \begin{array}{r}       132 \\       138 \\       144 \\       151 \\       158 \\       158     \end{array} $	$\begin{array}{c} 1.32 \\ 1.20 \\ 1.08 \\ .96 \\ .85 \end{array}$	124 131 137 145 152	$     \begin{array}{r}       1.56 \\       1.42 \\       1.27 \\       1.14 \\       1.00 \\       \end{array} $	$     \begin{array}{r}       116 \\       124 \\       131 \\       139 \\       147     \end{array} $	$     \begin{array}{r}       1.77 \\       1.61 \\       1.45 \\       1.29 \\       1.13     \end{array} $	$     \begin{array}{r}       110 \\       118 \\       126 \\       135 \\       143     \end{array} $	$     \begin{array}{r}       1.98 \\       1.79 \\       1.61 \\       1.44 \\       1.26     \end{array} $
6	$-20 \\ 0 \\ +20 \\ +40$	155 160 164 170	.95 .87 .78 .71	$     \begin{array}{r}       146 \\       152 \\       156 \\       162     \end{array} $	1.20 1.10 .99 .88	139 145 150 156	$1.44 \\ 1.31 \\ 1.18 \\ 1.05$	132 138 144 151	$     \begin{array}{r}       1.65 \\       1.50 \\       1.35 \\       1.20 \\     \end{array} $	$     \begin{array}{r}       125 \\       132 \\       139 \\       146     \end{array} $	$     \begin{array}{r}       1.83 \\       1.67 \\       1.51 \\       1.34     \end{array} $
7	- 20	167	.87	158	1.10	150	1.32	144	1.53	138	1.72
		1		1		1					

#### FINAL TEMPERATURES WITH VENTO CAST IRON HEATERS REGULAR SECTION—5-INCH CENTERS OF LOOPS STEAM 227°, 5 LBS. GAUGE

ks		Vel	locity 1	Throug	h Heat	er in F	t. per	Min. M	leasur	ed at 7	0°
Stac	re o Air	-	00	8	00	10	00	12	00	14	00
Number of Stacks Deep	Temperature of Entering Air	Final Temp. Air Leaving Heater	Cond. Lbs. per Sq. Ft. per Hour	F. T.	c.	F. T.	c.	F. T.	с.	F. T.	с.
1	0 + 20 + 40 + 60 + 70	43 58 74 90 97	$1.65 \\ 1.46 \\ 1.31 \\ 1.15 \\ 1.04$	38 54 70 86 94	$1.95 \\ 1.75 \\ 1.54 \\ 1.34 \\ 1.23$	35 51 68 84 92	2.24 1.99 1.80 1.54 1.41	32 49 66 82 90	2.46 2.23 2.00 1.69 1.54	47 64 81 89	2.42 2.16 1.89 1.71
2	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60 \\       +70     \end{array} $	63 75 87 100 112 118	$1.60 \\ 1.44 \\ 1.29 \\ 1.15 \\ 1.00 \\ .92$	55 68 81 94 107 114	$1.92 \\ 1.74 \\ 1.57 \\ 1.39 \\ 1.21 \\ 1.13$	49 62 76 90 103 110	$\begin{array}{r} 2.22 \\ 1.99 \\ 1.80 \\ 1.60 \\ 1.38 \\ 1.28 \end{array}$	$     \begin{array}{r}             44 \\             58 \\             72 \\             86 \\             100 \\             107         \end{array}     $	$\begin{array}{r} 2.46 \\ 2.23 \\ 2.00 \\ 1.77 \\ 1.54 \\ 1.42 \end{array}$	$     \begin{array}{r}       40 \\       54 \\       69 \\       83 \\       98 \\       105     \end{array} $	$\begin{array}{r} 2.69 \\ 2.42 \\ 2.20 \\ 1.93 \\ 1.71 \\ 1.57 \end{array}$
3	$-20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70$	91 101 110 121 131 136	$1.42 \\ 1.30 \\ 1.15 \\ 1.04 \\ .91 \\ .85$	82 93 103 114 124 130	$1.74 \\ 1.59 \\ 1.42 \\ 1.26 \\ 1.09 \\ 1.03$	75 86 97 109 120 126	$\begin{array}{r} 2.03 \\ 1.84 \\ 1.65 \\ 1.47 \\ 1.28 \\ 1.20 \end{array}$	69 81 92 104 116 122	$2.28 \\ 2.08 \\ 1.85 \\ 1.64 \\ 1.44 \\ 1.34$	64 76 88 100 113 119	$2.51 \\ 2.27 \\ 2.06 \\ 1.79 \\ 1.58 \\ 1.46$
4	$-20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70$	$114 \\ 121 \\ 130 \\ 138 \\ 146 \\ 150$	$     \begin{array}{r}       1.29 \\       1.16 \\       1.06 \\       .94 \\       .83 \\       .77     \end{array} $	$     \begin{array}{r}       103 \\       113 \\       122 \\       130 \\       139 \\       143     \end{array} $	$1.58 \\ 1.45 \\ 1.31 \\ 1.15 \\ 1.01 \\ .94$	96 106 115 124 134 138	$1.86 \\ 1.70 \\ 1.52 \\ 1.35 \\ 1.19 \\ 1.09$	$90 \\ 100 \\ 110 \\ 119 \\ 129 \\ 134$	$\begin{array}{r} 2.12 \\ 1.92 \\ 1.73 \\ 1.52 \\ 1.33 \\ 1.23 \end{array}$	84 95 105 115 125 131	$2.34 \\ 2.13 \\ 1.91 \\ 1.68 \\ 1.46 \\ 1.37$
5	-20 0 +20 +40 +60 +70	$     \begin{array}{r}       132 \\       138 \\       144 \\       151 \\       158 \\       162     \end{array} $	$     \begin{array}{r}       1.17 \\       1.06 \\       .95 \\       .85 \\       .75 \\       .71     \end{array} $	$     \begin{array}{r}       122 \\       129 \\       136 \\       144 \\       151 \\       155 \\       \end{array} $	$1.46 \\ 1.32 \\ 1.19 \\ 1.07 \\ .93 \\ .87$	$     \begin{array}{r}       114 \\       122 \\       130 \\       138 \\       145 \\       149 \\       149     \end{array} $	$     \begin{array}{r}       1.72 \\       1.56 \\       1.41 \\       1.26 \\       1.09 \\       1.01     \end{array} $	$     \begin{array}{r}       107 \\       115 \\       124 \\       132 \\       140 \\       144     \end{array} $	$     \begin{array}{r}       1.95 \\       1.77 \\       1.60 \\       1.42 \\       1.23 \\       1.14     \end{array} $	100 109 119 127 136 141	$2.15 \\ 1.96 \\ 1.78 \\ 1.56 \\ 1.36 \\ 1.27$
6	-20 0 +20 +40 +60	$     \begin{array}{r}       146 \\       152 \\       156 \\       162 \\       167 \\       \hline       167 \\       \hline       156 \\       167 \\       \hline       157 \\       167 \\       \hline       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       167 \\       156 \\       156 \\       167 \\       156 \\       167 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 \\       156 $	1.06 .97 .87 .78 .69	$     \begin{array}{r}       137 \\       143 \\       148 \\       154 \\       160 \\       \hline       155       \end{array} $	$1.34 \\ 1.22 \\ 1.10 \\ .97 \\ .85$	$     \begin{array}{r}       129 \\       135 \\       142 \\       148 \\       155 \\       \hline     \end{array} $	$1.59 \\ 1.44 \\ 1.30 \\ 1.15 \\ 1.02$	$     \begin{array}{r}       121 \\       129 \\       136 \\       143 \\       150 \\       \hline       129 \\       136 \\       143 \\       150 \\       \hline       121 \\       143 \\       150 \\       121 \\       129 \\       136 \\       143 \\       150 \\       121 \\       129 \\       136 \\       143 \\       150 \\       121 \\       129 \\       136 \\       143 \\       150 \\       121 \\       129 \\       136 \\       143 \\       150 \\       121 \\       121 \\       129 \\       136 \\       143 \\       150 \\       121 \\       121 \\       129 \\       121 \\       121 \\       129 \\       121 \\       129 \\       136 \\       143 \\       150 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\       121 \\   $	$     \begin{array}{r}       1.81 \\       1.65 \\       1.49 \\       1.32 \\       1.15 \\       \hline       1.15     \end{array} $	$     \begin{array}{r}       115 \\       123 \\       130 \\       138 \\       146 \\       \hline       138     \end{array} $	2.02 1.84 1.65 1.47 1.29
7	$-20 \\ 0 \\ +20 \\ +40$	159 163 167 171	.98 .90 .81 .72	$150 \\ 154 \\ 159 \\ 164$	$1.25 \\ 1.13 \\ 1.02 \\ .91$	$141 \\ 147 \\ 152 \\ 158$	$1.47 \\ 1.35 \\ 1.21 \\ 1.08$	$134 \\ 140 \\ 146 \\ 153$	$1.69 \\ 1.54 \\ 1.39 \\ 1.24$	$     \begin{array}{r}       128 \\       135 \\       141 \\       148     \end{array}   $	$1.90 \\ 1.73 \\ 1.55 \\ 1.39$
8	$-20 \\ 0 \\ +20 \\ +40$	168 172 175 179	.90 .83 .75 .67	159 164 167 171	1.15 1.05 .94 .84	$     \begin{array}{r}       151 \\       156 \\       161 \\       165     \end{array} $	$1.37 \\ 1.25 \\ 1.13 \\ 1.00$	144 150 155 160	$1.58 \\ 1.44 \\ 1.30 \\ 1.15$	138 144 150 155	$1.77 \\ 1.62 \\ 1.46 \\ 1.29$

## FINAL TEMPERATURES WITH VENTO CAST IRON HEATERS REGULAR SECTION-53/-INCH CENTERS OF LOOPS STEAM 227°, 5 LBS. GAUGE

S	Ī.,	Ve	locity	Throug	gh Hea	ter in	Ft. per	Min.	Measur	red at 70°	
tack	e of Air	6	00	8	00	10	00	12	00	14	00
Number of Stacks Deep	Temperature of Entering Air	Final Temp. Air Leaving Heater	Cond. Lbs. per Sq. Ft. per Hour	F. T.	c.	F. T.	c.	F. T.	c.	F. T.	c.
1	0 +20 +40 +60 +70	34 51 68 85 93	$1.54 \\ 1.40 \\ 1.27 \\ 1.13 \\ 1.04$	32 48 65 82 90	$1.93 \\ 1.69 \\ 1.51 \\ 1.33 \\ 1.21$	46 63 80 88	$1.96 \\ 1.73 \\ 1.51 \\ 1.36$	44 61 78 87	2.17 1.90 1.63 1.54	42 59 77 86	2.32 2.01 1.79 1.69
2	-20 0 +20 +40 +60 +70	49 62 76 90 104 110	$1.56 \\ 1.40 \\ 1.27 \\ 1.13 \\ 1.00 \\ .91$	43 57 71 85 99 106	$1.90 \\ 1.72 \\ 1.54 \\ 1.36 \\ 1.18 \\ 1.08$	38 52 67 82 96 103	$\begin{array}{r} 2.19 \\ 1.96 \\ 1.77 \\ 1.58 \\ 1.36 \\ 1.25 \end{array}$	34 48 64 79 94 101	2.44 2.17 1.99 1.76 1.54 1.40	45 61 76 92 99	2.382.161.901.691.53
3	-20 0 +20 +40 +60 +70	76 87 98 109 120 126	$     \begin{array}{r}       1.45 \\       1.31 \\       1.18 \\       1.04 \\       .90 \\       .84     \end{array} $	68 80 91 103 115 121	$ \begin{array}{r} 1.77\\ 1.61\\ 1.43\\ 1.27\\ 1.11\\ 1.03 \end{array} $	61 74 85 98 111 118	$\begin{array}{r} 2.04 \\ 1.86 \\ 1.63 \\ 1.46 \\ 1.28 \\ 1.21 \end{array}$	56 69 81 94 108 115	$\begin{array}{r} 2.29 \\ 2.08 \\ 1.84 \\ 1.63 \\ 1.45 \\ 1.36 \end{array}$	51 65 78 91 105 112	$\begin{array}{r} 2.50 \\ 2.25 \\ 2.04 \\ 1.79 \\ 1.58 \\ 1.48 \end{array}$
4	-20 0 +20 +40 +60 +70	97 105 115 125 135 140	$1.32 \\ 1.19 \\ 1.07 \\ .96 \\ .85 \\ .79$	88 97 108 118 128 133	$     \begin{array}{r}       1.63 \\       1.46 \\       1.33 \\       1.18 \\       1.02 \\       .95     \end{array} $	80 91 101 112 123 129	$     1.89 \\     1.72 \\     1.53 \\     1.36 \\     1.19 \\     1.11 $	74 86 96 108 119 125	$\begin{array}{r} 2.13 \\ 1.95 \\ 1.72 \\ 1.54 \\ 1.34 \\ 1.25 \end{array}$	69 81 92 104 116 122	$\begin{array}{r} 2.34 \\ 2.14 \\ 1.90 \\ 1.69 \\ 1.48 \\ 1.37 \end{array}$
5	-20 0 +20 +40 +60 +70	116 124 131 139 147 151	1.23 1.12 1.00 .89 .79 .73	106     115     123     131     140     145	$\begin{array}{r} 1.52 \\ 1.39 \\ 1.24 \\ 1.10 \\ .96 \\ .90 \end{array}$	98 107 117 126 135 140	$     1.78 \\     1.61 \\     1.46 \\     1.30 \\     1.13 \\     1.05   $	91 101 111 121 130 135	$2.01 \\ 1.83 \\ 1.65 \\ 1.46 \\ 1.26 \\ 1.17$	86 96 106 116 126 132	$\begin{array}{r} 2.24 \\ 2.03 \\ 1.82 \\ 1.60 \\ 1.39 \\ 1.31 \end{array}$
6	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \\ \end{array} $	$     \begin{array}{r}       131 \\       138 \\       144 \\       150 \\       157 \\       160     \end{array} $	$     1.14 \\     1.04 \\     .93 \\     .83 \\     .73 \\     .68   $	$     \begin{array}{r}       121 \\       128 \\       136 \\       143 \\       150 \\       154     \end{array} $	1.42 1.29 1.17 1.04 .91 .85	112 120 129 137 145 149	$\begin{array}{r} 1.66 \\ 1.51 \\ 1.37 \\ 1.22 \\ 1.07 \\ .99 \end{array}$	$     \begin{array}{r}       106 \\       114 \\       123 \\       132 \\       140 \\       145     \end{array} $	$\begin{array}{r} 1.90 \\ 1.72 \\ 1.55 \\ 1.39 \\ 1.21 \\ 1.13 \end{array}$	100 108 118 127 136 141	$\begin{array}{r} 2.11 \\ 1.90 \\ 1.72 \\ 1.53 \\ 1.34 \\ 1.25 \end{array}$
7	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \\ \end{array} $	$     \begin{array}{r}       145 \\       151 \\       153 \\       159 \\       165 \\       168 \\     \end{array} $	1.07 .98 .86 .77 .68 .63	$     \begin{array}{r} 135 \\     141 \\     146 \\     152 \\     158 \\     162 \\     \end{array} $	1.34 1.21 1.09 .96 .84 .79	$     \begin{array}{r}       127 \\       133 \\       140 \\       146 \\       153 \\       157     \end{array} $	$\begin{array}{r} 1.58 \\ 1.43 \\ 1.29 \\ 1.14 \\ 1.00 \\ .94 \end{array}$	$     \begin{array}{r}       120 \\       127 \\       134 \\       140 \\       148 \\       152     \end{array} $	$\begin{array}{r} 1.81 \\ 1.64 \\ 1.47 \\ 1.29 \\ 1.14 \\ 1.06 \end{array}$	$     113 \\     121 \\     129 \\     136 \\     144 \\     148   $	$\begin{array}{r} 2.00 \\ 1.82 \\ 1.64 \\ 1.45 \\ 1.27 \\ 1.18 \end{array}$
8	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60     \end{array} $	$     \begin{array}{r}       155 \\       160 \\       164 \\       169 \\       173     \end{array} $	.99 .90 .81 .73 .64	146 151 156 161 166	1.25 1.14 1.03 .91 .80	138 144 149 155 160	1.49 1.36 1.22 1.08 .94	131 137 143 149 155	$     \begin{array}{r}       1.71 \\       1.55 \\       1.39 \\       1.24 \\       1.07 \\     \end{array} $	125 131 138 144 151	$     \begin{array}{r}       1.91 \\       1.73 \\       1.56 \\       1.37 \\       1.20 \\       \end{array} $

#### FINAL TEMPERATURES WITH VENTO CAST IRON HEATERS NARROW SECTION-4%-INCH CENTERS OF LOOPS STEAM 227°, 5 LBS. GAUGE

ks		Ve	locity	Throug	gh Hea	ter in	Ft. per	Min.	Neasu	ed at 2	70°
Stacl	re ol Air	6(	00	80	00	10	00	12	00	14	00
Number of Stacks Deep	Temperature of Entering Air	Final Temp. Air Leaving Heater	Cond. Lbs. per Sq. Ft. per Hour	F. T.	c.	F. T.	c.	F. T.	с.	F. T.	C.
1	0 + 20 + 40 + 60 + 70	34 51 67 84 92	$1.59 \\ 1.45 \\ 1.27 \\ 1.13 \\ 1.03$	47 64 81 90	$1.68 \\ 1.49 \\ 1.31 \\ 1.25$	45 62 79 88	$1.95 \\ 1.72 \\ 1.49 \\ 1.40$	43 60 78 87	2.15 1.87 1.68 1.59	41 59 77 86	2.30 2.08 1.86 1.75
2	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60 \\       +70     \end{array} $	$ \begin{array}{r}     48 \\     62 \\     76 \\     90 \\     104 \\     111 \end{array} $	$1.59 \\ 1.45 \\ 1.31 \\ 1.17 \\ 1.03 \\ .96$	42 56 70 85 99 106	$1.94 \\ 1.75 \\ 1.56 \\ 1.40 \\ 1.22 \\ 1.13$	$37 \\ 51 \\ 66 \\ 82 \\ 96 \\ 103$	$2.22 \\ 1.99 \\ 1.80 \\ 1.64 \\ 1.41 \\ 1.29$	33 47 63 79 94 101	$\begin{array}{r} 2.48 \\ 2.20 \\ 2.02 \\ 1.83 \\ 1.59 \\ 1.45 \end{array}$	44 60 76 92 99	$2.40 \\ 2.19 \\ 1.97 \\ 1.74 \\ 1.59$
3	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60 \\       +70     \end{array} $	74 85 96 108 120 126	$1.47 \\ 1.33 \\ 1.19 \\ 1.06 \\ .94 \\ .87$	66 78 89 101 114 120	$     \begin{array}{r}       1.79 \\       1.62 \\       1.44 \\       1.27 \\       1.13 \\       1.04     \end{array} $	59 71 84 97 110 116	$\begin{array}{r} 2.06 \\ 1.85 \\ 1.66 \\ 1.48 \\ 1.30 \\ 1.20 \end{array}$	$54 \\ 66 \\ 80 \\ 93 \\ 106 \\ 113$	$2.31 \\ 2.06 \\ 1.87 \\ 1.65 \\ 1.44 \\ 1.34$	49 62 76 90 103 110	$2.51 \\ 2.26 \\ 2.04 \\ 1.82 \\ 1.57 \\ 1.46$
4	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \end{array} $	95 104 113 123 133 138	$\begin{array}{r} 1.35 \\ 1.22 \\ 1.09 \\ .97 \\ .86 \\ .80 \end{array}$	86 96 106 117 127 132	$1.66 \\ 1.50 \\ 1.34 \\ 1.20 \\ 1.05 \\ .97$	79 90 100 112 122 128	$     \begin{array}{r}       1.93 \\       1.75 \\       1.56 \\       1.40 \\       1.21 \\       1.13     \end{array} $	73 84 95 107 118 124	$2.18 \\ 1.97 \\ 1.76 \\ 1.57 \\ 1.36 \\ 1.27$	67 79 91 103 115 121	$2.38 \\ 2.16 \\ 1.94 \\ 1.72 \\ 1.50 \\ 1.39$
5	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \end{array} $	$     \begin{array}{r}       113 \\       120 \\       127 \\       137 \\       145 \\       150     \end{array} $	$\begin{array}{r} 1.25 \\ 1.13 \\ 1.00 \\ .90 \\ .80 \\ .75 \end{array}$	$     \begin{array}{r}       103 \\       112 \\       120 \\       130 \\       139 \\       144     \end{array} $	$\begin{array}{r} 1.54 \\ 1.40 \\ 1.25 \\ 1.12 \\ .98 \\ .91 \end{array}$	$     \begin{array}{r}       95 \\       104 \\       114 \\       124 \\       134 \\       139     \end{array} $	$\begin{array}{r} 1.79 \\ 1.62 \\ 1.47 \\ 1.31 \\ 1.16 \\ 1.08 \end{array}$	88 98 109 119 129 134	$\begin{array}{r} 2.02 \\ 1.84 \\ 1.67 \\ 1.48 \\ 1.29 \\ 1.20 \end{array}$	$     \begin{array}{r}                                     $	$\begin{array}{r} 2.23 \\ 2.01 \\ 1.84 \\ 1.64 \\ 1.42 \\ 1.33 \end{array}$
6	$-20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70$	$127 \\ 134 \\ 140 \\ 148 \\ 155 \\ 159$	$1.15 \\ 1.05 \\ .94 \\ .84 \\ .74 \\ .69$	$     \begin{array}{r}       117 \\       125 \\       132 \\       140 \\       148 \\       152     \end{array} $	$1.43 \\ 1.30 \\ 1.17 \\ 1.04 \\ .92 \\ .85$	$     \begin{array}{r}       109 \\       118 \\       125 \\       134 \\       142 \\       147     \end{array} $	$\begin{array}{r} 1.68 \\ 1.53 \\ 1.37 \\ 1.22 \\ 1.07 \\ 1.00 \end{array}$	$     \begin{array}{r}       103 \\       112 \\       119 \\       128 \\       137 \\       142     \end{array} $	$     \begin{array}{r}       1.92 \\       1.75 \\       1.55 \\       1.37 \\       1.20 \\       1.12     \end{array} $	$97 \\ 106 \\ 114 \\ 124 \\ 133 \\ 138$	$2.13 \\ 1.93 \\ 1.71 \\ 1.53 \\ 1.33 \\ 1.24$
7	$-20 \\ 0 \\ +20$	$     \begin{array}{r}       140 \\       146 \\       151     \end{array} $	1.07 .98 .88	$130 \\ 136 \\ 143$	1.34 1.21 1.10	$     \begin{array}{r}       121 \\       129 \\       136     \end{array} $	1.58 1.44 1.30	$     \begin{array}{r}       114 \\       122 \\       130     \end{array} $	1.80 1.63 1.47	$     \begin{array}{r}       108 \\       116 \\       125     \end{array} $	$2.00 \\ 1.81 \\ 1.64$
8	$-20 \\ 0$	150 155	1.00 .91	141 146	1.26 1.14	133 138	$1.49 \\ 1.35$	125 132	1.70 1.55	119 126	1.90 1.72

## VENTO HEATER TABLES

#### FINAL TEMPERATURE WITH VENTO CAST IRON HEATERS NARROW SECTION-5-INCH CENTERS OF LOOPS STEAM 227°, 5 LBS. GAUGE

s		Ve	locity '	Throug	h Hea	ter in l	Ft. per	Min. M	leasur	sured at 70°		
itack	re of Air	6	00	80	0	10	00	12	00	14	00	
Number of Stacks Deep	Temperature of Entering Air	Final Temp. Air Leaving Heater	Cond. Lbs. per Sq. Ft. per Hour	F. T.	c.	F. T.	с.	F. T.	с.	F. T.	C.	
1	+20 +40 +60 +70	47 64 82 90	$1.49 \\ 1.33 \\ 1.22 \\ 1.11$	45 62 80 88	$1.84 \\ 1.62 \\ 1.47 \\ 1.33$	43 60 78 86	2.12 1.84 1.66 1.47	41 58 76 85	$2.32 \\ 1.99 \\ 1.77 \\ 1.66$	39 57 75 84	2.45 2.19 1.94 1.81	
2	-20 0 +20 +40 +60 +70	41 56 70 85 99 106	$     \begin{array}{r}       1.69 \\       1.55 \\       1.38 \\       1.24 \\       1.08 \\       1.00 \\       \end{array} $	$     \begin{array}{r}       36 \\       51 \\       65 \\       80 \\       95 \\       102     \end{array} $	$\begin{array}{c} 2.06 \\ 1.88 \\ 1.66 \\ 1.47 \\ 1.29 \\ 1.18 \end{array}$	$31 \\ 46 \\ 62 \\ 77 \\ 92 \\ 100$	$2.35 \\ 2.12 \\ 1.93 \\ 1.70 \\ 1.47 \\ 1.38$	43 59 74 90 98	$2.38 \\ 2.16 \\ 1.88 \\ 1.66 \\ 1.55$	40 56 72 88 96	2.58 2.32 2.06 1.81 1.68	
3	$   \begin{array}{r}     -20 \\     0 \\     +20 \\     +40 \\     +60 \\     +70   \end{array} $	$ \begin{array}{r} 65 \\ 77 \\ 90 \\ 102 \\ 114 \\ 120 \end{array} $	$\begin{array}{r} 1.57 \\ 1.42 \\ 1.29 \\ 1.14 \\ .99 \\ .92 \end{array}$	58 70 84 97 109 115	$     \begin{array}{r}       1.92 \\       1.72 \\       1.57 \\       1.40 \\       1.20 \\       1.10 \\     \end{array} $	$52 \\ 65 \\ 79 \\ 92 \\ 105 \\ 112$	$\begin{array}{r} 2.21 \\ 2.00 \\ 1.81 \\ 1.60 \\ 1.38 \\ 1.29 \end{array}$	47 61 75 88 102 109	$\begin{array}{r} 2.47 \\ 2.25 \\ 2.03 \\ 1.77 \\ 1.55 \\ 1.44 \end{array}$	43 57 71 85 100 107	$2.71 \\ 2.45 \\ 2.19 \\ 1.94 \\ 1.72 \\ 1.59$	
4	$   \begin{array}{r}     -20 \\     0 \\     +20 \\     +40 \\     +60 \\     +70   \end{array} $	86 96 106 117 127 132	$1.46 \\ 1.33 \\ 1.19 \\ 1.06 \\ .93 \\ .86$	77 88 99 110 121 127	$     \begin{array}{r}       1.79 \\       1.62 \\       1.46 \\       1.29 \\       1.12 \\       1.05 \\     \end{array} $	70 82 93 105 117 123	$\begin{array}{r} 2.07 \\ 1.89 \\ 1.68 \\ 1.50 \\ 1.31 \\ 1.22 \end{array}$	64 77 88 101 113 119	$\begin{array}{r} 2.32 \\ 2.13 \\ 1.88 \\ 1.69 \\ 1.47 \\ 1.36 \end{array}$	59 72 84 98 110 116	$\begin{array}{r} 2.55 \\ 2.32 \\ 2.06 \\ 1.87 \\ 1.61 \\ 1.48 \end{array}$	
5	-20 0 +20 +40 +60 +70	$     \begin{array}{r}       102 \\       111 \\       120 \\       129 \\       138 \\       142     \end{array} $	$1.35 \\ 1.23 \\ 1.10 \\ .98 \\ .86 \\ .80$	93 103 113 122 132 136	$1.67 \\ 1.52 \\ 1.37 \\ 1.21 \\ 1.06 \\ .97$	86 96 106 117 127 132	$     \begin{array}{r}       1.95 \\       1.77 \\       1.58 \\       1.42 \\       1.23 \\       1.14     \end{array} $	79 90 101 112 123 128	$\begin{array}{r} 2.19 \\ 1.99 \\ 1.79 \\ 1.59 \\ 1.39 \\ 1.28 \end{array}$	$74 \\ 85 \\ 96 \\ 108 \\ 119 \\ 125$	$\begin{array}{r} 2.43 \\ 2.20 \\ 1.96 \\ 1.76 \\ 1.52 \\ 1.42 \end{array}$	
6	$     \begin{array}{r}       -20 \\       0 \\       +20 \\       +40 \\       +60 \\       +70     \end{array} $	$     \begin{array}{r}       116 \\       124 \\       132 \\       140 \\       148 \\       152     \end{array} $	$1.25 \\ 1.14 \\ 1.03 \\ .92 \\ .81 \\ .76$	$     \begin{array}{r}       107 \\       115 \\       124 \\       133 \\       142 \\       146     \end{array} $	$     \begin{array}{r}       1.56 \\       1.41 \\       1.28 \\       1.14 \\       1.01 \\       .93     \end{array} $	99 108 118 127 137 141	$1.83 \\ 1.66 \\ 1.51 \\ 1.34 \\ 1.18 \\ 1.09$	$92 \\ 102 \\ 112 \\ 122 \\ 132 \\ 136$	$\begin{array}{c} 2.06 \\ 1.88 \\ 1.70 \\ 1.51 \\ 1.33 \\ 1.22 \end{array}$	87 97 107 118 128 133	$\begin{array}{r} 2.30 \\ 2.09 \\ 1.87 \\ 1.68 \\ 1.46 \\ 1.36 \end{array}$	
7	$-20 \\ 0 \\ +20 \\ +40$	$130 \\ 136 \\ 142 \\ 150$	1.18 1.07 .96 .87	120 127 134 142	1.47 1.34 1.20 1.07	$     \begin{array}{r}       112 \\       120 \\       128 \\       136     \end{array} $	$     \begin{array}{r}       1.74 \\       1.58 \\       1.42 \\       1.26     \end{array} $	105 114 122 131	1.97 1.80 1.61 1.43	99 108 117 126	2.19 1.99 1.79 1.59	
8	$-20 \\ 0 \\ +20$	$     \begin{array}{r}       140 \\       146 \\       152     \end{array} $	1.11 1.01 .91	130 137 144	$\frac{1.38}{1.26}\\1.14$	122 129 137	$1.64 \\ 1.49 \\ 1.35$	115 123 131	1.87 1.70 1.53	109 118 125	2.08 1.90 1.69	

# FINAL TEMPERATURES WITH VENTO CAST IRON HEATERS NARROW SECTION-5%-INCH CENTERS OF LOOPS STEAM 227°, 5 LBS. GAUGE

ks		-	elocit	y Thro	ough H	eater i	n Ft. p	er Min	. Meas	ured a	t 70°
Stac	Air o		500		800	1	000	1	200	1	400
Number of Stacks Deep	Temperature of Entering Air	Final Temp. Air Leaving Heater	Cond. Lbs. per Sq. Ft.	F. T	с.	F. T.	с.	F. T.	с.	F. T.	с.
1	$^{+20}_{+40}_{+60}_{+70}$	42 60 78 86	$1.43 \\ 1.30 \\ 1.17 \\ 1.04$	40 58 76 84	1.56	3 38 5 56 74 83	1.95 1.73 1.52 1.41	37 55 73 82	2.21 1.95 1.69 1.56	36 54 72 81	$2.43 \\ 2.12 \\ 1.82 \\ 1.67$
2	0 +20 +40 +60 +70	46 61 77 93 101	$1.50 \\ 1.33 \\ 1.20 \\ 1.07 \\ 1.01$	42 57 73 89 97	$1.82 \\ 1.60 \\ 1.43 \\ 1.26 \\ 1.17$	38 54 71 87 95	$2.06 \\ 1.84 \\ 1.68 \\ 1.46 \\ 1.35$	25	$2.27 \\ 2.08 \\ 1.88 \\ 1.63 \\ 1.50$	32 50 67 83 91	2.43 2.28 2.05 1.75 1.59
3	$\begin{array}{c} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \end{array}$	52 65 79 92 105 112	$1.56 \\ 1.41 \\ 1.28 \\ 1.13 \\ .98 \\ .91$	46 59 73 87 101 108	$ \begin{array}{r} 1.90\\ 1.70\\ 1.53\\ 1.36\\ 1.19\\ 1.10 \end{array} $	40	$\begin{array}{r} 2.17\\ 1.95\\ 1.77\\ 1.55\\ 1.34\\ 1.26\end{array}$	36 50 66 80 94 102	$\begin{array}{r} 2.43 \\ 2.17 \\ 2.00 \\ 1.73 \\ 1.47 \\ 1.39 \end{array}$	33 47 63 77 92 100	$   \begin{array}{r}     1.39 \\     \hline     2.68 \\     2.38 \\     2.17 \\     1.87 \\     1.62 \\     1.52 \\   \end{array} $
4	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \end{array} $	$71\\82\\94\\106\\118\\124$	$1.48 \\ 1.33 \\ 1.20 \\ 1.07 \\ .94 \\ .88$	$\begin{array}{r} 63 \\ 75 \\ 88 \\ 100 \\ 112 \\ 118 \end{array}$	$ \begin{array}{c c} 1.80\\ 1.63\\ 1.47\\ 1.30\\ 1.13\\ 1.04 \end{array} $	57     69     83     95     108     114	$\begin{array}{r} 2.08 \\ 1.87 \\ 1.71 \\ 1.49 \\ 1.30 \\ 1.19 \end{array}$	$     \begin{array}{r}       102 \\       52 \\       65 \\       78 \\       91 \\       104 \\       111     \end{array} $	$\begin{array}{r} 1.03\\ \hline 2.34\\ 2.11\\ 1.89\\ 1.66\\ 1.43\\ 1.33\\ \end{array}$	$   \begin{array}{r}     100 \\     47 \\     61 \\     74 \\     88 \\     101 \\     108   \end{array} $	2.54 2.32 2.05 1.82 1.56
5	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \end{array} $	88 98 107 117 128 133	$     \begin{array}{r}       1.41 \\       1.27 \\       1.13 \\       1.00 \\       .88 \\       .82     \end{array} $	79 90 100 111 123 128	$\begin{array}{c c} 1.72 \\ 1.56 \\ 1.39 \\ 1.23 \\ 1.09 \\ 1.00 \end{array}$	$72 \\ 83 \\ 94 \\ 106 \\ 118 \\ 124$	1.99 1.80 1.60 1.43 1.26 1.17	$     \begin{array}{r}         111 \\             \overline{66} \\             78 \\             90 \\             102 \\             114 \\             120 \\             \end{array}     $	$   \begin{array}{r}     1.33 \\     2.24 \\     2.03 \\     1.82 \\     1.61 \\     1.41 \\     1.30 \\   \end{array} $	$     \begin{array}{r}       108 \\       61 \\       73 \\       86 \\       98 \\       111 \\       117 \\       117       \\       7       7       7       7       7       $	$     \begin{array}{r}       1.44 \\       2.46 \\       2.22 \\       2.00 \\       1.76 \\       1.55 \\       1.43 \\       \hline       1.43     \end{array} $
6	$ \begin{array}{r} -20 \\ 0 \\ +20 \\ +40 \\ +60 \\ +70 \end{array} $	$     \begin{array}{r}       102 \\       110 \\       119 \\       128 \\       138 \\       143     \end{array} $	$1.32 \\ 1.19 \\ 1.07 \\ .95 \\ .85 \\ .79$	93 102 111 121 131 137	$\begin{array}{r} 1.63 \\ 1.47 \\ 1.31 \\ 1.17 \\ 1.03 \\ .97 \end{array}$	85 95 105 116 126 132	$     1.90 \\     1.72 \\     1.54 \\     1.37 \\     1.19 \\     1.12 $	79 89 100 111 122 128	$   \begin{array}{r}     1.30 \\     2.74 \\     1.93 \\     1.73 \\     1.54 \\     1.34 \\     1.25 \\   \end{array} $	73 84 96 107 118 124	$     \begin{array}{r}       1.43 \\       2.35 \\       2.12 \\       1.92 \\       1.70 \\       1.47 \\       1.37 \\       \end{array} $
7	-20 0 +20 +40 +60	115 123 131 139 147	$1.26 \\ 1.14 \\ 1.03 \\ .92 \\ .81$	$106 \\ 114 \\ 123 \\ 131 \\ 140$	$1.56 \\ 1.41 \\ 1.28 \\ 1.13 \\ .99$	98 107 117 126 135	$\begin{array}{c} 1.83 \\ 1.65 \\ 1.50 \\ 1.33 \\ 1.16 \end{array}$	91 101 111 121 130	$\begin{array}{c} 2.06 \\ 1.88 \\ 1.69 \\ 1.51 \\ 1.30 \end{array}$	86 96 106 116 126	$   \begin{array}{r}     1.37 \\     2.30 \\     2.08 \\     1.86 \\     1.65 \\     1.43   \end{array} $
8	-20 0 +20 +40	126 133 140 147	1.19 1.08 .98 .87	$     \begin{array}{r}       117 \\       124 \\       132 \\       140     \end{array} $	1.48 1.34 1.21 1.08	109 117 126 134	1.75 1.59 1.44 1.27	102 111 120 129	1.98 1.80 1.62 1.45	96 105 115 124	2.20 1.99 1.80 1.59



## Left-Hand Bottom Horizontal Discharge Fan Drawing Through Heater



Full Housing Top Horizontal Discharge Fan Blowing Air Through and Underneath Heater

Velocity through Clear				Number	Number of Sections			
rea	-	8	m	4	co.	9	2	80
300 500	$\begin{array}{c} 0.009\\ 0.015\\ 0.024\end{array}$	0.017 0.031 0.049	0.026 0.046 0.073	0.035 0.062 0.095	0.043 0.077 0.104	0.052 0.092 0.144	0.060 0.108 0.168	0.069
600 800	$\begin{array}{c} 0.035\\ 0.047\\ 0.061 \end{array}$	0.069 0.094 0.123	$\begin{array}{c} 0.104\\ 0.141\\ 0.184\end{array}$	$\begin{array}{c} 0.138 \\ 0.188 \\ 0.245 \end{array}$	0.173 0.235 0.306	0.207 0.282 0.368	$\begin{array}{c} 0.242\\ 0.329\\ 0.429\end{array}$	0.276 0.376 0.490
000 0001	0.078 0.096 0.116	$\begin{array}{c} 0.155\\ 0.191\\ 0.232\end{array}$	0.233 0.287 0.347	$\begin{array}{c} 0.311 \\ 0.382 \\ 0.463 \end{array}$	$\begin{array}{c} 0.388\\ 0.479\\ 0.579\end{array}$	$\begin{array}{c} 0.466\\ 0.574\\ 0.695 \end{array}$	0.544 0.670 0.810	0.621 0.621 0.765 0.765
1200 1300 1400	$\begin{array}{c} 0.138 \\ 0.162 \\ 0.187 \end{array}$	0.276 0.324 0.375	$\begin{array}{c} 0.414 \\ 0.486 \\ 0.562 \end{array}$	$\begin{array}{c} 0.551 \\ 0.648 \\ 0.750 \end{array}$	0.689 0.810 0.936	$\begin{array}{c} 0.827\\ 0.972\\ 1.124\end{array}$	0.965	1.103
1500 1600 1700	$\begin{array}{c} 0.215\\ 0.245\\ 0.277\\ 0.310\end{array}$	$\begin{array}{c} 0.431 \\ 0.490 \\ 0.555 \\ 0.620 \end{array}$	$\begin{array}{c} 0.646 \\ 0.735 \\ 0.831 \\ 0.930 \end{array}$	$\begin{array}{c} 0.861 \\ 0.980 \\ 1.110 \\ 1.240 \end{array}$	1.077 1.226 1.387 1.550	1.293 1.471 1.664 1.860	1.508 1.716 1.940 2.167	1.722 1.961 2.218 2.480

FAN ENGINEERING-BUFFALO FORGE COMPANY

**44**6

## FRICTION OF AIR THROUGH VENTO HEATERS Loss in Pressure in Inches of Water

elocity Ft. per Min.		Regular Section 5-Inch Centers											
Ft. Mi	I Stack	2 Stack	3 Stack	4 Stack	5 Stack	6 Stack							
600 700 800	0.022 0.030 0.040	$\begin{array}{c} 0.040 \\ 0.055 \\ 0.072 \end{array}$	$0.058 \\ 0.080 \\ 0.104$	0.076 0.105 0.136	$\begin{array}{c} 0.094 \\ 0.130 \\ 0.168 \end{array}$	0.112 0.155 0.200							
900 1000 1100	0.051 - 0.063 - 0.076	$\begin{array}{c} 0.091 \\ 0.113 \\ 0.136 \end{array}$	$\begin{array}{c} 0.131 \\ 0.163 \\ 0.196 \end{array}$	0.172 0.213 0.257	$\begin{array}{c} 0.213 \\ 0.263 \\ 0.318 \end{array}$	$0.254 \\ 0.313 \\ 0.379$							
1200 1300 1400	$0.090 \\ 0.105 \\ 0.122$	$\begin{array}{c} 0.162 \\ 0.190 \\ 0.220 \end{array}$	$\begin{array}{c} 0.234 \\ 0.275 \\ 0.318 \end{array}$	$\begin{array}{r} 0.306 \\ 0.360 \\ 0.416 \end{array}$	$\begin{array}{c} 0.378 \\ 0.445 \\ 0.514 \end{array}$	$0.450 \\ 0.530 \\ 0.612$							
1500 1600	$\begin{array}{c} 0.140\\ 0.160\end{array}$	0.252 0.288	$\begin{array}{c} 0.364 \\ 0.416 \end{array}$	$0.477 \\ 0.544$	$0.590 \\ 0.672$	0.703 0.800							
Ft. per Min.	Narrow Section 5-Inch Centers												
Ft. Mi	2 Stack	3 Stack	4 Stack	5 Stack	6 Stack	7 Stack							
600 700 800	0.028 0.037 0.048	$0.043 \\ 0.057 \\ 0.075$	0.058 0.077 0.102	0.073 0.098 0.128	$0.088 \\ 0.119 \\ 0.155$	$0.103 \\ 0.140 \\ 0.181$							
900 1000 1100	0.061 0.075 0.090	$0.095 \\ 0.117 \\ 0.140$	$0.128 \\ 0.158 \\ 0.190$	$0.162 \\ 0.199 \\ 0.240$	$\begin{array}{c} 0.196 \\ 0.241 \\ 0.290 \end{array}$	$\begin{array}{c} 0.230 \\ 0.283 \\ 0.340 \end{array}$							
1200 1300 1400	0.107 0.126 0.147	$0.167 \\ 0.196 \\ 0.229$	$\begin{array}{c} 0.227 \\ 0.266 \\ 0.311 \end{array}$	0.287 0.336 0.392	$\begin{array}{c} 0.347 \\ 0.406 \\ 0.473 \end{array}$	$\begin{array}{c} 0.407 \\ 0.476 \\ 0.554 \end{array}$							
1500 1600	0.170 0.194	$\begin{array}{c} 0.263 \\ 0.300 \end{array}$	$\begin{array}{c} 0.356 \\ 0.406 \end{array}$	$0.449 \\ 0.512$	$\begin{array}{c} 0.542 \\ 0.617 \end{array}$	$\begin{array}{c} 0.635 \\ 0.722 \end{array}$							

From Catalog of American Radiator Company.

## **Friction Through Heaters**

On pages 446 and 447 will be found tables giving the friction loss or drop in pressure through both the Buffalo Standard Heaters and the Vento Cast Iron Heaters, with different velocities and depths of heaters. The values given for Buffalo heaters are based on tests made by the Buffalo Forge Company and will be found accurate for pipe coils. The table of loss through Vento heaters is based on tests made by the American Radiator Company.

## Sizes and Dimensions of Buffalo Standard Heaters

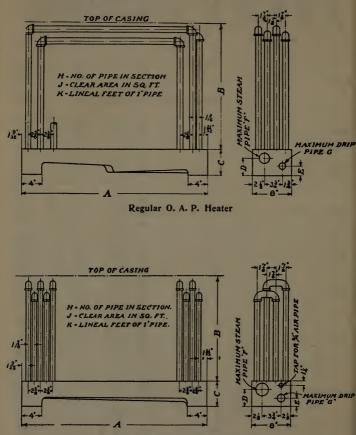
The table on page 449 of the Sizes and Dimensions of Buffalo Standard Heaters gives the information required for the selection of a heater for any specific case. The third column gives the length of the section (or of the cast-iron base) as also the number of rows of pipe in the section. The fifth row gives the various heights that are made on each base. Thus a heater  $4' \times 6'10''$ is 4 feet across the face by 6 feet 10 inches high.

Three columns are given showing measurements of the surface in the section. One gives the actual measured lineal feet of one inch pipe in each section. The next gives the actual effective square feet of heating surface in the section, counting in the exposed portions of the base as well as the surface of the pipe fittings. The third column gives the equivalent of this surface expressed in lineal feet of one inch pipe. Thus in the  $4' \times 6'10''$ section there are 428 feet of one inch pipe, but the total exposed heating surface is equivalent to 455 lineal feet of one inch pipe.

The column of clear areas gives the actual clear area, expressed in square feet, for the passage of air through the heater. Having the quantity of air and the velocity through the heater given, the values in this column decide the size of heater to be used. The number of sections in depth of the heater will depend on the desired temperature rise to be obtained. SIZES AND DIMENSIONS OF BUFFALO STANDARD HEATERS

3	SIZES AND DIMENSIONS OF BUFFALO STANDARD HEATERS										
Manner of Piping	Number of Pipes	Length of Section	Section Number	Extreme Height Section	Width of Section	Lin. Feet of 1-inch Pipe per Section	Total Effective Sq. Ft. Heating Surface	Equivalent in Lin. Feet of I-Inch Pipe	Clear Area for Air Passage Sq. Ft.	Weight	
R.O.A.	56	3′ 4 row	1 A 2 A 3 A 4 A 5 A 6 A	3' 4" 3' 10" 4' 4" 4' 10" 5' 4" 5' 10"	8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2"	140 168 196 224 252 280	54.7 64.2 74.0 83.7 93.3 102.5	159 186 215 243 271 298	$\begin{array}{r} 4.4 \\ 5.2 \\ 6.0 \\ 6.8 \\ 7.6 \\ 8.4 \end{array}$	473 515 565 616 656 708	
R.O.A.	72	4' 4 row	1 B 2 B 3 B 4 B	5' 4" 5' 10" 6' 4" 6' 10"	$\begin{array}{c} 8 \frac{1}{2}'' \\ 8 \frac{1}{2}'' \end{array}$	320 356 392 428	$     \begin{array}{r}       119.0 \\       131.5 \\       143.9 \\       156.5     \end{array} $	346 382 418 455	9.710.711.212.6	819 877 938 1003	
R.O.A.	80	4' 6" 4 row	1 C 2 C 3 C 4 C	5' 10" 6' 4" 6' 10" 7' 4"	$\frac{8\frac{1}{2}''}{8\frac{1}{2}''}{8\frac{1}{2}''}{8\frac{1}{2}''}{8\frac{1}{2}''}$	$396 \\ 436 \\ 476 \\ 516$	$\begin{array}{r} 148.2 \\ 162.0 \\ 174.8 \\ 188.6 \end{array}$	431 480 507 548	$12.1 \\ 13.1 \\ 14.2 \\ 15.3$	997 1055 1127 1174	
R.O.A.	88	5' 4 row	1 D 2 D 3 D 4 D	6' 4" 6' 10" 7' 4" 7' 10"	$\frac{8\frac{1}{2}''}{8\frac{1}{2}''}\\\frac{8\frac{1}{2}''}{8\frac{1}{2}''}\\\frac{8\frac{1}{2}''}{8\frac{1}{2}''}$	$\begin{array}{r} 476 \\ 520 \\ 564 \\ 608 \end{array}$	$174.3 \\189.3 \\204.8 \\219.8$	507 550 595 638	$     \begin{array}{r}       14.1 \\       15.4 \\       16.6 \\       17.7     \end{array} $	$     \begin{array}{r}       1182 \\       1262 \\       1325 \\       1407     \end{array} $	
R.O.A.	104	6' 4 row	1 E 2 E 3 E 4 E	7' 4" 7' 10" 8' 4" 8' 10"	$\frac{8\frac{1}{2}''}{8\frac{1}{2}''}\\\frac{81}{2}''}{8\frac{1}{2}''}\\\frac{81}{2}''}{8\frac{1}{2}''}$	674 726 778 830	$\begin{array}{r} 245.0 \\ 262.9 \\ 280.8 \\ 298.7 \end{array}$	712 763 816 868	$19.8 \\ 21.3 \\ 22.7 \\ 24.2$	1505     1600     1695     1770	
R.O.A.	64	7' 2 row	1 F 2 F 3 F 4 F	8' 4" 8' 10" 9' 4" 9' 10"	6" 6" 6"	477 509 541 573	$173.1 \\184.3 \\195.3 \\205.3$	503 535 567 596	$28.1 \\ 30.0 \\ 31.7 \\ 33.3$	$1198 \\ 1244 \\ 1303 \\ 1350$	
R.B.	128	7′ 4 row	1 G 2 G 3 G 4 G 6 G	7' 4" 7' 10" 8' 4" 8' 10" 9' 4" 9' 10"	8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2" 8 1/2"	796 860 924 988 1052 1116	$\begin{array}{c} 291.0\\ 313.2\\ 335.2\\ 357.2\\ 379.2\\ 401.2 \end{array}$	845 910 974 1037 1101 1163	$23.6 \\ 25.4 \\ 27.2 \\ 29.0 \\ 30.7 \\ 32.5$	$1845 \\1950 \\2055 \\2160 \\2280 \\2380$	
R.B.	154	8' 6" 4 row	1 H 2 H 3 H 4 H 5 H 6 H	8' 4" 8' 10" 9' 4" 9' 10" 10' 4" 10' 10"	10" 10" 10" 10" 10" 10"	$1119\\1196\\1273\\1350\\1427\\1504$	$\begin{array}{r} 410.2\\ 436.8\\ 463.5\\ 490.0\\ 516.6\\ 543.2\end{array}$	$     \begin{array}{r}       1190 \\       1265 \\       1345 \\       1421 \\       1499 \\       1578 \\     \end{array} $	33.2 35.3 37.6 39.8 41.8 44.0	$\begin{array}{r} 2675 \\ 2800 \\ 3075 \\ 3200 \\ 3325 \\ 3455 \end{array}$	
R.B.	170	9′ 6″ 4 row	1 I 2 I 3 I 4 I 5 I 6 I 7 I 8 I	8' 4" 8' 10" 9' 4" 9' 10" 10' 4" 10' 10" 11' 4" 11' 10"	10" 10" 10" 10" 10" 10" 10" 10"	$\begin{array}{r} 1231\\ 1316\\ 1401\\ 1486\\ 1571\\ 1656\\ 1741\\ 1826 \end{array}$	$\begin{array}{r} 452.3\\ 481.6\\ 510.9\\ 540.2\\ 569.5\\ 598.7\\ 628.0\\ 657.3\end{array}$	1313 1396 1481 1570 1651 1739 1821 1910	$\begin{array}{r} 36.7\\ 39.0\\ 41.4\\ 43.8\\ 46.0\\ 48.4\\ 50.8\\ 53.2 \end{array}$	$\begin{array}{r} 3205\\ 3350\\ 3485\\ 3625\\ 3770\\ 3910\\ 4060\\ 4200\\ \end{array}$	

# BUFFALO STANDARD PIPE COIL HEATERS

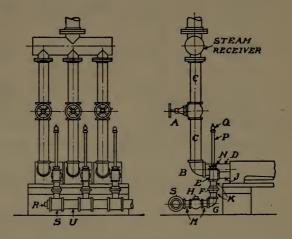


**Return Bend Heater** 

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e		1 " 1 " 1 "	1 14" 1 14" 1 14" 1 14"	$1 \frac{1}{14''}$ $1 \frac{14''}{14''}$ $1 \frac{14''}{14''}$	1112"	1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122'' 1122''' 1122''' 1122''' 1122''' 1122''' 1122''' 1122''' 1122''' 1122'''' 1122''''''''	$1 \frac{1}{12}$ $1 \frac{12}{12}$ $1 \frac{12}{2}$
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ũ	2	ด้ต้ต้ต้ต้ด	218" 218" 218" 218"	2218" 218" 218"	25/16" 25/16" 25/16" 25/16"	25/16" 25/16" 25/16" 25/16"	25/16" 255/16" 255/16" 255/16"
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2	9	34" 38" 50" 62"	56" 62" 68" 74"	62" 68" 74" 80"	68" 74" 80" 86"	80" 86" 92" 98"	$\begin{array}{c} 92''\\ 98''\\ 104''\\ 110''\end{array}$
	e	38 38% 38 38% 38 38% 38 38% 38 38% 38 38% 38 38%	$\begin{array}{c} 48\ 78''\\ 48\ 78''\\ 48\ 78''\\ 48\ 78''\\ 48\ 78''\\ 48\ 78''\\ 8\end{array}$	$\begin{array}{c} 541.8^{\prime\prime\prime}\\ 541.8^{\prime\prime\prime}\\ 541.8^{\prime\prime\prime}\\ 541.8^{\prime\prime\prime}\\ \end{array}$	59 38" 59 38" 59 38" 59 38"	69 7.8" 69 7.8" 69 7.8" 69 7.8"	85 58" 85 58" 85 58" 85 58"
tion	Height	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	5' 4" 5'10" 6' 4" 6'10"	5/10" 6/ 4" 6/10" 7/ 4"	6' 4" 6'10" 7' 4" 7'10"	7, 4" 7,10" 8, 4" 8'10"	$\begin{array}{c} 8' & 4'' \\ 8' 10'' \\ 9' & 4'' \\ 9' 10'' \end{array}$
Size of Section	Length	3 ft.	4 ft.	4 ft. 6 in.	5 ft.	ó ft.	7 ft.

# STEAM, DRIP AND AIR CONNECTIONS FOR **REGULAR O. A. P. HEATERS**



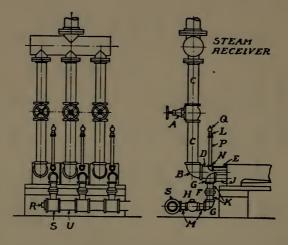
LIST OF FITTINGS FOR ONE SECTION

#### Main Drip

1 Pipe Plug "R" Tees "S." Same number as Number of Sections Nipples "U." One less than Number of Sections

O N N	ECT	10 N	S F	OR	REGULAR			0.	Α.	Р.	HEA	TER
Length of Nipples	Þ	6 <u>7</u> 6 <u>7</u> 8	673	612 612	6 12 6 12 2 22	6 <u>1</u> 2 6 <u>7</u> 2	6 1 <u>/</u> 6 1/ ₈	61% 61%	6 1/8 6 1/8	6 1/8 6 1/8	99	99
th of <b>N</b>	¥	~ ~ ~	ოო		m m	3 2 ½	5 5 3 3	272 272	222	222	51 53 72 72 72 72	222
Leng	-	44	44	44	44	44	<u>4</u> 4	44	44	44	44	44
	6 Sect.	50	2010	~ ~	22 22 22 22 22	2 12 2 12 2 12	10 12 12 12 12 12	01 01 7474	210 7272	1010		
Drip	5 Sect.	~~~~	0101	2101	20	$\frac{2}{2}\frac{1}{2}$	0101 27 28	0101 7474	01 01 767%	0101 7/2/2		00 00
Size of Main Drip	4 Sect.	1 1/3	172	1122	C1 C1	0101	0101	ଚାର	c1 C1	ଚାଚା	0101 725%	0107 1212 1227
Size (	3 Sect.	1 1/2	11%	$1 \frac{1}{122}$	$1 \frac{1}{12}$	$\frac{1}{2}$	$\frac{1}{2}$	ରାରା	ରାର	ଦାଦା	2 2 1 2 1 2 1 2 2 2 2 2 2 2 2 2 2 2 2 2	10 12 272 272
	2 Sect.	724	174	1 1/4	1747	1 1/4	11/4	11/2	1122	$1\frac{1}{2}$	20	2010
Size	Drip		11			1.14	114	114	114	114	$\frac{1}{1}\frac{1/2}{1/2}$	$\frac{1}{1}\frac{1}{2}$
Length of Nipples	D	99	99	çõ	99	$\frac{6}{7 y_2^2}$	$\frac{6}{7 \frac{1}{22}}$	71/2	7.7	7 1/2	00 00	00 00
Leng	v	12 12	18 18	18 18	18	18 18	18 18	18 18	18 18	18 24	$\frac{18}{24}$	24 24
ly	60 Lbs.				1 14	1 14 1 14	1 14	114	11/24/11	1222	$1\frac{1}{12}$	122
of Steam Supply Length of Size Size of Main Drip	20 Lbs. 60 Lbs.	11	114	114	11/2/2	$2^{1}_{2}$	2 2 1/2	ରାରା	ଦାଦା	ଦାଦା	1012	0101 /01/01
Size of Steam Supply	5 Lbs.	1 14	$\frac{1}{\frac{1}{2}}$	ମନା	ରାହା	2 2 <u>1/2</u>	23/2	0101 22/2 22/2	272 2122 2122	0101 22/2	er er	00 00
Si	0 Lbs.	1 1/2	0101	ରାରା	127	2 12 2 12 2 12	0101 7272	0101 7272	32 1/2	m m		
Size of	Heater	3'0"x3' 4" 3'0"x3'10"	3'0"X4' 4" 3'0"X4'10"	3'0"x5' 4" 3'0"x5'10"	4'0"x5' 4" 4'0"x5'10"	4'0"X6' 4" 4'0"X6'10"	4'6"x5'10" 4'6"x6' 4"	4'6"x6'10" 4'6"x7' 4"	5'0"x6' 4" 5'0"x6'10"	5'0"x7' 4" 5'0"x7'10"	6'0"X7' 4" 6'0"X7'10"	6'0"x8' 4" 7'0"x8'10"

# STEAM, DRIP AND AIR CONNECTIONS FOR RETURN BEND HEATERS



LIST OF FITTINGS FOR ONE SECTION

## Steam Connections

- 1 Globe Valve "A"
- 1 Elbow "B"
- 2 Nipples "C"
- 1 Nipple "D"

#### **Drip Connections**

- 2 Elbows "G"
- 1 Box Union "F"
- 1 Check Valve "H"
- 1 Nipple "J"

2 Nipples "K"2 Short Nipples "M"

#### **Air Connections**

- 1-3/4" Short Nipple "E"
- 1-3/1" Elbow "N"
- 1-3/1" Pipe "P" 18" long
- 1-34" x 14" Reducer "L"
- 1-14" Pet Cock "Q"
  - Male Thread

#### Main Drip

1 Pipe Plug "R." Tees "S." Same Number as Number of Sections Nipples "U." One less than Number of Sections

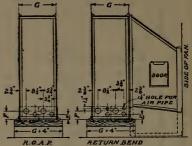
	pples	D	000 7272	800 7272 2222	000 7272 7272	6 7 8 7 8 7 8 7 8 9 9 9 9 9 9 9 9 9 9 9 9	69 8/% 8/% 8/%	0000 78%%	999	999	99
	Length of Nipples	к	ოოო	ოოო		2 ½ 3 %	2222	2000	000 2222	2222	272
	Lengt	7	***	<del>খ</del> শ শ	444	444	444	444	4.4.4	4.4.4.	4 1/2
		6 Sect.	ุกกฤ	ุกคล	000 727273	2222	2222	010101 XXX	ოოო	ოოო	m m
HEATERS	Drip	5 Sect.	ุลลล	ุลลล	ରାରାର	2 ² 2 ² 2 ²	000 787872	555% 557%	ოოო	ოოო	<b>m</b> m
BEND H	Size of Main Drip	4 Sect.	11222	7777	ରାରାର	ରାରାର	ରାରାର	000	2222	2222 2000	522
TURN B	Size	3 Sect.	11/2/2	2222	2222	$\frac{2}{1}$	ରାରାର	~~~	010101 XXXX	1000 1722 1722 1722 1722	2 72 72
STEAM, DRIP AND AIR CONNECTIONS FOR RETURN BEND		2 Sect.	1174	11 2411 2441	1174	1172	1111	111	000	ุกคค	00
TIONS	Size	Drip				1 1 1 2 4	1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	1111 7477	1111	1111	1 72
CONNEC	Length of Nipples	D	999	စစစ	000	7 ½ 6 7 ½	1111	2222	00 00 00	00 00 00	∞∞
D AIR 0	Leng	c	12 18 18	18 18 18	18 18 18	18 18 18	18 18 18	18 18 24	18 24 24	24 24 24	24 24
RIP AN	ly	60 Lbs.			1 1 24 1 24	111 22/2/2	1111 74774 74	11/2/2	111 XXX	~~~~	0101
EAM, D	am Supp	20 Lbs.	11/2	1111 747475	7777	2 1 ½	~~~~	~~~	866 877 878	010101 X2XX	27% 27%
ST	Size of Steam Supply	5 Lbs.	 7475	100 X	ดงง	2 7 2 7 2 7 2 7 2 7 2 7 2 7 2 7 2 7 2 7	000 797272	010101 727272	იიი	იიი	m m
	SI	0 Lbs.	21-1-03	ରାରାର	010101 747274	010103 727272	010101 727272	იიი	თთთ	იიიი	m m
	Size of	Heater	3'0"x3' 4" 3'0"x3'10" 3'0"x4' 4"	3'0"X4'10" 3'0"X5' 4" 3'0"X5'10"	4'0"x5' 4" 4'0"x5'10" 4'0"x6'4"	4'0"x6'10" 4'6"x5'10" 4'6"x6' 4"	4'6"x6'10" 4'6"x7' 4" 5'0"x6' 4"	5'0"x6'10" 5'0"x7' 4" 5'0"x7'10"	6'0"x7' 4" 6'0"x7'10" 6'0"x8' 4"	6'0"x8'10" 7'0"x8' 4" 7'0"x8'10"	7'0"x9' 4" 7'0"x9'10"

CONNECTIONS FOR

RETURN BEND HEATERS

# DIMENSIONS OF HEATER CASE FOR BUFFALO STANDARD HEATERS





H • DIA. OF HOLE FOR STEAM PIPE. J • DIA. OF HOLE FOR DRIP PIPE.

Size of a	Section								Н				
Length	Height	A	В	С	D	E	F	G	0 lbs.	5 Ibs.	20 lbs.	60 lbs.	J
3 ft.	3' 4" 3'10" 4' 4" 4'10" 5' 4" 5' 10"	$38\frac{3}{4}$ $38\frac{3}{4}$ $38\frac{3}{4}$ $38\frac{3}{4}$ $38\frac{3}{4}$ $38\frac{3}{4}$ $38\frac{3}{4}$ $38\frac{3}{4}$	38 ³ / ₈ 38 ³ / ₈	555555	$     \begin{array}{r}       34 \\       38 \\       44 \\       50 \\       56 \\       62     \end{array} $	2 2 2 2 2 2 2 2	3 ¹ / ₈ 3 ¹ / ₈		$2\frac{1}{8}$ $2\frac{1}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$	$1\frac{7}{8}\\1\frac{7}{8}\\2\frac{1}{8}\\2\frac{1}{8}\\2\frac{5}{8}\\2\frac{5}{8}$	$1\frac{1}{2}$ $1\frac{1}{2}$ $1\frac{1}{2}$ $1\frac{7}{8}$ $1\frac{7}{8}$ $1\frac{7}{8}$ $2\frac{1}{8}$	$ \frac{1}{12} $ $ \frac{1}{2} $	
4 ft.	5' 4" 5'10" 6' 4" 6'10"	$ \begin{array}{r}     49\frac{1}{4} \\     49\frac{1}{4} \\     49\frac{1}{4} \\     49\frac{1}{4} \\     49\frac{1}{4} \end{array} $	48 7/8 48 7/8 48 7/8 48 7/8 48 7/8	5 ⁵ /8 5 ⁵ /8 5 ⁵ /8 5 ⁵ /8 5 ⁵ /8	$56 \\ 62 \\ 68 \\ 74$	$\begin{array}{c} 2\frac{1}{8} \\ 2\frac{1}{8} \\ 2\frac{1}{8} \\ 2\frac{1}{8} \\ 2\frac{1}{8} \\ 2\frac{1}{8} \end{array}$	$3\frac{1}{2}$ $3\frac{1}{2}$ $3\frac{1}{2}$ $3\frac{1}{2}$ $3\frac{1}{2}$	SECTIONS	$\frac{3\frac{1}{8}}{3\frac{1}{8}}$ $\frac{31}{8}$ $\frac{31}{8}$ $\frac{31}{8}$	$2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $3\frac{1}{8}$	$2\frac{1}{8}$ $2\frac{1}{8}$ $2\frac{1}{8}$ $2\frac{1}{8}$ $2\frac{5}{8}$	$   \begin{array}{r}     1                                $	1 1/2 1 1/2 1 1/2 1 7/2
4 ft. 6 in.	5'10' 6' 4" 6'10" 7' 4"	$\begin{array}{r} 54\frac{1}{2} \\ 54\frac{1}{2} \\ 54\frac{1}{2} \\ 54\frac{1}{2} \\ 54\frac{1}{2} \\ 54\frac{1}{2} \end{array}$	$\begin{array}{r} 54\frac{1}{8} \\ 54\frac{1}{8} \\ 54\frac{1}{8} \\ 54\frac{1}{8} \\ 54\frac{1}{8} \\ 54\frac{1}{8} \end{array}$	558 558 558 558 558	$     \begin{array}{r}       62 \\       68 \\       74 \\       80     \end{array} $	$     \begin{array}{r}       2 \frac{1}{8} \\       2 \frac{1}{8} \\ $	$\frac{3\frac{1}{2}}{3\frac{1}{2}}{3\frac{1}{2}}{3\frac{1}{2}}{3\frac{1}{2}}{3\frac{1}{2}}$	OF SECT	$     3\frac{1}{8}     3\frac{1}{8}   $	$2\frac{5}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$	$2\frac{1}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$	$\frac{17_8}{17_8}\\17_8\\17_8\\17_8\\17_8$	1 1/2 1 7/8 1 7/8 1 7/8 1 7/8
5 ft.	6' 4'' 6'10'' 7' 4" 7'10"	$     59\frac{3}{4} \\     59\frac{3}{4} \\     59\frac{3}{4} \\     59\frac{3}{4} \\     59\frac{3}{4} $	$\begin{array}{r} 59\frac{3}{8}\\ 59\frac{3}{8}\\ 59\frac{3}{8}\\ 59\frac{3}{8}\\ 59\frac{3}{8}\\ 59\frac{3}{8}\end{array}$	$\begin{array}{r} 6\ \frac{3}{8} \\ 6\ \frac{3}{8} \\ 6\ \frac{3}{8} \\ 6\ \frac{3}{8} \\ 6\ \frac{3}{8} \end{array}$	68 74 80 86	$\begin{array}{c}2{}^{5}_{\overline{16}}\\2{}^{5}_{\overline{16}}\\2{}^{5}_{\overline{18}}\\2{}^{5}_{\overline{18}}\\2{}^{5}_{\overline{16}}\\2{}^{5}_{\overline{16}}\end{array}$	20 20 20 20 20 20 20 20 20 20 20 20	1/2" x No.	$     3\frac{1}{8}     3\frac{3}{4}     3\frac{3}{4}   $	$     3\frac{1}{8}     3\frac{1}{8}   $	$2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$	$1\frac{7}{8}$ $1\frac{7}{8}$ $2\frac{1}{8}$ $2\frac{1}{8}$	1 7/8 1 7/8 1 7/8 1 7/8 1 7/8
6 ft.	7' 4" 7'10" 8' 4" 8'10"	$70\frac{1}{4}$ $70\frac{1}{4}$ $70\frac{1}{4}$ $70\frac{1}{4}$ $70\frac{1}{4}$	$\begin{array}{r} 697/8\\ 697/8\\ 697/8\\ 697/8\\ 697/8\\ 697/8\\ \end{array}$	$\begin{array}{r} 6\frac{3}{8}\\ 6\frac{3}{8}\\ 6\frac{3}{8}\\ 6\frac{3}{8}\\ 6\frac{3}{8}\\ 6\frac{3}{8}\end{array}$	80 86 92 98	2 18 2 18 2 18 2 18 2 18 2 18 2 18 2 18	11111111 11111111111111111111111111111	80	33/4 33/4 33/4 33/4	33/4 33/4 33/4 33/4 33/4	$2\frac{5}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$	$2\frac{1}{8}$ $2\frac{1}{8}$ $2\frac{1}{8}$ $2\frac{5}{8}$	21/8 21/8 21/8 21/8 21/8
7 ft.	8' 4" 8'10" 9' 4" 9'10"	86 86 86 86	85 5/8 85 5/8 85 5/8 85 5/8 85 5/8	$ \begin{array}{r} 63/8 \\ 63/8 \\ 63/8 \\ 63/8 \\ 63/8 \\ 63/8 \\ \end{array} $	92 98 104 110	2 16 2 16 2 16 2 16 2 16 2 16 2 16 2 16	CC CC CC CC CC		$3\frac{3}{4}$ $3\frac{3}{4}$ $3\frac{3}{4}$ $3\frac{3}{4}$	3 ³ /4 3 ³ /4 3 ³ /4 3 ³ /4	$\frac{3\frac{1}{8}}{3\frac{1}{8}}$ $3\frac{1}{8}$ $3\frac{1}{8}$ $3\frac{1}{8}$	$2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$ $2\frac{5}{8}$	21/8 21/8 21/8 21/8 21/8

Note—Connection as shown in full lines for full Housing Fans up to and including 120". Connection as shown in dotted lines for full Housing Fans over 120" and all three-quarter Housing Fans.

## Heater Case for Buffalo Heaters

Detailed dimensions of the casing used for the Buffalo fan system heaters will be found on page 456. Care should be taken to have the connection between the fan and heater case of such a character that it will not restrict the flow of air or offer unnecessary resistance. This precaution is frequently overlooked, either throwing excessive pressure on the fan, or curtailing the quantity of air handled.

The following table gives the approximate lengths of connection advised for a draw through installation.

FOR DRAW THROUGH EQUIPMENT											
Size	of Fan										
Planoidal	Niagara Conoidal	Distance From Fan to Heater									
Up to 70" 70" to 100" 100" to 130" 130" to 170" 170" to 200"	Up to No. 7 7 to 10 10 to 13 13 to 17 17 to 20	18" to 24" 24" to 30" 36" 42" 48" to 54"									

#### **By-Pass Proportions**

It is common practice in indirect or fan system heaters to arrange a by-pass, usually beneath the heater, so that all or a part of the air may be taken direct without passing through the heating coils. The by-pass is generally made the full width of the heater with a height of one-third or more of the height of the heater. Since the clear area of the standard Buffalo heater is one-half the gross area, this makes the total area of the by-pass equal to two-thirds or more of the clear area of the heater.

The loss by friction through the by-pass is very slight since the distance the air travels is comparatively short. As ordinarily installed the by-pass is placed below the center of the fan so that the direction of the air is changed more or less several times in going through the by-pass. The loss of entrance and discharge at the by-pass may be taken at from 11/2 to 21/2 velocity heads, depending on the arrangement. An average loss might be considered as two velocity heads, or approximately the equivalent of the resistance of four Buffalo heater sections of the size to which the by-pass is proportioned. The blast area of the by-pass may be taken as approximately 70 per cent. of the actual area.

#### **Indirect Heaters**

This is a special form of pipe coil heater, details and dimensions of which will be found on page 459.

As the table shows, a variety of sizes are built, the smallest being six pipes wide and eight pipes long. Under the heading of "Size," the first row of figures gives the number of pipes across the steam supply and drip ends, and the second column the number of pipes in the length of the coil. Cast iron manifolds are used for the bases into which the pipes are screwed, as in the regular fan system heaters. The indirect heaters may be used in an upright or horizontal position, according to the requirements. These heaters are shown as the solid base type and a diaphragm in same compels the steam to flow evenly through all pipes. The steam supply enters the heater base at one end and the water of condensation is removed directly opposite. These coils are designed for the use of either live or exhaust steam.

## **Blast Area of Buffalo Heaters**

The blast area of any heater may be determined by the formula

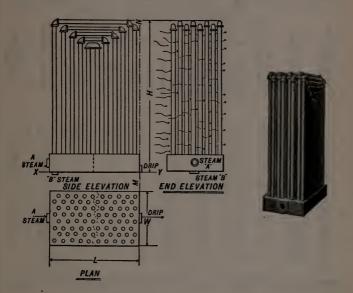
$$A_{b} = \frac{A. P. M.}{4005 \sqrt{\text{press. drop in in.}}}$$
(109)

Thus, if we assume a case where 10000 cu. ft. of air per minute is to be passed through five sections of Buffalo heater at a velocity of 1000 feet per minute, we find from the table on page 446 that the pressure loss will be 0.479 inch. Then from the above formula

Blast area = 
$$\frac{10000}{4005\sqrt{0.479}}$$
 = 3.61 sq. ft.

A general discussion on the subject of blast area, together with an example illustrating the application of the general formula to an entire heating system, will be found on page 126.

# INDIRECT HEATERS



ACTUAL LINEAL FEET 1-INCH PIPE IN EACH SECTION

No. Pipes	Size	40 ½"	46 1⁄2"	52 ½″	58 ½″	64 ½"	W	L
48	6 x 8	133	154	177	198	221	$     \begin{array}{r}       12\frac{1}{2} \\       16\frac{1}{4} \\       16\frac{1}{4}     \end{array} $	22
64,	6 x 8	177	206	236	265	295		22
80	8 x 10	221	258	295	332	369		27
100	10 x 10	276	323	369	415	462	20	27
120	10 x 12	346	387	443	498	553	20	32
140	10 x 14	387	451	517	581	645	20	37
144	12 x 12	398	464	532	598	663	$\begin{array}{c} 23 \frac{1}{4} \\ 23 \frac{1}{4} \\ 23 \frac{1}{4} \end{array}$	32
168	12 x 14	464	542	618	697	774		37
192	12 x 16	532	618	709	798	886		42
196	14 x 14	542	632	723	814	906	$27\frac{1}{2}$	37
256	16 x 16	708	827	945	1061	1181	$30\frac{1}{4}$	42

## VENTO CAST IRON HOT-BLAST HEATER REGULAR SECTION—RATINGS AND FREE AREAS Regular 40 Inch Section, 10.75 Sq. Ft. Height 411/64 Inch. Width 91/8 Inch

sdo	of ace	rface I Lineal Pipe	Loo		53%" C of Lo	enters pops	4 5/8" Co of Lo		of ds	
r of Loops Stack e Feet of g Surface			Stand 44% of		52% of	Face	37% of	Face	Pour	mate
Number of Loops in Stack	Square F Heating	*Equivalent in Fcet 1-inch	Net Air Space in Square Feet	†Width of Stack in Inches	Net Air Space in Square Feet	†Width of Stack in Inches	Net Air Space in Square Feet	†Width of Stack in Inches	Actual Weight of Stack in Pounds	Approximate Weights
7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24	$\begin{array}{c} 75.25\\ 86.00\\ 96.75\\ 107.50\\ 118.25\\ 129.00\\ 182.75\\ 150.50\\ 161.25\\ 772.00\\ 182.75\\ 193.50\\ 204.25\\ 215.00\\ 225.75\\ 226.50\\ 247.25\\ 258.00 \end{array}$	$\begin{array}{c} 226\\ 258\\ 290\\ 323\\ 355\\ 387\\ 419\\ 452\\ 484\\ 516\\ 548\\ 581\\ 613\\ 645\\ 581\\ 617\\ 710\\ 742\\ 774 \end{array}$	$\begin{array}{c} 4.34\\ 4.96\\ 5.58\\ 6.20\\ 6.82\\ 7.44\\ 8.06\\ 8.68\\ 9.30\\ 9.92\\ 10.54\\ 11.16\\ 11.78\\ 12.40\\ 13.02\\ 13.64\\ 14.26\\ 14.88\end{array}$	$\begin{array}{c} 35\\ 40\\ 45\\ 50\\ 55\\ 60\\ 65\\ 70\\ 75\\ 80\\ 95\\ 100\\ 95\\ 100\\ 115\\ 120\\ \end{array}$	$\begin{array}{c} 5.12\\ 5.85\\ 6.57\\ 7.29\\ 8.02\\ 8.74\\ 9.47\\ 10.19\\ 11.64\\ 12.369\\ 13.82\\ 14.54\\ 15.26\\ 15.98\\ 16.71\\ 17.43\\ \end{array}$	38 43 48 54 59 65 70 75 81 86 91 97 102 108 113 118 124 129	$\begin{array}{c} 3.67\\ 4.20\\ 4.72\\ 5.25\\ 5.77\\ 6.30\\ 6.82\\ 7.35\\ 7.87\\ 8.40\\ 8.92\\ 9.45\\ 9.97\\ 10.50\\ 11.02\\ 11.55\\ 12.07\\ 12.60\\ \end{array}$	32 37 42 46 51 55 60 65 69 74 79 83 88 89 97 102 106 111	$\begin{array}{c} 594\\ 670\\ 728\\ 851\\ 936\\ 1022\\ 1167\\ 1193\\ 1278\\ 1364\\ 1449\\ 1535\\ 1620\\ 1796\\ 1796\\ 1790\\ 1876\\ 1960\\ 2045 \end{array}$	7.92 lbs. per sq. ft. actual 9 lbs. per sq. ft. shipping weight

Regular 50 Inch Section, 13.5 Square Feet. Height 5029/32 Inch. Width 91/8 Inch

			5″ Cer	5" Centers		5 ³ / ₈ " Centers		4 ⁵ / ₈ " Centers		
7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24	$\begin{array}{c} 94.5\\ 108.0\\ 121.5\\ 135.0\\ 148.5\\ 162.0\\ 175.5\\ 189.0\\ 202.5\\ 229.5\\ 243.0\\ 229.5\\ 243.0\\ 229.5\\ 243.0\\ 235.5\\ 270.0\\ 235.5\\ 270.0\\ 235.5\\ 324.0\\ \end{array}$	284 324 365 405 446 527 567 608 648 689 729 770 810 851 851 891 932 972	$\begin{array}{c} 5.37\\ 6.14\\ 6.91\\ 7.68\\ 8.45\\ 9.22\\ 9.99\\ 10.76\\ 11.53\\ 12.30\\ 13.07\\ 13.84\\ 14.59\\ 15.36\\ 16.13\\ 16.90\\ 17.67\\ 18.44\\ \end{array}$	35 40 55 50 55 60 65 70 75 80 95 90 95 100 105 110 115 120	$\begin{array}{c} 6.35\\ 7.25\\ 8.15\\ 9.95\\ 9.95\\ 10.85\\ 11.75\\ 12.65\\ 13.55\\ 14.45\\ 15.35\\ 16.25\\ 17.15\\ 18.05\\ 18.95\\ 19.85\\ 20.75\\ 21.65\\ \end{array}$	38 43 48 54 59 65 70 75 81 86 91 97 102 108 113 118 124 129	$\begin{array}{c} 4.55\\ 5.20\\ 5.85\\ 6.50\\ 7.15\\ 7.80\\ 8.45\\ 9.10\\ 9.75\\ 10.40\\ 11.05\\ 11.70\\ 12.35\\ 13.00\\ 13.65\\ 14.30\\ 14.95\\ 15.60\\ \end{array}$	32 37 42 46 51 55 60 65 69 74 79 83 88 92 97 102 106 111	717 810 923 1026 1129 1232 1335 1436 1539 1644 1539 164 1747 1747 1747 1852 2060 2160 2263 2370 2263 2370	7.62 lbs. per sq. ft. actual 9 lbs. per sq. ft. shipping weight

[†]NOTE —Add to the width of stack 2½ inches for staggering of stacks. *NOTE —The actual length of one-inch pipe per square foot of outside. surface is 2.9 lineal feet but is nominally figured at 3 lineal feet, as shown in the third column of above table.

#### VENTO HEATER RATINGS

#### VENTO CAST IRON HOT-BLAST HEATER **REGULAR SECTION—RATINGS AND FREE AREAS** Regular 60 Inch Section, 16 Square Feet. Height 6011/16 Inch. Width 91% Inch

of ice	incal			5 3/8" C	enters oops	4 5/8" Co of Lo	enters oops	of ds	
f Lack		Standar of F	d 44% ace	52% of	Face	37% of	Face	eight Poun	imate
Square Heating	quivalen Feet 1-ii	vet Air pace in tare Feet	Vidth of tack in inches	let Air pace in tare Feet	Vidth of tack in inches	et Air pace in lare Feet	Vidth of ack in inches	Actual W Stack in	Approximate Weights
	*	Squ	₹ <u>s</u> -	N S S S	\$\$_	N Squ	\$1 SI		
$\begin{array}{c} 112.0\\ 128.0\\ 128.0\\ 160.0\\ 176.0\\ 192.0\\ 208.0\\ 224.0\\ 240.0\\ 224.0\\ 240.0\\ 224.0\\ 240.0\\ 225.0\\ 320.0\\ 320.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 336.0\\ 33$	336 384 432 480 528 576 624 672 720 768 816 864 912 960 1008 1008 1056 1104	$\begin{array}{c} 6.45\\ 7.37\\ 8.29\\ 9.21\\ 10.13\\ 11.05\\ 11.97\\ 12.89\\ 13.81\\ 14.73\\ 15.65\\ 16.57\\ 17.50\\ 18.42\\ 19.34\\ 20.26\\ 21.18\end{array}$	$\begin{array}{r} 35\\ 40\\ 45\\ 50\\ 55\\ 60\\ 65\\ 70\\ 75\\ 80\\ 95\\ 90\\ 95\\ 100\\ 105\\ 110\\ 115\\ 120\\ \end{array}$	$\begin{array}{c} 7.62\\ 8.70\\ 9.77\\ 10.85\\ 11.93\\ 13.00\\ 14.08\\ 15.15\\ 16.23\\ 17.31\\ 18.39\\ 19.46\\ 20.54\\ 21.62\\ 22.70\\ 23.78\\ 24.85\\ 25.92\\ 55.95\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55\\ 10.55$	38 43 48 54 59 65 70 75 81 86 91 97 102 108 113 118 124	$\begin{array}{c} 5.47\\ 6.25\\ 7.03\\ 7.81\\ 8.59\\ 9.37\\ 10.15\\ 10.93\\ 11.71\\ 12.49\\ 13.27\\ 14.05\\ 14.83\\ 15.61\\ 16.39\\ 17.17\\ 17.95\\ \end{array}$	32 37 42 46 51 55 60 65 69 74 79 83 88 97 102 102	864 988 1112 1238 1362 1486 1610 1734 1858 1982 2106 2230 2352 2478 2600 2352 2478 2600 2725 2850	7.74 lbs. per sq. ft. actual 9 lbs. per sq. ft. shipping weight
	$\begin{array}{c} 128.0\\ 144.0\\ 160.0\\ 176.0\\ 192.0\\ 208.0\\ 224.0\\ 244.0\\ 256.0\\ 272.0\\ 288.0\\ 304.0\\ 320.0\\ 3364.0\\ 3352.0\\ \end{array}$	auiii         51-1           auiii         51-1           bui         auiii           112.0         336           128.0         384           128.0         384           128.0         384           128.0         384           128.0         386           192.0         576           208.0         624           224.0         672           240.0         720           256.0         768           272.0         816           288.0         864           304.0         912           320.0         960           336.0         1008           336.0         1008           336.0         1008           336.0         1008	of LC         of LC           Standar         Standar           of F.         Standar           of Standar         Standar           of Standar         Standar           of	audi o truit         of Loops           audi o truit         of Loops           standard 44% of Face         of Face           audi of truit         audi of Face           audi of truit         audi truit           audi of truit         audi truit           audi of truit         audi truit           audi audi audi truit         audi truit           audi audi audi audi truit         audi truit           audi audi audi truit         audi truit           audi audi truit         audi truit           audi truit         audi truit           audi truit <td< th=""><th>Jogung         Jof Loops         of Loops           Jogung         Jof Loops         Jof Loops         Jof Loops           Jogung         Jogung         Jof Loops         Jof Loops         Jof Loops           Jogung         Jogung         Jogung         Jof Loops         Jof Loops         Jof Loops           Jogung         Jogung</th><th>Joginal         of Loops         of Loops         of Loops           Joginal         Joginal         Joginal         Joginal         Joginal         Joginal           Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Jogina         Jogina         Jogina<th>Joginal         of Loops         of Loops         of Loops         of Loops         of Loops           Joginal         uiii         Joginal         uiiii         Joginal         Jogi</th><th>of Loops         of Loops         of Loops         of Loops         of Loops           joging         initial         initial</th><th>Jorgans         of Loops         of Loops</th></th></td<>	Jogung         Jof Loops         of Loops           Jogung         Jof Loops         Jof Loops         Jof Loops           Jogung         Jogung         Jof Loops         Jof Loops         Jof Loops           Jogung         Jogung         Jogung         Jof Loops         Jof Loops         Jof Loops           Jogung         Jogung	Joginal         of Loops         of Loops         of Loops           Joginal         Joginal         Joginal         Joginal         Joginal         Joginal           Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Joginal         Jogina         Jogina         Jogina <th>Joginal         of Loops         of Loops         of Loops         of Loops         of Loops           Joginal         uiii         Joginal         uiiii         Joginal         Jogi</th> <th>of Loops         of Loops         of Loops         of Loops         of Loops           joging         initial         initial</th> <th>Jorgans         of Loops         of Loops</th>	Joginal         of Loops         of Loops         of Loops         of Loops         of Loops           Joginal         uiii         Joginal         uiiii         Joginal         Jogi	of Loops         of Loops         of Loops         of Loops         of Loops           joging         initial         initial	Jorgans         of Loops         of Loops

NARROW SECTION—RATINGS AND FREE AREAS Narrow 40 Inch Section, 7.5 Square Feet. Height 411/64 Inch. Width 631 Inch

			5" Centers		5 ³ / ₈ " Centers		4 ⁵ / ₈ " Centers			
7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24	$\begin{array}{c} 52.5\\ 60.0\\ 67.5\\ 75.0\\ 82.5\\ 90.0\\ 97.5\\ 105.0\\ 112.5\\ 120.0\\ 127.5\\ 135.0\\ 142.5\\ 150.0\\ 157.5\\ 180.0\\ \end{array}$	$\begin{array}{c} 158\\ 180\\ 203\\ 225\\ 248\\ 270\\ 293\\ 315\\ 338\\ 360\\ 405\\ 428\\ 450\\ 473\\ 495\\ 518\\ 540\\ \end{array}$	$\begin{array}{c} 4.34\\ 4.96\\ 5.58\\ 6.20\\ 6.82\\ 7.44\\ 8.06\\ 8.68\\ 9.92\\ 10.54\\ 11.16\\ 11.78\\ 12.40\\ 13.02\\ 13.64\\ 14.26\\ 14.88\\ \end{array}$	35 40 45 50 55 60 65 70 75 80 90 95 100 85 90 95 100 105 110 115 120	$\begin{array}{c} 5.12\\ 5.85\\ 6.57\\ 7.29\\ 8.74\\ 9.47\\ 10.19\\ 10.9\\ 11.64\\ 12.36\\ 13.09\\ 13.82\\ 14.54\\ 15.26\\ 15.98\\ 16.71\\ 17.43\\ \end{array}$	$\begin{array}{c} 38\\ 43\\ 48\\ 54\\ 59\\ 65\\ 70\\ 75\\ 81\\ 86\\ 91\\ 97\\ 102\\ 108\\ 113\\ 118\\ 124\\ 129 \end{array}$	$\begin{array}{c} 3.67\\ 4.20\\ 4.72\\ 5.25\\ 5.77\\ 6.30\\ 6.82\\ 7.35\\ 7.87\\ 8.40\\ 8.92\\ 9.45\\ 9.97\\ 10.50\\ 11.02\\ 11.55\\ 12.07\\ 12.60\\ \end{array}$	$\begin{array}{c} 32\\ 37\\ 42\\ 46\\ 51\\ 55\\ 60\\ 65\\ 69\\ 74\\ 83\\ 88\\ 92\\ 97\\ 102\\ 106\\ 111 \end{array}$	$\begin{array}{c} 420\\ 480\\ 540\\ 600\\ 660\\ 720\\ 780\\ 900\\ 900\\ 900\\ 1020\\ 1080\\ 1140\\ 1200\\ 1260\\ 1280\\ 1320\\ 1380\\ 1440\\ \end{array}$	8.00 lbs. per sq. ft. actual 9.25 lbs. per sq. ft. shipping weight

†NOTE —Add to the width of stack 2½ inches for staggering of stacks.
*NOTE —The actual length of one-inch pipe per square foot of outside surface is 2.9 lineal feet but is nominally figured at 3 lineal feet, as shown in the third column of above table.

#### VENTO CAST IRON HOT-BLAST HEATER NARROW SECTION—RATINGS AND FREE AREAS Narrow 50 Inch Section, 9.5 Square Feet. Height 502%2 Inch. Width 63/4 Inch

s		Lineal	5" Cent Loo	ers of ps	5 3/8" Co of Lo		4 5/8" Ce of Lo	enters ops	of	
in ur ck L		Pij	Stand 44% of	lard Face	52% of	Face	37% of	Face	Weight Pounds	Weights
ther of in Sta	Square F Heating S	rivalent Feet 1"	Vir in Feet	h of in es	Nir in Feet	h of in es	Nir in Feet	h of in ies		Actual W
Num	Sqı Hea	*Equivalent Feet 1"	Net Air Space i Square Fe	†Width Stack ir Inches	Net Air Space in Square Fe	†Width Stack in Inches	Net Air Space in Square Fe	†Width o Stack in Inches	Nominal Stack in	Acti
		*	č		Š.		Ň.			
7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	$\begin{array}{r} 66.5\\ 76.0\\ 85.5\\ 95.0\\ 104.5\\ 114.0\\ 123.5\\ 133.0\\ 142.5\\ 152.0\\ 161.5\\ 152.0\\ 161.5\\ 171.0\\ 180.5\\ 190.0\\ \end{array}$	$\begin{array}{c} 200\\ 228\\ 257\\ 285\\ 314\\ 342\\ 371\\ 399\\ 428\\ 456\\ 513\\ 513\\ 542\\ 570\\ \end{array}$	$\begin{array}{c} 5.37\\ 6.14\\ 6.91\\ 7.68\\ 9.22\\ 9.99\\ 10.76\\ 11.53\\ 12.30\\ 13.07\\ 13.84\\ 14.59\\ 15.36\end{array}$	35 40 45 50 55 60 65 70 75 80 85 90 95 100	$\begin{array}{r} 6.35\\ 7.25\\ 8.15\\ 9.05\\ 9.95\\ 10.85\\ 11.75\\ 12.65\\ 13.55\\ 14.45\\ 15.35\\ 16.25\\ 17.15\\ 18.05\\ \end{array}$	38 43 48 59 65 70 75 81 86 91 97 102 108	$\begin{array}{r} 4.55\\ 5.20\\ 5.85\\ 6.50\\ 7.15\\ 7.80\\ 9.10\\ 9.75\\ 10.40\\ 11.05\\ 11.70\\ 12.35\\ 13.00\\ \end{array}$	32 37 42 46 51 55 60 65 69 74 79 83 88 92	$\begin{array}{r} 515\\ 589\\ 663\\ 736\\ 810\\ 883\\ 957\\ 1030\\ 1105\\ 1178\\ 1252\\ 1326\\ 1400\\ 1472 \end{array}$	5 lbs. per sq. ft. actual . per sq. ft. shipping weight
21 22 23 24	$199.5 \\ 209.0 \\ 218.5 \\ 228.0$	570 599 627 656 684	$16.13 \\ 16.90 \\ 17.67 \\ 18.44$	$105 \\ 110 \\ 115 \\ 120$	$\begin{array}{c} 18.95 \\ 19.85 \\ 20.75 \\ 21.65 \end{array}$	$     \begin{array}{r}       113 \\       118 \\       124 \\       129     \end{array} $	$13.65 \\ 14.30 \\ 14.95 \\ 15.60$	97 102 106 111	$1546 \\ 1620 \\ 1693 \\ 1768$	9.25 lbs.

Narrow 60 Inch Section, 11 Square Feet. Height 6011/16 Inch. Width 63/4 Inch

		5" Centers		5 ³ / ₈ " Centers		4 ⁵ ⁄8″ Ce	nters			
7 8 9 10 11 12 13 14 15 16 17 18 19 20 21 22 23 24	$\begin{array}{c} 77.0\\ 88.0\\ 99.0\\ 110.0\\ 121.0\\ 132.0\\ 143.0\\ 154.0\\ 154.0\\ 165.0\\ 176.0\\ 198.0\\ 209.0\\ 220.0\\ 220.0\\ 223.0\\ 223.0\\ 242.0\\ 253.0\\ 264.0 \end{array}$	$\begin{array}{c} 231\\ 264\\ 297\\ 330\\ 363\\ 396\\ 429\\ 462\\ 495\\ 528\\ 561\\ 594\\ 627\\ 660\\ 693\\ 726\\ 759\\ 792\\ \end{array}$	$\begin{array}{c} 6.45\\ 7.37\\ 8.29\\ 9.21\\ 10.13\\ 11.05\\ 11.97\\ 12.89\\ 13.81\\ 14.73\\ 15.65\\ 16.57\\ 17.50\\ 18.42\\ 19.34\\ 20.26\\ 21.18\\ 22.10\\ \end{array}$	$\begin{array}{c} 35\\ 40\\ 45\\ 50\\ 555\\ 60\\ 65\\ 70\\ 75\\ 80\\ 90\\ 905\\ 100\\ 105\\ 110\\ 115\\ 120\\ \end{array}$	$\begin{array}{c} 7.62\\ 8.70\\ 9.77\\ 10.85\\ 11.93\\ 13.00\\ 14.08\\ 15.15\\ 16.23\\ 17.31\\ 18.39\\ 19.46\\ 20.54\\ 21.62\\ 22.70\\ 23.78\\ 24.85\\ 25.93\\ \end{array}$	$\begin{array}{c} 38\\ 43\\ 48\\ 54\\ 59\\ 65\\ 70\\ 75\\ 81\\ 99\\ 70\\ 75\\ 81\\ 102\\ 108\\ 113\\ 118\\ 124\\ 129 \end{array}$	$\begin{array}{c} 5.47\\ 6.25\\ 7.03\\ 7.81\\ 8.59\\ 9.37\\ 10.15\\ 10.93\\ 11.71\\ 12.49\\ 13.27\\ 14.05\\ 13.27\\ 14.05\\ 15.61\\ 16.39\\ 17.17\\ 17.95\\ 18.73\\ \end{array}$	32 37 42 46 51 55 60 65 69 74 79 83 88 92 97 102 106 111	$\begin{array}{c} 604\\ 691\\ 777\\ 864\\ 950\\ 1037\\ 1123\\ 1210\\ 1295\\ 1382\\ 1469\\ 1555\\ 1641\\ 1727\\ 1813\\ 1900\\ 1985\\ 2072 \end{array}$	7.85 lbs. per sq. ft. actual 9.25 lbs. per sq. ft. shipping weight

[†]NOTE —Add to the width of stack 2½ inches for staggering of stacks. *NOTE —The actual length of one-inch pipe per square foot of outside surface is 2.9 lineal feet but is nominally figured at 3 lineal feet, as shown in the third column of above table.

## **Determination of Guarantees**

The case often arises that a guarantee to heat a building to a certain specified temperature must be demonstrated at a time when the outside temperature is much higher than called for in the guarantee. It then becomes important to know the exact relation between the increase in outside and inside temperature when apparatus is operated to its full capacity. This relation has been published for heating with direct radiation, but it varies considerably from the results obtained with the fan system. Naturally the rise in indoor temperature will be less than the rise in outdoor temperature owing to the fact that the condensing capacity has been shown to be directly proportional to the difference in temperature between steam and air, while with direct radiation it is not directly proportional owing to the variation in convection currents. The same relation between indoor and outdoor temperature may be shown to hold true whether the system was designed to take the air from outdoors entirely or to recirculate air within the building. The formula expressing the relation between indoor and outdoor temperature in either case is:

$$t_{r} = \frac{t_{r}'(t_{s} - t_{1}) + t_{s}(t_{1} - t_{1}')}{t_{s} - t_{1}'}$$
(110)

When the guarantee is based on an outside temperature of 0° the formula becomes

$$t_{r} = \frac{t_{r}'(t_{s} - t_{1}) + t_{s} \times t_{1}}{t_{s}}$$
(111)

 $t_r$  = temperature of building obtained with outside temperature  $t_1$ .

 $t_1 = any$  outside temperature at which test is made.  $t_r' = temperature of building guaranteed.$ 

 $t_1' =$  specified outside temperature.

 $t_{s}$  = temperature of steam at pressure specified.

The table on page 464 gives corresponding indoor temperatures as derived from equation above for various outdoor temperatures with guarantees at 60° to 95° in zero weather.

The table on page 465 giving mean monthly temperatures in different localities will be found useful in many instances in laying out heating systems.

## TABLE OF AVERAGE INDOOR TEMPERATURES MAINTAINED AT VARIOUS OUTDOOR TEMPERATURES WITH 5 LBS. STEAM PRESSURE

Outdoor Temp.	Average Indoor Temperatures Deg. Fahr.									
-20 -15 -10	45.2 48.9 52.9	50.8 54.3 57.9	$56.1 \\ 59.7 \\ 63.1$	$61.6 \\ 64.9 \\ 68.3$	67.1 70.3 73.5	72.5 75.6 78.7	77.9 80.9 86.0	83.4 87.3 89.2		
-5 0 5	$56.3 \\ 60.0 \\ 63.7$	$61.4 \\ 65.0 \\ 68.6$	$     \begin{array}{r}       66.5 \\       70.0 \\       73.5     \end{array}   $	71.6 75.0 78.4	76.8 80.0 83.2	$81.9 \\ 85.0 \\ 88.1$	87.0 90.0 93.0	92.1 95.0 97.9		
10 15 20	$67.4 \\ 71.0 \\ 74.7$	72.1 75.7 79.3	76.9 80.3 83.9	$81.7 \\ 85.1 \\ 88.4$	86.5 89.7 92.9	$91.3 \\ 94.4 \\ 97.5$	96.0 99.1 102.1	$100.8 \\ 103.7 \\ 106.6$		
25 30 35	$78.4 \\ 82.1 \\ 85.8$	$82.9 \\ 86.4 \\ 90.0$	87.3 90.8 94.3	91.8 94.1 97.5	$96.2 \\ 99.4 \\ 102.6$	$100.7 \\ 103.8 \\ 106.9$	$105.1 \\ 108.1 \\ 111.2$	$109.5 \\ 112.4 \\ 115.3$		
40 45 50	89.4 93.1 96.8	93.6 97.1 100.7	97.7 101.2 104.7	$101.8 \\ 105.4 \\ 108.5$	$105.9 \\ 109.1 \\ 112.4$	$110.0 \\ 113.2 \\ 116.3$	$114.2 \\ 117.2 \\ 120.2$	$118.2 \\ 121.1 \\ 124.0$		
55 60 65 70	$100.5 \\ 104.2 \\ 107.8 \\ 111.5$	$104.3 \\ 107.8 \\ 111.4 \\ 115.0$	$108.1 \\ 111.6 \\ 115.0 \\ 118.5$	$111.9 \\ 115.2 \\ 118.6 \\ 121.9$	$115.6 \\ 118.8 \\ 122.1 \\ 125.3$	$119.4 \\122.6 \\125.7 \\128.8$	$123.3 \\ 126.3 \\ 129.3 \\ 132.4$	$126.9 \\ 129.8 \\ 132.7 \\ 135.6$		

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 $74.1 \\ 72.6$  $43.9 \\ 36.0$ 52.1 43.0 N. Y. N. Vew York, 30.6 37.8 48.7 59.8 69.0 66.5 55.6 28.8 197 Chicago, 24.025.7 $34.9 \\ 46.2$ 56.6 66.5 72.3 64.8 53.1  $\frac{48.7}{41.5}$ 32.0 $212 \\ 119$ 39.4  $53.5 \\ 62.6$ 68.0 66.2  $22.0 \\ 23.8 \\ 23.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 3.8 \\ 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Pa. 31.832.840.050.8  $62.2 \\ 71.2$  $75.8 \\ 73.8 \\$ 67.4 56.344.935.728.3 190 95 Atlanta, Ga.  $42.2 \\ 45.2$ 69.5 75.6 76.1  $51.9 \\ 44.6$ 60.951.422.0 52.4 61.1 72.1 139 54 43.9 35.4 St. Paul, Minn.  $28.2 \\ 45.8$ 57.7 67.2  $72.0 \\ 69.7$  $60.5 \\ 48.4$ 31.0 39.0 11.9  $223 \\ 154$ 43.556.1 31.0 66.575.1 79.177.2 70.058.4 $\frac{43.4}{35.5}$  $55.8 \\ 43.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\ 13.1 \\$ 28.5 .0 M 178 90 'sino'l 'is Portland, Ore. 67.3 66.6 61.3 53.7 45.7 40.2  $52.8 \\ 49.9$  $\frac{46.1}{51.8}$  $57.7 \\ 62.5$ 25.7 38.7 41.4 $203 \\ 92$ Difference between 70° and mean during heating August ..... months ...... October ..... June September l'ebruary January May July

F. Tweedy in "Power," June 16, 1912.

MEAN MONTHLY TEMPERATURES IN DIFFERENT LOCALITIES

MEAN MONTHLY TEMPERATURES

# BUFFALO DUPLEX AUTOMATIC FEED PUMPS AND RECEIVERS



The unit consists of a suitably constructed cast iron receiving tank, mounted in combination with a Boiler Feed Pump on a common bed plate. The tank is mounted slightly above the pump, giving a sufficient head of water above the suction valves to insure the pump always receiving a full supply of water.

Within the tank is provided a float connected to a chronometer valve controlling the steam supply to the pump. Inflowing water causes float to rise, thereby opening the steam supply and starting the pump. When the water level has been lowered, the float automatically cuts off the steam. In this way the condensation water is returned to the boiler as fast as it accumulates.

Diameter Steam Cylinders	Diameter Water Pistons	Length of Stroke	Pump Capacity Gallons per Minute	Square Feet Direct Radiation Apparatus will Drain	Lineal Feet of 1-Inch Pipe Fan System Heater Apparatus Will Drain	Minimum Lbs. Steam Pressure Recommended					
With Standard Boiler Feed Pumps											
3 4 ½ 5 ¼ 5 ¼ 6 7 7 ½	$2 \\ 3 \\ 3 \\ 3 \\ 2 \\ 3 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4 \\ 1 \\ 2 $	3 1/2 4 5 6 8 8	10 20 40 45 60 80 100	$\begin{array}{c} 5000\\ 10000\\ 20000\\ 25000\\ 40000\\ 50000\\ 60000 \end{array}$	$\begin{array}{c} 2500 \\ 5000 \\ 10000 \\ 12500 \\ 20000 \\ 25000 \\ 30000 \end{array}$	50 40 35 35 35 35 30 30					
With Low Steam Pressure Pumps											
3 4 ¹ / ₂ 6 7 ¹ / ₃	$     \begin{array}{r}       1 \frac{1}{2} \\       2 \\       2 \\       2 \\       2 \frac{1}{2}     \end{array} $	3 ¹ / ₂ 4 6 6	$\begin{array}{r} 6\\11\\16\\25\end{array}$	3000 6000 9000 15000	$     \begin{array}{r}       1500 \\       3000 \\       4500 \\       7500 \\       7500     \end{array} $	$     \begin{array}{r}       35 \\       25 \\       10 \\       10 \\       10     \end{array} $					

# BUFFALO CENTRIFUGAL AUTOMATIC FEED PUMPS AND RECEIVERS



Centrifugal Pumps and Receivers are designed primarily for returning condensation from low-pressure systems into boilers, especially where steam pressure is so low as to prevent using reciprocating steam pumps. Centrifugal pumps should be especially designed for handling hot water and equipped with enclosed type polished brass runners or impellers. Receivers should be cast iron or similar material, strong enough to stand 50 pounds pressure. Centrifugal pumps are ordinarily equipped with 40 gallon receivers but smaller size receivers can be used if desired. Larger size receivers are not desirable, as the accumulated water should be returned to boiler as promptly as possible before it loses temperature.

The general method of operation of all electric driven pumps and receivers is the same. The condensation collects in receiver tank, raising large seamless copper float, until at a maximum point the float, by its connection, closes the float-switch, and an automatic starter starts the motor driving the pump. As the pump drains the receiver the float falls, until at a minimum point the float-switch is opened and the motor stops.

In determining proper size outfit to use it is necessary to know amount of radiation, boiler pressure, lift and pipe friction to boiler and details of electric eurrent. On low steam pressure outfits about 30 per cent. margin should be allowed in figuring power, as water at 10 pounds pressure cannot be forced into a boiler carrying 10 pounds steam pressure.

## GAS HEATERS

Various forms of heaters have been devised for use in connection with fans, utilizing the heat of the gases direct rather than through the medium of a steam boiler.

The efficiency of a gas-fired steam boiler, according to tests by Jay M. Whitman, is seldom in excess of 65 to 70 per cent. Some forms of gas heaters have been short-lived, no provision having been made to prevent temperatures in the heating surfaces so high as to destroy them in one or two heating seasons. To be reasonably long-lived, the heat must be transmitted from gas to air through surfaces which are not exposed to temperatures above 1200° F., and the construction must permit the renewal of this heating surface at least as conveniently as in the case of a boiler. These requirements can best be met by a design in which the heating surface proper consists of boiler tubes expanded into heads, the gases passing through the tubes, and the air drawn across them by the fan, while for best economy the range of temperature for the gases is from 1200° to 400° F. With natural gas or producer gas fuel, this design of heater has been combined with a combustion chamber provided with fire brick checker work, which, becoming incandescent, provides for the complete combustion of the mixture of gas and air before it leaves the chamber; a mixing chamber in which the high temperature products of combustion are mixed with low temperature gases which have already passed through the heater, and which in any desired proportion may be recirculated by an induced draft fan: an exhaust chamber from which the induced draft fan draws the cooled gases, part of which are discharged and part recirculated, and a suitable setting with boiler fronts and inspection doors, so as to make the various chambers accessible.

With natural gas having a calorific value of 1000 B. t. u., the loss in the waste gases discharged at 400° is approximately 60 B. t. u., corresponding to an efficiency of 94 per cent. When running at part load, and allowing for possible poor regulation of the burners, such a heater still has an efficiency better than a good steam boiler. Where producer gas is available instead of natural gas, similar economy will be shown. The high temperature exhaust from gas engines, if of sufficient volume and regular in quantity, waste gases from furnaces, or even under some conditions from boiler plants, may be utilized to good advantage.

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# SECTION VI AIR CONDITIONING APPARATUS

## Air Washers

Air washers are generally used in connection with ventilating systems for public buildings, offices and residences. Their efficiency in purifying the air varies greatly with their construction and also depends in a large measure upon the nature and quantity of the impurities in the air to be washed. In general, the heavier particles in the air, such as street dust for instance, are comparatively easy to remove even with a washer of simple construction. On the other hand, the very fine particles often existing in city air, especially where it is taken some distance from the ground, where the impurities consist chiefly of fine ash and smoke particles, are exceedingly difficult to remove, and the most efficient air washer construction is required to get satisfactory results, or in fact, any results which will be worth the cost of installing an air washing device.

## **Principles of Air Washer Construction**

It has been found by experiment, and is now generally acknowledged by engineers, that in washing air or gas the first essential is to fill the chamber through which it is passed with a finely divided spray or mist in order to get as great a contact surface as possible between the water and air and to secure a thorough mixture. Probably the most satisfactory way of accomplishing this is by the use of a large number of uniformly spaced centrifugal nozzles with large orifices to prevent clogging with foreign material. It has been found practicable to use orifices %-inch in diameter in centrifugal nozzles which will give a satisfactory division and distribution of spray and at the same time will not clog. The nozzles should spray in the direction of the air flow.

An adequate filtering system should be provided, where the water is recirculated, in order to remove any large obstructions that might otherwise enter the spray system.

NOTE -For a general discussion on the subject of Humidity, see page 28; and on Air Washing, Cooling, Humidifying and Drying, see page 67.

The velocity through the washer for best results should be between 400 and 500 feet per minute. It is equally important that the air be distributed uniformly over the entire area of the washer. This is often difficult to accomplish and can only be secured by means of a diffuser or distributing plate at the washer inlet.

While some work may be done with a finely divided spray, it cannot be depended upon alone to give satisfactory cleaning effect. The air after having been moistened must be brought into repeated contact with wetted surfaces and subjected to the combined action of impact and centrifugal force. For the best results, the air should also be divided and broken up into as narrow layers or strata as may be possible mechanically, in order, 1st, that as great a contact surface may be secured as possible, and 2nd, that the solid particles contained in the air shall have as small a distance to travel as possible before coming into contact with a wetted surface where they will be entrained. This is best accomplished by placing in the eliminators large, independently flooded vertical surfaces. The plates forming this flooded surface should be placed as closely as possible, preferably about 1 inch apart, arranged vertically and flooded from the top. An extension of these surfaces should be provided with lips for the removal of all traces of free moisture. A satisfactory ratio has been found to be 64 sq. ft. of combined washing and eliminating surface per 1000 cu. ft. of air per minute.

In public building work provision should be made for heating the spray water and controlling the moisture content of the air in cold weather. The simplest method of accomplishing this is to regulate the temperature of the air leaving the washer by means of a thermostat, at the same time saturating the air by means of a heated spray at a variable temperature.

Air conditioning apparatus for controlling the humidity of air for manufacturing processes may be broadly classified, according to use, into humidifiers proper, which add moisture to the air in required amounts; and dehumidifiers, which remove a variable quantity of moisture from the air to reduce it to the required standard. The relative humidity of the air may also be altered, and in a measure regulated, simply by changing its temperature without affecting its moisture contents.

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## **Types of Humidifiers**

Humidifiers may be classified into the spray and evaporative types, the latter being divided again into direct and indirect. The humidity of the air may also be increased by the direct introduction of steam into the air supply or into the room. Since the total heat of the vapor at atmospheric temperature is somewhat less than the total heat at steam temperature, this raises the temperature of the air perceptibly and is therefore intolerable in the majority of cases. Added objections to the direct use of steam are that it frequently gives a noticeable odor and that it is difficult to regulate. The spray and evaporative types of humidifiers have a distinct value aside from humidifying in their possession of a cooling effect which is in direct proportion to their moistening effect. The direct spray type of humidifier is distinguished from the evaporative type in that it introduces a finely divided or atomized spray directly into the room in constant volume, while the evaporative type introduces only the water vapor. There is also a mixed type which discharges both moist air and free moisture into the room.

In what may be termed the indirect evaporative humidifier the air is partly or entirely taken from the outside and is humidified and conditioned before it is introduced into the room. In the direct evaporative type the water vapor passes directly into the air of the room. The indirect system of air conditioning is also termed the central system, and is known commercially as the Carrier System.

#### The Dehumidifier

In the dehumidifier, relatively cold spray water is used to condense the moisture out of the air. The water is either refrigerated or taken from an artesian well. When the water is artificially cooled the refrigerating coils are usually placed in a chamber underneath the spray chamber, and the water is so distributed as to flow uniformly over the cold surface, dropping to the tank underneath. The dehumidifier has its sprays opposed to the direction of air flow as in the humidifier, but differs from the latter in having usually two sets of sprays in series instead of one. Two or more dehumidifiers are frequently placed in series when the range of air temperature is great or when an economy of cooling water is essential.

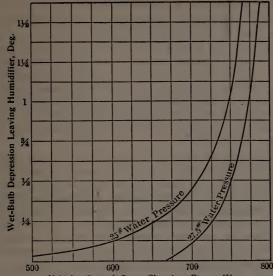
## **Elements of Design of Humidifiers**

The degree of saturation of the air leaving any type of air washer or humidifier depends upon the intimacy of the contact of the air and water, and upon the relation of the water temperature to the wet-bulb temperature of the entering air. It also depends to some degree upon the length of the spray chamber as well as upon the velocity of the air passing through it.

The size of the nozzle orifice is also a very important factor in determining the degree of saturation obtained. In general, the smaller the nozzle orifice the more perfect will be the humidifying effect with a given quantity of water. For humidifiers it is standard practice to use centrifugal nozzles having a 3-32 inch orifice, and where rotary strainers are employed for filtering the spray water the nozzle orifice may be reduced to 1-16 inch in diameter to advantage.

With the centrifugal type of spray nozzles the water pressure is a most important element affecting the degree of saturation. The accompanying diagram shows the humidifying effect secured with various velocities and at different pressures on the spray nozzle, in a standard humidifier having four 3-32 inch orifice centrifugal spray nozzles per square foot. This data was obtained from a test in which the wet-bulb depression of the entering air was maintained constant at 16°. It will be noted that an increase of 21/2 pounds in the spray pressure permitted a greatly increased velocity with perfect saturation, an effect which was undoubtedly due to the increased fineness of the spray rather than to the increase in the amount of water discharged. In this test, as in all standard humidifiers, the water was discharged in the direction opposite the air flow, increasing the efficiency of saturation.

When the spray water is recirculated without heating, as in warm weather, it remains at all times substantially at the wetbulb temperature of the entering air, while the wet-bulb temperature of the air leaving the washer or dehumidifier is unchanged; therefore it follows in conformance with the theory, that when the air is completely saturated as in the humidifier the air is cooled to the wet-bulb temperature of the incoming air. This cooling effect is due to evaporation and is therefore in direct proportion to the moisture added to the air. The wet-bulb depression in atmospheric air averages from 12° to 15° in summer,



Velocity through Spray Chamber, Ft. per Min.

while occasionally a depression of 20° to 30° is found in extremely hot and dry weather. In every case a properly designed humidifier will cool the incoming air a corresponding number of degrees.

When saturation is incomplete, as in the ordinary air washer, the wet-bulb depression of the air leaving the washer is found to be a constant percentage of the initial wet-bulb depression, when the air velocity remains constant.

It follows that the cooling effect is a constant percentage of the initial wet-bulb depression. This may be expressed by the formulae

$$\frac{t_2 - t'}{t_1 - t'} = R$$
$$\frac{t_1 - t_2}{t_1 - t'} = 1 - R = E$$

where

t' = constant wet-bulb temperature.

 $t_1 = temperature of air entering washer.$ 

 $t_2 = temperature of air leaving washer.$ 

R=constant ratio depending upon intimacy of contact, air velocity, etc.

 $\mathbf{E} = \text{efficiency of saturation.}$ 

## Elements of Design of Spray Type of Dehumidifiers

Dehumidifiers may be of the spray type previously described, or of the surface type. A knowledge of the relation of water temperature to the leaving air temperature in either type is essential. In the spray type of one stage having two banks of opposed nozzles, the air temperature leaving is practically identical with the temperature of the leaving water, the difference never exceeding one degree in a properly designed apparatus. The air will always be saturated when leaving and under some conditions there is a slight tendency to entrainment even after thorough elimination.

The degree of entrainment is dependent upon the range of temperature of both the air and the water. In general, the smaller the temperature range, the less the tendency is to moisture entrainment or supersaturation. This may be reduced where a considerable lowering of air temperature is required by passing it successively through two or more dehumidifiers in series. When the system is properly designed, the entrainment should not be sufficient to raise the true dew-point temperature more than one degree.

## **Refrigeration Required for Dehumidifying**

The heat to be removed in cooling a known weight of air from a given temperature and moisture content to a given dewpoint temperature, is evidently the difference of the total heat quantities contained in the air under these respective conditions. These values of total heat are given on the charts on pages 36 and 37. It is there shown that the total of latent and specific heat in one pound of pure air is dependent upon the wet-bulb temperature only. The upper table on page 475 shows the amount of refrigeration required to cool and dehumidify 1000 cu. ft. of air between various given wet-bulb temperatures and final dew-points.

### Power Required for Operating Humidifiers

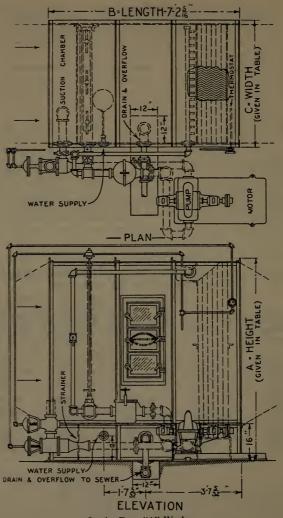
The lower table on page 475 exhibits the power required to saturate 1000 cu. ft. of air per minute at various velocities. This is based on overcoming the resistance of the humidifier, using a fan with a static efficiency of 45 per cent., a fair value.

#### B. T. U. REFRIGERATION REQUIRED TO COOL 1000 CU. FT. OF AIR (MEASURED AT 70 DEG. F.) FROM A GIVEN WET-BULB TEMPERATURE TO A GIVEN DEW-POINT

Dew-Point	emperature	re (Gauge)	mpressor 15 Lb.	power Com- orsepower ted Suction Lb. Gauge		Er	ntering	Wet-Bu	lb Tem	peratu	re	
Leaving De	Ammonia Tei	Suction Pressure	Per Cent. Co Ratings at	Per Cent. Horse pared with Ho Required at Ra Pressure of 15	50	55	60	65	70	75	80	85
65 60 55	45 40 35	$\begin{array}{c} 65.96 \\ 58.29 \\ 51.22 \end{array}$	270 244 220	45.5			221.5	259.0 480.5	296 553 777	606 865 1086	961 1220 1440	$1350 \\ 1609 \\ 1840$
50 45 40	30 25 20	44.72 38.73 33.25	199 182 164		185 359	203 388 569	425.0 611.0 791.0	683.0 869.0 1050.0	$980 \\ 1165 \\ 1345$	1290 1474 1656	1570 1830 2010	2030 2220 2400

#### RESISTANCE OF CARRIER HUMIDIFIERS AND HORSEPOWER REQUIRED TO HUMIDIFY 1000 CU. FT. OF AIR

Velocity Through Spray Chamber in Ft. per Min.	Resistance in In. of Water	Horsepower to Move 1000 Cu. Ft. Air per Min. at 45% Fan Efficiency	Horsepower for Spray per 1000 Cu. Ft. of Air (½6 Orifice Nozzle)	Total Horsepower Required per 1000 Cu. Ft. of Air
350	0.112	0.0391	0.1408	0.1799
400	0.147	0.0513	0.1231	0.1744
450	0.186	0.0652	0.1095	0.1747
500	0.229	0.0800	0.0985	0.1785
550	0.277	0.0968	0.0897	0.1865
600	0.330	0.1150	0.0822	0.1972
650	0.387	0.1350	0.0758	0.2108
700	0.450	0.1570	0.0704	0.2274
750	0.516	0.1810	0.0658	0.2468



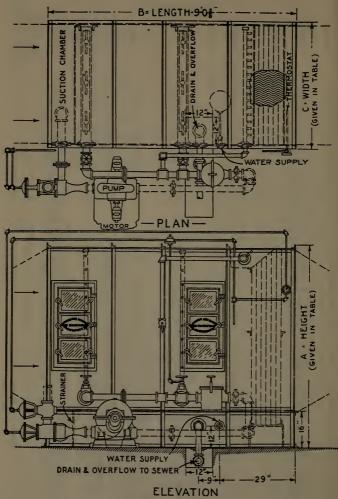
Carrier Type "A" Washer

## AIR WASHER DIMENSIONS

## DIMENSIONS FOR CARRIER TYPE "A" AIR WASHERS

					-					
Number	Capacity in C. F. M.	Height A	Length	Width	G. P. M. Circulated	Size Pump Inches	H. P. Motor	R. P. M. Motor	Size Water Supply Inches	Size Sewer Con- nection Inches
A B A C B A A B C B D C B C D C E D C D E D F E D E D F D E D F D E D F G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E G E F E 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Additional sizes and capacities on request.



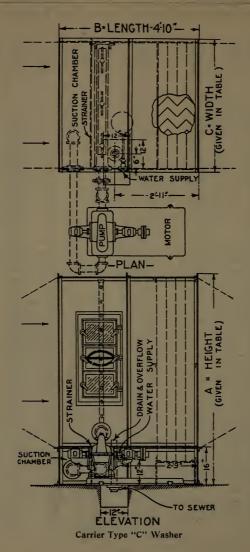
Carrier Type "B" Washer

#### AIR WASHER DIMENSIONS

### DIMENSIONS FOR CARRIER TYPE "B" AIR WASHERS

Number	Capacity in C. F. M.	Height A	Length B	Width	G. P. M. Circulated	Size Pump Inches	H. P. Motor	R. P. M. Motor	Size Water Supply Inches Size Sewer Con-
ABACB AABCB DCBCD CEDCD EDFED EFDED FDEFD EDFGE FEGEF 11212 344344 23543 53465 46457 65879 610871 9128710 91181210 1181210	1500 2100 3100 3200 6400 6700 69000 9400 10500 11300 14100 14300 21300 21300 24300 24300 29400 24300 29400 31000 33900 36700 366700 44500 49100 555000 555000 555000 60000 61000 62000 67000 68000 74000 755000	4'11%", ************************************	$\begin{array}{c} 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03''' \\ 9'03'''' \\ 9'03'''' \\ 9'03'''' \\ 9'03'''' \\ 9'03''''' \\ 9'03'''''''''''''''''''''''''''''''''''$	$\begin{array}{c} 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 5 \\ 1' & 0 \\ 1' & 1' \\ 2' & 9 \\ 1' & 0 \\ 2' & 9 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' & 0 \\ 1' &$	$\begin{array}{c} 23\\ 27\\ 46\\ 41\\ 54\\ 692\\ 81\\ 106\\ 104\\ 123\\ 164\\ 123\\ 164\\ 123\\ 164\\ 123\\ 164\\ 155\\ 205\\ 189\\ 247\\ 259\\ 247\\ 259\\ 247\\ 259\\ 311\\ 3314\\ 345\\ 440\\ 466\\ 463\\ 520\\ 573\\ 564\\ 440\\ 466\\ 463\\ 520\\ 573\\ 564\\ 461\\ 628\\ 694\\ 617\\ 772\\ 259\\ 566\\ 691\\ 777\\ 259\\ 566\\ 691\\ 777\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 694\\ 617\\ 772\\ 258\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 772\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 775\\ 758\\ 7758\\ 775\\ 758\\ 7758\\ 7758\\ 7758\\ 7758\\ 7758\\ 7758\\ 7758\\ 7758\\ 7758$	111111 112222 22222 22223 3 3 4 4 4 4 4 4 4 4 4 4	$\begin{array}{c} 2\\ 2\\ 2\\ 2\\ 2\\ 3\\ 3\\ 3\\ 3\\ 3\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\ 5\\$	1706 1700 1700 1700 1700 1700 1700 1700	S
9 G 13 E 11 F 14 E 10 G	79000 80000 82000 87000 88000	15'2'' $11'1_{34''}''$ $13'1_{34''}'''$ $11'1_{34''}'''$ 15'2'''	9'0 3'8" 9'0 3'8" 9'0 3'8" 9'0 3'8" 9'0 3'8" 9'0 3'8"	$\begin{array}{c} 12' & 0'' \\ 17' & 2 \frac{1}{4''} \\ 14' & 6 \frac{3}{4''} \\ 18' & 6'' \\ 13' & 3 \frac{1}{2''} \end{array}$	792 817 849 881 880	5 6 6 6	20 20 20 20 20 20	$ \begin{array}{c c} 1120\\ 1120\\ 1120\\ 1120\\ 1120\\ 1120\\ 1120\\ \end{array} $	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$

Additional sizes and capacities on request.



#### AIR WASHER DIMENSIONS

## DIMENSIONS FOR CARRIER TYPE "C" AIR WASHERS

Number	Capacity in C. F. M.	Height	Length	Width C	G. P. M. Circulated	Size Pump Inches	H. P. Motor	R. P. M. Motor
1 A 1 B 1 C 2 A 2 B 3 A	$     \begin{array}{r}       1700 \\       2300 \\       3400 \\       3500 \\       4800 \\       5400 \\     \end{array} $	4'1 ½" 5'1 ½" 7'1 ½" 4'1 ½" 5'1 ½" 4'1 ½"	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$\begin{array}{c} 1' & 5 & \frac{1}{4}'' \\ 1' & 5 & \frac{1}{4}'' \\ 1' & 5 & \frac{1}{4}'' \\ 2' & 9'' \\ 2' & 9'' \\ 2' & 9'' \\ 4' & 0 & \frac{3}{4}'' \end{array}$	9 11 18 18 22 27	$ \begin{array}{c} 1 \frac{1}{2} \\ 1 \frac{1}{2} $	$\begin{array}{c}2\\2\\2\\2\\2\\2\\2\\2\end{array}$	1700 1700 1700 1700 1700 1700
4 A 3 B 2 C 4 B 2 D 3 C	7300 7300 7300 9800 9800 11000	$\begin{array}{c} 4'1 \frac{1}{2}'' \\ 5'1 \frac{1}{2}'' \\ 7'1 \frac{1}{2}'' \\ 5'1 \frac{1}{2}'' \\ 9'1 \frac{1}{2}'' \\ 7'1 \frac{1}{2}'' \\ 7'1 \frac{1}{2}'' \end{array}$	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$5' 4 \frac{1}{2'}$ $4' 0 \frac{3}{4''}$ $2' 9''$ $5' 4 \frac{1}{2''}$ $2' 9'''$ $4' 0 \frac{3}{4''}$	36 33 36 43 47 54	$ \begin{array}{c} 1 \frac{1}{2} \\ \end{array} $	2 2 2 2 2 3	1700 1700 1700 1700 1700 1700
5 B 4 C 3 D 5 C 3 E 4 D	12300 14900 14900 18700 18700 20000	5'1 ½" 7'1 ½" 9'1 ½" 7'1 ½" 11'1 ¾" 9'1 ½"	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$\begin{array}{c} 6' & 8'' \\ 5' & 4 \frac{1}{2}'' \\ 4' & 0 \frac{3}{4}'' \\ 6' & 8'' \\ 4' & 1 \frac{1}{4}'' \\ 5' & 4 \frac{1}{2}'' \end{array}$	54 72 70 90 87 94	$     \begin{array}{r}       1 & \frac{1}{2} \\       1 & \frac{1}{2} \\       1 & \frac{1}{2} \\       2 \\       2 \\       2 \\       2     \end{array} $	3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3 3	1700 1700 1700 1700 1700 1700
6 C 5 D 4 E 6 D 4 F 5 E	$\begin{array}{c} 22500\\ 25200\\ 25200\\ 30300\\ 30300\\ 31600 \end{array}$	$\begin{array}{c} 7'1 \frac{1}{2''}\\ 9'1 \frac{1}{2''}\\ 11'1 \frac{3}{4''}\\ 9'1 \frac{1}{2''}\\ 13'1 \frac{3}{4''}\\ 11'1 \frac{3}{4''}\end{array}$	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$7'11\frac{3}{4}''$ $6'8''$ $5'5''$ $7'11\frac{3}{4}''$ $5'5''$ $6'8\frac{1}{2}''$	108 117 115 140 144 144	$2 \\ 2 \\ 2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/2 \\ 2 \\ 1/$	555555	1700 1700 1700 1700 1700 1700
7 D 6 E 5 F 8 D 7 E 9 D	$\begin{array}{r} 35400 \\ 38000 \\ 38000 \\ 40500 \\ 44500 \\ 45700 \end{array}$	$\begin{array}{c} 9'1 \frac{1}{2''} \\ 11'1 \frac{3}{4''} \\ 13'1 \frac{3}{4''} \\ 9'1 \frac{1}{2''} \\ 11'1 \frac{3}{4''} \\ 9'1 \frac{1}{2''} \end{array}$	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$\begin{array}{c} 9' \ 3 \ \frac{1}{2''} \\ 8' \ 0 \ \frac{1}{4''} \\ 6' \ 8 \ \frac{1}{2''} \\ 10' \ 7 \ \frac{1}{4''} \\ 9' \ 4'' \\ 11'11'' \end{array}$	164 173 180 187 202 210	$\begin{array}{c} 2 \frac{1}{2} \\ 2 \frac{1}{2} \end{array}$	5 5 5 5 7 1/2 7 7	1700 1700 1700 1700 1700 1700 1700
6 F 10 D 8 E 7 F 11 D 9 E	45800 50500 51000 53500 56000 57500	13'1 34" 9'1 ½" 11'1 34" 13'1 34" 9'1 ½" 11'1 34"	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$\begin{array}{c} 8' & 0 & \frac{1}{4''} \\ 13' & 2 & \frac{1}{2''} \\ 10' & 7 & \frac{3}{4''} \\ 9' & 4'' \\ 14' & 6 & \frac{1}{4''} \\ 11' 11 & \frac{1}{2''} \end{array}$	216 234 230 252 258 259	3 3 3 3 3 3 3 3	7 1/2 7 1/2 7 1/2 7 1/2 7 1/2 7 1/2 7 1/2	1700 1700 1700 1700 1700 1700 1700
12 D 8 F 7 G 10 E 9 F 11 E	$\begin{array}{c} 61000\\ 61000\\ 62500\\ 63500\\ 69000\\ 70000 \end{array}$	$\begin{array}{c} 9'1 \frac{1}{2''} \\ 13'1 \frac{3}{4''} \\ 15'2'' \\ 11'1 \frac{3}{4''} \\ 13'1 \frac{3}{4''} \\ 11'1 \frac{3}{4''} \end{array}$	4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$\begin{array}{c} 15'10''\\ 10'&7{}^{3}4''\\ 9'&4{}^{1}2''\\ 13'&3''\\ 10'&8{}^{1}4''\\ 14'&6{}^{3}4''\\ \end{array}$	281 288 290 288 324 317	3 3 3 4 4	$ \begin{array}{c} 7\frac{1}{2} \\ 7\frac{1}{2} \\ 7\frac{1}{2} \\ 7\frac{1}{2} \\ 7\frac{1}{2} \\ 10 \\ 10 \end{array} $	$     \begin{array}{r}       1700 \\       1700 \\       1700 \\       1700 \\       1120 \\       1120 \\       1120 \\       \end{array} $
8 G 12 E 10 F 9 G 13 E 11 F 10 G 14 E	$\begin{array}{c} 72000 \\ 76500 \\ 77000 \\ 81000 \\ 83000 \\ 85000 \\ 90000 \\ 90000 \end{array}$	15'2" 11'1 ³ 4" 13'1 ³ 4" 15'2" 11'1 ³ 4" 13'1 ³ 4" 15'2" 11'1 ³ 4"	4'10" 4'10" 4'10" 4'10" 4'10" 4'10" 4'10" 4'10" 4'10"	$\begin{array}{c} 11'11 \frac{1}{2''}\\ 15'10 \frac{1}{2''}\\ 13' 3''\\ 12' 0''\\ 17' 2 \frac{1}{4''}\\ 14' 6 \frac{3}{4''}\\ 13' 3 \frac{1}{2''}\\ 18' 6''\end{array}$	$\begin{array}{r} 332\\ 346\\ 360\\ 373\\ 375\\ 396\\ 414\\ 404 \end{array}$	4 4 4 4 4 4 4 4 4 4	1 10 10 10 10 10 10 10 10	$1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ 1120 \\ $

Water supply 34 inch, sewer connection 2 inches on all sizes. Additional sizes and capacities on request.

## SECTION VII

## STEAM ENGINES

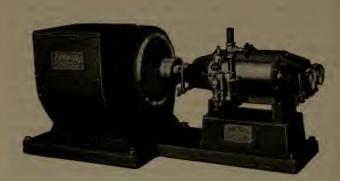
In the following section will be found capacity and specification tables of Buffalo Steam Engines.

Two diagrams are given, showing the water rate of high speed engines and the ratio of the water rate at any cut-off as compared to the rated water rate, when the engines are rated at 3% cut-off. As an example of the use of these diagrams, we will take a case of a 100 H. P. high speed engine with steam pressure at 100 pounds and cutting off at 3% stroke. From the curve on page 486 we find the steam consumption will be 28 pounds per indicated H. P., or a total of 2800 pounds per hour. In case this was a heating job this would then be a measure of the amount of exhaust steam available for use in the heating coils. If. for any reason, this engine should be set to cut off at 5% stroke, we may determine the resulting steam consumption from the diagram on page 487. From the point marked 5% cut-off on the right edge of the chart, pass horizontally to the left until the cut-off line is intersected, thence downward to the curve, and horizontally to the left edge, where we find the water rate will be 104.2 per cent. of the rated. That is,  $1.042 \times 28 = 29.2$  pounds per I. H. P. per hour.

The per cent. of rated load that will be developed may be determined from the scale at the bottom of the diagram. Drop vertically from the intersection of the  $\frac{5}{8}$  cut-off with the cut-off line to the bottom of the chart, where it will be found that the engine when cutting off at  $\frac{5}{8}$  stroke will develop 137.5 per cent. of the rated load, or  $1.375 \times 100 = 137.5$  I. H. P.

The table of mean effective pressures has been calculated from actual indicator cards taken from automatic high speed engines. These values are applicable to engines of this class when exhausting at atmospheric pressure. In case back pressure is carried on the engine a corresponding correction should be made. The horsepower tables for the various classes of engines give the brake horsepower per R. P. M., the maximum speed allowable and the corresponding horsepower developed. There are two factors limiting the speed of these engines; first, a maximum allowable piston speed; and second, the maximum load allowable, as indicated in the dimension table of each particular engine. In the case of the automatic engines the governors do not operate at a speed less than two-thirds of the maximum. There are a number of cases in the tables on pages 490 and 491 where, at certain steam pressures and cut-offs it was found necessary to limit the speed to less than two-thirds of the maximum in order to avoid overloading the corresponding engine frame. As indicated on the tables, these engines will have to be operated throttling, since the automatic governors will not be operative at these low speeds.

The two tables on pages 496 and 497 are applicable to Buffalo Class "A" automatic high speed engines. The maximum speed for each engine is shown, together with the minimum speed when operating with the automatic governor and also the brake horsepower that will be developed at the different steam pressures. Except as indicated these values are based on the engines operating at one-half cut-off. Those cases marked will have to cut off at less than one-half stroke in order to avoid overloading the engine.



Spiro Driven Niagara Conoidal (Type N) Fan for Forced Draft



Spiro Driven Gas Blower Unit

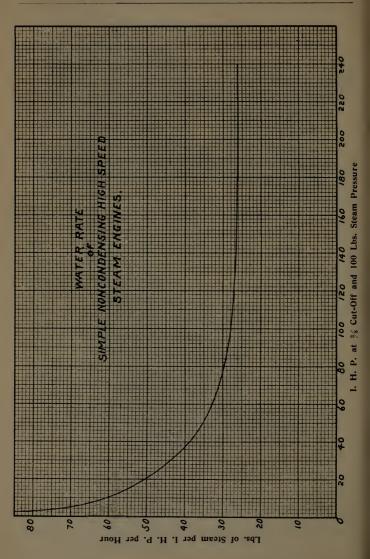
These illustrations show the adaptability of direct connecting various types of fans to Spiro Steam Turbines, which are made in sizes from 1 to 100 horsepower and operate very economically at a comparatively low speed.

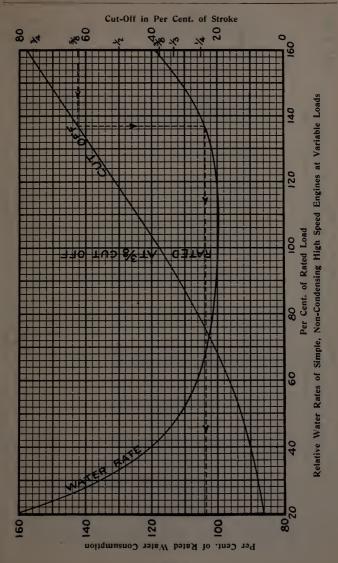
ure ge			Cut	-off		
Steam Pressure Gauge	1⁄4	1/8	3⁄8	⅔	5⁄8	3⁄4
15 20 25	3.0 4.8 6.7	4.4 6.6 8.7	5.1 7.4 9.7	6.8 9.4 12.1	$8.5 \\ 11.5 \\ 14.5$	$9.7 \\ 13.1 \\ 16.4$
30 35 40	$8.5 \\ 10.3 \\ 12.2$	10.8 13.0 15.1	$11.9 \\ 14.2 \\ 16.5$	$14.7 \\ 17.4 \\ 20.0$	$17.6 \\ 20.6 \\ 23.6$	19.8 23.1 26.4
45 50 55	14.0 15.8 17.7	$17.3 \\ 19.4 \\ 21.6$	$18.8 \\ 21.0 \\ 23.4$	$22.6 \\ 25.4 \\ 28.0$	$26.6 \\ 29.6 \\ 32.7$	29.8 33.1 36.5
60 65 70	19.5 21.4 23.2	23.7 25.8 28.0	25.7 28.0 30.2	30.7 33.4 36.0	$35.7 \\ 38.7 \\ 41.8$	39.8 43.2 46.5
75 80 85	$25.0 \\ 26.9 \\ 28.7$	$30.2 \\ 32.3 \\ 34.4$	$32.6 \\ 34.8 \\ 37.1$	38.6 41.2 43.9	44.8 47.9 50.8	49.9 53.1 56.5
90 95 100	30.6 32.4 34.3	36.6 38.8 40.8	$39.4 \\ 41.6 \\ 44.0$	46.7 49.3 51.9	53.9 57.0 . 60.0	59.9 63.3 66.5
105 110 115	$36.1 \\ 38.0 \\ 39.8$	43.0 45.2 47.4	46.3 48.5 50.8	$54.5 \\ 57.1 \\ 60.5$	63.7 66.1 69.0	70.0 73.3 76.6
120 125 130	$41.6 \\ 43.5 \\ 45.2$	$49.5 \\ 51.6 \\ 53.6$	53.1 55.3 57.7	63.0 65.0 67.9	72.0 75.1 78.2	80.0 83.4 86.6
135 140 150	47.1 49.0 52.7	55.9 57.9 62.4	$\begin{array}{c} 60.0 \\ 62.4 \\ 66.9 \end{array}$	70.5 73.2 78.5	81.1 84.3 90.2	90.0 93.4 100.0

## M. E. P. OF HIGH SPEED ENGINES*

Allowance Made for 10 Per Cent. Clearance and without Back Pressure

*Note-Based on indicator cards from an automatic high speed engine.





**60 lbs. 1** 

CLASS "A" HORIZONTAL AND VERTICAL-STEAM PRESSURE, 60 LB. GAUGE BUFFALO HIGH SPEED ENGINES

Brake Horsepower per R. P. M. and Maximum R. P. M. and Horsepower Allowable

	Max. B. H. P.	4.6 7.8 12.8 18.5	15.2 27.0 42.1	29.5 46.1 60.6	47.4 68.2 80.1	71.7 97.5 111.8	106.5 122.0 153.5 189.6
% Cut-off	Max. R.P.M.	550 475 410 410	400 400	350 350 320	300 300 300	270 270 270	225 225 200 200
	B. H. P. R. P. M.	.0084 .0164 .0284 .0452	.0379 .0674 .1053	.0843 .1317 .1897	.1580 .2276 .2671	.2651 .3609 .4142	.4747 .5402 .7681 .9480
	Max. B. H. P.	3.9 6.6 10.7 16.2	$12.8 \\ 22.7 \\ 35.5$	24.8 38.8 55.7	39.9 57.5 67.5	60.3 82.0 94.2	90.0 102.0 129.3 159.5
1/2 Cut-off	Max. R. P. M.	550 475 425 425	400 400 400	350 350 350	300 300 300	270 270 270	225 225 200 200
	B. H. P. Per R. P. M.	.0071 .0138 .0239 .0380	.0319 .0567 .0886	0709.1108.11596	.1330 .1915 .2248	.2231 .3038 .3485	.3995 .4544 .6462 .7976
	Max. B. H. P.	3:2 5:4 13:2 2:2	$10.4 \\ 18.5 \\ 29.0 \\ 29.0 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ 10.4 \\ $	20.3 31.8 45.7	32.6 47.0 50.9	49.4 67.2 77.0	73.6 83.8 105.8 130.6
% Cut-off	Max. R. P. M.	550 475 450 425	400 400 400	350 350 350	300 300 300	270 270 270	225 225 200 200
	B. H. P. Per R. P. M.	.0058 .0113 .0196 .0311	.0261 .0464 .0726	.0581 .0908 .1307	.1089 .1568 .1697	.1826 .2487 .2853	.3270 .3720 .5291 .6531
	Max. B. H. P.	$2.9 \\ 4.9 \\ 8.1 \\ 12.1$	$   \begin{array}{c}     9.5 \\     16.9 \\     26.5   \end{array} $	$   \begin{array}{r}     18.6 \\     28.9 \\     41.7   \end{array} $	29.8 42.9 50.4	45.0 61.2 70.3	67.3 76.4 78.6 119.1
1/8 Cut-off	Max. R.P. M.	550 475 425 425	400 400	350 350 350	300 300 300	270 270 270	225 225 200
4	B. H. P. R. P. M.	.0053 .0103 .0179 .0284	.0238 .0423 .0662	.0530 .0827 .1191	.0993 .1430 .1678	.1666 .2266 .2602	.2982 .3391 .4825 .5955
Cylinder	Diameter and Stroke	46514 XXXX 46514	6 x 8 8 x 8 10 x 8 8 8 8	8 x 10 10 x 10 12 x 10	10 × 12 12 × 12 13 × 12	12 x 14 14 x 14 15 x 14	15 x 16 16 x 16 18 x 18 20 x 18

Norm-Minimum speed to be not less than two-thirds the Maximum for Automatic Governors.

BUFFALO HIGH SPEED ENGINES

80 lbs.

CLASS "A" HORIZONTAL AND VERTICAL-STEAM PRESSURE, 80 LB. GAUGE

Brake Horsepower per R. P. M. and Maximum R. P. M. and Horsepower Allowable

	Max. B. H. P.	5.6 10.5 17.3 18.5	20.3 36.2 41.8	39.6 60.2 60.0	63.6 88.5 88.0	$   \begin{array}{c}     96.0 \\     125.5 \\     125.0 \\   \end{array} $	$\begin{array}{c} 143.2 \\ 162.9 \\ 206.0 \\ 254.4 \end{array}$	
5% Cut-off	Max. R. P. M.	490 475 450 305	400 400 295	350 340 235	300 290 245	270 260 225	225 225 200 200	
1.3/	B. H. P. R. P. M.	.0113 .0221 .0382 .0606	.0509 .0904 .1414	.1131 .1767 .2545	.2120 .3053 .3583	.3557 .4842 .5558	$\begin{array}{c} .6369\\ .7245\\ 1.0305\\ 1.2720\end{array}$	
	Max. B. H. P.	5.2 8.8 14.5 18.3	17.1 30.4 41.0	33.3 52.1 59.0	53.6 77.1 86.0	80.8 110.0 126.0	120.5 137.0 173.5 214.1	overnors.
1/2 Cut-off	Max. R. P. M.	550 475 450 360	400 400 345	350 350 275	300 300 285	270 270 270	225 225 200 200	tomatic G
Ĩ	B. H. P. Per R. P. M.	.0095 .0186 .0321 .0510	.0428 .0761 .1189	.0952 .1488 .2142	.1785 .2570 .3016	.2994 .4075 .4677	.5360 .6097 .8673 1.0705	um for Au
	Max. B. H. P.	4.3 7.3 11.9 17.7	14.2 25.2 39.3	27.6 45.2 57.6	44.3 63.9 74.8	66.7 91.0 104.3	99.5 113.0 143.3 176.8	e Maxim
3% Cut-off	Max. R. P. M.	550 475 450 420	400 400 400	350 350 325	$300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 $	270 270 270	225 225 200 200	o-thirds th
60/	B. H. P. R. P. M.	.0079 .0153 .0265 .0422	.0354 .0629 .0983	.0787 .1229 .1770	.1475 .2123 .2492	.2473 .3367 .3865	.4428 .5036 .7164 .8842	s than two
	Max. B. H. P.	4.0 6.7 10.9 16.5	13.0 23.1 36.1	25.3 39.5 56.8	40.6 58.5 68.8	61.3 83.5 96.0	$\begin{array}{c} 91.5\\ 104.0\\ 131.5\\ 162.3\end{array}$	e not les
15 Cut-off	Max. R.P.M.	550 475 450 425	400 400 400	350 350 350	300 300 300	270 270 270	225 225 200	speed to h
	B. H. P. R. P. M.	.0072 .0141 .0243 .0387	.0325 .0577 .0902	.0722 .1128 .1625	.1354 .1948 .2288	.2270 .3090 .3546	.4063 .4625 .6576 .8117	NOTE-Minimum speed to be not less than two-thirds the Maximum for Automatic Governors
Culinder	Diameter and Stroke	4654 X X X X X X 40554	6 x 8 8 x 8 10 x 8 8	8 x 10 10 x 10 12 x 10	10 × 12 12 × 12 13 × 12	12 x 14 14 x 14 15 x 14	15 x 16 16 x 16 18 x 18 20 x 18	Nore-

HORSEPOWER OF ENGINES

	Brake	norsepo	wer рег қ.	brake norsepower per K. P. M. and Maximum K.	MINAN		L. III. and Holsepower Allowable	ochower v				
L	f	1/3 Cut-off		<i>©</i> /	3/8 Cut-off		ŕ	3/2 Cut-off			5% Cut-off	
Diameter and Stroke	B. H. P. Per R. P. M.	R. P. M.	Max. B.H.P.	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B.H.P.	B. H. P. R. P. M.	Max. R. P. M.	Max. B.H.P.	B. H. P. R. Per	Max. R. P. M.	Max. B.H.P.
40.00	.0091 .0178 .0308 .0489	550 475 450 360	5.0 8.4 13.9 17.6	.0105 .0194 .0336 .0533	510 475 450 335	$5.4 \\ 9.2 \\ 15.1 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17.8 \\ 17$	.0120 .0234 .0405 .0643	455 465 450 285	$     \begin{array}{c}       5.5 \\       10.9 \\       18.2 \\       18.3 \\       18.3 \\     \end{array} $	.0142 .0276 .0478 .0760	395 405 390 240*	$     \begin{array}{c}       5.6 \\       11.2 \\       18.6 \\       18.3 \\       18.3     \end{array} $
	.0410 .0729 .1139	400 400 365	$16.4 \\ 29.2 \\ 41.6$	.0447 .0795 .1243	400 400 335	17.9 31.8 41.7	.0539 .0959 .1499	400 400 280	21.5 38.3 42.0	.0637 .1133 .1770	400 370 235*	25.4 42.0 41.6
000	.0912 .1425 .2051	350 280 280	$31.9 \\ 50.0 \\ 57.4$	.0994 .1554 .2238	350 350 260	34.8 54.4 58.0	.1199. $.1874$ . $.2760$	350 315 215*	42.0 59.0 59.5	.1417 .2213 .3185	350 275 185*	41.6 60.8 59.0
000	.1709 .2461 .2888	300 300 290	$51.2 \\ 74.0 \\ 83.8$	.1864 .2684 .3150	300 300 270	56.0 80.6 85.0	.2248 .3237 .3799	300 265 225	67.5 85.9 85.8	.2656 .3825 .4489	300 230 195	79.6 88.2 88.0
444	.2867 .3903 .4480	270 270 270	77.5 105.5 121.0	.3127 .4257 .4886	270 270 270	84.5 115.0 131.8	.3771 .5134 .5892	270 240 270	101.8 123.0 159.0	.4456 .6055 .6962	270 205 265	120.5 124.0 185.0
00000	.5133 .5839 .8305 1.0250	225 225 200	115.2 131.0 166.0 205.0	.5600 .6368 .9060 1.1182	225 225 200 200	126.0 143.0 181.0 223.7	.6752 .7680 1.0920 1.3480	225 225 200 200	$152.0 \\ 173.0 \\ 218.5 \\ 269.6$	$\begin{array}{c} .7978\\ .9074\\ 1.2910\\ 1.5935\end{array}$	225 225 200	$\begin{array}{c} 179.0 \\ 202.0 \\ 258.3 \\ 318.7 \\ 318.7 \end{array}$

Ibs. 125 CLASS "A" HORIZONTAL AND VERTICAL-STEAM PRESSURE, 125 LB. GAUGE Brake Horsepower per R.P.M. and Maximum R.P.M. and Horsepower Allowable BUFFALO HIGH SPEED ENGINES

Max. B. H. P. 123.0 121.0 [87.0 224.5255.0323.0319.0Those marked with a * are for  $\begin{array}{c}
 31.9 \\
 41.8 \\
 41.0 \\
 \end{array}$ 60.558.257.886.5 86.0 86.9 5.5 11.2 18.6 18.1 Max. R. P. M. 5% Cut-off 400 295 185* 340 210* 145* 260 180* 155* 220 160* 215 310* 325 310* 310* 225 225 225 225 225 200 160 R. P. M. B. H. P. .5576 .7595 .8714 .99861.1358 1.6155 1.9940  $\begin{array}{c} 0177\\ 0346\\ 0598\\ 0598\\ 0953 \end{array}$ .0797 .1418 .2219 .1773.2770.39853325 4785 5605Max. B. H. P. 190.3 216.0 244.0 301.3 NorE-Minimum speed to be not less than two-thirds the Maximum for Automatic Governors.  $\begin{array}{c}
 5.5 \\
 10.8 \\
 18.2 \\
 18.1 \\
 18.1 \\
 \end{array}$  $27.1 \\ 41.0 \\ 40.3$ 52.6 58.8 58.6 84.5 85.3 85.1 23.0 22.0 81.0 Max. R. P. M. ½ Cut-off 260 185* 245 365 370 360 220* 400 340 210* 350 250 300 210 175* 225 225 200 200 R. P. M. B. H. P. 8457 9620 .2205 .5064 4723 6565 7380 0676 1201 1920  $1502 \\ 2347 \\ 3452 \\ 3452 \\$ 0150 0293 0507 0822 2816 4054 4860 B. H. P. 106.0 158.0180.5227.5281.070.5
 84.5
 85.05.4 10.7 18.2  $22.5 \\ 40.0 \\ 40.8 \\ 40.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\ 10.8 \\$ 43.8 57.6 57.4 Max. R. P. M. 3% Cut-off 400 400 250* 350 295 195* 130 140 260 300 250 215 225 225 270 225 225 200 200 R. P. M. B. H. P. .7036.8004.1385.4052 $1250 \\ 1953 \\ 2940 \\ 2940 \\$ 3930 5350 61410125 0244 0422 0700 0562 0999 1630  $2343 \\ 3374 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\ 3959 \\$ B. H. P 146.0 166.0 210.0 259.3 98.0 123.0 153.0 5.3 10.6 17.5 20.736.939.640.457.0 57.5 65.0 83.0 83.6 R. P. M. 14 Cut-off 350 315 210* 265 270 225 225 200 200 160 1170 1150 1150 2200 R. P. M. B. H. P. .1153 .1801 .2740 2161 3113 3653 .6492.7384.0505.29650115 0225 0389 0618 0518 0922 1440  $3625 \\ 4936 \\ 5665 \\ 5665 \\ 6565 \\ 700 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\ 100 \\$ Cylinder Diameter and Stroke 0.088 20 00 00 222 202 444 16 x 20 x X X 70 ××× ×× × × × 0 & 0 245 202 5

HORSEPOWER OF ENGINES

Throttling Governors.

Cylinder	60	60 Lb. Pressure	sure	80	80 Lb. Pressure	sure	10(	100 Lb. Pressure	ssure
Diamcter and Stroke	B. H. P. R. P. M.	Max. R. P. M.	Max. B. H. P.	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B. H. P.	B. H. P. R. P. M.	Max. R. P. M.	B. H. P.
5 x 10 6 x 10	.0329	300 300	9.9 14.2	.0442 .0636	300 300	13.3 19.1	.0553	300 300	16.6 23.9
7 x 12 8 x 12	.0775	250 250	19.4 25.3	.1088	250 250	$\frac{27.2}{33.9}$	.1301	250 250	32.5 42.5
8 x 14 9 x 14	.1178	225 225	26.5 33.6	.1581.2001	22 <b>5</b> 225	$35.6 \\ 45.0$	.1981 .2506	225 225	44.6 56.4
10 x 20 12 x 20 15 x 20	.2631 .3788 .5922	100 90 80	26.3 34.1 47.4	.3530 .5084 .7943	100 80 80	35.3 45.8 63.5	.4422 .6368 .9950	100 90 80	44.2 57.3 79.7
16 x 24 18 x 24	.8091 1.0240	65 65	52.6 66.6	1.0863 1.3739	65 65	70.6 89.3	1.3600 1.7205	65 65	88.4 111.8
20 x 30 22 x 30 24 x 30	1.5805 1.9120 2.5757	65 65 65	102.7 124.3 148.0	2.1202 2.5658 3.0530	65 65 65	137.8 166.8 198.4	2.6560 3.2140 3.8240	65 65 65	$172.6 \\ 208.9 \\ 248.6$

FAN ENGINEERING-BUFFALO FORGE COMPANY

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Jiameter and Stroke 3 x 3 ½					% Cut-Off			2 Cut-off			3/8 Cut-orr	
x 3 ½	B.H.P. Per R.P.M.	R. P. M.	Max. B. H. P.	B. H. P. per R. P. M.	Max. R. P. M.	Max. B. H. P.	B. H. P. Per R. P. M.	Max. R.P.M.	Max. B. H. P.	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B. H. P.
x 3 ½					80 I	b. Pressure	sure	•				
	.0071	650	4.6	.0078	650	5.1	.0094	650	6.1	.0111	650	7.2
x 3 ½ 2	.0126	650 600	2 X X	.0138	650	9.0	.0167	650 600	11.4	.0198	650	12.9
X 4	.0226	600	13.6	.0246	009	14.8	.0298	009	17.9	.0354	525	18.6
x x vo	.0405 .0552	500 500	20.2 27.6	.0442 .0601	500 500	22.1 30.0	.0534	500 435	26.7 31.6	.0635	500 375	31.7
x 8	.1154	400	46.2	.1257	400	50.3	.1523	360	55.0	.1809	310	56.0
					100 I	Lb. Pressure	sure					
x 3 15	0600.	650	5.9	.0098	650	6.4	.0118	650	7.7	.0140	650	9.1
x 3 ½	.0160	650	10.4	.0174	650	11.3	.0210	650	13.7	.0248	650	16.1
**	00100	009	0.11	1150	000	01	.0240	000	14.4	.0204	000	10.0
**	0519	200	926	1100.	002	0.26	0673	475	31.0	07050	410	39.6
x x	.0697	440	30.6	0920.	410	31.2	.0017	345	31.6	.1083	300	32.5
x 8	.1458	360	52.5	.1590	335	53.5	.1918	285	54.6	.2265	245	55.6
		,			1251	Lb. Pressure	sure					
x 3 1/2	.0114	650	7.4	.0123	650	8.0	.0148	650	9.6	.0175	650	11.4
× 4 ×	.0231	009	13.9	.0250	009	15.0	.0301	009	18.1	.0355	525	18.6
X 4	.0361	490	17.7	10301	455	17.8	.0470	390	18.3	.0555	335	18.6
x S	.0647	475	30.6	.0702	445	31.2	.0843	380	32.0	.0996	325	32.4
x x x x	.0881 .1844	$350 \\ 285$	30.6 52.5	.1999	325 265	31.0	.1148 .2402	$275 \\ 225$	31.5 54.1	.1356 .2836	$240 \\ 195$	32.6 55.3

BUFFALO HIGH SPEED ENGINES DOUBLE VERTICAL—DOUBLE ACTING

## HORSEPOWER OF ENGINES

	SINGL Brake Horsepower	BUFFALO HIGH SPEED ENGINES SINGLE VERTICAL-CYLINDER BELOW SHAFT, CLASS "1" Brake Horsepower per R. P. M. and Maximum R. P. M. and Horsepower Allowable	BUFFALO HIGH SPEED ENGINES TICAL-CYLINDER BELOW SHAF P. M. and Maximum R. P. M. a.	NGINES W SHAFT, CLASS P. M. and Horse	, "I" power Allowable	
	9	60 Lb. Pressure			80 Lb. Pressure	
•	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B. H. P.	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B. H. P.
3 4 4 5 5 5 7 7 5 5 7 8 5 7 8 7 8 7 8 7 8 7 8	.0042 .0074 .0133 .0133 .0133 .0145 .0445	600 500 325 275 220	2.5 3.7 5.3 9.1 14.7	.0056 .0099 .0178 .0374 .0597 .0894	600 500 325 275 220 220	3.6 5.0 7.1 12.2 16.4 19.7
	DOUBLE VI Brake Horsepower	BUFFALO HIGH SPEED ENGINES DOUBLE VERTICAL-SINGLE ACTING-CYLINDER ABOVE SHAFT Brake Horsepower per R. P. M. and Morsepower Allowable 6.0.1.b. Decense	BUFFALO HIGH SPEED ENGINES LL-SINGLE ACTING-CYLINDER . P. M. and Maximum R. P. M. a. Doccura	NGINES LINDER ABOVE P. M. and Horse	SHAFT power Allowable 80 T h. Dressure	
Cylinder Diameter and Stroke	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B. H. P.	B. H. P. Per R. P. M.	Max. R. P. M.	Max. B. H. P.
	.0036 .0084 .0284	200 200 200 200	2.5 5.0 14.2	.0048 .0113 .0382	700 500 435	3.4 5.6 16.6
	•	100 Lb. Pressure	3		125 Lb. Pressure	Ð
	.0060 .0142 .0478	615 390 350	3.7 5.5 16.7	.0075 .0177 .0598	490 315 280	3.7 5.6 16.7

FAN ENGINEERING-BUFFALO FORGE COMPANY

#### BUFFALO LOW PRESSURE ENGINES AT THREE-QUARTER CUT-OFF AND 3-LB. BACK PRESSURE

Brake Horsepower per R. P. M. and Maximum R. P. M. and Horsepower Allowable at Different Steam Pressures

Cylinder Diameter and Stroke	B. H. P. Per R.P.M.	Max. R. P. M.	Max. B. H. P.	B. H. P. R. P. M.	Max. R.P.M.	Max. B. H. P.	B. H. P. Per R. P. M.	Max. R. P. M.	Max B. H. P.
Dian	10	Lb. Pre	ssure	15 1	b. Pres	sure	20 Lb	. Pres	sure
10x 8	0.00282 0.00460 0.0107	$350 \\ 325 \\ 325 \\ 325$	$1.0 \\ 1.5 \\ 3.5$	$\begin{array}{c} 0.00794 \\ 0.01522 \\ 0.0261 \end{array}$	$350 \\ 325 \\ 325 \\ 325$	$2.8 \\ 4.9 \\ 8.5$	$\begin{array}{c} 0.01313 \\ 0.02600 \\ 0.0417 \end{array}$	350 325 325	4.6 8.5 13.5
15x10	0.0218 0.0210 0.0264	325 300 300	$7.1 \\ 6.3 \\ 7.8$	$\begin{array}{c} 0.0457 \\ 0.0509 \\ 0.0604 \end{array}$	325 300 300	$14.8 \\ 15.3 \\ 18.1$	$\begin{array}{c} 0.0700 \\ 0.0813 \\ 0.0949 \end{array}$	325 300 300	$22.8 \\ 24.4 \\ 28.4$
15x12 18x12 18x14	0.0362	250	9.1	0.0514 0.0878 0.0897	250 250 200	$12.8 \\ 21.9 \\ 17.9$	$\begin{array}{c} 0.0876 \\ 0.1404 \\ 0.1510 \end{array}$	250 250 200	$21.9 \\ 35.1 \\ 30.2$
18x16				0.0863	200	17.3	0.1560	200	31.2
-	25	Lb. Pre	ssure	30 Lb. Pressure 40 Lb. Press					sure
10x 8 12x 8	0.01667 0.03654 0.0570	350 325 325	$6.4 \\ 11.9 \\ 18.5$	0.02835 0.05758 0.0720	350 325 325	9.9 18.8 23.4	0.03360 0.06850 0.1033	350 325 325	11.8 22.2 33.6
15x10	0.0935 0.1109 0.1285	325 300 300	$30.4 \\ 33.2 \\ 38.6$	$\begin{array}{c} 0.1174 \\ 0.1406 \\ 0.1624 \end{array}$	325 300 300	$38.2 \\ 42.2 \\ 48.8$	0.1656 0.2010 0.2308	250 300 260	$   \begin{array}{r}     41.5 \\     60.3 \\     60.0   \end{array} $
18x12	0.1233 0.1920 0.2108	$250 \\ 250 \\ 200$	30.8 48.0 42.2	$\begin{array}{c} 0.1588 \\ 0.2423 \\ 0.2702 \end{array}$	250 250 200	$39.7 \\ 60.7 \\ 54.1$	$\begin{array}{c} 0.2310 \\ 0.3465 \\ 0.3920 \end{array}$	250 250 200	57.8 86.7 78.5
18x16	0.2444	200	45.0	0.2925	200	58.5	0.4315	200	86.3

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RSEPOWER OF BUFFALO HIGH SPEED CLASS "A" ENGINE	SPEEDS AND ST	
HORSEPOWER OF 1	OUS SPEEDS AND ST	
HORSEPOWER OF	RIOUS SPEEDS AND ST	
HORSEPOWER OF	VARIOUS SPEEDS AND ST	
HORSEPOWER OF	AT VARIOUS SPEEDS AND STEAM PRESSURES OF 60, 80, 100 AND 125 LB. GAUGE	

oke nd neter		325 R. P. M.	P. M.			350 R	350 R. P. M.			375 R	375 R. P. M.			400 R	400 R. P. M.	
Diana and and and and and and and and and	60	80	001	125	60	80	100	125	09	80	100	125	60	80	100	125
<b>XXX</b> 400	4.5 7.8	6.0 10.4	7.6 13.2	$   \begin{array}{c}       9.5 \\       16.5   \end{array} $	4.8 8.4	$6.5 \\ 11.2$	8.2 14.2	10.2 17.7	2.7 5.2 9.0	3.6 7.0 12.0	4.5 8.8 15.2	5.6 11.0 18.0*	2.8 5.5 9.6	3.8 7.5 12.8	$   \begin{array}{c}     4.8 \\     9.4 \\     16.2   \end{array} $	6.0* 12.0* 18.0*
× × × 8 %	12.4 10.4 18.4	$   \begin{array}{r}     16.6 \\     13.9 \\     24.7   \end{array} $	$     \begin{array}{c}       18.0 \\       17.5 \\       31.2     \end{array} $	$     \begin{array}{c}       18.0 \\       22.0 \\       39.1     \end{array} $	13.3     11.2     11.2     19.8	$17.8 \\ 15.0 \\ 26.6$	18.0* 18.9 33.6	18.0* 23.5 45.0*	$14.3 \\ 12.0 \\ 21.2 \\ 21.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 31.2 \\ 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\\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ 322.7 \\ $	18.0*     17.1     30.4	18.0* 21.5 38.3	18.0* 27.1 45.0*
10 x 8 8 x 10 10 x 10	28.6 23.0 36.0	38.6 30.9 48.4	45.0* 39.0 61.0	45.0* 48.8 65.0*	$   \begin{array}{c}     31.0 \\     24.8 \\     38.8 \\   \end{array} $	$\frac{41.6}{33.3}$	45.0* 42.0 65.0*	45.0* 52.6 65.0*	33.2	45.0*	45.0*	45.0*	35.4	45.0*	45.0*	45.0*
x 10 x 12 x 12	51.9	65.0*	65.0* 65.0* 65.0* 55.9	65.0*	55.9	65.0*	65.0* 65.0*	65.0*					26.6 38.3	200 R. P. M. 35.7 45. 51.5 64.	. P. M. 45.0 64.7	56.4 81.4
13 x 12 12 x 14 14 x 14									39.1 53.2	<b>175 R. P. M</b> 52.4 66. 71.5 89.	<b>P. M.</b> 66.0 89.8	$\frac{82.7}{112.5}$	45.0 44.6 60.8	$60.4 \\ 59.9 \\ 81.5$	76.0 75.4 102.5	95.0* 94.5 135.0*
15 x 14 15 x 16 15 x 16 16 x 16					60.0 68.2		<b>150 R. P. M</b> 80.5 101.0 91.5 115.0	127.0 144.0	61.0 70.0 79.5	81.9 94.0 106.8	103.0 118.0 134.2	129.0 148.0 168.2	69.8 80.0 91.0	93.5 107.0 122.0	117.8 135.0 153.5	$\frac{147.5}{169.0}$ 192.0
x 18 x 18					$^{97.0}_{120.0}$	$130.1 \\ 160.0$	$\frac{130.1}{160.0} \frac{164.0}{202.4}$	$183.0 \\ 225.9$	113.1	151.5     187.0	$191.5 \\ 236.4$	214.0 264.1	129.3 159.6	173.5 214.2	218.5 269.7	244.0 301.2

DTE-H. P. marked * indicates engine cutting off at less than rated cut-o

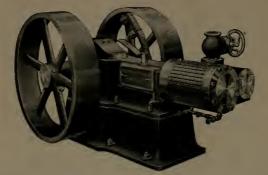
FAN ENGINEERING-BUFFALO FORGE COMPANY

$\begin{array}{cccccccccccccccccccccccccccccccccccc$	. * .* * .*	21.1 51.2 40.9 55.5 39.9 53.6 65.0* 65.0* 47.9 64.2 81.0 95.0* 56.8 75.5 95.0* 55.8 73.5 94.3 118.0 55.8 100 0135.0 135.0*
112.0		70.661 70.661 (120) 7.161 70.61 184.5

HORSEPOWER OF BUFFALO HIGH SPEED CLASS "A" ENGINES

NorE-H. P. marked * indicates engine cutting off at less than rated cut-off.

## BUFFALO HORIZONTAL ENGINES CENTER CRANK, CLASS "A"



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME High Pressure

Max.		Cylinder		Floo Spac			dard wheel	Stean Exhaus		Shipping Weight
Horse- power	Max. R. P. M.	Diameter and Stroke	Length	Width	Height	Diam.	Face	Steam	Exh.	Belted Engine 2 Wheels
45 45 65 65 95 95 135 135 200 285 285 350 350	400 400 350 350 300 270 270 270 225 225 200 200	$\begin{array}{c} 6 \ge 8\\ 8 \ge 8\\ 10 \ge 8\\ 8 \ge 10\\ 10 \ge 10\\ 12 \ge 10\\ 12 \ge 12\\ 12 \ge 12\\ 13 \ge 12\\ 12 \ge 12$ 12 \ge 12\\ 12 \ge 12 \ge 12\\ 12 \ge 12 12 \ge 12 12 = 12 12 = 12\\ 12 \ge 12 \ge 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 12 = 12 1	73 73 73 80 80 110 110 110 126 126 130 144 144 161 161	40 40 56 56 60 60 60 70 70 77 88 88 95 95	$\begin{array}{r} 42\\ 42\\ 60\\ 60\\ 65\\ 65\\ 75\\ 75\\ 75\\ 75\\ 80\\ 80\\ 88\\ 88\\ 88\end{array}$	39 39 39 49 49 57 57 57 66 66 66 66 66 72 72 84 84	$\begin{array}{c} 7\\ 7\\ 7\\ 11\\ 12\\ 13\\ 13\\ 13\\ 15\\ 15\\ 15\\ 16\\ 16\\ 18\\ 18\\ \end{array}$	2 2 3 12 2 2 3 3 2 2 1 2 2 2 3 3 3 4 4 4 5 5 6 6 6 7 7	23333445556667788	$\begin{array}{c} 3300\\ 3380\\ 3560\\ 6490\\ 6760\\ 9850\\ 10000\\ 10170\\ 15950\\ 16170\\ 16390\\ 22340\\ 30580\\ 31790 \end{array}$
				Lo	w Pr	essure				
45 45 65	$325 \\ 325 \\ 300$	$12 \times 8$ $15 \times 8$ $15 \times 10$	73 73 80	40 40 56	42 42 60	39 39 49	7 7 11 1/2	$3 \\ 3 \frac{1}{2} \\ 3$	$3\frac{1}{2}$ 4 3 ¹ / ₂	$3780 \\ 4000 \\ 7150$

 $110 \\ 110 \\ 126 \\ 130$ 

  $\frac{250}{250}$ 

 BUFFALO HORIZONTAL ENGINES SIDE CRANK, CLASS "A"



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

#### **High Pressure**

Max.	Max.	Cylinder Diameter	Flo	oor Spa	ace	Gove	dard ernor neel	Stean Exh Pig	aust	Shipping Weight
Horse- power	R. P. M.	and Stroke	Length	Width	Height	Diam.	Face	Steam	Exh.	Belted Engine 1 Wheel
20 45 45 45 65	$ \begin{array}{r} 450 \\ 400 \\ 400 \\ 400 \\ 350 \end{array} $	6 x 6 6 x 8 8 x 8 10 x 8 8 x 10	66 76 76 76 89	42 48 48 48 56	44 47 47 47 53	33 39 39 39 39 49	$     \begin{array}{c}       6 \\       7 \\       7 \\       7 \\       11 \frac{1}{2}     \end{array} $	$2 \\ 2 \\ 2 \\ 1/2 \\ 3 \\ 2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/2 \\ 1/$	$2\frac{1/4}{2\frac{1}{2}}$ 3\frac{1}{2} 3\frac{1}{2} 3	2940 3830 3920 4310 5390
65 65 95 95 95	350 350 300 300 300	10 x 10 12 x 10 10 x 12 12 x 12 13 x 12	89 89 110 110 110	$56 \\ 56 \\ 64 \\ 64 \\ 64 \\ 64$	53 53 62 62 62	49 49 57 57 57	$     \begin{array}{c}             11 & \frac{1}{2} \\             11 & \frac{1}{2} \\             13 \\             13 \\           $		$     3\frac{1}{2}     4     4     5     5     5   $	5580 5850 9300 9460 9570

#### Low Pressure

## BUFFALO HORIZONTAL ENGINES SIDE CRANK, CLASS "N"



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

Н. Р.	. P. M.	nder ter and oke		oor Spa Inches	ice		Standar Iy-who			m and ist Pipes	ping ght olete
Max.	Max. R.	Cylir Diameto Stro	Length	Width	Height	Diam.	Face	Weight	Steam	Exh.	Shipi Wei Comp
30 30 50	300 300 250	5 x 10 6 x 10 7 x 12	70 70 86	30 30 34	30 30 32	40 40 40		450 450 450	$     \begin{array}{c}       1 \frac{1}{2} \\       1 \frac{1}{2} \\       2     \end{array} $	$2\frac{1}{2}$ $2\frac{1}{2}$ 3	1980 2030 2750
50 65 65	250 225 225	8 x 12 8 x 14 9 x 14	86 102 102	34 40 40	32 37 37	40 49 49		450 900 900	$     \begin{array}{c}       2 \\       2 \\       2 \\       2 \\       1 \\       2     \end{array} $	$     \begin{array}{c}       3 \\       3 \\       3 \\       \frac{1}{2} \\       3 \\       \frac{1}{2}     \end{array} $	2970 3850 4070

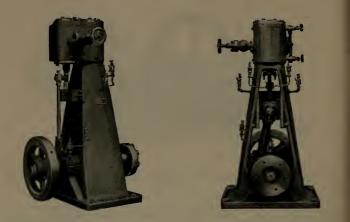
BUFFALO HORIZONTAL ENGINES SIDE CRANK, CLASS "S"



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

Н. Р.	R. P. M.	nder ter and oke	Floo	or Spa	ace	Standa	ard Fl	y=wheel	Stean Exh Pij	aust	ping ght olete sing
Max.	Max. R	Cylin Diamet Stro	Length	Width	Height	Diam.	Face	Weight	Steam	Exh.	Shipi Wei Comp
90 90 90	100 90 80	10 x 20 12 x 20 15 x 20	$     \begin{array}{r}       162 \\       162 \\       168     \end{array}   $	50 50 52	61 61 68	72 72 96	5 5 8	2850 2850 4000	$     \begin{array}{c}       2 \frac{1}{2} \\       2 \frac{1}{2} \\       4     \end{array} $	3 3 5	8250 8800 11000
125 125 275		16 x 24 18 x 24 20 x 30	178 178 192	60 60 64	72 72 76	96 96 108	9 9 10	6800 6800 10000	4 4 5	5 5 6	18370 20000 29700
275 275	65 65	22 x 30 24 x 30	192 192	66 66	80 80	108 108	10 10	10000 12000	5 6	6 7	31300 34300

## BUFFALO SINGLE VERTICAL ENGINES CLASS "O"



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

Max.		Cylinder		Floo Spac			dard wheel		n and st Pipes	Shipping Weight
Horse- power	Max. R.P.M.	Diameter and Stroke	Length	Width	Height	Diam.	Face	Steam	Exh.	Belted Engine 2 Wheels
6 12 18	550 475 450	4 x 4 5 x 5 6 x 6	34 37 41	$32 \\ 35 \\ 42$	47 55 65	27 31 33	$5\frac{1}{2}$ 6 $6\frac{1}{2}$	$     \begin{array}{c}       1 & \frac{1}{4} \\       1 & \frac{1}{2} \\       2     \end{array} $	$     \begin{array}{c}       1 & \frac{1}{2} \\       2 \\       2 & \frac{1}{2}     \end{array}   $	1320 1800 2440
30 45 65 95	425 400 350 300	7 x 7 8 x 8 10 x 10 12 x 12	41 43 52 58	$     \begin{array}{r}       42 \\       44 \\       56 \\       68     \end{array} $	73 76 96 116	33 39 49 57	$     \begin{array}{r}       6 \frac{1}{2} \\       7 \\       11 \frac{1}{2} \\       13 \\       13     \end{array} $	$22\frac{1}{2}$ 34	$2\frac{1}{2}$ 3 $3\frac{1}{2}$ 5	$2800 \\ 3840 \\ 6600 \\ 10000$

## BUFFALO SINGLE VERTICAL ENGINES CLASS "A"

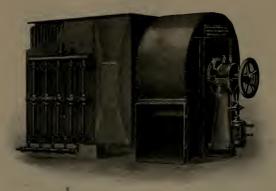


## MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

**High Pressure** 

Max.		Cylinder	Floor Space				ndard wheel	Steam and Exhaust Pipes		Shipping Weight	
Horse- power	Max. R. P. M.	Diameter and Stroke	Length	Width	Height	Diam.	Face	Steam	Exh.	Belted Engine 2 Wheels	
6 12 20 20 45 45 65 65 65 95 95	$550 \\ 475 \\ 450 \\ 425 \\ 400 \\ 400 \\ 350 \\ 350 \\ 350 \\ 350 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 \\ 300 $	$\begin{array}{c} 4 & x & 4 \\ 5 & x & 5 \\ 6 & x & 6 \\ 7 & x & 7 \\ 8 & x & 8 \\ 10 & x & 8 \\ 8 & x & 10 \\ 10 & x & 10 \\ 12 & x & 10 \\ 10 & x & 12 \\ 12 & x & 12 \end{array}$	$\begin{array}{r} 34\\ 37\\ 41\\ 41\\ 43\\ 52\\ 52\\ 52\\ 52\\ 62\\ 62\\ 62\\ \end{array}$	$\begin{array}{r} 32\\ 34\\ 37\\ 37\\ 40\\ 40\\ 52\\ 52\\ 52\\ 64\\ 64\\ \end{array}$	46 55 65 65 78 96 96 96 118 118	27 31 33 39 39 49 49 49 57 57	$5\frac{1}{2}$ $6\frac{1}{2}$ $6\frac{1}{2}$ $7$ $7$ $11\frac{1}{2}$ $11\frac{1}{2}$ $11\frac{1}{2}$ $13$	$ \begin{array}{c} 1 \\ 1 \\ 4 \\ 1 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\ 2 \\ 3 \\ 2 \\ 2 \\ 3 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4 \\ 4$	$ \begin{array}{c} 1 \frac{1}{2} \\ 2 \frac{1}{2} \\ 2 \frac{1}{2} \\ 3 \\ 3 \\ 4 \\ 4 \\ 5 \end{array} $	1260 1740 2400 2800 3270 3420 6070 6240 6460 8830 9000	
				Lo	w Pr	essure					
18 45 45 65 95 95	$ \begin{array}{r} 450 \\ 400 \\ 400 \\ 350 \\ 300 \\ 300 \\ 300 \end{array} $	8 x 6 12 x 8 13 x 8 15 x 8 15 x 10 15 x 12 18 x 12	41 43 43 52 62 62	$37 \\ 40 \\ 40 \\ 40 \\ 52 \\ 64 \\ 64$	65 78 78 96 118 118	33 39 39 39 49 57 57	$ \begin{array}{c} 6 \frac{1}{2} \\ 7 \\ 7 \\ 7 \\ 11 \frac{1}{2} \\ 13 \\ 13 \end{array} $	2 1/2 3 3 1/2 3 4 5	$     3 \\     3 \\     3 \\     4 \\     3 \\     5 \\     6   $	$\begin{array}{r} 2450\\ 3780\\ 4160\\ 6490\\ 7150\\ 10830\\ 11270\\ \end{array}$	

## BUFFALO SINGLE VERTICAL ENGINES CYLINDER BELOW SHAFT, CLASS "I"



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

Max. Horsepower	Max. R. P. M.	Cylinder Diameter	Steam an Pi	Weight of Engine with	
Horsepower	<b>K</b> , <b>I</b> , <b>M</b> ,	and Stroke	Steam	Exhaust	Hand Wheel
5 7½ 11	600 500 400	$\begin{array}{c} 3 & x \ 3 \ \frac{1}{2} \\ 4 & x \ 3 \ \frac{1}{2} \\ 4 \ \frac{1}{2} \ x \ 5 \end{array}$	1 1 1 ¼	$ \begin{array}{r} 1 \frac{1}{4} \\ 1 \frac{1}{4} \\ 1 \frac{1}{2} \end{array} $	340 370 780
18½ 25 30	$325 \\ 275 \\ 220$	$5\frac{1}{2} \times 7$ $6\frac{1}{2} \times 8$ $7\frac{1}{2} \times 9$	$     \begin{array}{c}       1 & \frac{1}{4} \\       1 & \frac{1}{2} \\       2     \end{array} $	$     \begin{array}{c}       1 \frac{1}{2} \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       2 \\       $	$1100 \\ 1500 \\ 2000$

## **BUFFALO DOUBLE VERTICAL ENGINES**



MAXIMUM HORSEPOWER ALLOWABLE FOR CORRESPONDING FRAME

. b.		er ter (e	Floor Space			Standard Fly-wheel			Steam and Ex- haust Pipes		ping ght Engine heels
Max. H.	Max. R. P. M. Cylinder Diameter and Stroke	Length	Width	Height	Diam.	Face	Weight	Steam	Exh.	Shippi Weig Belted Ei 2 Whe	
4 6 18	700 600 500	3 x 3 4 x 4 6 x 6	32 40 55	30 34 37	28 38 52	24 31 33	$4\frac{1}{2}$ 6 6 $\frac{1}{2}$	$175 \\ 225 \\ 425$	$1\\1\frac{1}{2}\frac{1}{4}$	$     \begin{array}{r}       1 & \frac{1}{4} \\       1 & \frac{1}{2} \\       2 & \frac{1}{2}     \end{array} $	780 1130 2700
				1	Double	Actin	g				
20 20 20	650 650 600	$ \begin{array}{r} 3 \times 3 \frac{1}{2} \\ 4 \times 3 \frac{1}{2} \\ 4 \times 4 \end{array} $	36 36 36	$34 \\ 34 \\ 34 \\ 34$	49 49 49	31 31 31	6 6 6	225 225 225	$\begin{array}{ c c c c c c c c c c c c c c c c c c c$	$     \begin{array}{c}       2 \\       2 \\       2 \\       \frac{1}{2}     \end{array} $	$1540 \\ 1600 \\ 1680$
20 35 35 60	600 500 500 400	5 x 4 6 x 5 7 x 5 8 x 8	$36 \\ 52 \\ 52 \\ 68$	$34 \\ 42 \\ 42 \\ 52$	49 70 70 88	31 39 39 49	$ \begin{array}{c c} 6 \\ 7 \\ 7 \\ 11 \frac{1}{2} \end{array} $	$225 \\ 520 \\ 520 \\ 1000$	2333	$\begin{array}{c} 2 \frac{1}{2} \\ 3 \frac{1}{2} \end{array}$	1760 2960 3080 6100

Single Acting

## SECTION VIII

# PRACTICAL APPLICATIONS AND THE SELECTION OF APPARATUS FOR HEATING AND VENTILATING

As has been previously shown, one of the most important applications of fans is in connection with the heating and ventilation of industrial and public buildings. This work will be considered under two general divisions or classes: First, to supply heat; and second, to supply ventilation, where the heating may be done by direct radiation or by means of the fan as circumstances may determine. The first class embraces such buildings as shops and factories. The second class is more likely to be confined to such buildings as theatres, churches, hotels, etc. These buildings may be supplied with ventilation only, or with a combination of heating and ventilation, but the fan system is seldom used in such cases for heating alone.

The following examples will serve to illustrate these various systems, and the use of preceding rules, tables and data required in connection therewith will be explained. There are three factors entering into such calculations, the air required, the heat loss due to transmission and infiltration to be cared for, and the rise in temperature of the air above room temperature. In the various examples two of these conditions are given and the third is to be determined.

Class I. Heat the building, using either all return air, all outdoor air or a mixture of the two. In this case, the total heat loss is assumed to be known. For heating work where part or all of the air is returned from the room to the apparatus, it is customary to use a heater six sections deep with low pressure steam or five sections deep with high pressure steam. Where all outdoor air is used, either six or seven sections may be used with low pressure steam and five or six sections with high pressure steam. Knowing the temperature of the air entering the heater and assuming a suitable velocity of the air through the clear area, we may find from the heater tables on pages 418 to 431 the final or leaving temperature and so determine the temperature rise. Knowing the heat loss in B. t. u. per hour and the temperature rise, we may determine the air requirement from the formula

$$Q = \frac{55.2 \text{ H}}{60 (t_2 - t_r)}$$

(for heating only)

where

Q = cu. ft. of air per min.

H = B, t. u. loss per hour due to transmission and infiltration.

t₂ = temperature of air leaving heater

 $t_r = room temperature.$ 

In case all return air is used, the above H is a measure of the heat required to be delivered to the air by the heating coils. Where all or part of the air entering the heater is outdoor air at a temperature  $t_1$ , a greater amount of heat, H', will be required, due to raising the temperature of this air from  $t_1$  to room temperature  $t_r$ . This total heat, H', is a measure of the condensation and steam requirement of the heating coils. It may be determined by the formula

$$H' = \frac{Q \times 60 (t_2 - t_1)}{55.2}$$
 (for heating)

where

H'=total heat required at the coils in B. t. u. per hour.

Q = cu. ft. of air per min.

 $t_1 = temperature of air entering heater.$ 

 $t_2 = temperature of air leaving heater.$ 

The three following examples illustrate in detail the various steps in the calculations of heating propositions:

Example 1. Supply heat only, using all return air.

**Example 2.** Supply heat, using all outdoor air. This condition frequently happens when the apparatus is so located that it is impracticable to run return ducts from the building to the heater.

**Example 3.** Heat the building, using part outdoor air and part return air.

Class II. Supply ventilation, either with or without heat. As already stated this is the usual requirement to be met in the case of public buildings. Here the known factors are the required amount of air for ventilation, the temperatures of the outdoor and of the room air, and the consequent temperature rise. The air to be delivered to the room at practically room temperature. The amount of heat and consequent size of heater is to be determined, the B. t. u. per hour to be supplied at the heater being indicated by the formula

$$H' = \frac{Q \times 60 (t_r - t_1)}{55.2}$$
 (for ventilation only)

where

H' = B. t. u. per hour required at heater.

Q = cu. ft. air per min. for ventilation.

 $t_r = room$  temperature.

 $t_1 = outdoor$ , or temperature entering heater.

The amount of steam required by the heater may be determined by

 $\frac{H'}{latent heat of steam} = lbs. condensation per hour.$ 

For ventilation work the final temperature of the air leaving the heater,  $t_2$ , is usually taken at the room temperature,  $t_r$ , when the room is heated by means of direct radiation, although it is customary to have the air leave the heater say from two to five degrees warmer to provide for radiation from the piping. In case both ventilation and heating are required, we have a different set of requirements. The known quantities then are the heat loss, H, to provide for the transmission and infiltration losses; the air quantity, Q, required for ventilation; and the temperature of the air entering the heater. The temperature of the air leaving the heater will have to be enough above the room temperature to care for the heat losses, and may be determined from the formula

$$t_2 = \frac{55.2 \text{ H}}{Q \times 60} + t_r \qquad (\text{for heating and ventilating})$$

As already explained, the heat required at the heater will be

$$H' = \frac{Q \times 60 \ (t_2 - t_1)}{55.2}$$

Knowing the temperature rise  $(t_2 - t_1)$  and the air quantity, and assuming a suitable velocity of the air through the heater, the depth of the heater may be found from the heater tables on pages 418 to 431.

The three following examples illustrate the calculations necessary under this class of installations.

Example 4. Supply ventilation only, with a specified air change.

Example 5. Supply ventilation only, with a specified amount of air per minute supplied a given number of people.

**Example 6.** Supply a specified amount of air for ventilation and heat the building.

As an illustration we will assume a brick building  $110 \times 200$ ft. in size, with a 13-inch brick wall and an average wall height of 20 ft. Building to be open to the roof, that is, no ceiling under the roof, which is to be of 2-inch boards, paper, tar and gravel. Loss from the floor to be neglected. Building to be warmed to 70° in zero weather.

From the tables of radiation coefficients we find that the factor for a 13-inch brick wall is 0.29, for glass surface is 1.1, and for a roof of this construction is 0.26. The total wall surface will be 12400 sq. ft. of which we will assume 3000 is glass surface and 9400 is brick wall. We will then have as the heat loss per hour per degree difference between the room and outdoor temperature.

	12000 B. t. u.
Roof 23000 sq. ft. $\times 0.26$	=5960
Glass 3000 sq. ft. $\times 1.1$	= 3300
Brick wall 9400 sq. ft. $\times 0.29$	=2740

or a total loss due to transmission of

 $H_t = 12000 \times 70 = 840000$  B. t. u. per hour.

The cubic contents of this building will be 440000 cu. ft.

Example 1. Supply heat only, using all return air.

As already shown, the heat loss from the building due to transmission will be 840000 B. t. u. per hour, to which we will add 10 per cent. giving the corrected loss as 924000 B. t. u. per hour.

In a system using return air at the heater, it is customary to allow for a certain amount of air leakage or infiltration, varying from once in one-half hour to once in two hours. This depends on several factors, such as the size and construction of the building, purposes for which it is used, etc. Assuming a loss due to infiltration of one change in two hours, we will have 220000 cu. ft. of air per hour to be warmed from 0° to 70°. The heat required to care for the infiltration loss will be

 $H_i = \frac{220000 \times 70}{55.2} = 379000$  B. t. u. per hour

The total heat required will then be

H = 924000 + 379000 = 1202000 B. t. u. per hour.

As already stated, when using exhaust or low pressure steam it is considered good practice with return air to use a heater six sections deep. As the air is to be returned from the room, it will enter the heater at from 60° to 70°. From the table on page 421 we find that when using steam at five pound pressure with an entering temperature,  $t_r$ , of 60°, with six sections of heater we will have a leaving or final temperature,  $t_2$ , of 145° if the velocity through the heater is 1000 feet per minute.

If it is desired to figure closely, and the heater is so located that there will be no loss in temperature in returning the airthat is, the air enters the heater at room temperature, or  $t_r =$ 70°—the above value of  $t_2 = 145^{\circ}$  will not be correct. As the table does not give the final temperature when the entering temperature is 70° it will be necessary to refer to the curve on page 433. We find from this diagram that with an entering temperature of 70° and a velocity of 1000 feet per minute, the final temperature, t₂, will be 149°. The method of using this diagram is as follows: Selecting a temperature of 70° on the left-hand margin of the chart pass to the right to the intersection of the 1000 velocity curve, and dropping from here to the base line we have a reading of 4.35 sections. Selecting a new point of 6+4.35=10.35 sections on this scale, pass upwards to the intersection of the vertical with the 1000 velocity curve and then to the left, where a final temperature of 149° is indicated.

The quantity of air at  $70^{\circ}$  required as a heat carrier will then be

$$Q = \frac{55.2 \times 1303000}{60 (149 - 70)} = 15200 A. P. M.$$

With a velocity of 1000 feet per minute through the heater we will require a clear area of  $15200 \div 1000 = 15.2$  sq. ft. From the table on page 449 we find that a heater 4'6" wide by 7'4" high will have a clear area of 15.3 sq. ft. We will then require a heater containing six sections of this size.

As we would use a draw-through apparatus in a case like this, the fan will handle the air at 149° instead of at 70°, and the volume of the air will be correspondingly greater. This volume will vary inversely as the weight per cubic foot of the air, and the ratio of the volume at different temperatures as compared to the volume at 70° may be found from the table on page 13. Thus we find the same amount or weight of air at 150° will have 1.1512 times the volume at  $70^{\circ}$ . Then the fan must be selected on a basis of

 $15200 \times 1.1512 = 17500$  cu. ft. per min.

Assuming that in an installation of this nature, the total resistance against which the fan is to operate will be equal to one inch of water pressure, we will find from the tables of rated fan capacity the size of fan required to deliver 17500 A. P. M. against one inch total pressure. From the table on page 229 we find that a No. 8. Niagara Conoidal fan will deliver 17340 cu. ft. of air per minute against one inch total pressure when operating at 253 R. P. M. and will require 3.87 H. P.

This horsepower based on the values given in the capacity table is for air at 70° while the fan is to handle air at 149°. At constant capacity and speed the horsepower will vary approximately inversely as the absolute temperature, hence it will require less than the rated horsepower to handle this air which is at 149°. The actual brake horsepower required by the fan will then be

 $3.87 \times \frac{460 + 70}{460 + 149} = 3.36$  H. P.

If the fan is to be motor driven, it will be necessary to select a motor of the next larger standard size, or 5 H. P. On account of the slow speed this fan should be belt driven.

Example 2. Heat the building, using all outside air at 0°.

As already explained under Example 1, when using return air it is customary to add 10 per cent. to the computed heat loss and also provide heat necessary to care for the infiltration loss. When using all outdoor air no provision is made for infiltration, but the calculated heat loss is generally increased by a greater margin—say 25 per cent. Sufficient heater must be provided to raise the temperature of the air from zero to room temperature, and enough higher to care for the heat loss from the building.

Adding 25 per cent. to the radiation loss gives 1050000 B. t. u. per hour required for heating. As shown by the heater table on page 420, with a velocity of 1000 feet per minute six sections of heater will raise the temperature of the air from 0° to  $117^{\circ}$ . Allowing a 2° drop due to the radiation loss from the piping gives a warm air temperature of  $115^{\circ}$  delivered to the room.

Then the quantity of air at 70° required will be  $Q = \frac{55.2 \times 1050000}{60 (115-70)} = 21450 \text{ A. P. M.}$ 

This means approximately a 20 minute change. If possible the apparatus should be so arranged that return air may be used in the morning in order to heat up rapidly.

As the velocity through the heater is to be 1000 feet per minute, this calls for a clear area of 21.45 sq. ft. From the table on page 449 we find that a heater  $6'0'' \times 7'10''$  will be the nearest standard size.

**Example 3.** Heat the building, using one-half outside air at  $0^{\circ}$  and one-half return air at  $70^{\circ}$ .

As already shown the heat loss from the building will be 840000 B. t. u. to which we will add 10 per cent., making the total loss 924000 B. t. u. per hour. This is the same as the loss figured for in Example 1, but since we are to use only one-half return air, we will allow but half the infiltration loss. This will require 190000 B. t. u. per hour. The total heat to be provided will then be

H = 924000 + 190000 = 1114000 B. t. u. per hour.

Since half the air entering the heater is to be at 0° and half at 70°, we will assume an average of 35°. As none of the heater tables show the temperature rise for an entering temperature of 35°, we will make use of the diagram on page 433. Assuming a velocity through the heater of 1000 feet per minute, we pass from a temperature of 35° on the left edge of the chart to the intersection of the horizontal with the curve marked 1000 feet per minute. Dropping from here to the base line we have a reading of 2.65 sections. Assuming that we will use a heater six sections deep we will point off a new location on the base line at 2.65 + 6.0 = 8.65 sections. Passing from here vertically to the intersection of the 1000 velocity curve and thence to the left edge of the diagram shows a temperature of 132° for the air leaving the heater. Allowing for 2° drop due to loss of heat from fan housing and piping gives an effective warm air temperature of 130°.

The quantity of air at 70° required will then be

$$Q = \frac{55.2 \times 1114000}{60 (130 - 70)} = 17100 A. P. M.$$

As we are to use a velocity of 1000 feet per minute through the clear area, a heater with a clear area of 17.10 sq. ft. will be required. From the table of heater dimensions on page 449, we find that a section of  $5'0'' \times 7'10''$  will have a clear area of 17.7 sq. ft. We will then use a heater  $5'0'' \times 7'10''$  six sections deep.

As shown above, the air required will be 17100 cu. ft. perminute at 70°, but if the fan is arranged to draw through the heater it will handle this air at 132°. The volume of the air will be greater than for the corresponding weight at 70°, theratio as given in the table on page 13 being 1.114. This means that the fan will be required to handle

### 17100×1.114 = 19100 A. P. M. at 132°.

It is probable that the static resistance of an installation of this nature will not be over one inch, due to the resistance of 0.574 inch through the heater, the friction loss in the piping and any entrance or discharge losses that may exist. By referring to the static pressure tables of the Niagara Conoidal Fans on pages 247, 249 and 251, we find that we may use either a No. 7, 8 or 9 fan. Either of these fans may be used to give approximately the required capacity, but we see from the following summary that the outlet velocity, speed, and horsepower will be different in each case.

Size	Outlet Vel.	A. P. M.	R. P. M.	Н. Р.
7	2600	18580	336	5.93
8	2100	19600	289	5.61
9	1600	18900	264	5.71

If low first cost is the main consideration rather than power consumption, and if a comparatively high outlet velocity will not be objectionable, we should use the No. 7 fan. If the fan were to be used for a school or public building where any slight noise might be objectionable, the outlet velocity should be kept below 2100 to 2200. Under these circumstances the No. 8 should be used. If very low outlet velocity is of greater importance than first cost, the choice should fall upon the No. 9 fan. Where a fan is to be direct connected, the speed may also be a governing factor. In any case, the horsepower as given on page 513 would be based on air at  $70^{\circ}$ , while the fan is to handle the air at  $132^{\circ}$ . That is, while the fan is to handle the 19100 cu. ft. per minute, due to the higher temperature, the density and therefore the horsepower required will be less than for the same volume at  $70^{\circ}$ . At constant capacity and speed, the horsepower will vary directly as the density of the air, and approximately inversely as the absolute temperature. We will then have the above horsepower decreased by the ratio

 $\frac{460+132}{460+70} = 1.114$ 

That is, the above horsepower should be divided by 1.114.

**Example 4.** Supply ventilation only, with a ten minute air change.

In this case the heating of the building is to be taken care of by direct radiation, and the air required for ventilation will be taken from outside at 0° and introduced into the room at room temperature, or 70°. We are not concerned with the heat loss, but merely in raising an amount of air equal to the cubic contents of the room through a 70° temperature rise once in ten minutes or six changes per hour. Then we will have as the air at 70° required

$$\frac{440000}{10} = 44000$$
 cu. ft. per min.

Assuming that this building is to be used for a factory, and inasmuch as the heater will be comparatively shallow with a corresponding low pressure drop, we may use a velocity of 1200 feet per minute through the heater. The total pressure against which the fan in such an installation is likely to operate will be about one inch. The temperature of the air leaving the heater should be about five degrees above room temperature to allow for radiation loss from the piping, etc.

From the heater table on page 420 we find that with five pound steam pressure and with 1200 velocity a temperature of 81.8° will be obtained with four sections of standard heater and will be the nearest temperature obtainable at this velocity. Since we are to handle 44000 cu. ft. per minute at 1200 velocity we will require a heater having a clear area of

 $\frac{44000}{1200}$  = 36.7 sq. ft.

From the table of heater dimensions on page 449 we find that a section  $9'6'' \times 8'4''$  has a clear area of 36.7 sq. ft. so this will be the size to use. We will then require a heater  $9'6'' \times 8'4''$  and four sections deep.

In a large room of this construction it is customary to use a draw-through system, attaching the piping directly to the fan outlet. As already stated, the total pressure required for an installation of this character using but four sections of heater would probably run about one inch.

Referring to the table of fan capacities we may select a fan that will deliver 44000 A. P. M. against a pressure of one inch. From page 208 we find that a 160-inch Planoidal Exhauster will deliver 41220 A. P. M. against one inch at a speed of 164 R. P. M. and require 14.2 H. P. The 44000 A. P. M. required is 106.5 per cent. of the above rated capacity so it will be necessary to operate at a speed of  $164 \times 1.065$  equals 175 R. P. M., and the power required will be  $14.2 \times (1.065)^3$  equals 17.2 H. P.

This method of arriving at the speed and power required is only approximate, since when operating at other than the rated point the pressure will not be constant. For small increments of over or under load the speed may be changed slightly to bring the pressure to the desired amount, but for accurate work the method of using the diagram on page 215 as explained under Example 5 should be followed.

**Example 5.** Supply ventilation only, with 30 cu. ft. of air per minute for each of 500 occupants. This will require

$$30 \times 500 = 15000$$
 A. P. M. at  $70^{\circ}$ 

which will be equivalent to  $440000 \div 15000 = 29$  or approximately two changes per hour.

With a velocity of 1200 feet per minute through the heater, this will require a clear area of 12.5 sq. ft. From the table on page 449 we find that a section of  $4'0'' \times 6'10''$  may be used. As the same temperature rise is required as in Example 4, the heater must be four sections deep and the final temperature  $81.8^{\circ}$ . If the heater and fan are located in the building so that there will be little or no radiation loss from the piping, the air may leave the heater at approximately 70°. We see from the heater table that with a velocity of 1000 feet per minute three sections will give a final temperature of 69.5°. By selecting a heater with a clear area slightly greater than indicated by 1000 velocity, we will obtain a final temperature somewhat above 70°. From the table of heaters we find that a 4'6" x 7'4" section will have a clear area of 15.3 sq. ft. and give a velocity of 980 feet per minute through the clear area. Thus we see that when using a final temperature of about 70° we may select three sections deep of 4'6" x 7'4" heater.

As we are using a low velocity and a heater only three sections deep, the loss in pressure through the heater will be only 0.287 inch, and it is probable that the static resistance of the entire system will not be over 0.6 inch. As under rated conditions the static pressure of a Planoidal Exhauster is 79 per cent. of the total pressure, if we use this type of fan operating at rated capacity the total pressure developed would be  $0.6 \div 0.79 = 0.76$ inch or approximately  $\frac{3}{4}$  inch.

From the table of fan capacities on page 207, we find that a 100-inch Planoidal Exhauster will deliver 13940 A. P. M. at 228 R. P. M. against ¾ inch total pressure and require 3.6 H. P. As 15000 A. P. M. is required, it will be necessary to operate this fan at greater than its rated capacity. We note from the diagram on page 214 that if this style of fan is operated at constant speed beyond its rated point the pressure will be less than the rated, so it will be necessary to operate at a speed corresponding to a certain higher pressure, in order to still have the required pressure when working over the rated capacity. The speed and horsepower to meet the required overload condition may be found approximately by means of the diagram on page 214, but as explained in the example on "Fan Selection" on page 183, the more accurate method is to use the diagram on page 215.

The outlet area of a 100-inch Planoidal Exhauster is 8.75 sq. ft., so at 15000 A. P. M. the outlet velocity will be 1715 feet per minute and the corresponding velocity pressure equals 0.183 inch. Since the static resistance of the system is 0.60 inch, the

rated total pressure will be 0.60 + 0.183 = 0.783 inch. The ratio of static to velocity pressure  $= 0.6 \div 0.183 = 3.28$ . From the diagram on page 215 we find that with the above ratio we will be operating at 105 per cent. of the fans rated capacity, with 102.5 per cent. of the rated H. P., and the speed will be the rated speed for this fan when developing a total pressure of 0.783 inch.

This fan will give the following rated performance at the two different total pressures.

0.75 in. - 13940 A. P. M. - 228 R. P. M. - 3.6 H. P.

0.783 in. - 14250 A. P. M. - 233 R. P. M. - 3.85 H. P.

But  $15000 \div 1.05 = 14300$  A. P. M. as the rated capacity required, which is practically as given for 233 R. P. M. Then the power required under the overload condition will be

 $3.85 \times 1.025 = 3.95$  H. P.

From the above we see that the 100-inch fan will deliver 15000 A. P. M. against a static pressure of 0.6 inch at 233 R. P. M. and require 3.95 H. P.

**Example 6.** Heat the building and supply a  $12\frac{1}{2}$  minute air change for ventilation.

The outdoor air to be handled by the fan will be

$$\frac{440000}{12\frac{1}{2}}$$
 = 35200 A. P. M. at 70°

This air must be raised to room temperature for ventilation, and enough higher to supply the heat lost by radiation and leakage.

As already shown the heat lost by radiation from this building will be 840000 B. t. u. per hour. It is customary to allow an extra 10 to 50 per cent., depending on the construction of the building and the purposes for which it is used, to care for the heat lost by leakage, opening of doors, and similar causes. Allowing an extra 30 per cent. we will have as the total heat loss

H = 840000 + 252000 = 1092000 B. t. u. per hour.

To determine the final temperature required we will have

$$t_2 = \frac{55.2 \times 1092000}{35200 \times 60} + 70 = 98.6^{\circ}$$

From the heater table on page 420 we find that with a velocity of 1000 feet per minute five sections of heater will raise the temperature of the air from 0° to 103°. As we are to handle 35200 A. P. M. at 1000 velocity, a heater having a clear area of 35.2 sq. ft. will be required. From the table on page 449 it may be seen that a heater section  $8'6'' \times 8'10''$  has a clear area of 35.3 sq. ft. so this will be the size to use, the heater being five sections deep. In case this heater is too tall for the particular space it is to occupy, we may use two sections placed back to back, each having a clear area of 17.6 sq. ft. This would call for ten sections of  $5'0'' \times 7'10''$  placed five sections deep.

## COMBINATION FAN, ENGINE AND HEATER TABLES

The four tables on pages 520 to 523 indicate what are considered as being the proper combinations of heaters and engines for the different sizes of Planoidal and Niagara Conoidal fans. The cubic feet of air at one inch for public buildings and two inches for industrial installations may be considered as the probable maximum conditions to be encountered. The engine sizes given are for direct connection, and in most cases could be made to answer for these extreme conditions. Several sizes and styles of engines are given in order that a choice may be made to meet different requirements. For instance, where a 7 x 7 and an 8 x 8 inch cylinder are given for the same size fan, a higher steam pressure would be required for the smaller cylinder. A steam pressure of from 20 to 25 pounds will be required for the low pressure, and from 80 to 100 pounds for the high pressure engines.

The heater sizes given in the table indicate the proper heaters for use with the different sizes of fans. A heater should be selected with a clear area that will give the desired velocity of the air through the heater. This will range anywhere from 800 to 1200 feet per minute, depending on the conditions. Lower velocities should be used for public buildings than for industrial installations.



Fan, Heater and Engine Installation

#### PLANOIDAL (TYPE L) EXHAUSTERS

### WITH PROPER COMBINATIONS OF HEATERS AND ENGINES FOR PUBLIC BUILDINGS AND INDUSTRIAL INSTALLATIONS

Size				Buffalo	•	Engine Size		
of Fan	l inch Total	2 inch Total Press.	Arrange- ment	Style	Size	Clear Area Sq. Ft.	Low Press. Steam	High Press. Steam
50	4030	5690	Single	R.O.A.	3'-0" x 3'- 4"	4.4		
55	4870	6890		R.O.A.	3'-0" x 4'- 4"	$\begin{smallmatrix} 5.2 \\ 6.0 \end{smallmatrix}$	}	3x3 ½ I
60	5800	8200	Single	R.O.A,	$3'-0'' \ge 4'-4''$ $3'-0'' \ge 4'-10''$ $3'-0'' \ge 5'-4''$	$     \begin{array}{r}       6.0 \\       6.8 \\       7.6     \end{array} $	} 8x6	4x3 ½ I
70	7890	11540	Single	R.O.A.	$3'-0'' \ge 5'-4''$ $3'-0'' \ge 5'-10''$ $4'-0'' \ge 5'-4''$	7.6 8.4 9.7	} 8x6	4x3½I
80	10300	14570	Single	R.O.A.	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$     \begin{array}{r}       10.7 \\       11.2 \\       12.6 \\       12.1 \\       13.1     \end{array} $	} 8x6	5x5 4½x5 I
90	13040	18440	Single	R.O.A.	$\begin{array}{c} \hline 4'-6'' \ge 6'-4'' \\ 4'-6'' \ge 6'-10'' \\ 4'-6'' \ge 7'-4'' \\ 5'-0'' \ge 6'-4'' \\ 5'-0'' \ge 6'-10'' \\ 5'-0'' \ge 7'-4'' \end{array}$	$\begin{array}{r} 13.1 \\ 14.2 \\ 15.3 \\ 14.1 \\ 15.4 \\ 16.6 \end{array}$	<b>8x6</b>	5 x5 4½x5 I
100	16100	22770	Single	R.O.A.	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$     \begin{array}{r}       15.4 \\       16.6 \\       17.7 \\       19.8     \end{array} $	$\left. \right\} 10x8$	6 x6 4 ¹ / ₂ x5 I 5 x10 N
110	19480	27540	Single	R.O.A. R.B.	6'-0" x 7'- 4" 6'-0" x 7'-10" 6'-0" x 8'- 4" 6'-0" x 8'-10" 7'-0" x 7'- 4"	$     \begin{array}{r}       19.8 \\       21.3 \\       22.7 \\       24.2 \\       23.6     \end{array} $	} 10x8	7 x7 6 x8 6 ¹ / ₂ x8 I 5 x10 N
120	23180	32780	Single	R.O.A. R.B.	6'-0" x 8'-4" 6'-0" x 8'-10" 7'-0" x 7'-4" 7'-0" x 7'-10" 7'-0" x 8'-4" 7'-0" x 8'-10"	$\begin{array}{r} 22.7 \\ 24.2 \\ 23.6 \\ 25.4 \\ 27.2 \\ 29.0 \end{array}$	} 12x8	7 x7 8 x8 6 ¹ / ₂ x8 I 6 x10 N
130	27210	38470	Single	R.B.	$\begin{array}{c} 7'-0'' \ge 8'-4'' \\ 7'-0'' \ge 8'-10'' \\ 7'-0'' \ge 9'-4'' \\ 7'-0'' \ge 9'-10'' \\ 8'-6'' \ge 8'-4'' \end{array}$	$\begin{array}{r} 27.2 \\ 29.0 \\ 30.7 \\ 32.5 \\ 33.2 \end{array}$	$\left.\right\}$ 12x8	8 x8 6½x8 I 6 x10 N
140	31560	44630	Single	R.B.	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{r} 30.7\\ 32.5\\ 33.2\\ 35.3\\ 37.6\\ 39.8\\ 41.8\\ 44.0\\ 36.7\\ 39.0\\ \end{array}$	} 15x8	8 x8 8 x10 7½x9 I 7 x12 N

### PLANOIDAL (TYPE L) EXHAUSTERS

#### WITH PROPER COMBINATIONS OF HEATERS AND ENGINES FOR PUBLIC BUILDINGS AND INDUSTRIAL INSTALLATIONS

	Cubic Feet of Air per Min.		Buffalo	Engine Size			
Size of Fan	l Inch 2 Inch Total Press. Press.	Arrange- ment	Style	Size	Clear Area Sq. Ft.	Low Press. Steam	High Press. Steam
150	36230 51220	Single	R.B.	8'-6" x 8'-10" 8'-6" x 9'-1" 8'-6" x 9'-10" 8'-6" x 10'-4" 8'-6" x 10'-10" 9'-6" x 8'-1" 9'-6" x 9'-10" 9'-6" x 9'-10" 9'-6" x 9'-10"	35.3 37.6 39.8 41.8 44.0 36.7 39.0 41.4 43.8 46.0	}15x8	10 x8 8 x10 7 ½x9 I 7 x12 N
160	41220 58270	Single Back to Back	R.B. R.O.A. R.B.	$\begin{array}{c} \hline & & & & \\ \hline & & & & \\ \hline \hline & & \\ \hline \hline \\ \hline & & \\ \hline \hline & & \\ \hline \hline \\ \hline & & \\ \hline \hline \hline \\ \hline & & \\ \hline \hline \hline \\ \hline & & \\ \hline \hline \hline \\ \hline \hline \hline \\ \hline \hline \hline \\ \hline \hline \hline \hline$	$\begin{array}{c} \hline & 39.8 \\ 41.8 \\ 44.0 \\ 41.4 \\ 43.8 \\ 46.0 \\ 48.4 \\ 50.8 \\ 53.2 \\ 39.6 \\ 41.6 \\ 45.4 \\ 48.4 \\ 47.2 \\ \end{array}$	} }15×10	10x10 8x12 N
170	46530 65790	Single Back to Back	R.B. R.O.A. R.B.	9'-6" x 10'-4" 9'-6" x 10'-10" 9'-6" x 11'-10" 9'-6" x 11'-10" 6'-0" x 8'-10" 7'-0" x 8'-10" 7'-0" x 7'-2" 7'-0" x 8'-10" 7'-0" x 8'-10" 7'-0" x 8'-10"	$\begin{array}{r} 46.0\\ 48.4\\ 50.8\\ 53.2\\ 45.4\\ 48.4\\ 47.2\\ 50.8\\ 54.4\\ 58.0\\ \end{array}$	}15×10	10x10 8x14 N 9x14 N
180	52160 73760	Back to Back	R.B.	7'-0" x 7'-10" 7'-0" x 8'- 4" 7'-0" x 8'-10" 7'-0" x 9'-4" 7'-0" x 9'-10" 8'-6" x 8'- 4"	54.4	}16×10	12x10 10x12 9x14 N
190	58120 82180	Back to Back	R.B.	$\begin{array}{c} 7'-0'' \ge 8'-10''\\ 7'-0'' \ge 9'-4''\\ 7'-0'' \ge 9'-10''\\ 8'-6'' \ge 8'-4''\\ 8'-6'' \ge 8'-10''\\ 8'-6'' \ge 9'-4''\\ 9'-6'' \ge 8'-4''\\ 9'-6'' \ge 8'-4''\\ \end{array}$	$\begin{array}{c} 58.0\\ 61.4\\ 65.0\\ 66.4\\ 70.6\\ 73.2\\ 73.4\end{array}$	}18x12	12x12 9x14 N

### NIAGARA CONOIDAL (TYPE N) FANS WITH PROPER COMBINATIONS OF HEATERS AND ENGINES FOR PUBLIC BUILDINGS AND INDUSTRIAL INSTALLATIONS

Fan	Cubic Feet of Air per Min.			Buffalo	Engine Size			
No.	l Inch Total Press.	2 Inch Total Press.	Arrange- ment	Style	Size	Clear Area Sq. Ft.	Low Press. Steam	High Press. Steam
4	4340	6130	Single	R.O.A.	3'-0" x 3'- 4" 3'-0" x 3'-10"	4.4 5.2		
41/2	5490	7760	Single	R.O.A.	3'-0" x 3'-10" 3'-0" x 4'- 4" 3'-0" x 4'-10"	5.2 6.0 6.8	}	4x4 A 3x3½ I
5	6770	9550	Single	R.O.A.		6.0 6.8 7.6 8.4	} 5x5	4x4 A 4x3 ½ I
5 1/2	8200	11590	Single	R.O.A.		7.6 8.4 9.7 10.7 11.2	6x6	4x4 A 4x3 ½ I
6	9750	13790	Single	R.O.A.	$\begin{array}{c} 4'-0'' x 5'-4'' \\ 4'-0'' x 5'-10'' \\ 4'-0'' x 6'-4'' \\ 4'-0'' x 6'-10'' \\ 4'-6'' x 5'-10'' \\ 4'-6'' x 5'-10'' \\ 4'-6'' x 6'-4'' \end{array}$	9.7 10.7 11.2 12.6 12.1 13.1	} 6x6	5 x5 A 4½x5 A
7	13280	18770	Single	R.O.A.	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$\begin{array}{r} 12.6\\ 12.1\\ 13.1\\ 14.2\\ 15.3\\ 14.1\\ 15.4\\ 16.6\\ 17.7\\ \end{array}$	} 8x6	5 x5 A 5½x7 I
8	17340	24520	Single	R.O.A.		$     \begin{array}{r}       16.6 \\       17.7 \\       19.8 \\       21.3 \\       22.7     \end{array} $	} 10x8	$\begin{array}{c} 6 \mathbf{x} 6 \mathbf{A} \\ 5 \frac{1}{2} \mathbf{x} 7 \mathbf{I} \end{array}$
9	21950	31020	Single	R.O.A.	6'-0" x 7'-4" 6'-0" x 7'-10" 6'-0" x 8'-4" 6'-0" x 8'-10" 7'-0" x 7'-4" 7'-0" x 7'-10" 7'-0" x 8'-4"	$     \begin{array}{r}       19.8 \\       21.3 \\       22.7 \\       24.2 \\       23.6 \\       25.4 \\       27.2 \\     \end{array} $	> 10x8	6 x6 A 6½x8 I
10	27090	38310	Single	R.B.	$\begin{array}{c} 7'{-}0'' \ge 7'{-}10'' \\ 7'{-}0'' \ge 8'{-}4'' \\ 7'{-}0'' \ge 8'{-}10'' \\ 7'{-}0'' \ge 9'{-}4'' \\ 7'{-}0'' \ge 9'{-}4'' \\ 7'{-}0'' \ge 9'{-}10'' \\ 8'{-}6'' \ge 8'{-}4'' \\ 8'{-}6'' \ge 8'{-}10'' \end{array}$	25.4 27.2 29.0 30.7 32.5 33.2 35.3	} 12x8	7 x7 A 6½x8 I 6 x10 N

#### NIAGARA CONOIDAL (TYPE N) FANS

#### WITH PROPER COMBINATIONS OF HEATERS AND ENGINES FOR PUBLIC BUILDINGS AND INDUSTRIAL INSTALLATIONS

Fan	Cubic Feet of Air per Min.		I	Buffalo :	Engine Size			
No.	Total	2 inch Total Press.	Arrange- ment	Style	Size	Clear Area Sq. Ft.	Low Press. Steam	High Press. Steam
11	32780	46360	Single	R.B.	$\begin{array}{c} & & & & & & & & & & \\ \hline 7'-0'' \times 9'-10'' \\ 8'-6'' \times 8'-4'' \\ 8'-6'' \times 8'-10'' \\ 8'-6'' \times 9'-10'' \\ 8'-6'' \times 9'-10'' \\ 8'-6'' \times 10'-10'' \\ 8'-6'' \times 10'-10'' \\ 9'-6'' \times 8'-4'' \\ 9'-6'' \times 8'-10'' \\ 9'-6'' \times 9'-10'' \\ 9'-6'' \times 9'-10'' \\ 9'-6'' \times 9'-10'' \\ \end{array}$	$\begin{array}{r} 30.7\\ 32.5\\ 33.2\\ 35.3\\ 37.6\\ 39.8\\ 41.8\\ 44.0\\ 36.7\\ 39.0\\ 41.4\\ 43.8\end{array}$	} 12x8	8x 8 A 7½x 9 I 7 x12 N
12	39010	55170	Single	R.B.	$\begin{array}{c} 8'{-6''} \times 8'{-10''} \\ 8'{-6''} \times 9'{-4''} \\ 8'{-6''} \times 9'{-10''} \\ 8'{-6''} \times 10'{-10''} \\ 8'{-6''} \times 10'{-10''} \\ 9'{-6''} \times 8'{-4''} \\ 9'{-6''} \times 8'{-4''} \\ 9'{-6''} \times 8'{-10''} \\ 9'{-6''} \times 9'{-10''} \\ 9'{-6''} \times 9'{-10''} \\ 9'{-6''} \times 10'{-10''} \\ 9'{-6'''} \times 10'{-10''} \\ 9'{-6'''} \times 11'{-4''} \end{array}$	$\begin{array}{c} 35.3\\ 37.6\\ 39.8\\ 41.8\\ 44.0\\ 36.7\\ 39.0\\ 41.4\\ 43.8\\ 46.0\\ 48.4\\ 50.8\\ \end{array}$	}15x8	10x 8 A 8x10 A 7x12 N
13	45780	64730	Single Back to Back	R.B. R.O.A. R.B.	$\begin{array}{c} 8'-6'' \ge 10'-4''\\ 8'-6'' \ge 10'-10''\\ 9'-6'' \ge 9'-4''\\ 9'-6'' \ge 9'-4''\\ 9'-6'' \ge 9'-10''\\ 9'-6'' \ge 10'-4''\\ 9'-6'' \ge 11'-4''\\ 9'-6'' \ge 11'-10''\\ 6'-0'' \ge 8'-4''\\ 6'-0'' \ge 8'-4''\\ 6'-0'' \ge 8'-4''\\ 7'-0'' \ge 7'-4''\\ 7'-0'' \ge 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ 8'-10''\\ $	$\begin{array}{c} 41.8\\ 44.0\\ 41.4\\ 43.8\\ 46.0\\ 48.4\\ 50.8\\ 53.2\\ 42.6\\ 45.4\\ 48.4\\ 47.2\\ 50.8\\ 54.4\\ 55.8\\ 54.4\\ 58.0\\ \end{array}$	> 15x8	10x 8 A 8x12 N
14	53100	75090	Single Back to Back	R.B. R.O.A. R.B.	$\begin{array}{c} 9'-6'' \times 10'-10''\\ 9'-6'' \times 11'-4''\\ 9'-6'' \times 11'-4''\\ 9'-6'' \times 11'-10''\\ 6'-0'' \times 8'-10''\\ 7'-0'' \times 8'-4''\\ 7'-0'' \times 8'-4''\\ 7'-0'' \times 8'-4''\\ 7'-0'' \times 9'-4''\\ 7'-0'' \times 9'-10''\\ 8'-6'' \times 8'-4''\\ 8'-6'' \times 8'-10''\\ 8'-6'' \times 8'-10''\\ \end{array}$	$\begin{array}{c} 48.4\\ 50.8\\ 53.2\\ 48.4\\ 50.8\\ 54.4\\ 58.0\\ 61.4\\ 65.0\\ 66.4\\ 70.6\end{array}$	}15x10	10x10 A 8x14 N

## PART V

## APPENDIX

Complete directions for conducting Fan Installation Tests are included in this part.

This section also includes complete specifications and guarantees for various types of fans, heaters, piping, engines, motors, air washers and humidifiers; and detailed dimensions of Planoidal Steel Plate, Niagara Conoidal Multiblade and Turbo-Conoidal High Speed Multiblade Fans.

Data for the design of chimneys, with table giving size of chimneys with appropriate horsepower of boilers is included.

Miscellaneous engineering data is also given, including size of steam pipes, area of circles, temperature and pressure conversion tables, steam tables, logarithms, dry kiln capacities, many useful factors, etc.

An extract of the report of the committee of the Am. Soc. of H. & V. Engrs. on "Standards for Ventilation Legislation for Motion Picture Show Places" as presented in Jan., 1913, is reproduced.

A very complete and thorough index and cross-index, in addition to "Outline of Contents" in Part I, is given in this part.

NOTE—All temperatures given in this book are in degrees Fahrenheit unless otherwise specified.

## DIRECTIONS FOR MAKING FAN INSTALLATION TESTS

The general subject of fan testing has been discussed on pages 190 to 204, with complete directions for using the pitot tube and for laying out a traverse of a pipe or duct. The detailed methods to be used in making a test on a fan installation, together with detailed instructions for working up the results of the test, will be given in the following:

## Measuring the Air Quantity

- 1. Traverse over outlet or inlet pipe.
- 2. Traverse over fan outlet.

The velocity of the air and the quantity delivered should be determined by means of the pitot tube as explained on page 190. Whenever the nature of the installation makes it possible the most accurate results are obtained by making a traverse in the discharge or inlet duct. These velocity pressure readings should be taken at least 10 diameters, in the direction of the air flow, from the fan outlet, or from any bend, elbow, change in section, or other detail of construction that will cause a disturbance in the flow of air preceding the point at which the readings are taken. Readings at the fan inlet should be taken one diameter or more from the inlet.

While a traverse of the pipe is preferable, it is usually impracticable in actual installations to find a point where the air flow is undisturbed. In such cases a traverse with the pitot tube over the outlet area of the fan should be made.

The outlet area should be divided into 25 or more equal rectangles (5 or more each way) and velocity pressure readings taken in the center of each small area. The velocity corresponding to each of these velocity pressure readings should then be calculated as explained on page 18, and an average taken of these velocities. This gives the average velocity over the entire fan outlet, which in turn when multiplied by the area of the outlet in square feet gives the quantity of air delivered in cubic feet per minute. It will be noted that the average velocity over the outlet should be obtained by taking an average of the various velocities and not of the various velocity pressure readings, since the velocity varies as the square root of the pressure.

In taking the velocity pressure by means of a pitot tube, the connection between the two legs of the tube and the two sides of the gauge should be the same, whether the readings are taken in a duct either on the inlet or on the outlet side of the fan.

### Measurement of Pressure Produced by the Fan

The relation between total, static and velocity pressure as produced by a fan has been explained on page 176. The measurement of the total or dynamic pressure is of especial importance since this is the pressure upon which the efficiency of the fan is based. This pressure is a measure of the total energy imparted to the air by the fan and is the difference between the average absolute total or dynamic pressure of the air on the two sides of the fan. The absolute pressure expressed in inches of water for air at 29.92 inches barometer will be the measured pressure plus 407 inches. The absolute total pressure at any point consists of the absolute static pressure plus the velocity pressure.

Since the total dynamic energy at any point in a stream of air is measured by the absolute total or dynamic pressure at that point, the gain or loss in energy between two points in a stream of air is measured by the difference between the absolute total pressures at these points. It follows that the total energy imparted by a fan to a given quantity of air is measured by the difference between the absolute total pressures measured at the inlet and outlet connections respectively and that the total or dynamic pressure produced by a fan is equal to the difference between the absolute total or dynamic pressures at these two points. Thus if an exhaust fan gives static and velocity pressure readings on the inlet side of 3" and 0.5" respectively, the absolute total pressure at the inlet will be (407-3)+0.5=404.5". If the static and velocity pressures on the outlet side are 2" and 1" respectively, the absolute total pressure at this point will be (407+2)+1=410. Then the total pressure against which the fan is operating will be 410 - 404.5 = 5.5''. This may be expressed in gauge pressure as follows:

The static pressure produced by a fan equals the total pressure minus the velocity pressure at the fan outlet. It follows that

Static pressure of fan equals The static pressure at the fan outlet +static vacuum at fan inlet (or - static pressure)

-velocity pressure at fan inlet.

The Difference in static pressure at the inlet and outlet of the fan equals

The static pressure produced by the fan +the velocity pressure at the fan inlet.

It should be noted that the static vacuum at the fan inlet minus the velocity pressure at the fan inlet is the total pressure at this point.

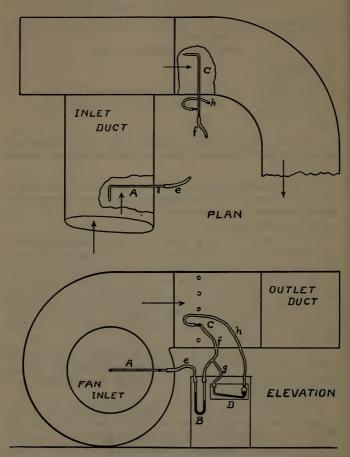
The static pressure as produced by the fan in accordance with the accepted definition does not necessarily correspond to the difference in static pressures as measured at the fan inlet and outlet respectively.

(a) Where the velocity in the inlet connection is negligible, the difference in static pressures at the inlet and outlet of the fan corresponds to the static pressure produced by the fan.

(b) If the inlet and outlet connections to the fan are equal, the difference in the static pressures will not correspond to the static pressure produced by the fan, but will be equal to the total pressure produced by the fan when measured as previously described.

(c) If the fan inlet connection is smaller than the outlet of the fan, the difference between the static pressure readings taken at the inlet and outlet will be greater than the total pressure produced by the fan.

This apparent discrepancy in the static pressures is due to the fact that a certain amount of static pressure may be produced by conversion from velocity pressure and is not produced by the fan itself. The static pressures specified for the various fans assume the fan to be exhausting from a large chamber having a negligible air velocity. It is evident that the pressures are greatly modified when exhausting through a duct.



Testing a Fan Installation

The proper arrangement of the gauges and the points at which the readings should be taken are shown on the drawing, page 528, which represents a fan drawing through one duct and blowing into another. A pitot tube is shown at A with the central or impact opening connected by a rubber hose to one side of a water column or draft gauge B. (For description of pitot tubes see page 190.) A second pitot tube is shown at C. having its impact or total pressure leg connected to the other side of the same gauge B. A cross connection is also made from this impact connection from pitot tube C to one leg of another gauge D and a connection made between the static leg of pitot tube C to the other side of this gauge. The readings obtained at D are then the difference between the total and static pressures, or the velocity pressure at the fan outlet. The gauge B gives the difference in total pressures at the two points A and C, or the total pressure developed by the fan. The static pressure will be the difference between the total and velocity pressure readings.

As already explained, a traverse should be made over the fan outlet, and the velocity pressure read at each point. The corresponding velocities should then be determined for each reading (see page 18) and an average taken of these various velocity readings. The velocity pressure corresponding to this final average velocity will be the average velocity pressure reading at the fan outlet, which on being added to the static pressure gives the total pressure on the fan.

### Method of Calculating Fan Tests

The following are the various factors entering into the calculation of the performance of a fan as based on the results of a test. The object of such a test is to determine the pressure developed, the air quantity delivered, the power required and the efficiency of the fan. The various steps in the calculation may be stated as follows:

1. The velocity pressure is the pressure corresponding to the average velocity over the area of either the inlet or outlet of the fan.

2. The total static pressure produced by the fan is the arithmetical sum of the static readings on the two sides of the fan minus the velocity pressure at the fan inlet.

3. The total or dynamic pressure is the sum of the velocity and static pressures.

4. The air quantity is the product of the average velocity pressure times the area of the duct in which the readings were taken.

5. In case the fan is motor driven the total power input will be the product of the volts times the amperes as shown by the meters connected at the motor.

6. Careful readings of the speed of the fan and motor should be made at time of taking other readings.

7. The I²R loss in watts for the current taken by the motor may be determined by means of a voltage drop test made with the wheel blocked. The I²R loss is frequently assumed as being from 2 to 3 per cent. of the full load current of the motor.

8. The belt and bearing loss may be determined by removing the wheel from the shaft and taking power readings. Where this is impractical this loss may be assumed at from 3 to 5 per cent. of the power input, depending on the bearing conditions and on whether the fan is direct connected or belt driven. Some allowance should also be made for belt slip.

9. No load power readings should be obtained from the motor by disconnecting it from the fan or throwing off the belt. This no load current may frequently be determined from the characteristics of the motor.

10. The actual power consumed by the fan will then be the total watts input minus the no load watts and the various losses enumerated above, equals (5) - [(7) + (8) + (9)].

11. The brake horsepower of the fan will be the net watts from item 10 divided by 746.

12. In case the fan is driven by means of a steam engine, indicator cards should be taken with the fan in operation and with the wheel removed or disconnected. The difference between the two sets of cards will give the brake horsepower consumed.

13. The air horsepower is the product of the air quantity handled in cubic feet per minute times the pressure in inches of water times a constant 0.000157 (see page 175).

14. The total or dynamic efficiency is the ratio of the product of the air quantity times the total or dynamic pressure in inches times 0.000157 divided by the brake horsepower.

Total eff. =  $\frac{A. P. M. \times \text{total press. in in.} \times 0.000157}{\text{Brake H. P.}}$ 

15. The static efficiency is the ratio of the product of the air quantity times the static pressure in inches times 0.000157 divided by the brake horsepower and may be expressed as above by inserting static for total pressure in the formula.

It frequently occurs that a fan is guaranteed to give a certain performance under other than actual test conditions as to speed and temperature. In this case the test results should be corrected to the guaranteed speed and air density. As shown on page 179, the pressure developed will vary as the square and the power consumed as the cube of the speed. Both the pressure and power consumed will vary directly as the density of the air and should be multiplied by the ratio of the air densities under the two conditions. The density of the air may be determined from the table on page 17. These corrections should be made to the average pressure and the net power readings, before the air quantity and efficiency of the fan are calculated.

### SPECIFICATIONS

### STEEL PLATE FAN

Furnish and erect ( ) —— inch steel plate three-quarter (or full) housing, —— discharge exhauster (or blower) having a capacity of — cubic feet of air per minute delivered against a static (or total) pressure of —— inches at a speed of —— R. P. M., and requiring not over —— H. P.

Housing to be constructed of the best commercial steel plate No. — gauge, with riveted lap seams and braced by vertical and horizontal angle irons, — x —, and with angle iron base frame, — x —, drilled for holding-down bolts.

Fan to have one (or two) inlet — inches in diameter and an outlet — x — inches. If fan has a single inlet (exhauster) there shall be a cone extending inward to the inlet of the blast-wheel, so as to gradually increase the velocity of the air entering the wheel and so reduce the loss at entrance.

Blast-wheel to be — inches in diameter, constructed with a heavy cast iron hub into which T-iron arms are cast, firmly mounted by means of a key and set screw on a steel shaft inches in diameter. The blades to be made of No. — gauge steel plate riveted to - x - T-iron spider arms cast into the hub. and to be tapering in shape, wider at the inlet than at the periphery. Side sheets of wheel to be flanged outward at the inlet and riveted to sides of blades

Blast-wheel to be carefully balanced to prevent vibration.

Bearings to be spherical self-aligning ring-oiled type, lined with best quality babbitt, and so designed as to allow easy adjustment for wear. Bearings to be provided with large oil reservoir, and in case a bearing is mounted in the fan inlet it is to be provided with suitable arrangement for preventing oil from being drawn along shaft and into the fan by the entering air.

### MULTIBLADE FAN

Furnish and erect ( ) No. --- multiblade three-quarter (or full) housing, —— discharge single (or double) width fan having a capacity of ---- cubic feet of air per minute delivered against a static (or total) pressure of —— inches with a velocity through the fan outlet of ---- feet per minute, at a speed of ----- R. P. M., and requiring not over ----- H. P.

Housing to be constructed of the best commercial steel plate No. - gauge, with riveted lap seams and braced by vertical and horizontal angle irons, ---- x ----, and with angle iron base frame, - x -, drilled for holding-down bolts.

Fan to have one (or two) inlet —— inches in diameter and an outlet ----- x ----- inches. If a double width fan is used, the wheel is to be composed of two separate single width wheels mounted back to back. Each inlet to be fitted with an inlet cone in the space between housing and wheel, having a minimum clearance with the flared inlet of the blast-wheel. In order to obtain the greatest possible conversion of velocity head at tip of blades into static pressure at fan outlet, the inner edge of the outlet is to be approximately tangent to periphery of wheel, and the height of the outlet approximately equal to wheel diameter.

Blast-wheel to be of the forward curved multiblade type, having thirty-two blades of No .-- gauge steel plate riveted at the back to a boiler plate disk which in turn is to be hot-riveted to a conical cast iron hub. These blades to be connected by a flange at the inlet edge of the wheel. Hub is to be attached to the shaft by key and set-screws and to the inlet flange by four heavy tierods. The mean diameter of the blast-wheel to be - inches

Blast-wheel to be carefully balanced to prevent vibration.

The heel or inner edge of the blades to be so arranged as to give a decreasing inlet diameter from front to back in order to give a uniform radial velocity through the wheel. The angle of the blades at entrance shall vary across the width in order to insure the entrance of air with the least possible loss by shock. The curvature of the blades to be such that at normal or rated capacity the air will leave the tips with a velocity pressure approximately twice the pressure corresponding to the peripheral velocity of the wheel, in order to reduce the required speed of rotation.

Bearings to be spherical self-aligning ring-oiled type, lined with best quality babbitt, and so designed as to allow easy adjustment for wear. Bearings to be provided with large oil reservoir, and in case a bearing is mounted in the fan inlet, it is to be provided with suitable arrangement for preventing oil from being drawn along shaft and into the fan by the entering air.

### HIGH SPEED MULTIBLADE FAN

Furnish and erect () three-quarter (or full) housing,—— discharge single (or double) width high speed multiblade fan having a capacity of ——cubic feet of air per minute delivered against a static (or total) pressure of —— inches at a speed suitable for direct connection to motor specified, and requiring not over —— H. P.

Housing to be constructed of the best commercial steel plate No. — gauge, with riveted lap seams and braced by vertical and horizontal angle irons, — x —, and with angle iron base frame, — x , drilled for holding-down bolts.

Fan to have one (or two) inlet — inches in diameter and an outlet — x — inches. If a double width fan is used, the wheel is to be composed of two separate single width wheels mounted back to back. Each inlet to be fitted with an inlet cone in the space between housing and wheel, having a minimum clearance with the flared inlet of the blast-wheel. In order to obtain the greatest possible conversion from the high velocity pressure at tip of blades into a correspondingly high static pressure at the fan outlet, the inner edge of the outlet is to be approximately tangent to periphery of wheel, and the height of the outlet approximately equal to wheel diameter. Blast-wheel to have thirty-two curved blades of No. gauge steel plate riveted at the back to a boiler plate disk which in turn is to be hot-riveted to a conical cast iron hub. These blades to be connected by a flange at the inlet edge of the wheel. The hub to be attached to the shaft by key and set-screws and to the inlet flange by four heavy tierods. Blast-wheel to be carefully balanced to prevent vibration.

The heel or inner edge of the blades to be so arranged as to give a decreasing inlet diameter from front to back in order to give a uniform radial velocity through the wheel. The angle of the blades at entrance shall vary across the width in order to insure the entrance of the air with the least possible loss by shock at this point. The angle of the blades at the tip, or periphery of the wheel, to be such that a uniform delivery and pressure will be obtained across the width of the wheel.

Bearings to be spherical self-aligning ring-oiled type, lined with best quality babbitt, and so designed as to allow easy adjustment for wear. Bearings to be provided with large oil reservoir, and in case a bearing is mounted in the fan inlet, it is to be provided with suitable arrangement for preventing oil from being drawn along shaft and into the fan by the entering air.

#### FAN SYSTEM HEATER

Furnish and erect — four-row sections of pipe coil fan system heater, each section to be — ft. — in. long x — ft. — in. high. Each section to have heating surface equivalent to lineal feet of 1-inch pipe, and a clear area of — sq. ft. for the passage of air.

The heater bases are to be of cast iron of uniform thickness, with heavy box section and extra heavy tops drilled and tapped for 1-inch pipe on  $2\frac{5}{8}$ -inch centers, adjacent rows to be staggered so as to bring the air in intimate contact with the heating surfaces. For the purposes of accelerating the circulation, the base is to be provided with a partition separating the inlet from the return space. Steam and drip connections to be tapped as may be directed. Pipes to be threaded at each end with standard dies and screwed into base. Sections to be tested and made tight at 100 lbs. cold water pressure.

Heater casings to be of No. 18 gauge steel plate, stiffened at all edges and seams with  $1\frac{1}{2}$ " x  $1\frac{1}{2}$ " angle iron and extended to connect with the fan. The heater casing is to extend to the foundation so as to entirely enclose the cast iron bases, preventing radiation losses. Casing to cover both sides, top, and bottom of the heater.

A cast iron steam receiver is to be furnished with companion flanges tapped for individual connections to the several sections, and with a flanged opening for main steam supply.

### FAN ENGINE

Furnish and erect ( ) — x — x — horizontal (or vertical) center (or side) crank engine for belt drive (or direct connection). Engine to have cylinder — inches in diameter by — inches stroke, and to operate at — R. P. M. with initial steam pressure of — lbs. Steam pipe to be — inches with exhaust pipe — inches in diameter.

Engine to have a balanced piston valve so constructed as to take up wear in the surface of valve and valve seats. The eccentric rod is to connect to the valve stem crosshead by phosphor bronze bearing. Crankshaft to be a steel forging to which cast iron counter balance disks are solidly fitted.

Connecting rod to be of steel, with locomotive type end for crank pin, and solid end for carrying the crosshead pin boxes. The crosshead pin boxes are to be of phosphor bronze. Crank pin boxes are to be of cast iron lined with the best babbitt metal. Both ends of the connecting rod are to be provided with adjustment for taking up wear on the pin.

Crosshead guides are to be bored and have ample bearing surface.

Crossheads to be of cast steel, fitted with wedge-adjustable shoes for taking up wear and keeping the wrist pin in alignment with the cylinder.

All running surfaces are to be true to form and well polished.

The engine is to be filled and given a well finished painted surface before leaving the factory.

The following fittings to be furnished: Throttle valve, sight feed lubricator, necessary oil and grease cups, and full set of wrenches.

## DUCT WORK

To be constructed and installed in accordance with Drawing No. —. Make all sheet metal ducts of best quality galvanized steel sheets, with slip joints in the direction of the air flow, rectangular ducts to have standing seams, and wide ducts to be stiffened by angle irons where necessary.

All round pipes of less than  $5\frac{1}{4}$  to 8 sq. ft. of No. 24 gauge; 8 to  $10\frac{1}{2}$  sq. ft. of No. 22 gauge;  $10\frac{1}{2}$  to  $13\frac{1}{4}$  sq. ft. of No. 20 gauge;  $13\frac{1}{4}$  to  $22\frac{1}{2}$  sq. ft. of No. 18 gauge; above  $22\frac{1}{2}$  sq. ft. of No. 16 gauge.

All rectangular pipes less than 18 inches wide are to be made of No. 26 gauge; from 19 to 30 inches of No. 24 gauge; from 31 to 60 inches of No. 22 gauge; from 61 to 118 inches of No. 20 gauge; above 118 inches wide of No. 18 gauge.

No square turns are to be used at any point where it is possible to use curves, so as to offer the least possible resistance to the passage of air. All joints are to be smooth and tight, and all pipes are to be firmly hung and rigidly fastened in place. The work is to be left in first-class condition throughout.

Each branch rectangular duct is to be provided with a damper and quadrant which may be set and locked in position.

Round branch outlets to have adjustable butterfly dampers.

After erection test and set dampers for proper air distribution.

### DIRECT CURRENT MOTOR

Furnish ( ) — H. P. — Volt direct current motor for direct (or belt) connection to fan at the speed specified. Motor to be of standard construction and equipped with starting rheostat, and furnished with

a-rheostat for starting duty only.

b—combined starting and speed regulating rheostat, capable of reducing the speed 50 per cent. below normal by armature resistance.

c—combined starting and speed regulating rheostat capable of increasing the speed — per cent. above normal by weakening the field circuit.

If direct connected to fan, motor is to be furnished without base rails or pulley, but with flanged coupling, key-seated, faced and polished.

If belted to fan, furnish pulleys of the proper size and single leather endless belt.

### ALTERNATING CURRENT MOTOR

Furnish ( ) — H. P. — Volt — cycle — phase motor of standard construction with starter complete.

If direct connected to fan, motor is to be furnished without base rails or pulleys, but with flanged coupling, key-seated, faced and polished.

If belted to fan, furnish pulleys of the proper size and single leather endless belt.

### SUBBASES

For fans direct connected to motors, furnish heavy steel plate subbase to be made tapering and with rounded corners and fitted with continuous angle iron extending around the base. Subbases must be braced inside and provided with hand hole for bolting down the motors. After erection the contractor is to fill the subbases with concrete to prevent transmission of sound.

## CARRIER TYPE "A" AIR WASHER AND HUMIDIFIER

Furnish and erect where shown on plans one (1) air washer of a design as specified herein. Washer is to have a capacity of ----- cu, ft. A. P. M.

The velocity of the air through the washer shall not be greater than 500 ft. per minute and the total guaranteed resistance of the washer shall not exceed .25 inch water. Washer is to be 7'  $25_{16}''$  long, — wide and — high.

**Casing.** The washer shall be constructed of galvanized iron of No. 18 gauge. Settling tank at least 16 inches high to extend under the entire washer and to be made of No. 16 gauge galvanized iron. The casing and tank shall be braced on the outside with  $1+\frac{1}{2}$ " x  $1+\frac{1}{2}$ " galvanized angles. These angles shall not be spaced further apart than 3 feet. All joints inside of casing shall be either soldered or made tight with rubber gaskets and bolts. All rivets and rivet holes shall be soldered over on inside of casing.

A perforated galvanized distributing plate on the inlet of the washer having 50 per cent. free area is to be provided.

Inspection Door. In the side of the washer casing is to be provided a door not less than  $15'' \ge 24''$  in size to allow easy and convenient access to the machine for inspection and cleaning. The door shall be of cast iron with two glass panels, each glass being not less than 9''  $\ge 12''$ . The door frame is also to carry a  $\frac{1}{4}'' \ge \frac{1}{4}''$  pure rubber gasket against which the door is to close. The frame is to be cast iron and riveted to the washer casing. The door is to be held closed by at least three cams on each side; and be sufficiently rigid to prevent cracking of glass when clamping tight against gasket.

Sprays. The brass spray nozzles shall be evenly spaced over the cross section of the washer and shall be placed at least 4 feet from the eliminator plates and in a plane parallel thereto. The spacing of these nozzles shall be such that the entire interior of the washer between the nozzles and eliminator plates shall be uniformly filled with a finely divided spray. There shall be at least five nozzles for every 2000 cu. ft. of air handled per minute. The nozzles shall give a finely divided "mist like" spray. No water passage or way to be smaller than 27/1000 sq. in. area, nor have less than  $\frac{3}{16}$ -inch minimum dimensions in any water passage. Stand-pipes shall be of  $1\frac{1}{4}$ -inch galvanized extra heavy wrought iron pipe screwed into a cast iron header. The flooding nozzles over the eliminators are to be spaced on 3inch centers and handle 1 G. P. M. each.

Eliminators. The eliminators shall set vertical in position and be made of No. 24 gauge galvanized iron. The angles of the eliminators shall not be greater than 35°. The eliminators shall be so set that the air in passing through is deflected at least six times. Eliminator plates to be bolted or riveted directly to galvanized iron supports. The angles of deflection in no case being greater than 35°. No separate metal clips will be allowed. The space of air passage between any two adjacent eliminator plates shall not exceed 1 inch.

The washer shall be so arranged that the first four bends of the eliminator plates shall become a washing surface. A separate set of sprays (independent of the main sprays) is to be provided for maintaining a constant sheet of water flowing down these four surfaces continually. The amount of washing surface thus provided shall not be less than 40 sq. ft. per 1000 cu. ft. of air per minute.

The last two bends of the eliminator plates are to remove effectively all free and entrained moisture. The 'total washing and eliminating surface shall not be less than 60 sq. ft. per 1000 cu. ft. of air per minute.

**Piping.** 2-inch galvanized overflow and 2-inch drain to sewer, the latter provided with gate valve.

The washer is to be provided with galvanized iron flanges for piping connections.

Note. All piping between the washer, settling tank and pump shall be galvanized and be installed by contractor in accordance with details furnished by the air washer manufacturer.

**Pump.** The air washer is to be furnished with a —— double suction centrifugal horizontally divided shell pump having a capacity of —— gallons per minute when discharging against sufficient head to obtain perfect spray effect of all nozzles.

The pump is to be of the horizontal type having enclosed runner and is to be provided with cast iron base plate for direct connection to a — H. P. motor of suitable current.

The casing of this pump is to be of grey cast iron, horizontally divided for convenient inspection, suitable to withstand an excess over the working pressure and designed with ample water ways for proper velocity.

All surfaces not machined shall be rubbed down, filled and painted a suitable dark color as directed.

The usual piping drains, fittings and grease cups are to be included.

Accessories. The washer is to be provided with an automatic float valve for maintaining a constant water level.

One strainer of 20-mesh copper screen is to be provided with the washer for straining all water recirculated by the pump. This strainer is to extend the entire width of the washer and shall have not less than 1 sq. ft. of surface for each 4000 cu. ft. of air handled per minute.

#### CARRIER TYPE "B" AIR WASHER AND HUMIDIFIER

Specifications for the Type "B" Air Washer and Humidifier are the same as for the Type "A" as given on pages 537 to 539 with the following exceptions:

Washer is 9'  $0\frac{3}{8}$ " long instead of 7'  $2\frac{5}{16}$ " long.

There shall be at least five nozzles for every 1000 cu. ft. of air handled per minute instead of five nozzles for every 2000 cu. ft. of air handled per minute.

## CARRIER TYPE "C" AIR WASHER AND HUMIDIFIER

The velocity of the air through the washer shall not be greater than 500 ft. per minute and the total guaranteed resistance of the washer shall not exceed .375 inch water. Washer is to be  $4' 10'' \log_2 - \cdots$  wide and  $- \cdots$  high.

**Casing.** The washer shall be constructed of galvanized iron of No. 18 gauge. Settling tank at least 16 inches high to extend under the entire washer and to be made of No. 16 gauge galvanized iron. The casing and tank shall be braced on the outside with  $1\frac{1}{2}$ " x  $1\frac{1}{2}$ " galvanized angles. These angles shall not be spaced further apart than 3 feet. All joints inside of casing shall be either soldered or made tight with rubber gaskets and bolts. All rivets and rivet holes shall be soldered over on inside of casing.

Inspection Door. In the side of the washer casing is to be provided a door not less than  $15'' \ge 24''$  in size to allow easy and convenient access to the machine for inspection and cleaning. The door shall be of cast iron with two glass panels, each glass being not less than 9"  $\ge 12''$ . The door frame is also to carry a  $\frac{1}{4}'' \ge \frac{1}{4}''$  pure rubber gasket against which the door is to close. The frame is to be cast iron and riveted to the washer casing. The door is to be held closed by at least three cams on each side, and be sufficiently rigid to prevent cracking of glass when clamping tight against gasket.

Sprays. The brass spray nozzles shall be evenly spaced over the cross section of the washer and to be placed at least 4 feet from the eliminator plates and in a plane parallel thereto. The spacing of these nozzles shall be such that the entire interior of the washer between the nozzles and eliminator plates shall be uniformly filled with a finely divided spray. There shall be at least five nozzles for every 2000 cu. ft. of air handled per minute. The nozzles shall give a finely divided "mist like" spray. No water passage or way to be smaller than 27/1000 sq. in. area, nor have less than  $\frac{3}{16}$ -inch minimum dimensions in any water passage. Stand pipes shall be of  $1\frac{1}{4}$ -inch galvanized extra heavy wrought iron pipe screwed into a cast iron header. **Eliminators.** The eliminators are to be made of corrugated sheets of No. 24 galvanized iron. These eliminators are to be set vertically in rows so that the air has a tortuous passage through them and they are to be evenly spaced not further apart than  $3\frac{1}{4}$ ". They shall be braced and stiffened with galvanized angles.

At least two of the corrugations of the sheet are to be provided with a lip for catching any entrained moisture which otherwise may pass through eliminator.

**Piping.** The washer is to be provided with galvanized iron flanges for piping connections.

One (1) overflow connection and drain is also to be provided.

Note. All piping between the washer, settling tank and pump shall be galvanized and be installed by contractor in accordance with details furnished by the air washer manufacturer.

**Pump.** The air washer is to be furnished with a —— double suction centrifugal horizontally divided shell pump having a capacity of ——— gallons per minute when discharging against sufficient head to obtain perfect spray effect of all nozzles.

The pump is to be of the horizontal type having enclosed runner and is to be provided with cast iron base plate for direct connection to a ——— H. P. motor of suitable current.

The casing of this pump is to be of grey cast iron, horizontally divided for convenient inspection, suitable to withstand an excess over the working pressure and designed with ample water ways for proper velocity.

All surfaces not machined shall be rubbed down, filled and painted a suitable dark color as directed.

The usual piping drains, fittings and grease cups are to be included.

Accessories. The washer is to be provided with an automatic float valve for maintaining a constant water level.

One strainer of 20-mesh copper screen is to be provided with the washer for straining all water recirculated by the pump. This strainer is to extend the entire width of the washer and shall have not less than 1 sq. ft. of surface for each 4000 cu. ft. of air handled per minute.

#### HUMIDITY CONTROL

The washer is to be provided with a system of humidity control arranged for maintaining a constant dew-point or saturated temperature of the air leaving the washer throughout the winter. This constant dew-point being maintained by varying the water temperature through which the air passes.

A thermostat is to be placed in the chamber between the washer and reheater coil. This thermostat shall be of a graduated action type to the approval of the engineer. In the suction line to the washer pump is to be provided an automatic combined ejector water heater and diaphragm valve to which a steam line is to be connected. In this steam line shall be placed a pressure reducing valve of the Mason Regulator Company's manufacture or equal by the steam contractor designed to maintain a pressure of 5 pounds per square inch on the ejector if high pressure steam is used. The operation of the automatic ejector water heater shall be gradual. This water heater is to be operated by a diaphragm operated by air pressure and a constant temperature thermostat placed between the eliminators and the reheating coil. A globe valve is to be provided in the steam line within a few feet of the water heater by the heating contractor.

Provide a reverse acting diaphragm steam valve which is to be placed in the steam line to the water heater and operated through a safety relay. The valve and relay are to be so connected that should either the water pressure or the air pressure fail, the steam supply to the ejector water heater will be automatically shut off.

One (1)  $\frac{1}{8}$ -inch opening will be left in the air supply line of the thermostatic control system for supplying compressed air to the thermostat mentioned above. The humidity control shall be set and left in proper adjustment by the manufacturer.

One (1) Pot Strainer. For insertion in the line running from the centrifugal pump to spray header is to be provided a cast iron galvanized pot strainer with two baskets, one to be used as a spare. The baskets of this strainer are to be made of 14-mesh copper wire cloth screen, giving an area of at least sixteen times area of pipe connection. The top of this strainer is to be held by clamp and screw so it can be instantly and easily removed and replaced with clean strainer.

A ——— steam line is to be run to reverse acting diaphragm valve.

#### **GUARANTEES**

#### Apparatus

The apparatus is guaranteed to be first class with reference to both workmanship and design. Parts which may prove defective within one year after shipment are to be replaced without charge.

#### Fan

The fan shall be capable of handling — cu. ft. of air per minute at — degrees F. and 29.92 inches barometer, at approximately — inches static (or total) pressure, when running at a speed not to exceed — R. P. M.

The fan will require under above conditions not over — H. P. Heater

The free area through the coils shall be of such size that the velocity of the air in passing through them shall not exceed — feet per minute and of ample capacity to heat — cu. ft. of air per minute from — to — degrees F. using steam at — pounds pressure per square inch gauge.

## Engine

The engine shall be belted (or direct connected) to —— fan, and shall be capable of running at —— R. P. M. with steam pressure of —— pounds per square inch gauge, when fan is delivering —— cu. ft. A. P. M. against —— in. static (or total) pressure.

### Heating

The apparatus is to be of sufficient capacity to heat the building to —— degrees F. when outside temperature is — degrees F., using —— per cent. return air— and —per cent. fresh air, and to give a — minute air change.

## Ventilating

The apparatus is to be of sufficient capacity to supply cu. ft. air per minute; (or in case of school, —— cu. ft. air per minute per pupil,) at —— degrees F. and 29.92 inches barometer. **Ducts and Outlets** 

The velocity shall not exceed: in the mains —— feet per minute; in the risers —— feet per minute.

The air shall enter the room — at not less than — feet from the floor, at a velocity not to exceed — feet per minute.

The vent shall be of the size of the inlet and shall be taken off at the floor line where practicable.

#### Air Washing

The washer is to remove 98 per cent. of the solid material carried by the entering air.

## **Humidity Control**

The apparatus is to automatically control the dew-point temperature within one degree of that desired, when the outside wet-bulb temperature is less than the dew-point for which the control is set.

## Cooling With Air Washer

The apparatus when recirculating water in summer and handling rated capacity of air, is to reduce the temperature of the air 70 per cent. of the entering wet-bulb depression (i. e., 70 per cent. of the difference between the dry and wet-bulb temperatures) of the incoming air.

The apparatus when using cold water in summer is to reduce the outgoing difference of air and water temperatures to less than 25 per cent. of the difference in the incoming temperatures. Cooling With Humidifier

Cool to the wet-bulb temperature of the entering air.

## Mechanical Draft

The fan shall be used for (induced or forced) draft for—boilers burning — pounds coal per hour, having a heat value of — B. t. u. The fan shall be of sufficient capacity to handle cubic feet air per minute at — degrees F. and 29.92 inches barometer and maintain a — pressure of — inches of water at the grate, when revolving at a speed not to exceed — R. P. M.

The fan will require under above conditions not over —— H. P.

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## PLANOIDAL (TYPE L) FANS

SPECIFICATIONS FOR PLANOIDAL (TYPE L) FANS

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SPECIFICATIONS FOR NIAGADA CONDIDAL (TYPE

wheel and shaft, which may vary, depending on operating conditions.

## CHIMNEYS

The following rules for the design of chimneys are given in "Steam," published by the Babcock & Wilcox Company.

(a)—To find the draft in inches of water produced by a given chimney. Divide 7.6 by the absolute temperature of the external air  $(t_a + 460)$ ; divide 7.9 by the absolute temperature of the gases in the chimney  $(t_g + 460)$ ; subtract the latter from the former, and multiply the remainder by the height of the chimney in feet. This may be expressed as

$$d = h \left( \frac{7.6}{t_a + 460} - \frac{7.9}{t_g + 460} \right)$$

(b)—To find the height of a chimney to give a specified draft expressed in inches of water: Proceed as above through the first two steps, then divide the required draft by the remainder, and the result will be the height of the chimney in feet. Expressed as a formula,

$$h = \frac{d}{\left(\frac{7.6}{t_a + 460}\right) - \left(\frac{7.9}{t_g + 460}\right)}$$

The draft attainable with any chimney when the temperature of the external air is 70° F, and the temperature of the flue gases  $550^{\circ}$  F, multiply the height above the grate in feet by 0.0065 and the product is the draft pressure in inches of water.

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Actual	Square	1.77 2.41 3.14	$3.98 \\ 4.91 \\ 5.94$	$\begin{array}{c} 7.07 \\ 8.30 \\ 9.62 \end{array}$	12.57 15.90 19.64	23.76 28.27 33.18	$38.48 \\ 44.18 \\ 50.27$	56.75 63.62 70.88	78.54 86.59 95.03	103.86
Effective	Square	0.97 1.47 2.08	2.78 3.58 4.48	5.47 6.57 7.76	$10.44 \\ 13.51 \\ 16.98$	20.83 25.08 29.73	34.76 40.19 46.01	52.23 58.83 65.83	73.22 81.00 89.19	97.75 106.72
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						981 1181 1400	$1637 \\1893 \\2167$	2462 2773 3003	3452 3820 4205	4608 5031
	175 Ft. 200 Ft.				748	918 1105 1310	$1531 \\ 1770 \\ 2027$	$\frac{2303}{2594}$	3230 3573 3935	4311 4707
er	150 Ft.				551 692	849 1023 1212	1418 1639 1876	$2133 \\ 2402 \\ 2687 \\ $	2990 3308 3642	3991 4357
lorsepow	125 Ft.				389 503 632	776 934 1107	1294 1496 1720	$ \frac{1946}{2192} 2459 $		
Height of Chimneys and Commercial Horsepower	110 Ft.			271	365 472 593	728 876 1038	1214 1415 1616			
and Com	100 Ft.			182 219 258	348 449 565	694 835 995	1163 1344 1537			
iimneys a	90 Ft.		113 141	173 208 245	330 427 536	658 792				
ght of Ch	80 Ft.	63	83 107 133	163 196 231	311 363 505					
Hci	70 Ft.	58 58 88	78 100 125	152 183 216						
	60 Ft.	25 38 54	72 92 115	141						
	50 Ft.	828 564 40	13 75							
Diam.	Inches	855 857	27 30 33	36 39 42	48 54 60	66 72 78	86 96 96	102 114 114	120 132	138

CHIMNEYS

TABLE OF AREA AND CIRCUMFERENCE OF CIRCLES

Diameter	Ar	ea	Circumference	One Side of a
in Inches	Square Inches	Square Feet	in Feet	Square
1 2 3 4 5	.7854 3.140 7.070 12.57 19.63	.0054 .0218 .0491 .0873 .1364	$\begin{array}{r} .2618\\ .5236\\ .7854\\ 1.047\\ 1.309\end{array}$	$\begin{array}{r} .8862 \\ 1.7724 \\ 2.6587 \\ 3.4549 \\ 4.4311 \end{array}$
6 7 8 9 10	$\begin{array}{c} 28.27 \\ 38.48 \\ 50.27 \\ 63.62 \\ 78.54 \end{array}$.1964 .2673 .3491 .4418 .5454	$\begin{array}{c} 1.571 \\ 1.833 \\ 2.094 \\ 2.356 \\ 2.618 \end{array}$	$\begin{array}{c} 5.3174 \\ 6.2036 \\ 7.0898 \\ 7.9760 \\ 8.8623 \end{array}$
11 12 13 14 15	95.03 113.1 132.7 153.9 176.7	$\begin{array}{r} .6600\\ .7854\\ .9218\\ 1.069\\ 1.227\end{array}$	$\begin{array}{c} 2.880 \\ 3.142 \\ 3.403 \\ 3.665 \\ 3.927 \end{array}$	$\begin{array}{r} 9.7485\\ 10.6347\\ 11.5209\\ 12.4072\\ 13.2934\end{array}$
16 17 18 19 20	$\begin{array}{c} 201.0\\ 226.9\\ 254.4\\ 283.5\\ 314.1 \end{array}$	$\begin{array}{c} 1.396 \\ 1.576 \\ 1.767 \\ 1.969 \\ 2.182 \end{array}$	$\begin{array}{r} 4.189\\ 4.451\\ 4.712\\ 4.974\\ 5.236\end{array}$	$\begin{array}{c} 14.1796 \\ 15.0659 \\ 15.9521 \\ 16.8383 \\ 17.7245 \end{array}$
21 22 23 24 25	346.3380.1415.4452.3 2490.8	$2.405 \\ 2.640 \\ 2.885 \\ 3.142 \\ 3.409$	5.498 5.760 6.021 6.283 6.545	$\begin{array}{c} 18.6108 \\ 19.4910 \\ 20.3832 \\ 21.2694 \\ 22.1557 \end{array}$
26 27 28 29 30	530.9 572.5 615.7 660.5 706.8	3.687 3.976 4.276 4.587 4.909	$\begin{array}{c} 6.807 \\ 7.069 \\ 7.330 \\ 7.592 \\ 7.854 \end{array}$	$\begin{array}{r} 23.0419\\ 23.9281\\ 24.8144\\ 25.7006\\ 26.5868\end{array}$
31 32 33 34 35	754.7 804.2 855.3 907.9 962.1	$5.241 \\ 5.585 \\ 5.940 \\ 6.305 \\ 6.681$	8.116 8.378 8.639 8.901 9.163	$\begin{array}{c} 27.4730\\ 28.3594\\ 29.2455\\ 30.1317\\ 31.0179\end{array}$
36 37 38 39 40	$\begin{array}{c} 1017.8 \\ 1075.2 \\ 1134.1 \\ 1194.5 \\ 1256.6 \end{array}$	7.069 7.467 7.876 8.296 8.727	$\begin{array}{r} 9.425\\ 9.686\\ 9.948\\ 10.21\\ 10.47\end{array}$	$\begin{array}{c} 31.9042\\ 32.7904\\ 33.6766\\ 34.5628\\ 35.4491 \end{array}$
41 42 43 44 45	$1320.2 \\ 1385.4 \\ 1452.2 \\ 1520.5 \\ 1590.4$	$\begin{array}{r} 9.168\\ 9.621\\ 10.08\\ 10.56\\ 11.04\end{array}$	$10.73 \\ 10.99 \\ 11.26 \\ 11.52 \\ 11.78$	$\begin{array}{r} 36.3353\\ 37.2215\\ 38.1078\\ 38.9444\\ 39.8802 \end{array}$
46 47 48 49 50	1661.9 1734.9 1809.5 1885.7 1963.5	$11.54 \\ 12.05 \\ 12.51 \\ 13.09 \\ 13.64$	$12.04 \\ 12.30 \\ 12.57 \\ 12.83 \\ 13.09$	$\begin{array}{r} 40.7664\\ 41.6527\\ 42.5839\\ 43.4251\\ 44.3113\end{array}$

TABLE OF AREA AND CIRCUMFERENCE OF CIRCLES

Diameter in	Are	ea	Circumference	One Side of a
Inches	Square Inches	Square Feet	in Feet	Square
51 52 53 54 55	$2043 \\ 2124 \\ 2206 \\ 2290 \\ 2376$	$14.19 \\ 14.75 \\ 15.32 \\ 15.90 \\ 16.50$	$13.35 \\ 13.61 \\ 13.88 \\ 14.14 \\ 14.40$	$\begin{array}{r} 45.9760\\ 46.0838\\ 46.9700\\ 47.8562\\ 48.7425\end{array}$
56 57 58 59 60	2463 2552 2642 2734 2827	17.10 17.72 18.35 18.99 19.63	$\begin{array}{c} 14.66\\ 14.92\\ 15.18\\ 15.45\\ 15.71\end{array}$	$\begin{array}{r} 49.6287\\ 50.5149\\ 51.4012\\ 52.2874\\ 53.1736\end{array}$
61 62 63 64 65	2922 3019 3117 3217 3318	$\begin{array}{c} 20.29 \\ 20.97 \\ 21.65 \\ 22.34 \\ 23.04 \end{array}$	$\begin{array}{c} 15.97 \\ 16.23 \\ 16.49 \\ 16.76 \\ 17.02 \end{array}$	$\begin{array}{c} 54.0598\\ 54.9061\\ 55.8323\\ 56.7185\\ 57.6047\end{array}$
66 67 68 69 70	3421 3526 3632 3739 3848	$\begin{array}{c} 23.76 \\ 24.48 \\ 25.22 \\ 25.97 \\ 26.73 \end{array}$	$17.28 \\ 17.54 \\ 17.80 \\ 18.06 \\ 18.33$	$\begin{array}{c} 58.4910 \\ 59.3772 \\ 60.2634 \\ 61.1497 \\ 62.0359 \end{array}$
71 72 73 74 75	$\begin{array}{c} 3959 \\ 4072 \\ 4185 \\ 4301 \\ 4418 \end{array}$	$\begin{array}{c} 27.49 \\ 28.27 \\ 29.07 \\ 29.87 \\ 30.68 \end{array}$	$18.59 \\18.85 \\19.11 \\19.37 \\19.63$	$\begin{array}{c} 62.9221 \\ 63.8083 \\ 64.9946 \\ 65.5808 \\ 66.4670 \end{array}$
76 77 78 79 80	4536 4657 4778 4902 5027	31.50 32.34 33.18 34.04 34.91	$19.90 \\ 20.16 \\ 20.42 \\ 20.68 \\ 20.94$	$\begin{array}{c} 67.3500\\ 68.4800\\ 69.1500\\ 70.0290\\ 70.8950\end{array}$
81 82 83 84 85	$5153 \\ 5281 - 5411 \\ 5542 \\ 5675$	35.78 36.67 37.57 38.48 39.41	$21.21 \\ 21.47 \\ 21.73 \\ 21.99 \\ 22.25$	$\begin{array}{c} 71.8000 \\ 73.3500 \\ 73.5540 \\ 74.4460 \\ 75.4785 \end{array}$
86 87 88 89 90	$5809 \\ 5945 \\ 6082 \\ 6221 \\ 6362$	40.34 41.28 42.24 43.20 44.18	$\begin{array}{c} 22.51 \\ 22.78 \\ 23.04 \\ 23.30 \\ 23.56 \end{array}$	$\begin{array}{c} 76.2170 \\ 77.1038 \\ 77.9871 \\ 78.8733 \\ 79.7621 \end{array}$
91 92 93 94 95	6504 6648 6793 6940 7088	$\begin{array}{r} 45.17\\ 46.16\\ 47.17\\ 48.19\\ 49.22\end{array}$	$\begin{array}{c} 23.82 \\ 24.09 \\ 24.35 \\ 24.61 \\ 24.87 \end{array}$	$\begin{array}{c} 80.6473 \\ 81.5389 \\ 82.4196 \\ 83.3060 \\ 84.1902 \end{array}$
96 97 98 99 100	7238 7390 7543 7698 7855	$50.27 \\ 51.32 \\ 52.38 \\ 53.46 \\ 54.54$	$\begin{array}{c} 25.13\\ 25.39\\ 25.66\\ 25.92\\ 26.18\end{array}$	85.0760 85.9650 86.8500 87.7380 88.6280

Below $+32$ $+14$ -4 -22 -40 -58 -76 -94 $\vec{0.1}$ $\vec{0.1}$ 32 50 68 86 104 122 140 158 $\vec{0.1}$ 232 590 688 866 104 122 140 158 $\vec{3.23}$ 300 572 590 698 248 806 874 842 800 878 $\vec{3.33}$ 300 572 590 968 1004 122 130 338 $\vec{3.44}$ 600 1112 1130 1148 1100 1288 1900 1292 1310 1288 1202 1290 1384 1202 1290 1388 1200 1298 1386 1202 1290 1288 1200 1298 1386 1200 1298 1386 1202 1290 1298 1296 1290		Deg. Cent.	•	2	30	Deg	40 40 rees Fah	Degrees Centigrade= C. 1 40 50 0 Degrees Fahrenheit= F.	Е. 60 	20	80	
Above 32 50 68 104 122 140 158 100 392 410 458 246 284 302 338 200 392 410 458 446 462 500 518 200 372 590 458 446 462 500 518 300 772 770 788 806 824 462 500 518 400 772 770 788 806 1034 1022 1040 158 700 1122 1130 1148 1106 1184 1202 1200 1388 900 1122 1130 1388 1506 1384 1592 1700 1388 900 1652 1670 1688 1886 1904 1922 1700 1778 900 1652 1670 1688 1896 1904 1958 1760 1778	F.= C.	Below 0	+32	+ 14	4	- 22	- 40	1 58	- 76	- 94		
100 212 230 248 266 284 302 320 338 200 572 540 644 662 630 338 400 752 770 788 806 824 842 800 538 500 932 950 968 986 1004 1022 1040 1058 500 1112 1130 1148 1106 1328 1904 1033 700 1222 1340 1328 1544 1502 1204 1058 700 1222 1340 1388 1904 1933 1238 700 1322 1540 1384 1302 1340 1388 900 1652 1670 1888 1904 1952 1760 1778 11000 1833 1846 1904 1922 1940 1958 11000 2012 2030 2038 2046 2064	$0.56 \\ 1.11 \\ 1.67 \\ $	Above 0	32	50	68	86	104	122	140	158	176	
400 752 770 788 806 824 842 860 878 600 1113 1146 1064 1004 1022 1040 1058 700 1472 1130 1148 1166 1184 1202 1240 1368 700 1472 1670 1328 1346 1364 1382 1400 1368 700 1652 1670 1838 1706 1774 1742 1408 900 1652 1670 1888 1904 1922 1940 1598 1100 1833 1856 1846 2064 2932 1393 1742 1742 1760 1778 1100 2012 2030 2044 2084 2044 2160 2138 1200 2012 2030 2046 2044 2362 2303 2318 1300 2022 2304 2382 2462 2494 2493	 $2.22 \\ 2.78 \\ 3.33 \\ 3.33 \\ 3.32 \\ 3.22 \\ 3.33 \\ $	100 200 300	212 392 572	230 410 590	24 8 428 608	266 446 626	284 464 644	302 482 662	320 500 680	338 518 698	356 536 716	
700 1292 1310 1328 1346 1382 1400 1418 800 1472 1490 1508 1526 1544 1562 1500 1778 900 1652 1670 1688 1706 1744 1562 1760 1778 1000 1833 1856 1888 1904 1922 1940 1778 1000 1833 1856 1886 1904 1922 1940 1778 1000 1833 1856 2066 2084 2102 2136 1200 2192 2210 22246 2944 2462 2490 2188 1300 2372 2390 2408 2946 2944 2642 2493 2318 1300 2372 2570 2588 2606 3624 2642 2493 2793 1300 2732 2750 2588 2606 2644 2622 2490 2768	 3.89 4.44 5.00	400 500 600	752 932 1112	$\begin{array}{c} 770\\950\\1130\end{array}$	$ \begin{array}{c} 788 \\ 968 \\ 1148 \end{array} $	$ \begin{array}{c} 806 \\ 986 \\ 1166 \end{array} $	824 1004 1184	$842 \\ 1022 \\ 1202 \\ 1$	860 1040 1220	878 1058 1238	896 1076 1256	
1000 1832 1850 1808 1904 1922 1940 1958 1100 2012 2030 2048 2066 2084 2020 2138 1200 2012 2030 2048 2066 2084 2120 2138 1200 2012 2030 2264 2264 2282 2300 2318 1300 2372 2390 2486 2444 2462 2496 2188 1300 25572 2570 2568 2064 2642 2496 2498 1500 25532 2570 2568 2064 2642 2600 2078 1500 2753 2750 2583 2766 2642 2490 2678	 5.56 6.11 6.67	700 800 900	$1292 \\ 1472 \\ 1652 \\ 1652 \\ 1$	1310 1490 1670	$ \begin{array}{c} 1328 \\ 1508 \\ 1688 \\ 1688 \\ \end{array} $	$\frac{1346}{1526}$	$1364 \\ 1544 \\ 1724$	$1382 \\ 1562 \\ 1742$	$1400 \\ 1580 \\ 1760$	1418 1598 1778	1436 1616 1796	
1300 2372 2390 2408 2426 2444 2462 2490 2498 1400 2552 2570 2588 2606 2642 2462 2498 1400 2552 2570 2588 2606 2642 2640 2788 1500 2732 2776 2786 2804 2822 2840 2858	7.22 7.78 8.33	1000 1100 1200	1832 2012 2192	1850 2030 2210 2210	$ \begin{array}{c} 1868 \\ 2048 \\ 2228 \\ \end{array} $	1886 2066 2246	$1904 \\ 2084 \\ 2264$	$1922 \\ 2102 \\ 2282 \\ 2282 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ $	$ \begin{array}{c} 1940 \\ 2120 \\ 2300 \\ \end{array} $	$\frac{1958}{2138}$ 2318	1976 2156 2336	
	 8.89 9.44 10.00	1300 1400 1500	2372 2552 2732	2390 2570 2750	2408 2588 2768	2426 2606 2786	$2444 \\ 2624 \\ 2804$	$2462 \\ 2642 \\ 2822 \\ 2822 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \\$	2480 2660 2840	2498 2678 2858	2516 2696 2876	

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FAN ENGINEERING-BUFFALO FORGE COMPANY

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PRESSURE IN INCHES OF MERCURY EXPRESSED IN EQUIVALENT POUNDS PER SQUARE INCH

In.	.0 .	.1	.2	.3	.4	.5	.6	.7	.8	.9
0 1 2	$0.00 \\ 0.49 \\ 0.98$	$0.05 \\ 0.54 \\ 1.03$	$0.10 \\ 0.59 \\ 1.08$	$0.15 \\ 0.64 \\ 1.13$	$0.20 \\ 0.69 \\ 1.18$	$0.25 \\ 0.74 \\ 1.23$	0.29 0.79 1.28	0.34 0.84 1.33	0.39 0.88 1.38	$0.44 \\ 0.93 \\ 1.42$
3 4 5	$1.47 \\ 1.96 \\ 2.46$	$1.52 \\ 2.01 \\ 2.51$	$1.57 \\ 2.06 \\ 2.55$	$1.62 \\ 2.11 \\ 2.60$	$1.67 \\ 2.16 \\ 2.65$	$1.72 \\ 2.21 \\ 2.70$	$1.77 \\ 2.26 \\ 2.75$	$1.82 \\ 2.31 \\ 2.80$	$1.87 \\ 2.36 \\ 2.85$	1.91 2.41 2.90
6 7 8	$2.95 \\ 3.44 \\ 3.93$	$3.00 \\ 3.49 \\ 3.98$	$3.05 \\ 3.54 \\ 4.03$	$3.09 \\ 3.59 \\ 4.08$	$3.14 \\ 3.63 \\ 4.13$	$3.19 \\ 3.68 \\ 4.18$	$3.24 \\ 3.73 \\ 4.22$	3.29 3.78 4.27	3.34 3.83 4.32	3.39 3.88 4.37
9 10 11	$4.42 \\ 4.91 \\ 5.40$	$4.47 \\ 4.96 \\ 5.45$	$4.52 \\ 5.01 \\ 5.50$	$4.57 \\ 5.06 \\ 5.55$	$4.62 \\ 5.11 \\ 5.60$	$4.67 \\ 5.16 \\ 5.65$	$4.72 \\ 5.21 \\ 5.70$	$4.76 \\ 5.26 \\ 5.75$	$4.81 \\ 5.30 \\ 5.80$	$4.86 \\ 5.35 \\ 5.85$
12 13 14	$5.89 \\ 6.39 \\ 6.88$	$5.94 \\ 6.43 \\ 6.93$	$5.99 \\ 6.48 \\ 6.97$	$\begin{array}{c} 6.04 \\ 6.53 \\ 7.02 \end{array}$	$6.09 \\ 6.58 \\ 7.07$	$ \begin{array}{r} 6.14 \\ 6.63 \\ 7.12 \end{array} $	$6.19 \\ 6.68 \\ 7.17$	6.24 6.73 7.22	6.29 6.78 7.27	$6.34 \\ 6.83 \\ 7.32$
15 16 17	$7.37 \\ 7.86 \\ 8.35$	$7.42 \\ 7.91 \\ 8.40$	$7.47 \\ 7.96 \\ 8.45$	7.52 8.01 8.50	7.56 8.06 8.55	$7.61 \\ 8.10 \\ 8.60$	$7.66 \\ 8.15 \\ 8.64$	7.71 8.20 8.69	7.76 8.25 8.74	7.81 8.30 8.79
18 19 20	8.84 9.33 9.82	8.89 9.38 9.87	8.94 9.43 9.92	8.99 9.48 9.97	$9.04 \\ 9.53 \\ 10.02$	9.09 9.58 10.07	9.14 9.63 10.12		9.23 9.73 10.22	9.28 9.77 10.27
21 22 23	$10.32 \\ 10.81 \\ 11.30$	$10.37 \\ 10.86 \\ 11.35$	$10.41 \\ 10.90 \\ 11.40$	10.46 10.95 11.44	$10.51 \\ 11.00 \\ 11.49$	$10.56 \\ 11.05 \\ 11.54$	$10.61 \\ 11.10 \\ 11.59$	11.15	$10.71 \\ 11.20 \\ 11.69$	$10.76 \\ 11.25 \\ 11.74$
24 25 26	$11.79 \\ 12.28 \\ 12.77$	$\frac{11.84}{12.33}\\12.82$	$11.89\\12.38\\12.87$	$11.94 \\ 12.43 \\ 12.92$	11.99 12.48 12.97	$12.03 \\ 12.53 \\ 13.02$	$12.08 \\ 12.57 \\ 13.07$	$\begin{array}{c} 12.13 \\ 12.62 \\ 13.11 \end{array}$	$\begin{array}{c} 12.18 \\ 12.67 \\ 13.16 \end{array}$	$\frac{12.23}{12.72}\\13.21$
27 28 29 30	$\begin{array}{c} 13.26 \\ 13.75 \\ 14.24 \\ 14.74 \end{array}$	$\begin{array}{c} 13.31 \\ 13.80 \\ 14.29 \\ 14.78 \end{array}$	$13.36 \\ 13.85 \\ 14.34 \\ 14.83$	$13.41 \\ 13.90 \\ 14.39 \\ 14.88$	$13.46 \\ 13.95 \\ 14.44 \\ 14.93$	14.00	$13.56 \\ 14.05 \\ 14.54 \\ 15.03$	$14.10\\14.59$	$13.66 \\ 14.15 \\ 14.64 \\ 15.13$	$13.70 \\ 14.20 \\ 14.69 \\ 15.18$

FAN ENGINEERING-BUFFALO FORGE COMPANY

SIZE OF STEAM PIPES 100-Foot Length

ur			0 Lb	S.					5 L	.bs.		
Steam per Hour				Velocit	ty of S	team ii	ı Ft. p	er Mir	ute			
Steam	600	00	90	00	120	000	60	00	9	000	12	2000
Lbs. 3	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.
200 400 600	$\frac{2''}{2\frac{1}{2}''}{3''}$	$2.1 \\ 4.2 \\ 6.3$	$\frac{1\frac{1}{2}''}{2_{12}''}$	$1.40 \\ 2.81 \\ 4.21$	$\frac{1\frac{1}{4}''}{1\frac{1}{2}''}{2''}$	$1.05 \\ 2.10 \\ 3.16$	$\frac{12''}{2''}$ $\frac{21}{2}''$	$1.6 \\ 3.2 \\ 4.8$	$\frac{1\frac{1}{2}''}{2''}$	1.07 2.14 3.20	${1'' \over 1{1\over 2}'' \over 2''}$	$0.8 \\ 1.6 \\ 2.4$
800 1000 1200	$3\frac{1''}{3\frac{1}{2}''} \\ 4''$	$8.4 \\ 10.5 \\ 12.6$	$\frac{3''}{3''}{3\frac{1}{2}''}$	$5.61 \\ 7.03 \\ 8.40$	$\frac{2\frac{1}{2}''}{3''}{3''}$	$\begin{array}{c} 4.21 \\ 5.25 \\ 6.30 \end{array}$	$\begin{array}{c} 3'' \\ 3\frac{1}{2}'' \\ 3\frac{1}{2}'' \end{array}$	$ \begin{array}{r} 6.4 \\ 8.0 \\ 9.6 \end{array} $	$2\frac{1}{3''}$ 3'' 3''	$4.27 \\ 5.34 \\ 6.41$	$2''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21'''_{21''''_{21''''_{21''''_{21''''_{21'''''_{21''''''''''$	$3.2 \\ 4.0 \\ 4.8$
1400 1600 1800	$4\frac{1}{2}'' 5'' 5''$	$14.8 \\ 16.9 \\ 19.0$	$3\frac{1}{2}'' \\ 4'' \\ 4''$	$\begin{array}{c} 9.80 \\ 11.22 \\ 12.62 \end{array}$	$3\frac{1''}{3\frac{1}{2}}''$ $3\frac{1}{2}$ ''' $3\frac{1}{2}$ '''	$7.40 \\ 8.45 \\ 9.50$	$\begin{array}{c} 4'' \\ 4'' \\ 4\frac{1}{2}'' \end{array}$	$11.2 \\ 12.8 \\ 14.4$	$3^{1''}_{22}_{32}_{32}_{32}_{32}_{32}_{32}_{32$	$7.48 \\ 8.55 \\ 9.62$	3″ 3″ 3″	5.6 6.4 7.2
2000 2200 2400	${6'' \atop 6'' \\ 6''}$	$21.1 \\ 23.2 \\ 25.3$	4½" 4½" 5″	$14.0 \\ 15.4 \\ 16.8$	4" 4" 4"	$10.5 \\ 11.6 \\ 12.6$	41″ 5″ 5″	$16.0 \\ 17.6 \\ 18.2$	4" 4" 4"	$10.7 \\ 11.7 \\ 12.8$	31/" 31/2" 321/2	8.0 8.8 9.1
2600 2800 3000	6″ 7″ 7″	$27.4 \\ 29.5 \\ 31.6$	5″ 5″ 6″	$18.2 \\ 19.6 \\ 21.1$	$\begin{array}{c} 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \end{array}$	$13.7 \\ 14.7 \\ 15.8$	$5'' \\ 6'' \\ 6''$	$20.8 \\ 22.4 \\ 24.0$	$\begin{array}{c} 4\frac{1}{2}'' \\ 4\frac{1}{2} \\ 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \end{array}$	$13.9 \\ 14.9 \\ 16.0$	4" 4" 4"	$10.4 \\ 11.2 \\ 12.0$
3200 3400 3600	7″ 7″ 7″	33.7 35.8 37.9	6" 6" 6"	$22.4 \\ 23.9 \\ 25.3$	5″ 5″ 5″	16.8 17.9 18.9	6" 6" 6"	25.6 27.2 28.8	5″ 5″ 5″	$17.1 \\ 18.2 \\ 19.3$	$\begin{array}{c} 4'' \\ 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \end{array}$	$12.8 \\ 13.6 \\ 14.4$
3800 4000 4200	8″ 8″ 8″	$\begin{array}{c} 40.1 \\ 42.2 \\ 44.3 \end{array}$	6″ 6″ 7″	$26.7 \\ 28.1 \\ 29.5$	5" 6" 6"	$20.0 \\ 21.1 \\ 22.1$	7" 7" 7"	$30.4 \\ 32.0 \\ 33.6$	6" 6" 6"	$20.3 \\ 21.4 \\ 22.5$	$4\frac{1}{2}''$ $4\frac{1}{2}''$ 5'''	$15.2 \\ 16.0 \\ 16.8$
4400 4600 4800	8″ 8″ 8″	$46.4 \\ 48.5 \\ 50.6$	7″ 7″ 7″	30.9 32.3 33.7	6" 6" 6"	$23.2 \\ 24.2 \\ 25.3$	7" 7" 7"	$35.2 \\ 36.8 \\ 38.4$		$23.5 \\ 24.6 \\ 25.7$	5″ 5″ 5″	$17.6 \\ 18.4 \\ 19.2$
5000 5500 6000	9″ 9″ 9″	$52.7 \\ 58.0 \\ 63.2$	7″ 7″ 8″	$35.1 \\ 38.6 \\ 42.1$	6" 7" 7"	$26.3 \\ 29.0 \\ 31.6$	8" 8" 8"	$40.0 \\ 44.0 \\ 48.0$	6″ 6″ 7″	$26.7 \\ 29.4 \\ 32.0$	$5'' \\ 6'' \\ 6''$	$20.0 \\ 22.0 \\ 24.0$
6500 7000 7500	10" 10" 10"	68.5 73.6 79.0	8" 8" 9"	$45.6 \\ 49.1 \\ 52.6$	7" 7" 7"	$34.2 \\ 36.8 \\ 38.5$	8″ 9″ 9″	$52.0 \\ 56.0 \\ 60.0$	7″ 7″ 8″	$34.7 \\ 37.4 \\ 40.0$	6″ 6″ 7″	$26.0 \\ 28.0 \\ 30.0$
8000 8500 9000	$12'' \\ 12'' \\ 12''$	84.2 89.5 94.7	9″ 9″ 9″	$56.1 \\ 59.6 \\ 63.2$	8" 8" 8"	$42.1 \\ 44.7 \\ 47.3$	9" 10" 10"	64.0 68.0 72.0	8" 8" 8"	$\begin{array}{r} 42.7 \\ 45.4 \\ 48.0 \end{array}$	7″ 7″ 7″	32.0 34.0 36.0
9500 10000	12" 12"	100.0 105.3	10″ 10″	66.7 70.2	8″ 9″	$\begin{array}{c} 50.0\\ 52.6\end{array}$	10″ 10″	76.0 80.0	8″ 9″	50. 7 53.4	7″ 8″	38.0 40.0

SIZE OF STEAM PIPES

100-Foot Length

			20 Lb	S.					40 I	.bs.		
er Hour				Velocit	y of S	team in	Ft. p	er Min	ute			
Lbs. Steam per Hour	6(000	9(000	12	000	60	000	9(000	120	000
Lbs. 5	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.
200 400 600	$\frac{14''}{12''}$ 2''	$0.94 \\ 1.87 \\ 2.81$	$\frac{1''}{1\frac{1}{4}''}\\1\frac{1}{2}''$	$0.62 \\ 1.25 \\ 1.87$	$\frac{1''}{1\frac{1''}{4}}\\1\frac{1}{2}''$	$0.47 \\ 0.93 \\ 1.41$	$\frac{1''}{\frac{1}{4''}}{\frac{1}{2''}}$	$0.61 \\ 1.22 \\ 1.84$	$\frac{1''}{1\frac{1}{4}''}\\\frac{1}{2}''$	$0.41 \\ 0.82 \\ 1.23$	1" 1" 1 <u>4</u> "	$\begin{array}{c} 0.30 \\ 0.61 \\ 0.92 \end{array}$
800 1000 1200	$2\frac{1}{2}''$ $2\frac{1}{2}''$ 3''	$3.75 \\ 4.68 \\ 5.61$	$\frac{2''}{2''_{\frac{1}{2}''}}$	$2.50 \\ 3.12 \\ 3.76$	${1 \frac{1}{2}'' \atop 2'' \\ 2'' \end{cases}$	$1.87 \\ 2.34 \\ 2.80$	$2''_{2''_{2^{1}}}$	$2.45 \\ 3.07 \\ 3.68$	${1 \frac{1}{2}'' \over 2'' \\ 2'' \\ 2''$	$1.64 \\ 2.04 \\ 2.45$	$\begin{array}{c} 1\frac{1''}{4}\\ 1\frac{1''}{2}\\ 1\frac{1}{2}'' \end{array}$	$1.22 \\ 1.53 \\ 1.84$
1400 1600 1800	$3''_{3\frac{1}{2}''}_{3\frac{1}{2}''}$	$\begin{array}{c} 6.57 \\ 7.49 \\ 8.42 \end{array}$	$2\frac{1}{2}$ $2\frac{1}{2}$ 3"	$4.37 \\ 5.00 \\ 5.63$	$2''_{2\frac{1}{2}''}_{2\frac{1}{2}''}$	$3.28 \\ 3.74 \\ 4.21$	$2\frac{1}{2}''$ $2\frac{1}{2}'''$ 3'''	$4.28 \\ 4.89 \\ 5.50$	$2''_{2''_{2}}$	$2.86 \\ 3.27 \\ 3.68$	2" 2" 2"	$2.14 \\ 2.44 \\ 2.75$
2000 2200 2400	$3\frac{1}{2}''$ 4''' 4''	$9.36 \\ 10.30 \\ 11.22$	$\frac{3''}{3''}{3\frac{1}{2}''}$	$\begin{array}{c} 6.25 \\ 6.88 \\ 7.50 \end{array}$	$\frac{21''}{3''}$	$4.68 \\ 5.15 \\ 5.61$	$\frac{3''}{3''}{3\frac{1}{2}''}$	$\begin{array}{c} 6.12 \\ 6.74 \\ 7.35 \end{array}$	$\begin{array}{c} 2\frac{1''}{2\frac{1}{2}''}\\ 2\frac{1}{2}''\\ 2\frac{1}{2}'' \end{array}$	$4.09 \\ 4.50 \\ 4.90$	$2''_{2\frac{1}{2}''_{2\frac{1}{2}''}}$	$3.06 \\ 3.38 \\ 3.67$
2600 2800 3000	$\begin{array}{c} 4'' \\ 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \end{array}$	$12.18 \\ 13.10 \\ 14.05$	$3\frac{1''}{3\frac{1}{2}}''$ $3\frac{1}{2}''$	$8.13 \\ 8.75 \\ 9.38$	3″ 3″ 3″	$\begin{array}{c} 6.09 \\ 6.55 \\ 7.02 \end{array}$	$31''_{31'''_{31'''_{31'''_{31'''_{31'''_{31'''_{31'''_{31'''_{31''''_{31''''_{31'''''_{31'''''_{31'''''''_{31''''''''''$	7.96 8.58 9.18	3″ 3″ 3″	$5.32 \\ 5.73 \\ 6.14$	$2\frac{1}{2}$	$3.98 \\ 4.29 \\ 4.59$
3200 3400 3600	$4\frac{1''}{4\frac{1}{2}''}$ 5'''	$15.00 \\ 15.95 \\ 16.82$	31″ 4″ 4″	$\begin{array}{c} 10.00 \\ 10.62 \\ 11.25 \end{array}$	$3\frac{1''}{3\frac{1''}{2}}$ $3\frac{1''}{2}$	$7.50 \\ 7.98 \\ 8.41$	$3\frac{1}{2}'' \\ 4'' \\ 4''$	9.80 10.41 11.04	$3'' \\ 3'' \\ 3^{1}_{2}''$	$\begin{array}{c} 6.54 \\ 6.95 \\ 7.35 \end{array}$	$\frac{21''}{3''}$	$4.90 \\ 5.20 \\ 5.52$
3800 4000 4200	5″ 5″ 5″	17.78 18.75 19.70	$\begin{array}{c} 4'' \\ 4'' \\ 4\frac{1}{2}'' \end{array}$	$\begin{array}{c} 11.85 \\ 12.50 \\ 13.20 \end{array}$	$3\frac{1''}{3\frac{1}{2}}''$ $3\frac{1}{2}''$	8.89 9.37 9.85	4" 4" 4"	$11.64 \\ 12.25 \\ 12.87$	$3\frac{1}{2}$ $3\frac{1}{2}$ $3\frac{1}{2}$	$7.77 \\ 8.18 \\ 8.60$	3″ 3″ 3″	$5.82 \\ 6.12 \\ 6.43$
4400 4600 4800	6" 6" 6"	$20.60 \\ 21.60 \\ 22.50$	41" 41" 41" 41"	$13.75 \\ 14.35 \\ 15.00$	4" 4" 4"	$10.30 \\ 10.80 \\ 11.25$	4 <u>1</u> " 4 <u>1</u> " 4 <u>1</u> " 4 <u>1</u> "	$13.48 \\ 14.10 \\ 14.70$	31/2 31/2 31/2 32/2	9.00 9.40 9.80	$\frac{3''}{3''_{2}}$	$\begin{array}{c} 6.74 \\ 7.05 \\ 7.35 \end{array}$
5000 5500 6000	6" 6" 6"	$23.40 \\ 26.80 \\ 28.10$	41″ 5″ 5″	$15.60 \\ 17.15 \\ 18.70$	4″ 5″ 5″	$11.70 \\ 13.40 \\ 14.10$	$4\frac{1}{2}''$ 5" 5"	$15.31 \\ 16.80 \\ 18.40$	4" 4" 4"	$10.20 \\ 11.20 \\ 12.30$	$3\frac{1}{2}^{''}$ $3\frac{1}{2}^{''}$ $3\frac{1}{2}^{''}$	$7.66 \\ 8.40 \\ 9.20$
6500 7000 7500	7″ 7″ 7″	$30.50 \\ 32.80 \\ 35.20$	5″ 6″ 6″	$20.30 \\ 21.80 \\ 23.40$	5″ 5″ 5″	$15.20 \\ 16.40 \\ 17.60$	$5'' \\ 6'' \\ 6''$	$19.80 \\ 21.40 \\ 23.00$	$4\frac{12''}{4\frac{12''}{4\frac{12''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12'''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{2\frac{12'''''}{212''''''''''''''''''''''''''''''''''$	$13.30 \\ 14.30 \\ 15.30$	31″ 4″ 4″	9.90 10.70 11.50
8000 8500 9000	7″ 8″ 8″	$37.50 \\ 39.80 \\ 42.20$	6″ 6″ 6″	$24.90 \\ 26.50 \\ 28.00$	5″ 5″ 6″	$18.80 \\ 19.90 \\ 21.10$	6" 6" 6"	$24.50 \\ 26.00 \\ 27.60$	5″ 5″ 5″	$16.30 \\ 17.30 \\ 18.30$	4" 4 <u>1</u> " 4 <u>1</u> "	$12.20 \\ 13.00 \\ 13.80$
9500 10000	8″ 8″	$\begin{array}{c} 44.50\\ 46.80\end{array}$	7″′ 7″′	$29.60 \\ 31.20$	6″ 6″	$22.20 \\ 23.40$	7″ 7″	$29.10 \\ 30.70$	$5''_6''$	$19.40 \\ 20.40$	4 <u>1</u> " 4 <u>1</u> "	$14.60 \\ 15.30$

SIZE OF STEAM PIPES

100=Foot Length

Hour			60 I	.bs.					80	Lbs.		
er He			,	elocity	of Ste	eam in	Ft. pe	r Minu	te			
Steam per	60	00	90	00	120	000	60	00		9000	12	000
Lbs. St	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.
200 400 600	$\frac{1''}{1\frac{1''}{4}}\\\frac{1\frac{1''}{2}}{1\frac{1}{2}''}$	0.46 0.92 1.37	$\frac{1''}{1''}$ $1\frac{1}{4}''$	0.31 0.61 0.92	1" 1" 1"	$\begin{array}{c} 0.23 \\ 0.46 \\ 0.68 \end{array}$	1" 1" 1 <u>1</u> "	$0.37 \\ 0.73 \\ 1.10$	1" 1" 1"	$0.24 \\ 0.49 \\ 0.73$	1" 1" 1"	0.18 0.36 0.55
800 1000 1200	$\frac{1\frac{1}{2}''}{2''}$	$1.83 \\ 2.29 \\ 2.75$	${}^{1\frac{1}{4}''}_{1\frac{1}{2}''}_{1\frac{1}{2}''}$	$1.22 \\ 1.53 \\ 1.83$	$\frac{1\frac{1''}{4}}{1\frac{1}{4}''}$	$0.91 \\ 1.14 \\ 1.37$	$1\frac{1''}{1\frac{1}{2''}}$ 2''	$1.47 \\ 1.82 \\ 2.20$	$\frac{1}{4}''$ $\frac{1}{4}''$ $\frac{1}{2}''$	$\begin{array}{c} 0.98 \\ 1.23 \\ 1.47 \end{array}$	$\frac{1''}{1\frac{1}{4}''}\\\frac{1}{4}''$	$\begin{array}{c} 0.73 \\ 0.91 \\ 1.10 \end{array}$
1400 1600 1800	$2''_{2\frac{1}{2}''}_{2\frac{1}{2}''}$	$3.21 \\ 3.67 \\ 4.13$	2" 2" 2"	$2.14 \\ 2.44 \\ 2.75$	$\frac{1\frac{1}{2}''}{1\frac{1}{2}''}{2''}$	$1.60 \\ 1.83 \\ 2.06$	2" 2" 2"	$2.57 \\ 2.93 \\ 3.30$	$\frac{1\frac{1}{2}''}{2''}$	$1.71 \\ 1.96 \\ 2.21$	$\begin{array}{c} 1 \frac{1}{4}'' \\ 1 \frac{1}{2}'' \\ 1 \frac{1}{2}'' \\ 1 \frac{1}{2}'' \end{array}$	$1.28 \\ 1.46 \\ 1.65$
2000 2200 2400	$2\frac{1}{2}''$ $2\frac{1}{2}'''$ 3'''	$4.59 \\ 5.05 \\ 5.50$	$\begin{array}{c} 2'' \\ 2\frac{1}{2}'' \\ 2\frac{1}{2}'' \end{array}$	$3.15 \\ 3.36 \\ 3.67$	2" 2" 2"	$2.29 \\ 2.52 \\ 2.75$	$21''_{22''}_{22''}_{22''}$	$3.67 \\ 4.04 \\ 4.40$	2" 2" 2"	$2.46 \\ 2.70 \\ 2.94$	${11^{2''}\over 2''} 2''$	$1.83 \\ 2.02 \\ 2.20$
2600 2800 3000	3″ 3″ 3″	$5.96 \\ 6.43 \\ 6.88$	$2\frac{1}{2}''$ $2\frac{1}{2}''$ $2\frac{1}{2}''$	$3.97 \\ 4.28 \\ 4.58$	$\frac{2''}{2''_{2^{\frac{1}{2}''}}}$	$2.98 \\ 3.21 \\ 3.44$	$2\frac{1''}{2\frac{1}{2}''}$ 3''	$4.77 \\ 5.12 \\ 5.50$	$2''_{2\frac{1}{2}''}_{2\frac{1}{2}''}$	$3.19 \\ 3.43 \\ 3.68$	2" 2" 2"	$2.38 \\ 2.56 \\ 2.75$
3200 3400 3600	$3\frac{1}{2}''$ $3\frac{1}{2}'''$ $3\frac{1}{2}'''$	7.35 7.80 8.26	$2\frac{1}{2}''$ $2\frac{1}{2}'''$ 3'''	$4.89 \\ 5.19 \\ 5.50$	$2\frac{1}{2}''$ $2\frac{1}{2}'''$ $2\frac{1}{2}''$	$3.67 \\ 3.90 \\ 4.13$	3″ 3″ 3″	$5.88 \\ 6.22 \\ 6.60$	$2\frac{1''}{2\frac{1}{2}}$ $2\frac{1''}{2\frac{1}{2}}$	$3.92 \\ 4.17 \\ 4.42$	$\frac{2''}{2''_2}$	$2.94 \\ 3.11 \\ 3.30$
3800 4000 4200	$3\frac{1''}{3\frac{1}{2}''}$ $3\frac{1}{2}''$ $3\frac{1}{2}''$	$8.71 \\ 9.18 \\ 9.63$	3″ 3″ 3″	$5.80 \\ 6.11 \\ 6.42$	$2\frac{1''}{2\frac{1}{2}''}$ $2\frac{1}{2}''$ $2\frac{1}{2}''$	$4.35 \\ 4.59 \\ 4.81$	$3''_{3\frac{1}{2}''}_{3\frac{1}{2}''}$	6.98 7.33 7.70	$2\frac{1}{2}''$ $2\frac{1}{2}''$ $2\frac{1}{2}''$	$4.67 \\ 4.92 \\ 5.16$	$2\frac{1''}{2\frac{1}{2}}$ $2\frac{1}{2}$	$3.46 \\ 3.66 \\ 3.85$
4400 4600 4800	4" 4" 4"	$10.10 \\ 10.55 \\ 11.00$	$\frac{3''}{3''}{3\frac{1}{2}''}$	6.73 7.02 7.34	$2\frac{1}{2}''$ 3''' 3'''	$5.05 \\ 5.27 \\ 5.50$	$3\frac{1''}{3\frac{1}{2}''}$ $3\frac{1}{2}''$	$8.08 \\ 8.45 \\ 8.80$	3" 3" 3"	$5.40 \\ 5.65 \\ 5.90$	$21''_{22''}_{22''}_{21''}_{22''}$	$\begin{array}{c} 4.04 \\ 4.22 \\ 4.40 \end{array}$
5000 5500 6000	$4''_{4''_{4^{\frac{1}{2}''}}}$	$11.48 \\ 12.60 \\ 13.80$	$3\frac{1}{2}''$ $3\frac{1}{2}'''$ $3\frac{1}{2}'''$	$7.64 \\ 8.42 \\ 9.18$	3″ 3″ 3″	$5.74 \\ 6.30 \\ 6.90$	$3\frac{1}{2}'' \\ 4'' \\ 4''$	9.18 10.10 11.00	$\frac{3''}{3''}{3^{\frac{1}{2}''}}$	$\begin{array}{c} 6.15 \\ 6.76 \\ 7.39 \end{array}$	$rac{21''}{21''} \ 3''$	$\begin{array}{c} 4.59 \\ 5.05 \\ 5.50 \end{array}$
6500 7000 7500	$4\frac{1}{2}''$ $4\frac{1}{2}''$ 5''	$14.90 \\ 16.10 \\ 17.20$	4" 4" 4"	$9.95 \\ 10.70 \\ 11.50$	$3\frac{1''}{3\frac{1''}{3\frac{1}{2}''}}$	$7.45 \\ 8.10 \\ 8.60$	$\frac{4''}{4''}{4rac{1}{2}''}$	11.90 12.80 13.70	$3\frac{1''}{3\frac{1}{2}''}$ $3\frac{1}{2}''$	-8.00 8.60 9.23	3″ 3″ 3″	$5.95 \\ 6.40 \\ 6.85$
8000 8500 9000	5″ 5″ 6″	$18.30 \\ 19.50 \\ 20.60$	$\begin{array}{c} 4'' \\ 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \end{array}$	$12.30 \\ 13.00 \\ 13.80$	$3\frac{1''}{3\frac{1}{2}''}$ 4''	$9.15 \\ 9.75 \\ 10.30$	$\begin{array}{c} 4\frac{1}{2}'' \\ 4\frac{1}{2}'' \\ 5'' \end{array}$	$14.70 \\ 15.60 \\ 16.50$	${3\frac{1}{2}''\over 4''}{4''}$	$9.84 \\ 10.40 \\ 11.10$	$\frac{3\frac{1}{2}''}{3\frac{1}{2}''}{3\frac{1}{2}''}$	$7.35 \\ 7.80 \\ 8.25$
9500 10000	6″ 6″	$21.80 \\ 23.00$	$4\frac{1}{2}''$ $4\frac{1}{2}''$	14.50 15.30	4" 4"	10.90 11.50	5″ 5″	17.40 18.30	4" 4"	11.70 12.30	$\frac{3\frac{1}{2}''}{3\frac{1}{2}''}$	8.70 9.15

SIZE OF STEAM PIPES 100-Foot Length

lour			100 Lb	·S.	200 Lbs.									
per H			Ve	elocity of	Stea	m in I	² t. pe	er Min	ute					
Lbs. Steam per Hour	6	000	\$	000	Ľ	2000	6	000	9	000	1	12000		
Lbs.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.	D.	Sq. In.		
200 400 600	$\frac{1''}{1''}$ $\frac{1}{4}''$	$\begin{array}{c} 0.31 \\ 0.61 \\ 0.92 \end{array}$	1" 1" 1"	$0.20 \\ 0.41 \\ 0.61$	1" 1" 1"	$0.15 \\ 0.31 \\ 0.46$	1" 1" 1"	$0.17 \\ 0.34 \\ 0.51$	1" 1" 1"	$0.11 \\ 0.23 \\ 0.34$	1" 1" 1"	0.08 0.17 0.25		
800 1000 1200	$\frac{1 \frac{1''}{4}}{1 \frac{1''}{2}}$	$1.22 \\ 1.63 \\ 1.83$	$\begin{array}{c} 1'' \\ 1 \frac{1}{4}'' \\ 1 \frac{1}{4}'' \\ 1 \frac{1}{4}'' \end{array}$	$0.82 \\ 1.02 \\ 1.22$	1" 1" 1 <u>1</u> "	$0.61 \\ 0.76 \\ 0.92$	$\frac{1''}{\frac{1}{4}''}{\frac{1}{4}''}$	$0.68 \\ 0.85 \\ 1.02$	1" 1" 1"	$0.45 \\ 0.57 \\ 0.68$	1" 1" 1"	$0.34 \\ 0.42 \\ 0.51$		
1400 1600 1800	2" 2" 2"	$2.14 \\ 2.45 \\ 2.76$	$\frac{1\frac{1}{2}''}{1\frac{1}{2}''}$	$1.43 \\ 1.63 \\ 1.83$	1 1" 1 4" 1 4" 1 2"	$1.07 \\ 1.22 \\ 1.38$	$\begin{array}{c} 1 \frac{1}{4}'' \\ 1 \frac{1}{2}'' \\ 1 \frac{1}{2}'' \end{array}$	$1.19 \\ 1.36 \\ 1.53$	$\frac{1''}{1\frac{1''}{4}}\\1\frac{1}{4}''$	$0.79 \\ 0.91 \\ 1.02$	1" 1" 1"	0.59 0.68 0.76		
2000 2200 2400	$2''_{2\frac{1}{2}''}_{2\frac{1}{2}''}$	3.06 3.37 3.67	2" 2" 2"	$2.04 \\ 2.24 \\ 2.45$	$\begin{array}{c}1\frac{1}{2}''\\1\frac{1}{2}''\\1\frac{1}{2}''\end{array}$	$1.53 \\ 1.68 \\ 1.84$	$\frac{1}{2''}$ $\frac{1}{2''}$	$1.70 \\ 1.87 \\ 2.04$	$\frac{1\frac{1''}{4}}{1\frac{1''}{4}}$	$1.13 \\ 1.25 \\ 1.36$	$\frac{1\frac{1}{4}''}{1\frac{1}{4}''}{1\frac{1}{4}''}$	0.85 0.93 1.02		
2600 2800 3000	$21''_{21''}_{21''_{21''}}_{21''_{21''}}$	$3.98 \\ 4.28 \\ 4.59$	2" 2" 2"	$2.65 \\ 2.85 \\ 3.06$	2" 2" 2"	$1.99 \\ 2.14 \\ 2.29$	2" 2" 2"	$2.21 \\ 2.38 \\ 2.55$	$\frac{12''}{12''}$ $\frac{12''}{12''}$	$1.47 \\ 1.59 \\ 1.70$	$\frac{1\frac{1}{4}''}{1\frac{1}{4}''}$	1.10 1.19 1.27		
3200 3400 3600	21″ 3″ 3″	$4.90 \\ 5.20 \\ 5.52$	$\begin{array}{c} 2'' \\ 2\frac{1}{2}'' \\ 2\frac{1}{2}'' \end{array}$	$3.26 \\ 3.47 \\ 3.67$	2" 2" 2"	$2.45 \\ 2.60 \\ 2.76$	2" 2" 2"	$2.72 \\ 2.89 \\ 3.06$	$\frac{1\frac{1}{2}''}{2''}$	$1.81 \\ 1.93 \\ 2.04$	$\frac{1\frac{1}{2}''}{1\frac{1}{2}''}{1\frac{1}{2}''}$	$1.36 \\ 1.44 \\ 1.53$		
3800 4000 4200	3″ 3″ 3″	$5.82 \\ 6.13 \\ 6.44$	$2\frac{1}{2}''$ $2\frac{1}{2}''$ $2\frac{1}{2}''$	$3.88 \\ 4.08 \\ 4.29$	2" 2" 2"	$2.91 \\ 3.06 \\ 3.22$	$\frac{2''}{2\frac{1}{2}''}$	$3.23 \\ 3.40 \\ 3.57$	2" 2" 2"	$2.15 \\ 2.26 \\ 2.38$	$\frac{1\frac{1}{2}''}{1\frac{1}{2}''}\\1\frac{1}{2}''$	$1.61 \\ 1.70 \\ 1.78$		
4400 4600 4800	3″ 3″ 3½″	$ \begin{array}{r} 6.75 \\ 7.05 \\ 7.35 \end{array} $	$2\frac{1}{2}''$ $2\frac{1}{2}''$ $2\frac{1}{2}''$	$4.49 \\ 4.69 \\ 4.90$	$21''_{22''}_{22''}_{21''}_{21''}$	$3.37 \\ 3.52 \\ 3.67$	$2\frac{1}{2}''$ $2\frac{1}{2}''$ $2\frac{1}{2}''$	$3.74 \\ 3.91 \\ 4.08$	2" 2" 2"	$2.49 \\ 2.61 \\ 2.72$	$\frac{11''}{2''}{2''}{2''}$	$1.87 \\ 1.96 \\ 2.04$		
5000 5500 6000	31" 31?" 31?"	7.65 8.42 9.18	$2\frac{2}{2}''$ 3''' 3'''	$5.10 \\ 5.62 \\ 6.13$	$\frac{21''}{212}''$	$3.82 \\ 4.21 \\ 4.59$	$2\frac{1''}{2\frac{1}{2}}$ $2\frac{1}{2}$	$4.25 \\ 4.68 \\ 5.10$	$2''_{2''_{2}}$	$2.83 \\ 3.12 \\ 3.40$	2" 2" 2"	$2.12 \\ 2.34 \\ 2.55$		
6500 7000 7500	4" 4" 4"	$9.95 \\ 10.70 \\ 11.46$	$3'' 3'' 3^{\frac{1}{2}''}$	$\begin{array}{c} 6.64 \\ 7.15 \\ 7.66 \end{array}$	$\frac{21''}{3''}$	$4.97 \\ 5.35 \\ 5.73$	3" 3" 3"	$5.53 \\ 5.95 \\ 6.48$	$2\frac{1''}{2\frac{1}{2}}''_{2\frac{1}{2}}''_{2\frac{1}{2}}$	$3.68 \\ 3.97 \\ 4.25$	2" 2" 2"	$2.76 \\ 2.97 \\ 3.24$		
8000 8500 9000	4" 4½" 4½"	$12.22 \\ 13.00 \\ 13.75$	31″ 31″ 31″	8.17 8.68 9.19	3″ 3″ 3″	$\begin{array}{c} 6.11 \\ 6.50 \\ 6.87 \end{array}$	$\frac{3''}{3''}$	$\begin{array}{c} 6.80 \\ 7.22 \\ 7.65 \end{array}$	$\frac{21''}{21''}$ $\frac{21''}{21''}$	$4.53 \\ 4.82 \\ 5.10$	21" 21" 21"	$3.40 \\ 3.61 \\ 3.82$		
9500 10000	$4\frac{1}{2}''$ $4\frac{1}{2}''$	$\begin{array}{c} 14.50\\ 15.26 \end{array}$	$3\frac{1}{4''}$	$\begin{array}{c} 9.70\\10.20\end{array}$	$\frac{31''}{31''}$	7.25 7.63	$\frac{3\frac{1}{2}''}{3\frac{1}{2}''}$	$\frac{8.08}{8.50}$	3″ 3″	$\begin{array}{c} 5.38\\ 5.66\end{array}$	$\frac{2\frac{1}{2}''}{2\frac{1}{2}''}$	$4.04 \\ 4.25$		

1-2

Temp.	Approx. Gauge Press.	Density	Spec. Vol. Cu. Ft. per Lb.	Heat of Liquid	Latent Heat	Total Heat
212 215 219	$\begin{array}{c} 0 \\ 1 \\ 2 \end{array}$.03732 .03945 .04243	26.79 25.35 23.57	180.00 183.00 187.10	970.4 968.4 965.9	$1150.4 \\ 1151.5 \\ 1152.9$
222 224 227	3 4 5	.04477 .04640 .04892	$22.34 \\ 21.55 \\ 20.44$	$190.10 \\ 192.10 \\ 195.20$	$963.9 \\ 962.6 \\ 960.7$	$1154.0\\1154.8\\1155.8$
230 232 235	6 7 8	$.05160 \\ .05340 \\ .05620$	19.39 18.72 17.78	$\begin{array}{c} 198.20 \\ 200.20 \\ 203.20 \end{array}$	958.7 957.4 955.4	$\begin{array}{c} 1156.9 \\ 1157.6 \\ 1158.7 \end{array}$
237 239 250	9 10 15	.05820 .06020 .07240	$17.17 \\ 16.60 \\ 13.82$	$205.30 \\ 207.30 \\ 218.50$	$954.1 \\ 952.8 \\ 945.3$	$1159.4 \\ 1160.0 \\ 1163.8$
259 267 274	20 25 30	.08370 .09490 .10570	$11.95 \\ 10.54 \\ 9.46$	$227.60 \\ 235.80 \\ 242.90$	939.1 933.5 928.6	$1166.7 \\ 1169.3 \\ 1171.5$
281 287 292	$35 \\ 40 \\ 45$	$.11740 \\ .12830 \\ .13800$	8.51 7.79 7.24	$250.10 \\ 256.20 \\ 261.30$	923.5 919.1 915.4	$1173.6 \\ 1175.3 \\ 1176.8$
298 307 316	50 60 70	.15040 .17070 .19300	$\begin{array}{c} 6.65 \\ 5.86 \\ 5.19 \end{array}$	$267.50 \\ 276.80 \\ 286.10$	$911.0 \\ 904.2 \\ 897.3$	$1178.5 \\ 1181.0 \\ 1183.3$
324 331 338	80 90 100	$\begin{array}{c} .21480 \\ .23530 \\ .25750 \end{array}$	$4.66 \\ 4.25 \\ 3.88$	$294.30 \\ 301.60 \\ 308.90$	891.0 885.5 879.9	$^{1185.4}_{1187.1}_{1188.8}$
344 350 356	$110 \\ 120 \\ 130$	$\begin{array}{c} .27780 \\ .29920 \\ .32210 \end{array}$	$3.60 \\ 3.34 \\ 3.10$	$315.10 \\ 321.40 \\ 327.70$	$875.1 \\ 870.1 \\ 865.2$	$1190.2 \\ 1191.5 \\ 1192.9$
361 366	140 150	.34230 .36310	2.92 2.75	332.90 338.20	861.0 856.8	$1193.9 \\ 1195.0$

PROPERTIES OF SATURATED STEAM

From the steam tables of Marks & Davis

1	C. a. a.	Fan System Heater	553 1108 1385 1385 1980 2730 2990	1980 2730 3270 4860	2730 3270 4860 6350	3270 4860 5960 8030 9020	10340 12700 16640	DEDOT
<u>}_</u>		Size of Fan in Inches	90000000000000000000000000000000000000	70 80 110	80 110 120	$ \begin{array}{c} 90 \\ 110 \\ 120 \\ 140 \\ 2-120 \\ \end{array} $	2 - 130 2 - 140 3 - 150	2007
	ado	Wire Ro	******	021 071 071	255 255 255 255			
9	S S S	Vo. of Sh Pulley	xx xx xx xx xx xx xx	16 16 16	2000 00 00 4 4 4 4 4	88888 4	48 64 80	200
n Kiln		12=Ib. T=Rails in Feet	96 126 140 169 189 252 315	252 378 504 630	378 576 756 940	504 672 1008 1260 1575	1890 2520 3150	- nn nn
racks i	Number of	Bolts and Nuts with Washers	48 84 132 168 168	$120 \\ 192 \\ 264 \\ 336 \\ 336$	180 288 396 504	240 384 528 672 804	1008 1344 1680	D001
For Three Tracks in Kiln	Num	Truck Wheels and Spindles	24 28 28 28 28 28 28 28 28 28 28 28 28 28	$ \begin{array}{c} 60 \\ 96 \\ 132 \\ 168 \\ 16$	$ \begin{array}{c} 90 \\ 144 \\ 198 \\ 252 \end{array} $	120 192 264 336 420	504 672 840	ME O
For T		Trucks Lumber	$ \begin{array}{c} 12 \\ 23 \\ 23 \\ 23 \\ 23 \\ 24 \\ 21 \\ 25 \\ 21 \\ 21 \\ 22 \\ 23 \\ 23 \\ 24 \\ 24 \\ 25 \\ 24 \\ 25 \\$	30 48 84 84 84	45 72 99 126	$ \begin{array}{c} 60 \\ 96 \\ 132 \\ 168 \\ 210 \\ \end{array} $	252 336 420	07F
Kiln		12=16. T=Rails in Feet	84 84 126 150 1150 210	164 252 336 420	252 373 500 625	336 504 672 840 1050	1260 1680 2100	2017
For Two Tracks in Kiln	Number of	Bolts and Nuts with Washers	56 56 56 56 56 56 56 56 56 56 56 58 56 58 56 58 56 58 56 58 56 58 56 58 56 56 56 56 56 56 56 56 56 56 56 56 56	80 128 176 224	$ \begin{array}{c} 120 \\ 264 \\ 336 \\ 336 \end{array} $	160 256 352 448 560	672 896 1120	
wo Tr	Num	Truck Wi eels and Spindles	54522255 8543225 854325 85432 85432 85432 85432 85432 85432 85432 85432 85432 85432 85432 85432 85432 855532 855532 85552 85532 855552 855552 855552 855555 8555555 8555555 855555555	40 64 112 88 112	60 96 132 168	80 128 176 224 280	336 448 560	2000
For 1		Ті ucks Lumber	282264112 282264112 282264	20 24 56 44 56	30 86 86 86 86 86 86 86 86 86 86 86 86 86	40 64 88 112 140	168 224 280	202
	Hold-	capac- ity of Kiln	8000 12000 20000 24000 36000 50000	24000 50000 75000 100000	$ \begin{array}{c} 36000 \\ 75000 \\ 110000 \\ 150000 \end{array} $	$\begin{array}{c} 48000\\ 96000\\ 144000\\ 192000\\ 2240000\end{array}$	300000 400000 500000	annon
	Size of	Appara- tus House in Feet	12 x 8 12 x 8 13 x 8 13 x 8 13 x 8 13 x 8 15 x 10 15 x 10	13 x 8 14 x 9 15 x 10 17 x 12	14 x 9 15 x 10 17 x 12 20 x 14	$\begin{array}{c} 14 \ x & 9 \\ 17 \ x & 12 \\ 20 \ x & 14 \\ 22 \ x & 26 \\ 24 \ x & 20 \end{array}$	XXX	ł.
Cira of Daw Kills		Size of Each Room in Feet	15 x 17 x 9 22 x 17 x 9 22 x 17 x 9 33 x 17 x 9 33 x 17 x 9 64 x 17 x 9 64 x 17 x 9 85 x 17 x 9	22 x 17 x 9 43 x 17 x 9 64 x 17 x 9 85 x 17 x 9	22 x 17 x 9 43 x 17 x 9 64 x 17 x 9 85 x 17 x 9	22 x 17 x 9 43 x 17 x 9 64 x 17 x 9 85 x 17 x 9 85 x 17 x 9	x 17 x x 17 x x 17 x	V IT V
Ciro of	0 3710	No. of Drying Rooms	00000000000000000000000000000000000000	Two Two Two	Three Three Three Three	Four Four Four Five	TIL	
			Sindle Kiln	Double	Triple Kila	Quadruple		

BUFFALO PROGRESSIVE LUMBER DRY KILN STANDARD SIZES

559

DRY KILN

Nos.	0	1	2	3	4	5	6	7	8	9			Pro	por	tio	ıal	Par	ts	
Nat.									0		1	2	3	4	5	6	7	8	9
10 11 12		0453	0492	0531	0569	0607	$\begin{array}{c} 0253 \\ 0645 \\ 1004 \end{array}$	0682	0719	0755	4	8	11	15	19		26	33 30 28	$37 \\ 34 \\ 31$
13 14 15	1461	1492	1523	1553	1584	1614	$1335 \\ 1644 \\ 1931$	1673	1703	1732	3	6	9	$ \begin{array}{c} 13 \\ 12 \\ 11 \end{array} $	15	19 18 17	21	$26 \\ 24 \\ 22$	29 27 25
16 17 18	$2041 \\ 2304 \\ 2553$	$2068 \\ 2330 \\ 2577$	$2095 \\ 2355 \\ 2601$	$2122 \\ 2380 \\ 2625$	$2148 \\ 2405 \\ 2648$	$2175 \\ 2430 \\ 2672$	$2201 \\ 2455 \\ 2695$	2227 2480 2718	$2253 \\ 2504 \\ 2742$	$2279 \\ 2529 \\ 2765$	$\frac{3}{2}$	5555		$ \begin{array}{c} 11 \\ 10 \\ 9 \end{array} $		$16 \\ 15 \\ 14$	17		24 22 21
19 20 21	3010	3032	3054	3075	3096	3118	2923 3139 3345	3160	3181	3201	2		7 6 6	9 8 8	11 11 10	13 13 12	15		20 19 18
22 23 24	3617	3636	3655	3674	3692	3711	3541 3729 3909	3747	3766	3784	2	4	6 6 5	8 7 7	10 9 9	$12 \\ 11 \\ 11 \\ 11$	13	$15 \\ 15 \\ 14$	$17 \\ 17 \\ 16 \\ 16$
25 26 27	4150	4166	4183	4200	4216	4232	$\begin{array}{r} 4082 \\ 4249 \\ 4409 \end{array}$	4265	4281	4298	2	3	5 5 5	$7 \\ 7 \\ 6$	9 8 8	10		13	$15 \\ 15 \\ 14$
28 29 30	4624	4639	4654	4669	4683	4698	$4564 \\ 4713 \\ 4857$	4728	4742	4757	1	3	5 4 4	$\begin{array}{c} 6 \\ 6 \\ 6 \end{array}$	8 7 7	9	10	12	$14 \\ 13 \\ 13$
31 32 33	5051	5065	5079	5092	5105	5119	$\begin{array}{r} 4997 \\ 5132 \\ 5263 \end{array}$	5145	5159	5172	1	3333	4 4 4	6 5 5	$\frac{7}{7}$ 6	888	10 9 9	11 11 10	$12 \\ 12 \\ 12 \\ 12$
34 35 36	5441	5453	5465	5478	5490	5502	$5391 \\ 5514 \\ 5635$	5527	5539	5551	1	3 2 2	4 4 4	5555	$\begin{array}{c} 6 \\ 6 \\ 6 \end{array}$	8 7 7	9 9 8	$10 \\ 10 \\ 10 \\ 10$	$ \begin{array}{c} 11 \\ 11 \\ 11 \\ 11 \end{array} $
37 38 39	5798	5809	5821	5832	5843	5855	5752 5866 5977	5877	5888	5899	1	$\frac{2}{2}$	3333	5 5 4	6 6 5	7 7 7	8 8 8	9 9 9	10 10 10
40 41 42	6128	6138	6149	6160	6170	6180	$6085 \\ 6191 \\ 6294$	6201	6212	6222	1	$\frac{2}{2}$	က က က	4 4 4	5 5 5	6 6 6	8 7 7	9 8 8	10 9 9
43 44 45	6435	6444	6454	6464	6474	6484	$\begin{array}{c} 6395 \\ 6493 \\ 6590 \end{array}$	6503	6513	6522	1	$^{2}_{2}_{2}$	00 00 00	4 4 4	5 5 5	$\begin{array}{c} 6\\ 6\\ 6\end{array}$	7 7 7	8 8 8	9 9 9
46 47 48	6721	6730	6739	6749	6758	6767	$\begin{array}{c} 6684 \\ 6776 \\ 6866 \end{array}$	6785	6794	6803	1	2	00 00 00 00	4 4 4	5 5 4	655 5	$\begin{array}{c} 7 \\ 6 \\ 6 \end{array}$	7 7 7	888
49 50 51	6990	6998	7007	7016	7024	7033	6955 7042 7126	7050	7059	7067	1	2 2 2	00 00 00 00	$\frac{4}{3}$	4 4 4	555	6 6 6	7 7 7	80 80 80
52 53 54	7160 7243 7324	7168 7251 7332	7177 7259 7340	7185 7267 7348	7193 7275 7356	7202 7284 7364	7210 7292 7372	7218 7300 7380	7226 7308 7388	7235 7316 7396	1 1 1	2 2 2	2 2 2	333	4 4 4	5 5 5	6 6 6	7 6 6	7777

LOGARITHMS

LOGARITHMS

Nos.	0	1	2	3	4	5	6	7	8	9	P	ro	po	rtio	ona	al	Pa	rts	5
Nat.			-			3		-	Ů		1	2	3	4	5	6	7	8	9
55 56 57					7435 7513 7589			$7459 \\ 7536 \\ 7612$	$7466 \\ 7543 \\ 7619$	$7474 \\ 7551 \\ 7627$	1 1 1	$\frac{2}{2}$	$\frac{2}{2}$	333	4 4 4	555	555	6 6 6	7 7 7
58 59 60	7709	7716	7723	7731	7664 7738 7810	7745	7752	7686 7760 7832	7694 7767 7839	$7701 \\ 7774 \\ 7846$	1 1 1	1 1 1	$^{2}_{2}_{2}$	333	4 4 4	4 4 4	5 5 5	$\begin{array}{c} 6\\ 6\\ 6\end{array}$	7 7 6
61 62 63	7853 7924 7993	7860 7931 8000	7868 7938 8007	7875 7945 8014	7882 7952 8021	7889 7959 8028	7896 7966 8035	7903 7973 8041	7910 7980 8048	$7917 \\7987 \\8055$	1 1 1	1 1 1	$2 \\ 2 \\ 2$	3 3 3	$\frac{4}{3}$	4 4 4	5 5 5	6 6 5	6 6 6
64 65 66					8089 8156 8222			$\begin{array}{r} 8109 \\ 8176 \\ 8241 \end{array}$	$\begin{array}{r} 8116 \\ 8182 \\ 8248 \end{array}$	8122 8189 8254	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	333	3 3 3 3	4 4 4	5 5 5	5555	$\begin{array}{c} 6 \\ 6 \\ 6 \end{array}$
67 68 69	8261 8325 8388	8267 8331 8395	8274 8338 8401	8280 8344 8407	$8287 \\ 8351 \\ 8414$	8293 8357 8420	$8299 \\ 8363 \\ 8426$	8306 8370 8432	$\begin{array}{r} 8312 \\ 8376 \\ 8439 \end{array}$	8319 8382 8445	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	$\frac{3}{2}$	3 3 3	4 4 4	5 4 4	5 5 5	$\begin{array}{c} 6\\ 6\\ 6\end{array}$
70 71 72	8513	8519	8525	8531	8476 8537 8597	8543	8549	$\begin{array}{r} 8494 \\ 8555 \\ 8615 \end{array}$	$8500 \\ 8561 \\ 8621$	8506 8567 8627	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	$\frac{2}{2}$	3333	4 4 4	4 4 4	5 5 5	6 5 5
73 74 75	8692	8698	8704	8710	8657 8716 8774	8722	8727	8675 8733 8791	8681 8739 8797	8686 8745 8802	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	$2 \\ 2 \\ 2 \\ 2$	3333	4 4 3	4 4 4	555	5 5 5
76 77 78	8865	8871	8876	8882	8831 8887 8943	8893	8842 8899 8954	8848 8904 8960	8854 8910 8965	8859 8915 8971	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	$\frac{2}{2}$	3333	3033	4 4 4	5 4 4	5 5 5
79 80 81	8976 9031 9085	8982 9036 9090	8987 9042 9096	8993 9047 9101	8998 9053 9106	9004 9058 9112	9009 9063 9117	9015 9069 9122	9020 9074 9128	9025 9079 9133	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	$\frac{2}{2}$	333	333	4 4 4	4 4 4	5 5 5
82 83 84	9191	9196	9201	9206	9159 9212 9263	9217	9222	9175 9227 9279	9180 9232 9284	9186 9238 9289	1 1 1	1 1 1	$2 \\ 2 \\ 2 \\ 2$	$ \frac{2}{2} 2 $	3033	3033	4 4 4	4 4 4	5 5 5
85 86 87	9345	9350	9355	9360	$9315 \\ 9365 \\ 9415$	9370	9375	9330 9380 9430	9335 9385 9435	9340 9390 9440	1 1 0	1 1 1	$2 \\ 2 \\ 1$	$ \frac{2}{2} 2 $	$3 \\ 3 \\ 2$	3333	443	4 4 4	5 5 4
88 89 90	9445 9494 9542	9450 9499 9547	9455 9504 9552	9460 9509 9557	9465 9513 9562	9469 9518 9566	9474 9523 9571	9479 9528 9576	9484 9533 9581	9489 9538 9586	0 0 0		1 1 1	$ \frac{2}{2} 2 $	$2 \\ 2 \\ 2 \\ 2$	3333	3033	4 4 4	4 4 4
91 92 93					9609 9657 9703			9624 9671 9717	9628 9675 9722	9633 9680 9727	0000	1 1 1	1 1 1	$ \frac{2}{2} 2 $	$2 \\ 2 \\ 2$	3333	3333	4 4 4	4 4 4
94 95 96	9777	9782	9786	9791	9750 9795 9841	9800		9763 9809 9854	9768 9814 9859	9773 9818 9863	0 0 0	1 1 1	1 1 1	$2^{2}_{2}_{2}$	2 2 2	3000	3333	4 4 4	4 4 4
97 98 99	9912	9917	9921	9926	9886 9930 9974	9934	9939	9899 9943 9987	9903 9948 9991	9908 9952 9996	0000	1 1 1	1 1 1	2222	$\frac{2}{2}$	3333	3333	4 4 3	444

USEFUL FACTORS

1 gal. (U. S.)	=231 cu. in.
	=0.13368 cu. ft.
1 gal. (British)	=277.274 cu. in.
1 cu. ft.	=7.4805 gals.
1 cu. ft. water at 60° F.	= 62.37 lbs.
1 gal. water at 60° F.	= 8.34 lbs.
1 cu. ft. water at 212° F.	=59.76 lbs.
1 gal. water at 212° F.	= 7.99 lbs.
1 barrel water at 60° F.	$=31\frac{1}{2}$ gals. $=262.7$ lbs.
1 in. mercury	$=1\frac{1}{8}$ ft. or 13.6 in. water
	=0.491 lb. per sq. in.
1 lb. per sq. in. press.	$=2.304$ ft. water at 60°
Height of a column of water	
in feet $ imes 0.434$	=lb. press. per sq. in.
A column of water 1 sq. in.	
and 2¼ ft. high	= approximately 1 lb.
1 calorie	=3.97 B. t. u.
1 kilogram	
	=2.2046 lbs.
Calories per kilo \times 1.8	= 2.2046 lbs. = B. t. u. per lb.
Calories per kilo \times 1.8	= B. t. u. per lb.
Calories per kilo \times 1.8 1 kilowatt (1000 watts)	= B. t. u. per lb. = 1.3405 H. P.
Calories per kilo \times 1.8 1 kilowatt (1000 watts) 1 horsepower	= B. t. u. per lb. = 1.3405 H. P. = 0.746 K. W.
Calories per kilo × 1.8 1 kilowatt (1000 watts) 1 horsepower 1 kilowatt	= B. t. u. per lb. = 1.3405 H. P. = 0.746 K. W. = 56.9 B. t. u. per min.
Calories per kilo × 1.8 1 kilowatt (1000 watts) 1 horsepower 1 kilowatt	 = B. t. u. per lb. = 1.3405 H. P. = 0.746 K. W. = 56.9 B. t. u. per min. = 42.4 B. t. u. per min. = 2545 B. t. u. per hour = '33000 ft. lbs. per min.
Calories per kilo × 1.8 1 kilowatt (1000 watts) 1 horsepower 1 kilowatt	= B. t. u. per lb. = 1.3405 H. P. = 0.746 K. W. = 56.9 B. t. u. per min. = 42.4 B. t. u. per min. = 2545 B. t. u. per hour
Calories per kilo × 1.8 1 kilowatt (1000 watts) 1 horsepower 1 kilowatt 1 mech. horsepower	 = B. t. u. per lb. = 1.3405 H. P. = 0.746 K. W. = 56.9 B. t. u. per min. = 42.4 B. t. u. per min. = 2545 B. t. u. per hour = '33000 ft. lbs. per min.
Calories per kilo × 1.8 1 kilowatt (1000 watts) 1 horsepower 1 kilowatt 1 mech. horsepower 1 boiler horsepower	 = B. t. u. per lb. = 1.3405 H. P. = 0.746 K. W. = 56.9 B. t. u. per min. = 42.4 B. t. u. per min. = 2545 B. t. u. per hour = 33000 ft. lbs. per min. = 33479 B. t. u. per hour

WATER CONVERSION FACTORS*

U. S. gallons	$\times 8.33$	= pounds
U. S. gallons	imes 0.13368	=cu. ft.
U. S. gallons	$\times 231.$	= cu. in.
U. S. gallons	imes 3.78	=liters
Cu. in. water at 39.1°	$\times 0.036024$	= pounds
Cu. in. water at 39.1°	$\times 0.004329$	= U. S. gal.
Cu. in. water at 39.1°	imes 0.576384	=ounces
Cu. ft. water at 39.1°	$\times 62.425$	= pounds
Cu. ft. water at 39.1°	imes 7.48	= U. S. gal.
Cu. ft. water at 39.1°	imes 0.028	=tons
Pounds of water	imes 27.72	=cu. in.
Pounds of water	$\times 0.01602$	=cu. ft.
Pounds of water	$\times 0.12$	= U. S. gal.

MEASURES OF PRESSURE AND WEIGHT[†]

1 lb. per sq. in.	= {	144 lbs. per sq. ft. 2.0416 in. mercury at 62° F. 2.309 ft. water at 62° 27.71 in. water at 62°
1 oz. per sq. in.	= {	0.1276 in. mercury at 62° 1.732 in. water at 62°
1 atmosphere (14.7 lbs. per sq. in.) = {	2116.3 lbs. per sq. ft 33.947 ft. water at 62° 30 in. mercury at 62° 29.922 in. mercury at 32°
1 in. water at 62° F.	= }	0.03609 lb. or .5774 oz. per sq. in. 5.196 lbs. per sq. ft.
1 ft. water at 62° F.	= }	, 0,433 lb. per sq. in. / 62,355 lbs. per sq. ft.
1 in. mercury at 62° F	·. = {	0.491 lb. or 7.86 oz. per sq. in. 1.132 ft. water at 62° 13.58 in. water at 62°

*American Machinist Hand Book.

†Kent's Mechanical Engineers' Pocket Book.

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REPORT OF COMMITTEE OF AMERICAN SOCIETY OF HEAT-ING AND VENTILATING ENGINEERS ON STAND-ARDS FOR VENTILATION LEGISLATION FOR MOTION PICTURE SHOW PLACES

January, 1913

Ventilation and sanitation requirements cannot be too strongly emphasized when dealing with the question of legislation relating to motion picture show places. The widespread neglect, in a very large number of communities throughout the country, of proper ventilation and sanitation in such motion picture show places, has many times been correctly characterized as a "menace to public health"—materially affecting the moral tone as well.

Allowing the great importance of fire protection and structural requirements for the protection of life; elimination of lowclass vaudeville, enforced lighting during performances, supervision of pictures exhibited, and other essential matters for the protection of morals; ventilation and sanitation requirements loom up large for the protection of health.

The Committee has been appointed to deal with the subject of ventilation and this question is, of course, vitally concerned with all the conditions of the air breathed, particularly temperature, air purity, air motion, humidity, and freedom from dust (impurities from breathing, skin exhalations, dust, etc., being constantly released in large quantities in every audience hall).

With a view of suggesting minimum requirements that are practical to secure, the following recommendations are made as standards for legislation to cover this important phase of the needed general regulations for motion picture show places.

MINIMUM VENTILATION STANDARDS

1. Floor Area per Occupant.

A minimum of 4½ sq. ft. of floor area, as a seating space, per occupant, exclusive of aisles and public passageways, shall be provided in the audience hall.

2. Cubic Space per Occupant.

A minimum of 80 cu. ft. of air space, per occupant, shall be provided in the audience hall.

3. Quantity of Outdoor Air.

A positive supply of outdoor air from an uncontaminated source shall be provided the audience hall at all times while the show place is open to the public, and the quantity of this positive supply of outdoor air shall be based on a minimum requirement of 15 cu. ft. per minute, per occupant.*

4. Temperature.

The temperature of the air in the audience hall shall at all times, while the show place is open to the public, be maintained throughout at the breathing line (persons being seated) within the range of 62° F. to 70° F. (except when the outside temperature is sufficiently high not to require the air supply for ventilation to be heated). The temperature, distribution and diffusion of the supplied outdoor air shall be such as to maintain the temperature requirement without uncomfortable drafts.

5. Direct Heat Sources.

Any good heat source which does not contaminate the air will be accepted to supplement the warmed outdoor air supply. Gas radiators are prohibited.

6. Machine Booth Ventilation.

Enclosures or booths for the motion picture machines shall be provided with special exhaust ventilation with a capacity to exhaust at all times not less than 60 cu. ft. of air per minute through a one-machine booth, not less than 90 cu. ft. of air per minute through a two-machine booth, and not less than 120 cu. ft. of air per minute through a three-machine booth.

This requirement shall include a number of small metal screened openings (equipped with special dampers and automatic appliance with fusible link to automatically close tight in case

^{*}The ordinance in force in the City of Chicago at the present time requires that the air in the auditorium in the class of buildings in which motion picture show places are included, shall be changed so as to supply for each person for whom seating accommodation is provided, at least 1500 cu. ft. of air per hour for new buildings, and at least 1200 cu. ft. of air per hour for buildings constructed prior to the passage of the ordinance, which requirements the Illinois Chapter of the Society considers practical to obtain and desirable to require by legislation for motion picture show places.

Higher standards of ventilation than set forth as minimum in the committee's report are urged wherever possible to obtain.

of fire in the booth) on the sides of the booth near the bottom, aggregating 180 sq. in. for a one-machine booth, 210 sq. in. for a two-machine booth, and 240 sq. in. for a three-machine booth; and this requirement shall also include a metal or other fireproof flue, extending from the top or side at the top of the booth, and carried to a proper place of discharge outdoors. The ventilation should be augmented by mechanical or other means, so as to exhaust at least the quantity of air as herein stated.

The size of this special fireproof vent flue shall be not less than 96 sq. in. clear area for a one-machine booth, not less than 120 sq. in. clear area for a two-machine booth, and not less than 144 sq. in. clear area for a three-machine booth, and this special vent flue shall be provided with an adjustable damper, operated from the booth, and equipped with an automatic appliance and a fusible link to operate so as to open the damper wide automatically in case of fire in the booth. The machine booth ventilation shall be kept in operation at all times when the booth is in use.

It will be noted that the foregoing regulations are simple, and that violations may be readily detected, also that care has been exercised to leave large latitude for design of the ventilating apparatus.

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It should be especially noted that the foregoing regulations call for a minimum of all requirements as compulsory, and that it should be the aim of the administrative department having enforcement of the regulations in charge to encourage motion picture show owners and managers to provide as comprehensive, liberal, and high-class equipment as possible, with a view to catering to the comfort and health of the patrons and thus add to the popularity of the show place as compared with others which may have barely come within the legal requirements.

Elimination of dust from the air supply by means of air filters or air washers is desirable under the best conditions and is imperative under some conditions of especially dusty air supply. This question is dealt with by suggestion in the following general clauses.

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The controlling of relative humidity is desirable, whenever possible, but the Committee decided to omit from the regulations any humidity requirement.

The machine booth ventilation, as per recommended regulations, would be greatly improved, especially for summer conditions, by providing a duct connection from out of doors to the bottom of the booth, for the introduction of outdoor air directly to the booth. * * * * * * *

Strong emphasis is placed on the need of having the administrative feature of legislation of the kind here advocated, placed in the control of a responsible department, * * * * * and that such department be supplied with a special inspector or inspectors, experienced in heating, ventilation, and sanitation, and that such department be given reasonable latitude by legislation, such as to require approval of plans preceding installation or to require special extra equipment for special cases, such as dust filters for air supply where the air supply is especially dust laden; exhaust ventilation of toilets where building laws do not properly cover this matter; fans in the auditorium, to keep the air in motion where diffusion is insufficient, etc., it being made clear in the legislation that such latitude should in no case include the right to reduce the stated minimum requirements. The administrative department should also be given the support of other local or state departments, as the case may be, such as the fire department, police department, health department, etc.

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